

# **Evaluating strategies for integrating bacterial cells into a biosensor designed to detect electrophilic toxins**

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## **Abstract**

To improve the process stability of wastewater treatment plants, the construction of a whole-cell bacterial biosensor is explored to harness the natural stress response of the bacterial cells. The stress response selected in this work is the glutathione-gated potassium efflux (GGKE) system, which responds to electrophilic stress by effluxing potassium from the interior to the exterior of the cell. Thus, the bulk potassium in solution can be monitored as an indicator of bacterial stress. By utilizing this stress response in a biosensor, the efflux of potassium can be correlated to the stress response of the immobilized culture, providing an early warning system for electrophilic shock. This type of shock is a causative factor in many process upset events in wastewater treatment plants, so the application of the sensor would be an early warning device for such plants.

The research conducted here focused on the biological element of the biosensor under development. Three immobilization matrices were explored to determine the cell viability and potassium efflux potential from immobilized cells: a calcium alginate, a photopolymer, and a thermally reversible gel. The calcium alginate was unstable, and dissolved after five days, such that the long-term impact of immobilization on the cells could not be determined in the matrix. The photopolymer resulted in very low activity and viability of immobilized cells. Of the three matrices tested, indicating that the composition of the polymer was toxic to the cells. Of the matrices tested, the thermally-reversible gel showed the best response for further study, in that the matrix did not inhibit cell activity or potassium efflux.

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## **Introduction**

Process upset in wastewater treatment plants results in permit violations, low quality effluent, and detrimental impacts on receiving waters. Even the most well-designed plant may experience occasional process upset due to shock loads of toxic and/or inhibitory compounds. Unfortunately, the precise causes of these upset events are often unclear, and due to the lack of real-time monitoring, operators are typically unaware that upset is occurring until the biomass is already damaged. The implementation of a real-time sensing system would provide operators with warning that a toxin is approaching and give them time to proactively respond to reduce the impact of the shock, instead of merely reacting to an upset event already underway.

In a survey performed by Love and Bott in 2000, operators reported that the most common modes of process upset are ineffective biological oxygen demand (BOD) removal, ineffective nitrification, deflocculation, and sludge bulking. Although the causes of these upsets have been speculated, operators generally do not have sufficient information to identify the source of the problem. However, when asked, operators suggested that heavy metals and toxic organic compounds (which include electrophilic chemicals) are among the most common sources of these upsets (Love and Bott, 2000). Thus, the major types of upset events are thought to be due in part to electrophilic shock loads. Creating a sensor for electrophilic compounds would provide warning of these types of upset events, although it would not be useful for upsets due to other classes of compounds, such as oil and grease.

Because electrophiles elicit a natural stress response from bacterial cells, this stress response can be harnessed to create a biosensor for electrophilic toxins. During an electrophilic toxin upset event, the bacterial biomass initiates the glutathione-gated potassium

efflux (GGKE) system (Bott and Love, 2002), in which potassium ions are effluxed from within the cell (Apontoweil and Berends, 1975 a and b). By creating a biosensor with bacterial cells containing the GGKE response, the intrinsic stress response of the bacterial culture is harnessed and genetic engineering of the bacteria is not required. Many existing biosensors have been slow to commercialize, mostly due to the limitations on genetically engineered organisms. The commercial Microtox<sup>®</sup> assay, which uses naturally luminescent *Vibrio fischerii* bacteria, is widely used as an indicator of toxicity, whereas many promising biosensors with better response times and repeatability that use genetically modified bacteria remain limited to laboratory use (for example, Philp *et al.*, 2003; Gu and Choi, 2002). Because the sensor developed in this work does not require genetic modification, it has an advantage in terms of eventual commercialization and field application.

By monitoring bulk potassium as an indicator of cellular stress, the biosensor will monitor for electrophilic compounds that have been shown to cause upset in the activated sludge process. The microscale biosensor under development includes a whole cell biological element, potassium detection membranes, and microfluidic componentry that compose a lab-on-a-chip device. The biological element consists of bacterial cells immobilized in a hydrogel polymer matrix. Immobilization of the bacterial cells is important because it keeps the cell concentration constant by maintaining the viability of the immobilized cells while reducing cell division. Additionally, immobilized cells cannot slough off as a biofilm layer could and clog the microfluidic channels in the device.

A series of screening experiments were conducted in this work to select an appropriate polymer matrix for bacterial cell immobilization within the biosensor under development, and are discussed in Chapter 2. The ideal matrix is physically and chemically



stable over several weeks, non-toxic to the cells, and does not limit the diffusion of oxygen, compounds that are necessary for cell growth, the electrophiles that would trigger a stress response, or the potassium that would indicate that a stress response has been initiated.

Three matrices were examined here, including calcium alginate, several photopolymerizable hydrogels, and a thermal polymer. The alginate showed good viability, but poor mechanical stability, while the photopolymerizable polymers showed poor viability. The thermal polymers were the best choice for continued study, in that the bacterial culture showed extended viability after immobilization and the matrix did not inhibit the efflux response.

### **Experimental Objectives**

The overall objectives of this research were:

- Elucidate potassium efflux in response to a model electrophile from planktonic cultures of *P. aeruginosa* and *E. coli* at various growth states
- Select the growth state and the strain with maximal potassium efflux per cell for further study
- Screen a series of immobilization hydrogels for cell viability within the matrix
- Quantify potassium efflux from immobilized bacterial culture selected

The specific results and methods used to meet these objectives will be discussed within the following chapters of the thesis.

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## **Chapter 1: Literature Review**

### **Introduction**

Process upset events in wastewater treatment plants result in high nutrient and pathogen loading to receiving waters, endangering public health and stability of waterways. Electrophilic compounds are one cause of upset events, typically resulting in deflocculation, which is thought to be due to potassium efflux through the glutathione-gated potassium efflux (GGKE) mechanism (Bott and Love, In Press). Controls to eliminate such upset events are limited by the scarcity of real-time toxicity monitoring devices. Biosensors show promise in the field and have been developed to respond to specific compounds (for example, Strachan *et al.*, 2001 and Reid *et al.*, 1998) as well as general stress and oxidative damage (for example, Belkin *et al.*, 1997 and Elasri *et al.*, 2000). Most biosensors employ genetically modified bacteria, which limits their potential for commercialization. Non-engineered strains have been used to some degree, but more work is needed in this area. To create a real-time live cell sensor, a flow-through system is required. Microfluidic technology can be applied to create micro-scale sensors containing bacteria immobilized in hydrogels (for example, Heo *et al.*, 2003), because these sensors provide rapid response and require low sample volumes. Incorporating these microfluidic sensors into a real-time monitoring system can provide forewarning of toxic shock loads to treatment plants, allowing operators time to proactively mitigate the threat.

### **Toxic shocks cause treatment upset**

Wastewater treatment plants employing biological treatment schemes to reduce or remove organic and inorganic pollutants play a pivotal role in pollution reduction. The

optimal functioning of these plants is critical for receiving stream health and downstream water reuse capacity. Despite the dependence on these plants for pollutant removal, even the most well designed plant may experience occasional process upset events due to changes in flow pattern or waste composition, or due to toxic loads of inhibitory chemicals.

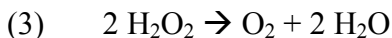
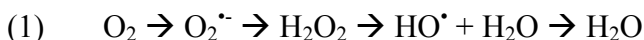
A survey of Water Environment Research Foundation subscribers revealed that the common modes of process upset are ineffective BOD removal, deflocculation, ineffective nitrification, and sludge bulking (Love and Bott, 2000). Some survey responders reported that the most common causes of upsets they experienced were high flow, toxic organics, oil and grease, and heavy metals (Love and Bott, 2000). Unfortunately, in most cases, the cause of the upset is commonly not discovered until well after the event, if at all. Interestingly, several of the purported causative factors can be grouped as electrophiles, such as the heavy metals and selected toxic organics.

During process upset from a shock load of an electrophilic compound, the treatment plant loses treatment efficiency because the chemical stressors cause deflocculation of the activated sludge flocs. This loss of biomass from the system is believed to occur because stress response mechanisms cause bacteria to efflux potassium (Bott and Love, 2002). The additional monovalent cations in the floc matrix is believed to increase the intrafloc divalent to monovalent cation ratio (Bott and Love, 2002), which is an important predictor of floc strength (Higgins and Novak, 1997a and 1997b). Disrupting this balance causes the flocs to lose stability and results in loss of biomass from the system (Murthy *et al.*, 1998).

## Bacterial stress responses

### *Oxidative stress mechanisms in bacteria*

Damaging oxidative (electrophilic) chemicals enter cells either from the outer environment or are generated internally as part of cellular metabolism. The types of oxidative stressors generated within the cell (reviewed in Storz and Imlay, 1999) are superoxide anions, hydrogen peroxide, and hydroxyl radicals, as well as methylglyoxal (Kalapos, 1999). Superoxide anions,  $O_2^{\bullet-}$ , are reduced to  $O_2$  and  $H_2O_2$  by superoxide dismutase. Hydrogen peroxide originates from the reduction of superoxide by its dismutase or by reduction of oxygen. Hydroxyl radicals ( $HO^{\bullet}$ ) are produced from superoxide and  $H_2O_2$ , and are very reactive with and damaging to DNA. Example equations illustrating these reactions (reviewed in Storz and Imlay, 1999) are provided below. Equation 1 shows the complete stepwise reduction of the superoxide radical through peroxide and hydroxyl radical to water. Equation 2 shows the reduction of the oxygen radical to peroxide, a reaction catalyzed by superoxide dismutase. Equation 3 shows the reduction of peroxide to water, a reaction catalyzed by catalase.



The types of damage caused by oxidative stress include DNA damage and mutagenesis, as well as membrane and protein damage.

The presence of these electrophiles changes the intracellular oxidation state. Two genes, *oxyR* and *soxR*, exist to detect such shifts in redox potential. Redox regulation is defined as the control of protein activity by oxidation and reduction and is a major means of

cellular control (as reviewed in Demple, 1996 and Pomposiello and Demple, 2001). The first step in protecting cells against damage is sensing the oxidants, achieved by the proteins OxyR and SoxR. These proteins are bound to the promoter region of the genes under their control such that the conformational change occurring upon oxidation allows transcription of these response genes (as reviewed in Pomposiello and Demple, 2001).

As reviewed in, for example, Storz and Imlay (1999) and Pomposiello and Demple (2001), OxyR is activated and deactivated by the formation and reduction of disulfide bonds. Peroxide exercises direct control over the activation of OxyR by reducing pairs of sulfur-hydrogen bonds to disulfide bonds. When oxidized by an electrophilic compound, the OxyR protein self-regulates the *oxyR* gene, as well as *dps* (protein to bind iron and DNA), *gorA* (GSH reductase), *grxA* (glutaredoxin), *katG* (peroxidase), *ahpCF* (NADPH reductase), and *fur* (iron binding protein to prevent iron transport). Additionally, through its control of *oxyS* and production of OxyS protein, OxyR controls other regulatory genes such as *rpoS* and *flhA*. The majority of the information on the OxyR system has been obtained from *E. coli*, but homologs have been found in many other species. After oxidation, OxyR is returned to the reduced state by the GSH-glutaredoxin-1 (*grxA*) system (as reviewed in Storz and Imlay, 1999 and Pomposiello and Demple, 2001).

The SoxR protein is constitutively expressed at a minimal level within the cell and functions through the activity of its [2Fe-2S] centers, which can be oxidized and reduced by a one-electron shift (Ding and Demple, 1997) as reviewed in, for example, Storz and Imlay (1999) and Pomposiello and Demple (2001). Superoxide exercises direct control over the activation of SoxR by shifting the oxidation state of  $\text{Fe}^+$  to  $\text{Fe}^{2+}$  in the iron-sulfur centers. The controlling compound for oxidation may be superoxide or depletion of NADPH. The

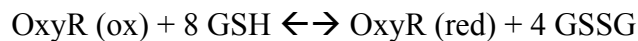
SoxR responds in the presence of heavy metals, antibiotics, and organic compounds, all superoxide-generating compounds, and also responds to nitric oxide (Zheng and Storz, 2000). When activated by an oxidant, SoxR initiates expression of the *soxS* gene. The genes under control of the *soxRS* regulon are *sodA* (superoxide dismutase to deactivate oxidants), *zwf* (glucose-6-phosphate dehydrogenase to recreate the NADPH pool), *fldA* and *fldB* (flavodoxins to reduce metals in constituent groups on intracellular molecules), *fpr* (NADPH reductase), *fur* (iron binding protein to prevent iron transport), *nfo* (DNA repair gene), *arcAB* (efflux pump to remove toxic chemicals), and *micF* (reduces porin expression and thus cell permeability). All of these genes that are controlled by SoxR work to prevent or mitigate damage caused by oxidants. These genes were elucidated in *E. coli*, but many other bacterial strains contain SoxR homologs (as reviewed in Storz and Imlay, 1999 and Pomposiello and Demple, 2001).

Another type of intracellular oxidative stress arises from methylglyoxal, an electrophilic byproduct of metabolism, also called pyruvaldehyde, pyruvic aldehyde, 2-oxopropanal, 2-ketopropion-aldehyde, or acetyl-formaldehyde. Methylglyoxal generation occurs during upswings in the electron donor concentration, accumulating in starving cells that are suddenly exposed to high concentrations of carbon source. The pathways for glucose oxidation become overwhelmed, and methylglyoxal is formed to release some of the excess carbonaceous energy (Kalapos, 1999). It has been shown (Ness *et al.*, 1997) that the glutathione-gated potassium efflux system evolved as a mechanism of protecting the cell from electrophilic damage from methylglyoxal.

### *Glutathione-gated potassium efflux (GGKE)*

Reduced glutathione (GSH) (N-(N-L- $\gamma$ -glutamy-L-cysteinyl)glycine) is constitutively expressed in the cell (reviewed in Storz and Imlay, 1999). Due to the activity of its sulfhydryl group, GSH acts in a sacrificial role to bind electrophiles and oxidizes into GSSG, as well as oxidized glutathione-S-conjugates (GSX) (Apontoweil and Berends, 1975 a and b). GSX triggers the cell stress response of potassium efflux through the glutathione-gated potassium efflux (GGKE) mechanism controlled by the KefB and KefC membrane transport proteins (Apontoweil and Berends, 1975 a and b; Booth *et al.*, 1993; Elmore *et al.*, 1990, Ferguson *et al.*, 1995; Munro *et al.*, 1991). GGKE shuttles potassium ions out of the cell in an ion exchange for hydrogen into the cell. The transport of these hydrogen ions dissipates the proton gradient, but acidifies the cytoplasm, causing the DNA to supercoil protecting it from oxidative damage (Ferguson *et al.*, 2000).

The glutathione control system is involved in the OxyR stress response, in that OxyR is reduced by enzymatic reaction with glutaredoxin 1 (Grx1), produced through OxyR control to reduce oxidized glutathione back to the reduced form, GSH (Zheng *et al.*, 1998). Because the production of Grx1 is regulated by OxyR, the reduction of OxyR is autoregulated. Zheng and Storz (1998) presented a conceptual equation for this reaction obtained through both molecular and biochemical studies:



Interestingly, OxyR is reduced by sacrificially oxidizing GSH into GSSG (Zheng and Storz 1998). Further, the redox potential of OxyR was found to be  $-185 \text{ mV}$ , much higher than the typical unstressed cell redox potential, indicating that OxyR is primarily in the reduced form normally (Zheng and Storz, 1998).



Overall, bacteria respond to electrophilic stress, detected by OxyR, SoxR, and glutathione, by a number of protective mechanisms. The GGKE system is linked to the OxyR system through the reduction of the oxidized proteins back to their reduced forms. Although SoxR and OxyR control many intracellular responses, such as the activation of protective genes, the GGKE system differs in its interaction with the Kef potassium efflux channels because the system triggers an observable extracellular effect. The efflux of potassium appears to cause deflocculation in wastewater sludge flocs, a typical symptom of process upset caused by toxic shock.

### **Real time information on wastewater toxicity**

The key to successful control of toxic shock events is awareness of their impending arrival at the plant as well as the causative toxin and its potential effect. Recognizing that a threat is approaching gives the operators time to respond in order to mitigate the threat. Control of wastewater plants is typically performed by operators with the help of computerized systems such as the Supervisory Control and Data Acquisition (SCADA) system. However, these systems are limited by the lack of real-time monitoring devices (for example, Dieu, 2001). Parameters that can be evaluated quickly include flowrate, pH, temperature, and dissolved oxygen, which are inadequate to accurately predict plant functionality (Bungay and Andrews, 1970, Olsson and Andrews, 1981). The five-day BOD test clearly takes too much time to be helpful in identifying problems in treatment. Even the chemical oxygen demand (COD) test, which can be completed in a few hours, is too long to wait to mediate an upset because the upset has already begun by the time the effluent COD spike is seen. Therefore, these tests fail as process control techniques. One simple way to

use existing technology to improve process control is the use of the dissolved oxygen (DO) profile. The variations in DO along the length of the biological reactor comprise the DO profile. Monitoring this profile permits operators to reduce the energy used to aerate the tank and to estimate the oxygen uptake rate. Shifts in the uptake rate as an alteration in the respirometry response can signal process upset (Olsson and Andrews, 1981, Bergeron and Paice, 2001).

Most control systems use “feed-back” setups, in that data from the effluent determines if treatment is effective (Bungay and Andrews, 1970). In order to effectively control plant function, “feed-forward” control is necessary to alert operators to potential problems, which would link real-time on-line sensors to global control systems within the plant (Bungay and Andrews, 1970). The limitation on these control systems is the lack of real-time sensors for causative factors in process upset. Lab analyses of the components in the influent are time consuming and costly, particularly when the target compound is unknown. The use of biosensors to provide real-time feedback on toxicity or process conditions shows promise for improving process control in wastewater treatment.

### **Immobilized cells as biological elements in biosensors**

A biosensor is generally defined as an analytical tool that pairs a biological component with a detection system to produce a measurable response, which can be quantified into the amount of analyte present in a sample (Belkin, 2003). The response is often measured electrochemically or optically. The types of biological components that can be used are enzymes, antibodies, proteins, nucleic acids, or whole cells. Whole cells are less expensive to use because their components require no isolation and purification, as in the cell

component assay systems. Also, whole cells provide information on the bioavailability of the toxins within the sample instead of simply reporting the concentration present. However, whole cells have a certain limited lifespan, require longer response times than isolated components, and may show significant variability between cell batches (Ramanathan, 2000).

### *Reporter genes*

Much work to date with whole cell biosensors has focused on genetically engineering bacterial strains to elicit specific responses to particular compounds. Three types of reporter genes are typically used: *lux*, *luc*, and *gfp*. First, bacterial luciferase (*lux*) produces the oxyluciferin protein by combining the substrate luciferin with oxygen in the presence of the luciferase enzyme. The oxyluciferin product is in the excited state and produces a photon, which can be detected and used to quantify the response (Hastings, 1983). The yield of this reaction is low, only about 0.1 yield units, and it consumes reducing power, the precursor to ATP formation. Further, the reaction requires a substantial amount of oxygen to proceed, limiting its use to aerobic conditions only (Lewis *et al.*, 1998). The *lux* gene was originally isolated from three bacterial species: *Vibrio* and *Photobacterium*, both marine, and *Photobacterium*, a terrestrial species (Keane *et al.*, 2002). Second, firefly luciferase (*luc*) was isolated from the beetle *Photinus pyralis* and also produces oxyluciferin, but requires a two-step enzyme reaction and consumes ATP. This reaction has a yield of 0.88 (Lewis *et al.*, 1998) and a wide linear range. However, the reaction only proceeds below 30°C (Keane *et al.*, 2002), so it is less frequently used in bacterial work, as the cells typically require higher temperatures for optimal growth. Third, green fluorescent protein (*gfp*) from the jellyfish *Aequorea victoria* requires a much smaller amount of oxygen than *luc* or *lux* and the light

chromophore is directly incorporated within the crystal structure. Production of the response protein is much slower than the luciferase-based systems (Keane *et al.*, 2002).

The selection of the reporter gene for a particular application is typically based on the desired time response of the reporter. Luciferase systems, in which the fluorescent proteins are broken down in a short time, are used for time-based assays in which repeated measurements are needed. Green fluorescent protein systems are best for single measurement studies where one yes or no answer is desired because hours are required to produce and properly fold the protein. Additionally, once generated, the fluorescent signal remains robust for much longer than the luciferase signals, resulting in a longer measuring window with a constant signal output (Keane *et al.*, 2002).

Two methods exist for adding response genes to cells, which can be classified as “lights on” and “lights off”, or induced and constitutive. Inserting the reporter gene into a general cell maintenance section of the genome will result in constant production of green fluorescence, while reduced intensity indicates some type of insult has occurred (Belkin, 2003). Alternately, the reporter can be linked with a promoter that regulates gene expression of a desired reporting characteristic, such as DNA repair. In this setup, an increase in light level functions as the indicator (Belkin, 2003).

#### *Genetically engineered strains in biosensors*

Several groups have used genetically modified strains to create biosensors specific to certain chemicals. A biosensor using *Pseudomonas aeruginosa* containing the *lux* operon to respond to polycyclic aromatic hydrocarbons (PAHs) was created by immobilizing the cells in poly(vinyl alcohol) (Philp *et al.*, 2003), which showed good repeatability on standards but

variable results on real samples. Also, *E. coli*, *P. fluorescens*, and *P. putida* with a *lux* reporter gene were used to construct a biosensor to respond to PAHs via bioluminescence (Reid *et al.*, 1998) and, although real samples were not tested, the sensor showed a stable, linear, and dose-dependent response to standards. A heavy metal responsive plasmid was constructed using *luc* to respond with production of luciferase and inserted into *Staphylococcus aureus* and *Bacillus subtilis* (Taurianinen *et al.*, 1998). This sensor responded within three hours to lab samples and responsivity was not reduced by freeze-drying the cells before use. Kohler *et al.* (2000) used *E. coli* modified with the *lux* operon to make a biosensor for detecting 4-chlorobenzoic acid by immobilizing cells in alginate in a microtiter plate, but more work was needed to optimize the system before real samples can be tested. Strains of *Pseudomonas* and *Achromobacter* were used to perform preliminary work towards creating a biosensor for surfactants using amperometric detection (Taranova *et al.* 2002). Gu and Choi (2002) used freeze-dried *E. coli* with a reporter bound to the phenol degradation pathway to create a biosensor for phenol detection in a complete portable field-ready kit. A range of phenols were tested with rapid, repeatable results, but no results from field samples were reported.

Hansen *et al.* (2000) used *E. coli* to create a biosensor for detecting mercury by fusing the  $P_{mer}$ , a promoter induced by Hg, and the *mer* reporter gene for Hg to *luxCDABE*, *lacZYA*, and *gfp*. These constructs produce luminescence, beta-galactosidase, and green fluorescent protein, respectively. Each construct was cloned into a delivery vector to permit its insertion into any bacterial strain desired. *P. aeruginosa* was used as an example. Other groups (Ramanathan *et al.*, 1997; Lyngberg *et al.*, 1999; Rasmussen *et al.*, 2000; Selifonova *et al.*, 1993) had performed similar research with the *mer* reporter gene encoded on a plasmid, but

mixed results were obtained because the plasmids were unstable. However, Petanen and Romantschuk (2002) used plasmids with a *luc* response to mercury and arsenite in *P. fluorescens* and obtained results comparable to traditional analytical methods, but much faster.

Howbrook *et al.* (2001) created a whole cell biosensor for glucose using *E. coli* with a luminescence reporter bound to the *katG* gene, which is tightly controlled by the OxyR system such that it responds to oxidative stress. As proof of concept, the glucose oxidase enzyme was added to the sensor to produce H<sub>2</sub>O<sub>2</sub> when glucose is present, thus creating oxidative stress within the cell to trigger the OxyR response system and initiating the *lux* reporter. Any such oxidase enzyme could be included to target sensor specificity for a wide variety of compounds. The assays were conducted in liquid culture with samples generated in the laboratory.

Creating a general response biosensor is typically approached by developing a panel of bacteria, each responsive to a different threat. Panels of *E. coli* bacteria were engineered to create sensors for heat shock, oxidative stress, and protein damage (Belkin *et al.*, 1997), DNA damage (Belkin, 2003), oxidative damage, membrane damage, DNA damage, and protein damage (Kim and Gu, 2003), and heat shock, oxidative stress, fatty acids, peroxides, and genotoxicity (Premkumar *et al.*, 2003). A *lux*-containing *E. coli* strain immobilized in poly (vinyl alcohol) (PVA) was used to create a slow release biosensor for general stress where the PVA matrix was dissolved using KCl over time so that new cells were being used for each toxicity test (Horsburgh *et al.*, 2002). Biosensors for genotoxicants were created by inserting a *lux* reporter into the *recA* promoter region for DNA damage repair in *E. coli*.

(Polyak *et al.*, 1997; Belkin, 2003; Polyak, 2001). Elasri *et al.* (2000) created a similar sensor using *P. aeruginosa*.

Two well-known assays for genotoxics and cytotoxics are the SOS-*Lux* test and the *Lac*-Fluoro test. The SOS-*Lux* test was created by adding the *lux* reporter under the control of the SOS DNA damage repair system to identify genotoxics. The *Lac*-Fluoro test uses constitutive expression of *gfp*, which is inserted to report cell maintenance function and to indicate cytotoxins. Decreases in fluorescence shows cytotoxicity, or impacts to cell metabolism and function (Baumstark-Khan *et al.*, 2001).

The toxicity of heavy metals (chromium, zinc, copper, nickel, and arsenic) was evaluated using a microtiter plate setup and two strains of *Salmonella typhimurion*, one modified for the SOS-*Lux* and one for the *Lac*-Fluoro test (Rabbow *et al.*, 2002).

Improvements to the sensitivity of the SOS-*Lux* test were obtained by inserting the reporter plasmid into *E. coli* containing a *tolC* mutation, which made the membrane more permeable to hydrophobic substances. The sensitivity was further improved by using a *S. typhimurion* strain with a defect in the cell membrane, which again increases the membrane permeability (Rettberg *et al.*, 2001). The SOS-*Lux* and the *Lac*-Fluoro tests developed by Rabbow *et al.* (2002) have been applied in practice on the international space station to determine toxicity of recycled water supplies on the station. A different sensor formulation with the similar genetic modifications has been used to determine the threat from radiation on the space station (Rabbow *et al.*, 2003).

On the whole, genetically engineered strains used in biosensors have not been commercialized to a large degree. The difficulty in overcoming the genetically modified organism (GMO) regulations makes such sensors primarily useful only in laboratory settings,

where the threat of accidental release is not applicable. Despite their advantages in terms of robust, repeatable responses, engineered strains have yet to be widely commercialized.

#### *Non-engineered strains*

One drawback of the majority of work to date is that most sensors employ genetically modified bacteria as the reporter. A notable exception is the commercial Microtox<sup>®</sup> assay, which uses naturally luminescent *Vibrio fischerii* bacteria. Non-engineered cells do not mandate such strict controls on release as those that have genetic modifications. While engineered cells may yield a more robust response, wild-type cells facilitate eventual commercialization of a sensor. Additionally, the use of indigenous wild type cells more accurately reflects the conditions under observation than the use of an engineered lab strain. Using wild-type cells means that the intrinsic cell processes must be harnessed to detect the compounds of interest or to determine if the cells are inhibited.

BOD sensors typically do not require genetic engineering to create a functional sensor since the concentration of oxygen in a sample can be easily monitored. These sensors are typically constructed using an immobilized bacterial culture contained between a dialysis membrane and a gas permeable membrane. The sample fluid diffuses through the dialysis membrane and passes through the culture where some of the oxygen in the sample is consumed. The amount of oxygen remaining in the sample is measured using a dissolved oxygen electrode placed above the gas permeable membrane. The respiration rate of the culture is calculated from the difference in oxygen concentrations between the amount in the sample initially and that detected by the electrode after exposure to the cells (Liu and Mattiasson 2002). Current work (Heim *et al.* 1999) has focused on combining two pure



cultures to expand the limited range of compounds detected when one pure culture is used, or an ensemble of bacteria, which shows unstable response over time as different species dominate (Tan and Wu 1999). In general, these sensors are complicated to apply because the respiration rate shifts depending on the amount of substrate present in the sample. Adjusting for this variation, this type of BOD sensor has been shown to be as effective as the traditional five-day BOD test but with a response within minutes. However, the variability between sensors of the same construction is significant (Liu and Mattiasson 2002).

In addition to BOD sensors, amperometric biosensors have been developed that function by binding cells to a screen printed electrode to measure the transfer of electrons during substrate consumption. One example of this type of sensor was developed by Skladal *et al* (2002) to create a phenol sensitive biosensor. *Pseudomonas* strains were immobilized on a screen-printed electrode such that the uptake of phenol as a carbon and energy source by the cells can be detected by the electrode as electrons are transferred. The sensor showed a rapid, reproducible response. However, the sensing surface had to be prepared and used on the same day and the response varied depending on the ionic strength of the sample.

Natural products of cells can also be monitored to determine if they are inhibited. For example, Guven *et al.* (2003) created a bioassay for inhibition of enzyme biosynthesis to monitor the concentrations of two enzymes, one produced by *E. coli* and the other produced by *Bacillus subtilis*. Colorimetric tests were used to monitor beta-galactosidase synthesis in *E. coli*, which is created during consumption of glucose and is metabolism related, and alpha-amylase synthesis in *B. subtilis*, which is created during late log stage and is growth phase related. Changes in the concentrations of these enzymes indicated the presence of toxic compounds. The system worked very well for pesticides, the model organics tested, but was

less repeatable with heavy metals. This type of assay takes much longer than an engineered “lights on” or “lights off” strain, because up to eight hours are required to determine if a decrease has occurred in the enzyme synthesis.

#### *Cell components in biosensors*

The use of cell components (purified enzymes) in biosensors is an attractive alternative to whole, living cells, which require a constant supply of nutrients and oxygen. These systems typically consist of the sensing element (enzyme) bound to an electrode such that the change in concentration of a product is converted into an electric signal monitored by a detector (reviewed in Karube and Nomura, 2000). An example of such a system was created by Moser *et al.* (2002) in which oxidase enzymes specific to glucose, lactate, glutamate, and glutamine were immobilized into a flow through microfluidic device. The response was rapid and repeatable and a single sensor could perform continuous monitoring of all four compounds of interest. However, isolation of the enzymes used in this type of sensor is costly and time consuming and enzymes alone are less stable than whole cells (Karube *et al.*, 1995).

Using whole cells that have been killed provides a useful method of preserving the enzymes and eliminates the purification step. Tan and Zhenrong (1998) used thermally killed *Bacillus subtilis* cells immobilized in a membrane bound to the end of a DO probe to create a sensor for BOD. The BOD reported by the sensor correlated well with BOD<sub>5</sub> assays performed on identical samples, with results available within half an hour. This type of biosensor functions by incorporating the active components necessary to catalyze the

oxidation of carbon sources, specifically, enzymes and cofactors, but without including the difficult and time consuming step of isolating these enzymes from living cells.

### **Microfluidic sensors**

These macroscale sensors using whole cells or cell components can be improved by miniaturization. Reducing the size of a sensor to the microscale to create microelectromechanical systems (MEMS) presents several advantages in sensing ability. Microsensors require much lower sample and analyte volumes, present a more rapid response than full-scale sensors, and can be made disposable because of the small size and volumes involved, thus creating a highly cost-effective analysis system. However, the robustness of these systems to harsh environments has not been proven and they have also been slow to commercialize.

Several groups have used microfluidic technology to create biosensors. One prominent example relevant to environmental engineering is the class of BOD sensors created by Yang *et al.* (1996, 1997), where whole cells were immobilized directly onto the surface of a microscale DO probe. The cells used were *Trichosporon cutaneum*, useful for BOD sensors because they consume a wide range of carbon sources, not a limited few compounds. In this way, they report a BOD closer to the BOD<sub>5</sub> than what would be reported by a sensor using a strain such as *Pseudomonas*, which prefers to grow on acetate. With the sensor, this group was able to achieve sensor BOD to BOD<sub>5</sub> ratios of 0.65 to 1.70 with real wastewater samples and a repeatability of plus or minus eight percent was reported. The response time was twenty minutes and the sensor was linear for a BOD range of 0.2 to 18 mg/L BOD. Additionally, because it is on the microscale, the device is smaller and easy to

handle. Such a sensor would be useful to indicate spikes in influent and effluent BOD; for such an application, the limited precision of the device is less of a factor because the purpose of the sensor is to provide nearly real-time monitoring, not reportable BOD values.

In addition to whole cells, enzymes are commonly used within the microscale sensors as reporters for the presence of certain compounds. Zhan *et al.* (2002) immobilized a pH reporting dye and enzymes to catalyze specific reactions in a microreactor within a microfluidic channel array to create a biosensor for potentially any compound of interest. Adding the correct enzymes created a pH shift, reported by the dye, and the magnitude of the shift correlated to the concentration of the analyte that reacted with the enzymes. Moser *et al.* (2002) created a bio-MEMS using enzymes bound within a flow channel with electrodes to report changes in current as the enzymes reacted with the species of interest, which were glucose, lactate, glutamate, and glutamine. Petrou *et al.* (2002, 2003) created a bio-MEMS sensor for glucose and lactate by immobilizing enzymes in a microchannel and measuring the response with a dialysis probe made of polyacrylonitrile fiber. Zimmerman *et al.* (2003) created a flow-through glucose sensor by immobilizing glucose oxidase enzyme in polyvinyl alcohol (PVA) polymerized by UV light within a microfluidic system. Due to high fabrication temperatures associated with the anodic bonding between wafer sheets, it was important that the enzymes were immobilized in situ after device fabrication.

These types of sensors were designed for medical applications, such as monitoring the concentrations of sugars in blood samples. Although the concept could be modified for application in environmental engineering processes by changing the enzymes used in the sensors, this design is less useful for general monitoring. Such sensors are primarily useful for monitoring the concentration of a few known compounds, and so could be applied to

sensing compounds known to be present in environmental samples. However, such sensors do not address the need for monitoring a wide range of toxic compounds.

### **Immobilization Matrices**

The immobilization of cells within a microfluidic sensor is critical to the functionality of the system. Using a biofilm of cells adhered to the bottom of the flow channel is likely to be unstable, as cells and chunks of film can slough off with time and foul the detector or clog the channel. Immobilizing cells within hydrogels prevents sloughing, provides some degree of protection for the cells, and exposes the cells to an environment similar to that within a biofilm (Junter *et al.*, 2002). There are two primary types of hydrogels, those that are chemically polymerizable and those that are photopolymerizable.

Chemically polymerized hydrogels, such as sodium alginate, are useful for macroscale work by forming beads from the gel precursor solution (Drury *et al.*, 2004). However, downsizing the bead to microscale may prove difficult to form. Therefore, photopolymerized polymers are typically used for microfluidic applications because they can easily be formed into a variety of shapes in situ by using various photomasks to control what areas of the polymer precursor are polymerized. First, Beebe *et al.* (2000) created various shapes of hydrogels by polymerizing acrylic acid and methacrylate in situ in a microchannel, showing the ease of handling with the photopolymer. Further, this group used pH-sensitive polymers to control flow within a microfluidic channel matrix by placing polymers of varying compositions at critical points in the flow matrix such that shifts in pH would cause expansion or contraction of the polymer patch and, thus, either allow or block flow through particular regions of the channels. This passive method of flow control simplifies

microfluidic componentry, but for biological systems, the pH extremes required to change the flow regime would prove detrimental to the cells in the system. Moving from flow control to the development of a reporting system, Zhan *et al.* (2002) immobilized the glucose oxidase enzyme within several micropatches in a microfluidic device. The device reported the concentration of glucose by shifts in the intensity of the reporter dye co-immobilized with the enzyme. This sensor would be used for medical applications, but still shows the usefulness of the photopolymer in microfluidic work.

Enzymes as well as viable cells have been immobilized within photopolymers. Koh *et al.* (2002) encapsulated mammalian cells within polyethylene glycol (PEG) diacrylate (PEG-DA) with Darocure 1173 as the photoinitiator polymerized with UV light. Cells were viable up to a week after polymerization based on observations using the LIVE/DEAD viability/cytotoxicity fluorescence staining. This application was for tissue engineering and not biosensor development. However, Heo *et al.* (2003) immobilized *E. coli* cells in PEG-DA within a microfluidic channel constructed of polydimethylsiloxane (PDMS) using photopolymerized micropatches of gel spanning the height of the channel, but not the width, to permit flow around the edges of the hydrogels. The authors attempted to prove cell viability using LIVE/DEAD staining and 2', 7'-bis-(2-carboxyethyl)-5-(and-6)-carboxyfluorescein (BCECF-AM) staining. The LIVE/DEAD stain was ineffective because the hydrogel fluoresced strongly green, so live cells could not be observed above the background fluorescence. Additionally, the BCECF-AM stain indicated enzyme activity, not true viability, because enzymes remain active after a cell is no longer considered viable. This work did not develop a field-deployable sensor with the photopolymer, but simply tried to prove viability within the matrix.

One difficulty associated with the photopolymerizable systems is mixing the cells with the gel precursor solution because the components are highly viscous and the shear stresses on the cells during mixing may increase cell mortality. Modifications to the gel structure have been undertaken in an attempt to create a low molecular weight hydrogel based on alginate. Kong *et al.* (2003) created different molecular weight alginates by irradiation and the viscosity of each was measured by shear stress and shear rate. Results showed that higher radiation doses reduced the molecular weight most significantly, but doses in the mid-range of those tested made the gels stiffer because only the flexible connectors of the gel matrix broke during radiation, leaving the strong bonds intact. At low doses, no change in stiffness was observed. Osteoblasts were mixed with the gels before polymerization. The lower molecular weight gels resulted in greatly improved viability as measured visually by microscopy using the Trypan blue stain, which cannot enter cells with intact membranes, but stains the nuclei of cells with compromised membranes.

Overall, the photopolymerizable system is preferable for microfluidic work because it can be formed into a variety of shapes by changing the photomask prior to polymerization. Photopolymerizable polymers have been used to successfully immobilize both eukaryotic and prokaryotic cells, as well as to immobilize enzymes for the creation of a sensor. However, the major challenges that users of photopolymerizable polymers face are the toxicity of the polymer components and the difficulty visualizing cells within the polymer microscopically, because the polymer tends to absorb stains such as the green stain of the LIVE/DEAD package.

## Scope of Research

Based on this review of biosensors developed previously, it is clear that the need for a non-engineered bacterial sensor for a range of toxic compounds has not yet been addressed. Many groups have created compound-specific sensors using both whole cells as well as purified enzymes, but no general stress response sensor has been developed yet. Microtox<sup>®</sup> uses a non-engineered strain, but quantifies toxicity, not stress. In wastewater treatment, electrophilic stress results in process upset and reduced treatment capacity. To reduce instances of process upset, a sensor that responds to electrophilic insult quantified by monitoring the intrinsic stress response of the immobilized cells, not by engineering a known response into the cells, can be developed.

The objective of this work is to evaluate the performance of an immobilized bacterial culture that will comprise the biological sensing element within a biosensor for detecting electrophilic compounds based on activation of the GGKE mechanism. The biosensor will consist of bacterial cells immobilized in a hydrogel matrix in a microfluidic flow through setup. In its ultimate application, the biosensor will direct water to be monitored over the immobilized cells. Any electrophilic toxins in the flow will trigger potassium efflux from the cells. The potassium concentration will be measured using an ion-selective film (Kopelman *et al.*, 1997) over which the flow will pass both before and after contacting the cells. The change in potassium will be monitored and, if efflux is indicated, the device will implicate the presence of electrophilic toxins. For wastewater treatment applications, electrophilic toxins have been linked to deflocculation and, thus, to process upset. A positive response by the sensor would give plant operators early warning of process upset potential in the influent so that the toxic slug could be rerouted to storage and slowly fed in for treatment to avoid



upset. For surface, ground, or drinking water applications, many chemical agents that could be used to threaten homeland security are classified as electrophiles, such as nerve agents, and could be effectively sensed. On the whole, the sensor under development would improve process stability at wastewater plants and improve confidence in water supply at drinking water plants.

To determine the feasibility of a biosensor based on the intrinsic potassium efflux stress response, the potassium efflux potential of polymer-immobilized bacterial culture was evaluated experimentally by comparing to non-immobilized planktonic cultures. Furthermore, a model was developed to determine of the number of cells needed to efflux detectable levels of potassium, while estimating the oxygen requirement for these cells to determine if oxygen would be limiting within the system. Three matrices, alginate, a photopolymerizable polymer, and a thermally reversible gel, were evaluated as possible hydrogels for immobilization. Both the viability and the potassium efflux from immobilized cells were elucidated. This work will become the basis for the incorporation of the immobilized cells into the microfluidic device.

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**Evaluating strategies for integrating bacterial cells into a  
biosensor designed to detect process upset  
Part A: viability and activity**

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**Abstract:** The biological element of a biosensor to predict process upset in wastewater treatment plants is characterized. The bacterial culture was immobilized in a range of hydrogel polymers: a calcium alginate, a series of photopolymerizable polymers, and a thermally-reversible gel. Oxygen uptake rates and LIVE/DEAD staining were used to determine the activity and viability of the immobilized cultures. The alginate showed good viability, but poor mechanical stability in that the matrix dissolved after five days. The photopolymerizable polymers resulted in high mortality, although the matrix remained stable. The thermal polymer showed extended viability up to 12 days after immobilization, and the material did not deteriorate with time.

## **1. Introduction**

Biosensors show promise for real time monitoring of toxicity in environmental samples. A biosensor is generally defined as an analytical tool that pairs a biological element with a detection system to produce a measurable response, which can be quantified into the amount of analyte present in a sample (Belkin, 2003). The response is typically measured by electrochemical or optical means. Biological elements are typically enzymes, antibodies, proteins, nucleic acids, or whole cells (Belkin, 2003). Whole cells have a certain limited lifespan, have longer response times than isolated components, and may show significant variability between cell batches (Ramanathan *et al.*, 2000). On the other hand, whole cells are less expensive to use because their components require no isolation and purification as in the cell component assay systems. Also, whole cells provide information on the bioavailability of toxins being monitored instead of simply reporting the concentration present. Overall, whole cell biological elements provide a means to monitor more elaborate biological responses than biosensors based on *in vitro* biochemical responses.

For general environmental monitoring, many compounds may be responsible for the toxicity of a sample, and so development of sensors that indicate many different toxic compounds are required. Creating a general response biosensor is typically approached by developing a panel of bacteria, each responsive to a different threat. Panels of *E. coli* bacteria were engineered to create sensors for heat shock, oxidative stress, and protein damage (Belkin *et al.*, 1997), DNA damage (Belkin, 2003), and oxidative damage, membrane damage, DNA damage, and protein damage (Kim and Gu, 2003). A field-ready biological element was developed by Premkumar *et al.* (2003), who immobilized bacteria that were engineered to report on heat shock, oxidative stress, fatty acids, peroxides, and genotoxicity in thick silicate films, which maintained viability and activity for over a month (Premkumar *et al.*, 2003).

On the whole, genetically engineered strains used in biosensors have not been commercialized to a large degree. The difficulty in overcoming the genetically modified organism (GMO) regulations makes such sensors primarily useful only in laboratory settings, where the threat of accidental release is minimized. Despite their advantages in terms of robust, repeatable responses, engineered strains have yet to be widely commercialized.

Non-engineered cells do not mandate such strict controls on release as those that have genetic modifications. While engineered cells may yield a more robust response, wild-type cells facilitate eventual commercialization of a sensor, exemplified by the Microtox<sup>®</sup> assay, which uses naturally luminescent *Vibrio fischerii* bacteria. Additionally, the use of indigenous, wild-type cells may more accurately reflect the conditions under observation than the use of an engineered lab strain. Using wild-type cells means the intrinsic cell

processes must be harnessed to detect the compounds of interest or determine if the cells are inhibited.

The purpose of this work was to explore strategies for immobilizing non-engineered bacterial cells for inclusion into a biosensor designed to predict process upset in wastewater treatment plants. Process upset is commonly characterized by such symptoms as ineffective biological oxygen demand (BOD) removal, ineffective nitrification, deflocculation, and sludge bulking (Love and Bott, 2000). These process effects observed during an upset event result in poor treatment and possibly permit violations. Developing a biosensor based on the natural cell physiological response to chemical insult would give an early warning that toxic chemicals were present. This warning would significantly benefit wastewater treatment operations by allowing operators time to respond to the approaching threat, and could also clarify the type of operational adjustment needed to prevent or remediate treatment process damage.

For this study, bacterial cells were immobilized in a range of polymer matrices and cell viability and activity was assessed. Immobilization of the bacterial cells was important because it keeps the cell concentration relatively constant by maintaining cell viability while reducing cell division. Additionally, immobilized cells cannot slough off as a biofilm layer and clog downstream channels in the device. Such clogging is particularly problematic if a liquid microfluidic conveyance system is used. Chemically polymerized hydrogels, such as sodium alginate, are useful for macroscale work and form beads from the gel precursor solution (Drury *et al.*, 2004). Photopolymerized polymers have also been used for microfluidic applications because they can easily be formed into a variety of shapes in situ by using various photomasks to control the areas of the precursor that are polymerized (Beebe *et*

*al.*, 2000; Heo *et al.*, 2003). Further, viable cells have been immobilized within photopolymers. One type of photopolymer, polyethylene glycol (PEG) diacrylate (PEG-DA) with Darocure 1173 as the photoinitiator polymerized with UV light, has been used to immobilize *E. coli* cells (Heo *et al.*, 2003) within a microfluidic channel constructed of polydimethylsiloxane (PDMS). The authors attempted to prove cell viability using LIVE/DEAD staining, but found the stain ineffective because the hydrogel fluoresced strongly green, so live cells could not be observed above the background fluorescence. Overall, photopolymers have been used for cell immobilization because it is easy to form them into a variety of shapes *in situ*, while the alginate is suited only for macroscale applications because the ability to control the shape of the polymerized product is limited.

In the current work, a set of three polymers was investigated for use as the immobilization matrix in the biological element of the biosensor: a calcium alginate, a series of photopolymerizable polymers, and a thermally-reversible gel. The specific goals of the work were to evaluate viability and activity of immobilized cells to determine a preferred matrix for further study of detectable physiological responses to chemical perturbations.

## **2. Materials and Methods**

### **2.1 Bacterial culturing**

#### **2.1.1 Growth conditions**

*Pseudomonas aeruginosa* was isolated previously from a local wastewater treatment plant and was grown in a mineral salt medium denoted PA M9. This medium consisted of NaH<sub>2</sub>PO<sub>4</sub>, 3.0 g; Na<sub>2</sub>HPO<sub>4</sub>\*7H<sub>2</sub>O, 6.0 g; NH<sub>4</sub>Cl, 1.0 g; NaCl, 0.50 g; MgSO<sub>4</sub><sup>2-</sup>\*7H<sub>2</sub>O, 0.246 g; CaCl<sub>2</sub>, 0.0147g; FeSO<sub>4</sub>\*7H<sub>2</sub>O, 2.5 mg; ZnCl<sub>2</sub>, 0.25 mg; MnSO<sub>4</sub>\*H<sub>2</sub>O, 0.185 mg; CuSO<sub>4</sub>, 0.030 mg; NaMoO<sub>4</sub>\*2H<sub>2</sub>O, 0.006 mg; CoCl<sub>2</sub>\*6H<sub>2</sub>O, 0.001mg; H<sub>3</sub>BO<sub>3</sub>, 0.03 mg; glacial

acetic acid, 0.89 mL per liter solution. A second medium denoted PA BT was used to improve alginate stability when it was the immobilizing hydrogel. The PA BT media consisted of:  $\text{NaH}_2\text{PO}_4$ , 0.3 g;  $\text{Na}_2\text{HPO}_4 \cdot 7\text{H}_2\text{O}$ , 0.6 g;  $\text{NH}_4\text{Cl}$ , 0.1 g;  $\text{NaCl}$ , 0.05 g; Bis Tris, 1.0 g;  $\text{MgSO}_4^{2-} \cdot 7\text{H}_2\text{O}$ , 0.246 g;  $\text{CaCl}_2$ , 0.0147g;  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , 2.5 mg;  $\text{ZnCl}_2$ , 0.25 mg;  $\text{MnSO}_4 \cdot \text{H}_2\text{O}$ , 0.185 mg;  $\text{CuSO}_4$ , 0.030 mg;  $\text{NaMoO}_4 \cdot 2\text{H}_2\text{O}$ , 0.006 mg;  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , 0.001mg;  $\text{H}_3\text{BO}_3$ , 0.03 mg; and glacial acetic acid, 0.89 mL per liter solution. After preparing media but before autoclaving, the pH was adjusted to 7.0 using 50% w/v NaOH (approximately 3 mL per liter PA M9 media, and about 4.5 mL per liter PA BT media).

*Escherichia coli* strain K-12, ATCC 29947, was grown on mineral salt medium M9. This media consisted of  $\text{NaH}_2\text{PO}_4$ , 3.0 g;  $\text{Na}_2\text{HPO}_4 \cdot 7\text{H}_2\text{O}$ , 6.0 g;  $\text{NH}_4\text{Cl}$ , 1.0 g;  $\text{NaCl}$ , 0.50 g;  $\text{MgSO}_4^{2-} \cdot 7\text{H}_2\text{O}$ , 0.246 g;  $\text{CaCl}_2$ , 0.0147g; Thiamine HCl, 1.0 mg; and D-glucose, 2.0 g per liter solution. No pH adjustment was required for this media. All media components were obtained from Fisher Scientific (Pittsburgh, PA).

Potassium stock was eliminated from the culture media to reduce the dilution required for the potassium efflux experiments. Potassium contamination from the sodium phosphate buffers, sodium chloride, and sodium hydroxide appeared to be adequate for growth requirements, and resulted in media concentration of about 2 mg/L.

Cultures were maintained in 250 mL Erlenmeyer flasks using a gyratory water bath shaker (Model G76, New Brunswick Scientific, Edison, NJ) set at 37°C and were transferred to fresh media every two days using a 1:100 dilution factor. To expand the volume of culture, cells were transferred at the appropriate dilution to a five liter jug that was aerated using an aquarium pump and diffuser with magnetic stirring placed in an incubator at 37°C. Monthly, cultures were restarted from frozen stock by streaking frozen culture on Luria-

Bertani (LB) agar plates consisting of: NaCl, 10g; tryptone/peptone, 10 g; yeast extract, 5 g; and Bacto agar, 10 g per liter solution. The streaked plate was incubated overnight at 37°C. Then, a single colony was placed aseptically into fresh sterile media.

### 2.1.2 Growth Curve Preparation

A growth curve was determined for each strain using sidearm flasks containing 100 mL growth media incubated in a rotary water bath shaker maintained at 37°C. Transmittance through the media was measured at 590 nm on a spectrophotometer (Spectronic 20, Bausch and Lomb, Philadelphia, PA). Separate growth curves were determined spectrophotometrically for cultures grown in five liter batches.

## 2.2 Immobilization polymer preparations

### 2.2.1 Alginate immobilization

The calcium alginate hydrogel matrix, a copolymer of  $\beta$ -D-mannuronate (M-residue) and  $\alpha$ -L-guluronate (G-residue) (reviewed in Rehm 1998), was used as the preliminary immobilization matrix for the cells because this matrix has been used extensively by others (for example, Elasri *et al.*, 2000; Kohler, 2000; Polyak *et al.*, 1997, 2001; Webb *et al.*, 1997). To form alginate beads, five liters *P. aeruginosa* were grown overnight to mid-log growth state. The cells were concentrated by centrifugation in multiple bottles for 20 minutes at 4420 x g and the supernatant was discarded. The cells were resuspended in about 20 mL of fresh media and divided into aliquots of equal cell number for the immobilization. The resuspended bacterial concentrate was added to a 2% solution (w/v) of sodium alginate (Protanal LF10/60, FMC BioPolymer, Philadelphia, PA, USA) in water using approximately a 10:1 (v/v) ratio of alginate to cell solution. The solution was well mixed and slowly

dropped by a 21-gauge syringe into a 10% solution (w/v) of calcium chloride in water to form spheres. The beads were rinsed with nanopure water and placed in PA BT media.

PA BT media was used for alginate bead experiments because the beads were found to be unstable in the PA M9 media. The central modification for the BT media was the substantial reduction in sodium concentration. Because the alginate polymerizes by substitution of calcium for sodium within the polymer matrix, it was thought that ion exchange could compromise alginate stability and return the beads to the liquid state, which occurred within an hour in the PA M9 media.

The number of cells per batch was determined by dividing the cell concentration by the number of beads per batch. Cell concentration was determined by plating triplicate serial dilutions in sterile nanopure water of the resuspended culture on Luria-Bertani (LB) agar. The plates were incubated overnight at 37°C, and the cell count was determined by counting the number of colonies per plate and correcting for the dilution factor.

### 2.2.2 *Photo-polymer immobilization*

The photopolymerization procedure made it very difficult to create immobilizing beads; therefore, flat disks approximately 0.5 cm in diameter and 0.1 cm in thickness were formed instead. The resuspended bacterial concentrate was added to one of two versions of the photopolymer:

- Photo 1 contained a pre-mixed solution of 5% (w/v) bis(2,4,6-trimethylbenzoyl)-phenylphosphineoxide (Irgacure 819, Ciba, Suffolk, VA, USA) with poly(ethylene glycol) (PEG) (MW 400) containing acrylate ends (SR 344, Sartomer, Exton, PA, USA) mixed with the bacterial concentrate to yield a 25% (w/v) polymer solution.

- Photo 2 contained a pre-mixed solution of 1% (w/v) Irgacure 819 with PEG mixed with the bacterial concentrate to yield a 22 % (w/v) polymer solution.

For both compositions, the cells were concentrated into a volume of about 8 mL of media as described in Section 2.2.1, and the concentrated cell solution was mixed with the polymer precursor. The mixture was dropped by pipette onto a plastic sheet and cured for 10 minutes using an aquarium lamp with peak emission at 420 nm. The cured disks were removed from the sheet and rinsed with nanopure water, and then placed in PA M9 media.

A third photopolymer composition, Photo 3, was created using a different initiator. This solution contained the initiator 2-hydroxy-1-[4-(2-hydroxyethoxy)phenyl]-2-methyl-1-propanone (sold as Irgacure 2959, Ciba, Suffolk, VA, USA) in the Irgacure 819 PEG monomer base. The solutions were premixed as 1% (w/v) of Irgacure 2959 in PEG. The bacterial concentrate was then added and mixed as described above to yield a 22% (w/v) polymer solution. Curing was performed using the same lamp with a cure time of 15 minutes. The disks were rinsed and placed in PA M9 media immediately afterwards. The cell concentration per batch was calculated as described in Section 2.2.1.

### 2.2.3 *Thermal polymer immobilization*

A thermal polymer was also tested. As with the photopolymer, small beads were difficult to generate. To form the thermal polymer sphere, the cells were concentrated into about 20 mL of media as described in Section 2.2.1. The concentrated cell solution was mixed at room temperature in a scintillation vial with a 15% (w/v) solution of liquid thermal polymer, N-isopropylacrylamide-co-acrylic acid (NIPA-co-Aac), a copolymer with 98 mole percent NIPA and 2 mole percent AAc, to result in a 10% (w/v) polymer solution. The vial was equilibrated in a water bath at 40°C for about five minutes until the mixture solidified



into a white gel-like sphere about 1.5 cm in diameter. The somewhat spherical gel was removed from the vial and wrapped in single mesh fabric (21 holes per inch) to facilitate handling. The gel was then placed in the gyratory water bath shaker in PA M9 media at 40°C to maintain the polymer in the gelled state. The cell concentration in the matrix was determined by cell counts, as described in Section 2.2.1.

### 2.3 *Cell activity and viability experiments*

Bacterial activity and viability within the planktonic and immobilized cultures were evaluated respirometrically using oxygen uptake rates and microscopically using a LIVE/DEAD<sup>®</sup> stain, respectively. The LIVE/DEAD<sup>®</sup> stain has been widely used to determine the viability of cells in a population by comparing the number that stain red, representing dead cells, to the number that stain green, representing live cells.

#### 2.3.1 *Oxygen uptake rates*

Oxygen uptake rates (OURs) were used to determine the activity of planktonic and immobilized bacteria over time, with the procedure shown schematically in Figure 1. Measurements were performed with planktonic cultures in parallel with immobilized cultures at time zero, and continued with immobilized cultures over time. For alginate-immobilized cultures, beads were prepared and wrapped in mesh fabric (21 holes per inch) to facilitate handling. Beads were maintained aerobically under sterile conditions in 250 mL Erlenmeyer flasks containing 100 mL of PA BT media, and were transferred to fresh media daily. To determine the OUR, the mesh-bundled beads were transferred from the growth flask to a 300 mL BOD bottle, which was brought to a volume of 300 mL with media and sealed with the dissolved oxygen (DO) probe (Orion 97-08-99, Beverly, MA). The decrease in dissolved oxygen concentration was monitored over time using a computerized data acquisition system

(LabView version 6.0, National Instruments, Austin, TX) with data collected by an attached meter (Accument Research AR25 Dual Channel pH/Ion Meter, Fisher Scientific, Pittsburgh, PA). After the oxygen uptake rate analysis, the mesh-bundled beads were transferred to a sterile flask with fresh media so that measurements could be performed at a later time using the same immobilized cells. All SOUR tests were performed in duplicate.

To determine OURs for the photopolymer immobilized cells, the disks were placed in 300 mL BOD bottles and PA M9 media was added. The bottles were sealed with the DO probes, and the experiment proceeded as described above.

To determine OURs for the thermal polymer immobilized cells, the fabric-bundled gel was removed from its maintenance flask and transferred to a 300 mL BOD bottle. PA M9 media at 40°C was added to the bottles, which were sealed with the DO probes. The test proceeded as above, except that the bottle was immersed in a 40°C water bath for the duration of the SOUR test. To compensate for the temperature variation, a planktonic control tested at day zero was evaluated at the same temperature.

### 2.3.2 *LIVE/DEAD<sup>®</sup> staining*

The LIVE/DEAD<sup>®</sup> BacLight™ Bacterial Viability Kit (Molecular Probes, Eugene, Oregon, USA) was used with a fluorescent microscope (Zeiss Axioscope 2 Plus, Thornwood, NY, USA) and camera system (Zeiss AxioCam MRm, Thornwood, NY, USA) to visually compare the numbers of viable and nonviable cells at 20 and 40x magnification. The kit contents were mixed 1:1 and three microliters of the mixture were added to each milliliter of cells to be stained. To stain all gels, an aliquot of the gel was placed in a microcentrifuge tube with 1 mL of water and stained with the same amount of dye.

### 3. Results and Discussion

#### 3.1 *Oxygen uptake rates (OURs) show extended activity in thermal gels, low activity in photopolymer, and activity until material failure in alginate gels*

OURs performed on cells immobilized in the first formulation of the photopolymer (Photo 1) showed near-zero activity after polymerization, as shown in Figure 2. Therefore, the concentration of initiator was reduced as much as possible without compromising curing quality or time. This new formulation, which contained 1% rather than 5% initiator, was polymer Photo 2. Unfortunately, this reduction still resulted in very low activity (Figure 2). Therefore, the initiator was changed to Irgacure 2959 at 1% (w/v) (polymer Photo 3), but the results continued to show low activity (Figure 2). Changing the cell type may improve the activity, but the current combination of cells and photo-matrices resulted in an immediate and severe reduction in cell respirometric activity when immobilized in the matrix.

In comparison, cell activity was good in the alginate and thermal matrices, although the OUR results indicated more limited activity initially as compared to planktonic controls containing the same number of cells. Figure 2 summarizes the OUR results from these matrices relative to planktonic controls measured at  $t=0$ . Because several groups show elevated OURs relative to control, oxygen diffusion into the polymers appeared uninhibited. In the alginate, the increased OURs probably indicate cell division and colonization within the structure, as observed by Mater *et al.* by microscopy of alginate beads containing immobilized *Pseudomonas* strains. This colonization occurs within the pores of the alginate matrix, which are large enough to permit cell division. The pore size of the thermal polymer is unknown. Because the OURs in the thermal gel also increase over the control, cell division may also be occurring within the polymer structure. In the alginate matrix, the rates

increase consistently, which supports the hypothesis that the cells are using the alginate as a carbon source, creating space for cell division as they consume the structure within which they are contained. Perhaps because of this consumption, the matrix deteriorated within a week of bead manufacture, preventing quantification of the long-term viability of the alginate-immobilized cells. However, an experiment performed to determine whether the cells could use alginate as a sole carbon source showed no difference in initial oxygen uptake rates between immobilized cells (0.050 mg DO per cell per minute) and planktonic cells (0.045 mg DO per liter per minute), both in media without the acetate carbon source. By day two, the OUR for immobilized cells had dropped to 0.019 mg DO per cell per minute, much lower than control, indicating that the cells were losing activity because the carbon source was unacceptable. Perhaps the alginate is metabolized along with HAC, but alone the cells do not consume the polymer.

The thermal polymer showed excellent material stability, with no deterioration observed for over two weeks. The oxygen uptake rates fluctuate relative to the control, as shown in Figure 2, but on the whole the cells remained viable. Clearly, the thermal polymer is a good choice for the immobilization matrix because it is nontoxic to the cells and supports extended viability. However, integrating the thermal polymer into the biosensor is a challenge because of the temperature requirements of this matrix. To overcome this constraint, the sensor requires a small heater to maintain the temperature at the appropriate level (for example, by incorporating titanium/platinum films to permit temperature measurement and regulation, as reviewed in Erickson and Li, 2004). Alternately, the polymer could be modified to shift the critical temperature to a range below ambient (about 25°C). In either case, the thermal polymer showed the most promise for cell activity and,

thus, for inclusion in the biosensor.

### 3.2 *LIVE/DEAD<sup>®</sup> staining is effective in determining immobilized viability in thermal polymer*

The stain was applied to cells immobilized in all matrices tested, but was only effective for the thermal polymer. The spherical bead structure of the alginate prevented the microscope camera from focusing on a single plane of bacteria. Attempts to flatten the beads to permit adequate observation showed a strong background fluorescence with the green stain, making observations of live cells difficult (Figure 3). The photopolymer matrix also fluoresces very strongly green, making observations of live cells difficult, as shown in Figure 3. The thermal polymer showed the ideal response to the dye, in that zero background fluorescence was observed after allowing the polymer to liquefy at room temperature.

The staining of the thermal and photopolymers reinforces the results obtained from the OUR experiments. As shown in Figure 3, all the bacteria immobilized in the photopolymer stain red, whether or not the cells were dropped on the surface of the polymer or mixed with it prior to polymerization. The images shown are typical of those from the other photopolymer formulations. Because the background fluorescence is so strongly green, one could argue that live cells are present that cannot be observed with this method. While that is possible, the extremely low OURs combined with the number of red cells observed in the photopolymers support the conclusion that the survivability in the matrix was very low. The thermal polymer shows good viability, even after 10 days within the matrix, because green cells dominate over red. On the whole, these results replicate the SOUR data, showing that the photopolymer has low viability, while the thermal polymer cells remain mostly viable.

#### **4. Conclusions**

A series of experiments were conducted in this work to identify the most appropriate polymer matrix for bacterial cell immobilization for a biosensor. The ideal matrix is physically and chemically stable over several weeks, non-toxic to the cells, and will not limit the diffusion of oxygen, compounds necessary for cell growth, or compounds, which would trigger a stress response. Three matrices were examined here: a calcium alginate, several photopolymerizable hydrogels, and a thermal polymer.

The sodium alginate matrix was unstable, although bacterial consumption of the matrix as a substrate was not validated as the cause. The material degraded within a week, rendering it incapable of containing the bacteria. The photopolymer was toxic to the cells, resulting in significant cell death immediately after polymerization. Changes to the concentration and the composition of the initiator did not reduce the matrix toxicity. Finally, the thermal polymer matrix was non-toxic, stable, and did not hinder oxygen diffusion. The only limitation on the incorporation of the thermal polymer within the microfluidic sensor is the need to maintain a higher-than-ambient temperature in the cell chamber (40°C). However, adding a micro-scale heater such as that reviewed in Erickson and Li (2004) would meet this need. Alternatively, the polymer could be modified to change its immobilization temperature. By modifying the polymer structure, the critical temperature could be reduced below ambient, and thus reduce the need for a heating element. On the whole, even without such chemical modifications the thermal polymer shows great potential for incorporation in the biosensor.

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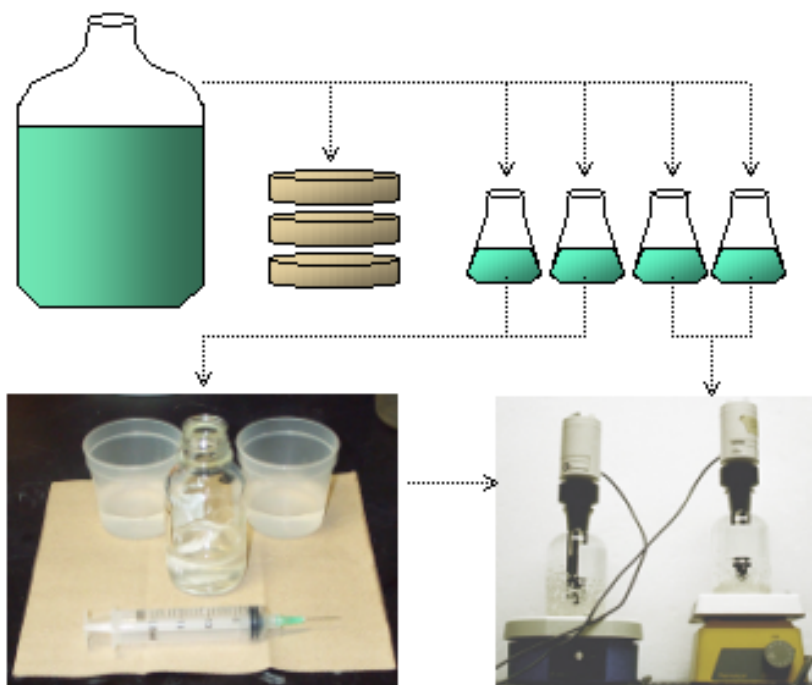


Figure 1: Diagram of the OUR experiment protocol. Cells were grown up in 5 L jugs, concentrated by centrifugation, resuspended, and an aliquot was taken for plate counts. Next, the concentrated cells were divided into four equal batches, with two sets being immobilized in the polymer, and two remaining in the planktonic state. Here, alginate immobilization is shown as an example. The oxygen uptake rates were determined using oxygen probes and a computerized data acquisition system in duplicate for the immobilized cells as well as the planktonic cells.

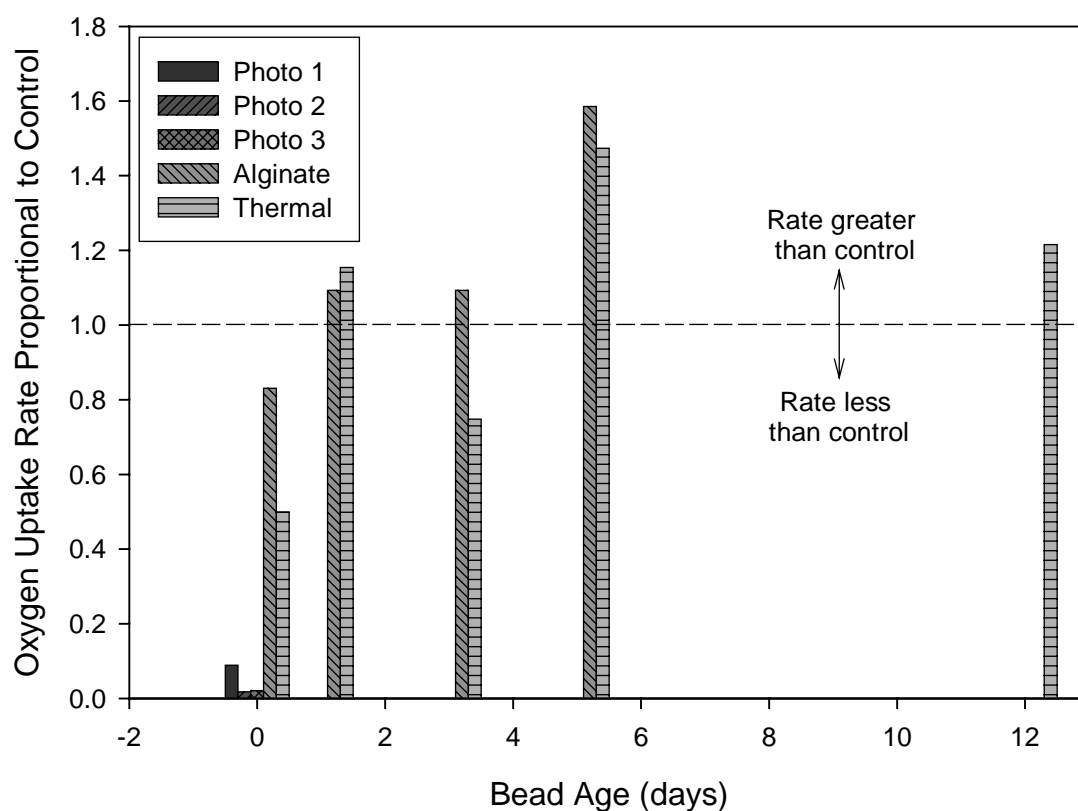


Figure 2: OUR tests for cells immobilized in each polymer matrix. Data is normalized to a planktonic control with equal cell density by dividing the observed rate within the gels by the average rate observed in the controls at  $t=0$ . Photopolymers show near zero oxygen uptake, while thermal and alginate matrices show extended viability. The alginate deteriorated within a week, so further testing with that matrix was impossible.

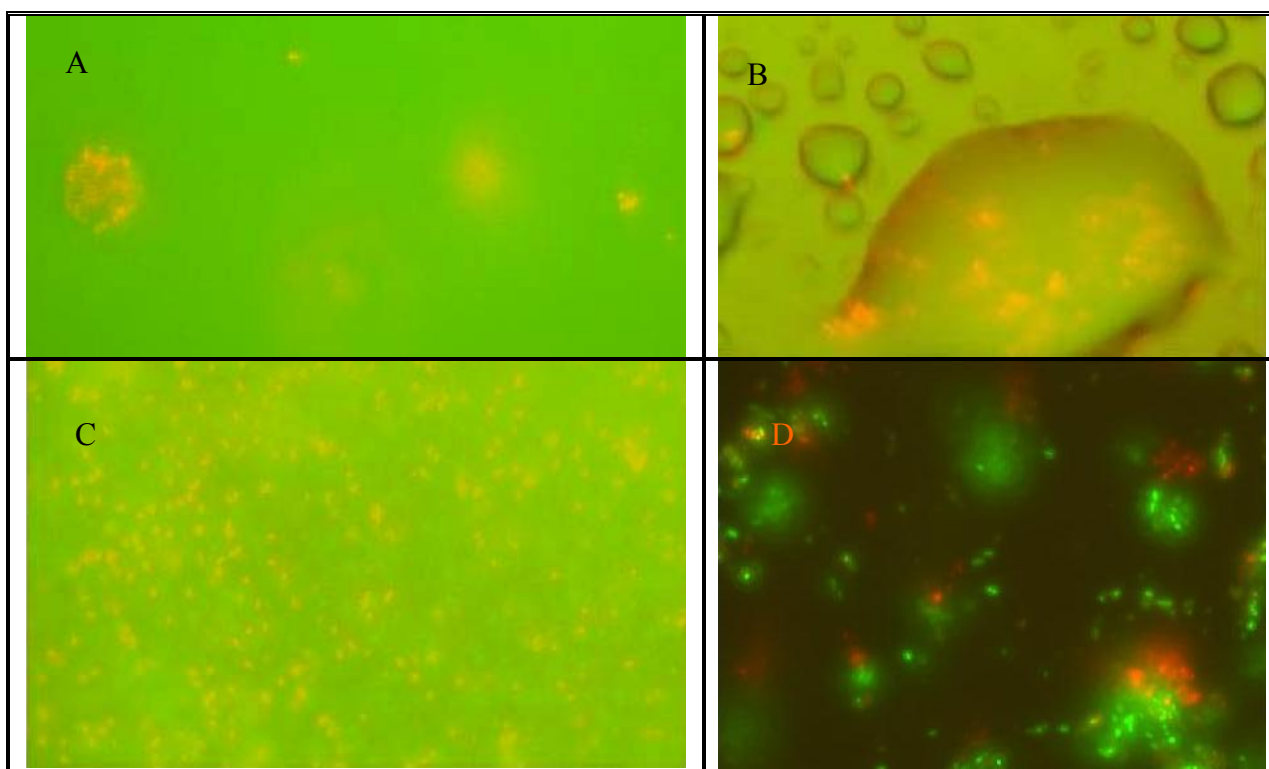


Figure 3: Representative LIVE/DEAD<sup>®</sup> stains of immobilized cells in photopolymer Photo 1 (A and B), alginate (C), and thermal polymer (D). Cells were dropped on the surface of the polymer before polymerization in Image B, while in A cells were completely mixed with the polymer before polymerization. Photopolymer and alginate images were taken immediately after polymerization, while Image D shows the thermal polymer 10 days after immobilization.

**Evaluating strategies for integrating bacterial cells into a  
biosensor designed to detect electrophilic toxins  
Part B: potassium efflux**

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**Abstract:** The biological element of a biosensor to detect electrophilic compounds by harnessing the glutathione-gated potassium efflux (GGKE) stress response system through the detection of effluxed potassium is characterized. The potassium efflux caused by a model electrophile is elucidated in planktonic cultures of *Psuedomonas aeruginosa* and *Escherichia coli*. *P. aeruginosa* was selected for further study because it is an environmentally relevant strain and effluxed comparable potassium per cell to *E. coli*. The bacterial culture was immobilized in two hydrogel polymers: a calcium alginate and a thermally-reversible gel. The potassium efflux from immobilized cells caused by N-ethyl maleimide, a model electrophile, was elucidated. The efflux from the alginate and thermal polymers was strong initially, but deteriorated with time, probably due to potassium limitation in the media.

## **1. Introduction**

Real-time monitoring of toxicity in environmental samples is primarily performed through biosensors or bioassays, because laboratory analytical techniques take more time and require knowledge of the compound of interest in the sample. A number of whole-cell biosensors have been developed using genetically modified bacterial strains that respond to particular compounds, such as phenol (Philp *et al.*, 2003; Gu and Choi, 2002), polycyclic aromatic hydrocarbons (PAHs) (Reid *et al.*, 1998), and heavy metals (Taurianinen *et al.*, 1998). One drawback with most whole cell biosensors is that they employ genetically modified bacteria as the reporter, the use of which is prohibited in many locations. One notable exception is the commercial Microtox<sup>®</sup> assay, which uses naturally luminescent *Vibrio fischerii* bacteria. Non-engineered cells do not mandate strict controls on release whereas those that have genetic modifications are heavily regulated. Additionally, the use of indigenous wild type cells more accurately reflects the conditions under observation than do

engineered lab strains. With wild-type cells the intrinsic cellular physiology must be harnessed to detect the presence of compounds of interest or to determine if the cells are inhibited or stressed.

Electrophiles are a class of compounds that have been shown to trigger measurable stress responses in bacterial cells (Bott and Love, 2002). Industrially relevant electrophilic (oxidative) toxins include a range of chemicals, such as heavy metals and organic compounds containing chloro- and imide- constituents. This class of toxins, commonly found in industrial wastewater, is believed to impair biomass function in biological treatment plants when present at shock loads, and can result in process upset (Bott and Love, 2002). The most common modes of process upset are ineffective biological oxygen demand (BOD) removal, ineffective nitrification, deflocculation, and sludge bulking (Love and Bott, 2000). Although there is substantial speculation about the origin of these upsets, operators generally have insufficient information to identify the source of the problem. However, when asked, operators suggested that heavy metals and toxic organic compounds (which include electrophilic chemicals) are among the most common sources of these upsets (Love and Bott, 2000).

It is speculated that electrophilic chemicals cause process upset by triggering stress response mechanisms in the biomass. Activated sludge deflocculation, one common component of process upset, has been linked to bacterial activation of a stress response called the glutathione-gated potassium efflux (GGKE) response (Bott and Love, 2002). This mechanism is initiated when an electrophile enters the cell and the reaction between the electrophile and glutathione (N-(N-L- $\gamma$ -glutamy-L-cysteinyl)glycine) activates potassium efflux pumps located in the cell membrane (Apontoweil and Berends, 1975 a and b) (shown

in Figure 1). GGKE transports potassium ions out of the cell in exchange for hydrogen ions transported into the cell, which acidify the cytoplasm and cause activation of secondary stress responses that protect cells from oxidative damage (Ferguson *et al.*, 2000).

In biomass, the GGKE response results in an increase in extracellular potassium, adding additional monovalent cations in the floc matrix, and increasing the intrafloc monovalent to divalent cation ratio (Bott and Love, 2002). This ratio is an important predictor of floc strength (Higgins and Novak, 1997 a and b). Disrupting that ratio makes flocs unstable and results in loss of biomass from the system (Murthy *et al.*, 1998). This type of upset encompasses the modes of upsets observed with electrophilic shock, namely, ineffective BOD removal, deflocculation, and sludge bulking. The development of sensors around this GGKE response to detect electrophilic compounds entering sewers or wastewater treatment plants would improve process operation and effluent quality by predicting the process effect linked to such upset events, and thus allow the adjustment of process operations to accommodate and minimize the process impact.

The goal of this project was to develop a biosensor based on the GGKE stress response system. By monitoring bulk potassium as an indicator of the stress experienced by the cells, the biosensor will monitor for electrophilic compounds that have been shown to cause deflocculation in the activated sludge process. The microscale biosensor under development includes a whole cell biological element, potassium detection membranes, and microfluidic componentry that compose a lab-on-a-chip device.

Within the biological element, bacterial cells will be immobilized in a polymer matrix. Immobilization of the bacterial cells is important because it as compared to a biofilm, it keeps the cell concentration more constant by maintaining the viability of the

immobilized cells while reducing cell division. Additionally, immobilized cells cannot slough off as a biofilm layer could and clog the microfluidic channels in the device.

The focus of this work was on the design and characterization of the biological element of the biosensor, with the specific goal of quantifying the impact of immobilization on the rate and degree of potassium efflux in response to a model electrophile. In the current work, two polymers were investigated for use as the immobilization matrix: a calcium alginate and a thermally-reversible gel. In the completed sensor, the concentration of potassium will be monitored as an indicator of bacterial stress. By utilizing the intrinsic response of wild type cells and monitoring the change in potassium ion efflux from them, the device is devoid of genetically modified cells and its eventual use and commercialization are simplified greatly.

## **2. Materials and Methods**

### *2.1 Bacterial culturing*

#### *2.1.1 Growth conditions*

*Pseudomonas aeruginosa* was isolated previously from a local wastewater treatment plant and was grown in a mineral salt medium denoted PA M9. This medium consisted of NaH<sub>2</sub>PO<sub>4</sub>, 3.0 g; Na<sub>2</sub>HPO<sub>4</sub>\*7H<sub>2</sub>O, 6.0 g; NH<sub>4</sub>Cl, 1.0 g; NaCl, 0.50 g; MgSO<sub>4</sub><sup>2-</sup>\*7H<sub>2</sub>O, 0.246 g; CaCl<sub>2</sub>, 0.0147g; FeSO<sub>4</sub>\*7H<sub>2</sub>O, 2.5 mg; ZnCl<sub>2</sub>, 0.25 mg; MnSO<sub>4</sub>\*H<sub>2</sub>O, 0.185 mg; CuSO<sub>4</sub>, 0.030 mg; NaMoO<sub>4</sub>\*2H<sub>2</sub>O, 0.006 mg; CoCl<sub>2</sub>\*6H<sub>2</sub>O, 0.001mg; H<sub>3</sub>BO<sub>3</sub>, 0.03 mg; glacial acetic acid, 0.89 mL per liter solution. A second medium denoted PA BT was used to improve alginate stability when it was the immobilizing hydrogel. The PA BT media consisted of: NaH<sub>2</sub>PO<sub>4</sub>, 0.3 g; Na<sub>2</sub>HPO<sub>4</sub>\*7H<sub>2</sub>O, 0.6 g; NH<sub>4</sub>Cl, 0.1 g; NaCl, 0.05 g; Bis Tris, 1.0 g; MgSO<sub>4</sub><sup>2-</sup>\*7H<sub>2</sub>O, 0.246 g; CaCl<sub>2</sub>, 0.0147g; FeSO<sub>4</sub>\*7H<sub>2</sub>O, 2.5 mg; ZnCl<sub>2</sub>, 0.25 mg;



MnSO<sub>4</sub>\*H<sub>2</sub>O, 0.185 mg; CuSO<sub>4</sub>, 0.030 mg; NaMoO<sub>4</sub>\*2H<sub>2</sub>O, 0.006 mg; CoCl<sub>2</sub>\*6H<sub>2</sub>O, 0.001mg; H<sub>3</sub>BO<sub>3</sub>, 0.03 mg; and glacial acetic acid, 0.89 mL per liter solution. After preparing media but before autoclaving, the pH was adjusted to 7.0 using 50% w/v NaOH (approximately 3 mL per liter PA M9 media, and about 4.5 mL per liter PA BT media).

*Escherichia coli* strain K-12, ATCC 29947, was grown on mineral salt medium M9. This media consisted of NaH<sub>2</sub>PO<sub>4</sub>, 3.0 g; Na<sub>2</sub>HPO<sub>4</sub>\*7H<sub>2</sub>O, 6.0 g; NH<sub>4</sub>Cl, 1.0 g; NaCl, 0.50 g; MgSO<sub>4</sub><sup>2-</sup>\*7H<sub>2</sub>O, 0.246 g; CaCl<sub>2</sub>, 0.0147g; Thiamine HCl, 1.0 mg; and D-glucose, 2.0 g per liter solution. No pH adjustment was required for this media. All media components were obtained from Fisher Scientific (Pittsburgh, PA).

Potassium stock was eliminated from the culture media to reduce the dilution required for the potassium efflux experiments. Potassium contamination from the sodium phosphate buffers, sodium chloride, and sodium hydroxide appeared to be adequate for growth requirements, and resulted in media concentration of about 2 mg/L.

Cultures were maintained in 250 mL Erlenmeyer flasks using a gyratory water bath shaker (Model G76, New Brunswick Scientific, Edison, NJ) set at 37°C and were transferred to fresh media every two days using a 1:100 dilution factor. To expand the volume of culture, cells were transferred at the appropriate dilution to a five liter jug that was aerated using an aquarium pump and diffuser with magnetic stirring placed in an incubator at 37°C. Monthly, cultures were restarted from frozen stock by streaking frozen culture on Luria-Bertani (LB) agar plates consisting of: NaCl, 10g; tryptone/peptone, 10 g; yeast extract, 5 g; and Bacto agar, 10 g per liter solution. The streaked plate was incubated overnight at 37°C. Then, a single colony was placed aseptically into fresh sterile media.

### 2.1.2 Growth Curve Preparation

A growth curve was determined for each strain using sidearm flasks containing 100 mL growth media incubated in a rotary water bath shaker maintained at 37°C. Transmittance through the media was measured at 590 nm on a spectrophotometer (Spectronic 20, Bausch and Lomb, Philadelphia, PA). Separate growth curves were determined spectrophotometrically for cultures grown in five liter batches.

## 2.2 Immobilization polymer preparations

### 2.2.1 Alginate immobilization

The calcium alginate hydrogel matrix, a copolymer of  $\beta$ -D-mannuronate (M-residue) and  $\alpha$ -L-guluronate (G-residue) (reviewed in Rehm, 1998), was used as the preliminary immobilization matrix for the cells because this matrix has been used extensively by others (for example, Elasri *et al.*, 2000; Kohler, 2000; Polyak *et al.*, 1997, 2001; Webb *et al.*, 1997). To form alginate beads, five liters *P. aeruginosa* were grown overnight to mid-log growth state. The cells were concentrated by centrifugation in multiple bottles for 20 minutes at 4420 x g and the supernatant was discarded. The cells were resuspended in about 20 mL of fresh media and divided into aliquots of equal cell number for the immobilization. The resuspended bacterial concentrate was added to a 2% solution (w/v) of sodium alginate (Protanal LF10/60, FMC BioPolymer, Philadelphia, PA, USA) in water using approximately a 10:1 (v/v) ratio of alginate to cell solution. The solution was well mixed and slowly dropped by a 21-gauge syringe into a 10% solution (w/v) of calcium chloride in water to form spheres. The beads were rinsed with nanopure water and placed in PA BT media.

PA BT media was used for alginate bead experiments because the beads were found to be unstable in the PA M9 media. The central modification for the BT media was the

substantial reduction in sodium concentration. Because the alginate polymerizes by substitution of calcium for sodium within the polymer matrix, it was thought that ion exchange could compromise alginate stability and return the beads to a liquid state, which occurred within an hour in the PA M9 media.

The number of cells per batch was determined by dividing the cell concentration by the number of beads per batch. Cell concentration was determined by plating triplicate serial dilutions in sterile nanopure water of the resuspended culture on Luria-Bertani (LB) agar. The plates were incubated overnight at 37°C, and the cell count was determined by counting the number of colonies per plate and correcting for the dilution factor.

#### *2.2.2 Thermal polymer immobilization*

A thermal polymer was also tested. As with the photopolymer, small beads were difficult to generate. To form the thermal polymer immobilization gel, the cells were concentrated into about 20 mL of media as described in Section 2.2.1. The concentrated cell solution was mixed at room temperature in a scintillation vial with a 15% (w/v) solution of liquid thermal polymer, N-isopropylacrylamide-co-acrylic acid (NIPA-co-Aac), a copolymer with 98 mole percent NIPA and 2 mole percent AAc, to result in a 10% (w/v) polymer solution. The vial was equilibrated in a water bath at 40°C for about five minutes until the mixture solidified into a white gel-like sphere about 1.5 cm in diameter. The somewhat spherical gel was removed from the vial and wrapped in single mesh fabric (21 holes per inch) to facilitate handling. The gel was then placed in the gyratory water bath shaker in PA M9 media at 40°C to maintain the polymer in the gelled state. The cell concentration in the matrix was determined by cell counts, as described in Section 2.2.1.

### 2.3 Potassium Efflux Experiments

Potassium efflux experiments at various time points on the growth curve with planktonic cultures were carried out by growing five liters *P. aeruginosa* or *E. coli* overnight to the desired growth state in the appropriate growth medium. The cells were concentrated by centrifugation in multiple bottles for 20 minutes at 4420 x g and the supernatant was discarded. The cells were resuspended in fresh media, combined, and the volume was adjusted to 700 mL with fresh media. Samples were taken from the well mixed flask for soluble potassium and plate counts. The resuspended culture was divided evenly among six flasks with 100 mL per flask. The flasks were placed on a multiple position stir plate and aerated using an aquarium pump to ensure oxygenation during the experiment. One milliliter automatic pipetter tips were placed on the end of the air tubing in each flask to reduce bubble size and to prevent contamination of the tubing. Each of three flasks was shocked with 1 mL of a 5 mg/mL N-ethyl maleimide (NEM) stock, resulting in a dose of 50 mg/L of NEM. Three control flasks remained undosed with NEM. Samples for potassium measurement were taken over a one-hour time period by filtering the media through 0.2 µm nitrocellulose MCE filters (25 mm diameter, Fisher Scientific, Pittsburgh, PA). Samples were acidified with concentrated nitric acid for preservation, and then diluted 1:10 with nanopure water. One milliliter of diluted sample was removed and replaced with 1 mL of 12.7 g/L cesium chloride stock solution (Alfa Aesar, Ward Hill, MA) to minimize interference from sodium. Potassium standards were prepared using a potassium reference solution (Fisher Scientific, Fairlawn, NJ) and the same concentration of cesium chloride was added to standards. The samples were analyzed on an Atomic Absorption Spectrometer (AA) (5100 PC Atomic Absorption Spectrometer, Perkin Elmer, Norwalk, CT). All glassware used in the potassium

measurements was prepared by acid washing in 10% nitric acid, followed by triple rinsing with nanopure water. Error for potassium efflux potential was calculated from the standard deviation of averages for analysis from three flasks and included standard deviation from the cell counts. Cell counts were determined by plating serial dilutions in sterile nanopure water of the resuspended culture on Luria-Bertani (LB) agar. The plates were incubated overnight at 37°C, and the cell count was determined by counting the number of colonies per plate and correcting for the dilution factor.

Potassium efflux experiments with immobilized cultures (procedure shown in Figure 2) were carried out by growing 5 L culture overnight to mid-log growth state (absorbance of the media was between 0.10 and 0.20 at 590 nm) in PA BT media. The polymer immobilization was carried out as described in Section 2.2. Once complete, the immobilized cells were equally divided among six flasks containing 100 mL media each. The experiment on the potassium concentration effluxed per cell after a shock with NEM proceeded in the same manner as described for the planktonic samples, but the experiment time was extended to two hours.

#### *2.4 Alginate bead material stability testing*

The material stability of the alginate beads after exposure to equivalent concentrations of potassium to that observed during efflux was determined using a texture analyzer (TA-XT2i Texture Analyzer, Texture Technologies Corporation, Scarsdale, NY). The instrument was operated to measure force in compression, with a test speed of 0.1mm/s using the 5 kg load cell. Rupture was deemed as the peak of the force curve before reaching the stage.

To determine the effect of potassium on the bead stability, alginate beads without immobilized cells were incubated for two weeks in deionized water containing potassium at a range bracketing the values that would be observed per bead from cell efflux. The maximum efflux per cell was scaled down based on the cell loading per bead to determine the potassium dose per bead. Ten beads were used for each concentration, and the concentrations selected were 0.3 and 0.6 mg potassium per 1.1 mL of liquid to bracket the possible range of efflux potential. The control consisted of 10 beads in 1.1 mL deionized water with no added potassium.

### **3. Results and Discussion**

#### *3.1 Planktonic efflux experiments show no difference between bacterial strains*

A series of potassium efflux experiments were conducted on planktonic cultures of *P. aeruginosa* and *E. coli* across their growth curves to determine which strain effluxed the most potassium per cell, and to determine which growth state elicits the strongest efflux response. A typical result from a batch efflux experiment is shown in Figure 3. Figure 4 shows the series of batch experiments that were performed to compare the potassium efflux potential of the two strains at various growth states on media containing comparable potassium concentration. The average  $K^+$  efflux in planktonic cultures grown to mid log state was  $(4.50 \pm 0.4) \times 10^{-10}$  mg  $K^+$  per cell for *P. aeruginosa* and  $(5.54 \pm 0.8) \times 10^{-10}$  mg  $K^+$  per cell for *E. coli*, while cells in late log phase averaged a potassium efflux of  $(3.07 \pm 0.4) \times 10^{-10}$  mg  $K^+$  per cell for *P. aeruginosa* and  $(4.15 \pm 0.3) \times 10^{-10}$  mg  $K^+$  per cell for *E. coli*. Although it appears that late log phase (0.20-0.25 and 0.25-0.30 absorbance units measured at 590 nm for *E. coli* and *P. aeruginosa*, respectively) experiments produced somewhat lower efflux potential than mid log phase cells (0.025-0.20 and 0.025-0.25 absorbance units

measured at 590 nm for *E. coli* and *P. aeruginosa*, respectively) no difference exists in the average efflux potentials based on a statistical t-test between mid and late log phase experiments with either culture. Further, no difference exists between the average efflux potentials between the cultures at either growth state. Since the activated sludge *P. aeruginosa* isolate used in these experiments effluxes comparable  $K^+$  on average per cell, we continued to use *P. aeruginosa* in further experiments because it may more accurately represent conditions at wastewater plants than the laboratory *E. coli* strain.

### 3.2 *Material failure in alginate beads cannot be attributed to $K^+$ efflux*

Because the alginate matrix degraded after only five days of polymerization, experiments were conducted to determine if the potassium efflux from the cells caused the breakdown of the polymer structure. The alginate polymerizes by substitution of calcium for sodium within the matrix, and matrix stability was hypothesized to be affected by re-equilibration in sodium. Because of the similarity in the properties of sodium and potassium, it was thought that the potassium effluxed from the cells interacts with the matrix and aids in its degradation. However, the concentration of potassium that would be effluxed into the bulk liquid had no effect on the bead stability as measured by a texture analyzer to measure force in compression, as shown in Figure 5.

### 3.2 *Potassium efflux from alginate-immobilized cells is reduced as compared to planktonic cultures, but nearly equal for thermal polymer-immobilized cells*

Experiments to determine the amount of potassium effluxed per cell while immobilized were carried out with *P. aeruginosa* at mid-log growth state in calcium alginate beads. Sample results from initial efflux experiments conducted with alginate-immobilized cells are shown in Figure 6. A t-test showed that the potassium concentration at point four

was statistically different from the initial value, indicating that efflux occurred. The efflux potential with the immobilized culture was  $(1.3 \pm 0.1) \times 10^{-10}$  mg K<sup>+</sup> per cell, as shown in Table 1, which is much lower than the efflux from planktonic cultures. However, efflux was significantly reduced in experiments conducted on the same immobilized cells after five days (shown in Figure 7), probably because the maintenance media had a very low potassium concentration, and the cells were unable to replenish their internal potassium stocks. The large variability and the reduced initial efflux potential observed in the data from the alginate immobilized cells is likely due to electrophilic diffusion limitations into the beads and K<sup>+</sup> out of the beads, although these limitations were not explored or quantified.

On the other hand, the efflux potential from the thermal polymer-immobilized cells was higher than that from the alginate and comparable to the results for planktonic culture, as shown in Table 1. The efflux observed one day after immobilization was  $(4.6 \pm 0.8) \times 10^{-10}$  mg K<sup>+</sup>/cell, four times greater than that of the alginate-immobilized cells (Figure 8). As in the alginate, the efflux potential decreased with time. Figure 9 shows the efflux results from cells immobilized for five days. The figure shows no clear efflux trend, although the control seems to be uptaking potassium. Again, it is thought that the reduced efflux potential with time is attributed to the low-potassium maintenance media.

Table 1: The efflux potential from immobilized *P. aeruginosa* in two polymer matrices on day one as compared to the average of four planktonic experiments

<b>Matrix</b>	<b>Efflux Potential (mg K<sup>+</sup> / cell)</b>	<b>n</b>
None (Planktonic)	$(4.50 \pm 0.4) \times 10^{-10}$	4
Alginate	$(1.3 \pm 0.1) \times 10^{-10}$	1
Thermal	$(4.6 \pm 0.8) \times 10^{-10}$	1



#### **4. Conclusions**

A series of experiments were conducted in this work to select an appropriate polymer matrix for bacterial cell immobilization within the biosensor under development. The ideal matrix will be physically and chemically stable over several weeks, will be non-toxic to the cells, and will not limit the diffusion of oxygen, compounds necessary for cell growth, or the electrophiles which would trigger a stress response. Two matrices were examined here: a calcium alginate and a thermal polymer.

Both polymers showed stable initial efflux results, but later efflux experiments on the polymers resulted in unstable and reduced efflux, perhaps because the potassium concentration in the matrix was limited, thus preventing the cells from replenishing their potassium stocks. The sodium alginate matrix was materially unstable and unable to contain the bacterial cells after five days, but the cause could not be attributed to the potassium effluxed from the cells. Efflux from the alginate beads was four times lower than that from the thermal or the planktonic cells, and the variability was much higher. The thermal polymer was non-toxic, stable, and the initial efflux potential from thermal polymer-immobilized cells was nearly equal to that from planktonic cells. The only limitation on the incorporation of the thermal polymer within the microfluidic sensor is the need to maintain a higher-than-ambient temperature in the cell chamber. On the whole, the thermal polymer shows great potential for incorporation in the biosensor.

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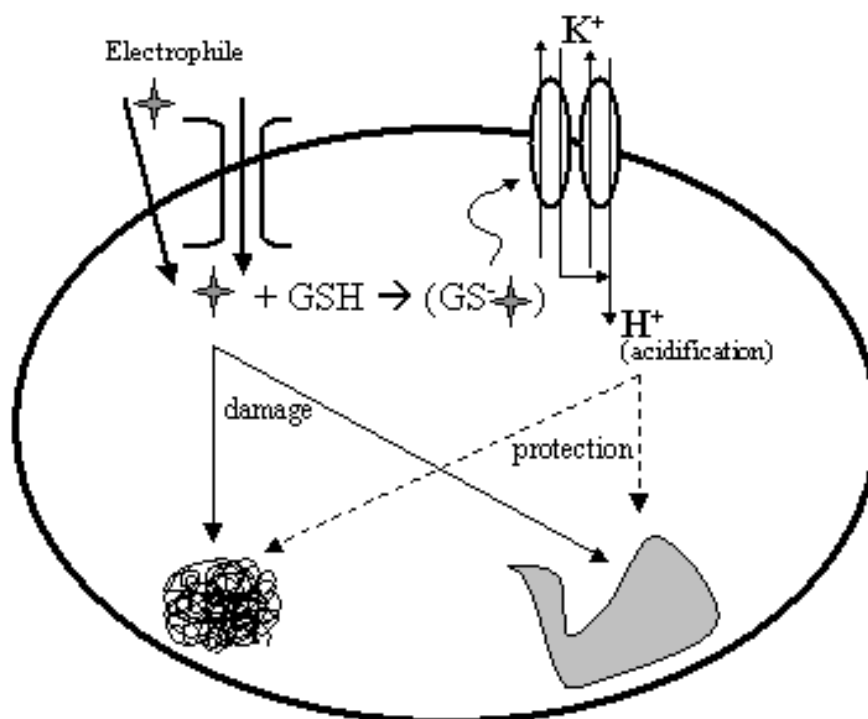


Figure 1: The glutathione-gated potassium efflux (GGKE) system. When an electrophile enters a cell, it can damage DNA and proteins by oxidation. Cells have developed the GGKE stress response to reduce this type of damage. Reduced glutathione, GSH, reacts with the electrophile to create a glutathione-electrophile conjugate. The presence of this conjugate within the cells triggers efflux channels that efflux potassium outside the cell while concurrently importing hydrogen ions. These hydrogen ions acidify the cytoplasm, and the pH drop affords protection from the electrophile for the DNA and proteins within the cell. Overall, the GGKE stress response system is characterized by potassium efflux in response to an electrophilic challenge. (After Dr. Charles Bott, 2001)

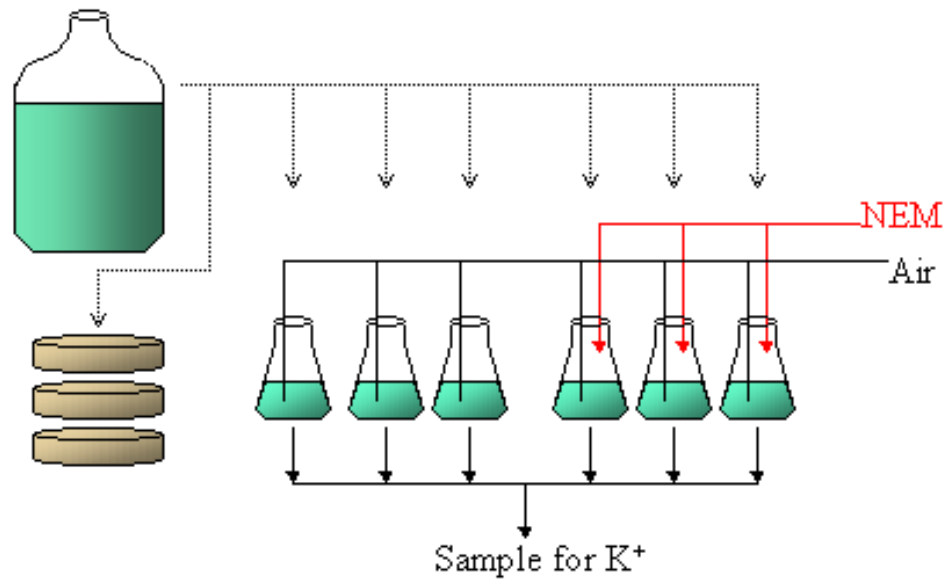


Figure 2: The experimental setup for potassium efflux experiments. Culture was grown to the appropriate growth state in a 5 L jug, then concentrated by centrifugation and resuspended. An aliquot for plate counts was removed. The concentrated culture was divided among six flasks, which were aerated and, at time=0, dosed with NEM. Samples for potassium were taken over time to determine the increase in potassium concentration due to cell efflux.

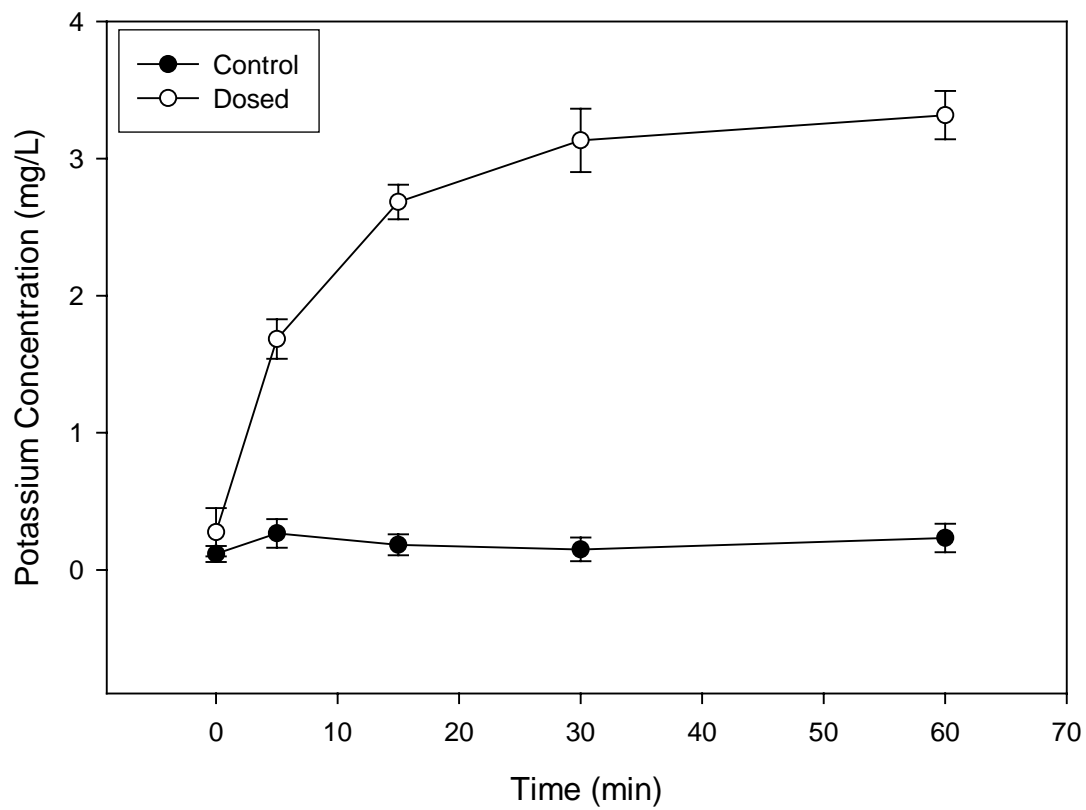


Figure 3. Batch  $K^+$  efflux experiment with planktonic *P. aeruginosa* at an absorbance (measured at 590 nm) of 0.215 after exposure to 50 mg/L N-ethylmaleimide (NEM) versus an unshocked control. Error bars represent the standard deviation of the averages for three flasks.

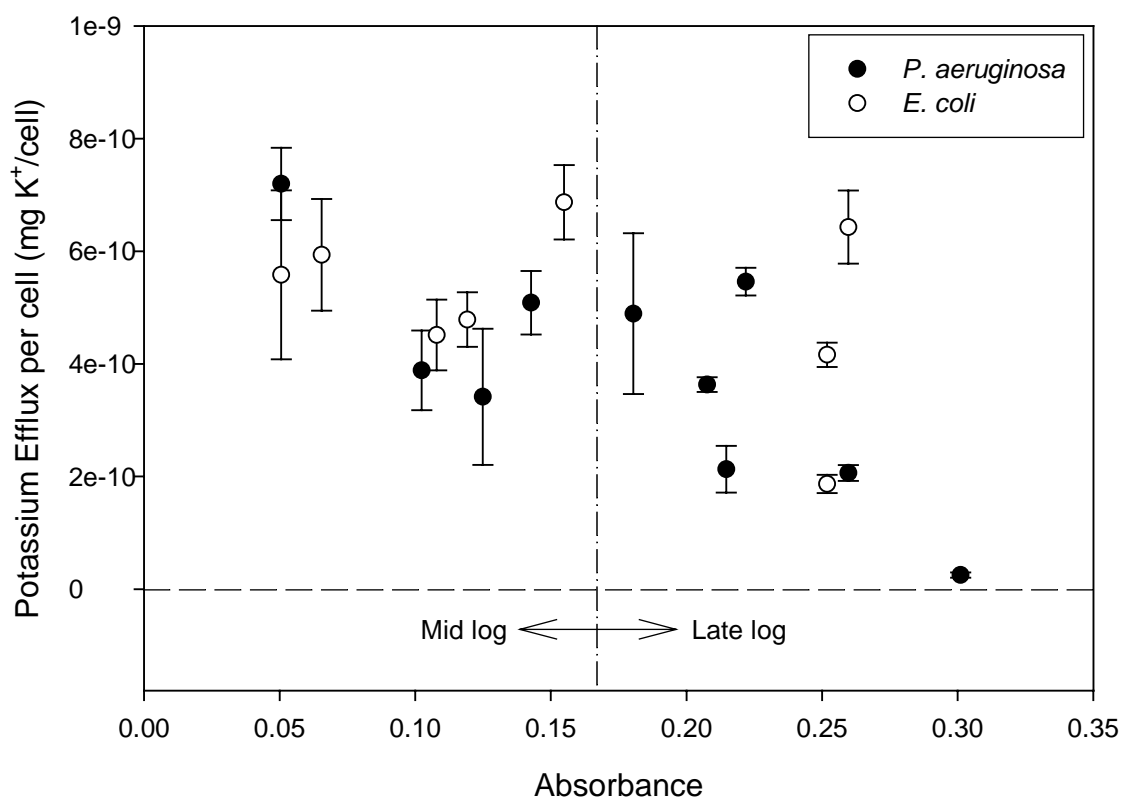


Figure 4. K<sup>+</sup> efflux potentials (mg K<sup>+</sup> effluxed per cell) versus planktonic culture density, measured as absorbance (at 590 nm), for *P. aeruginosa* and *E. coli*.



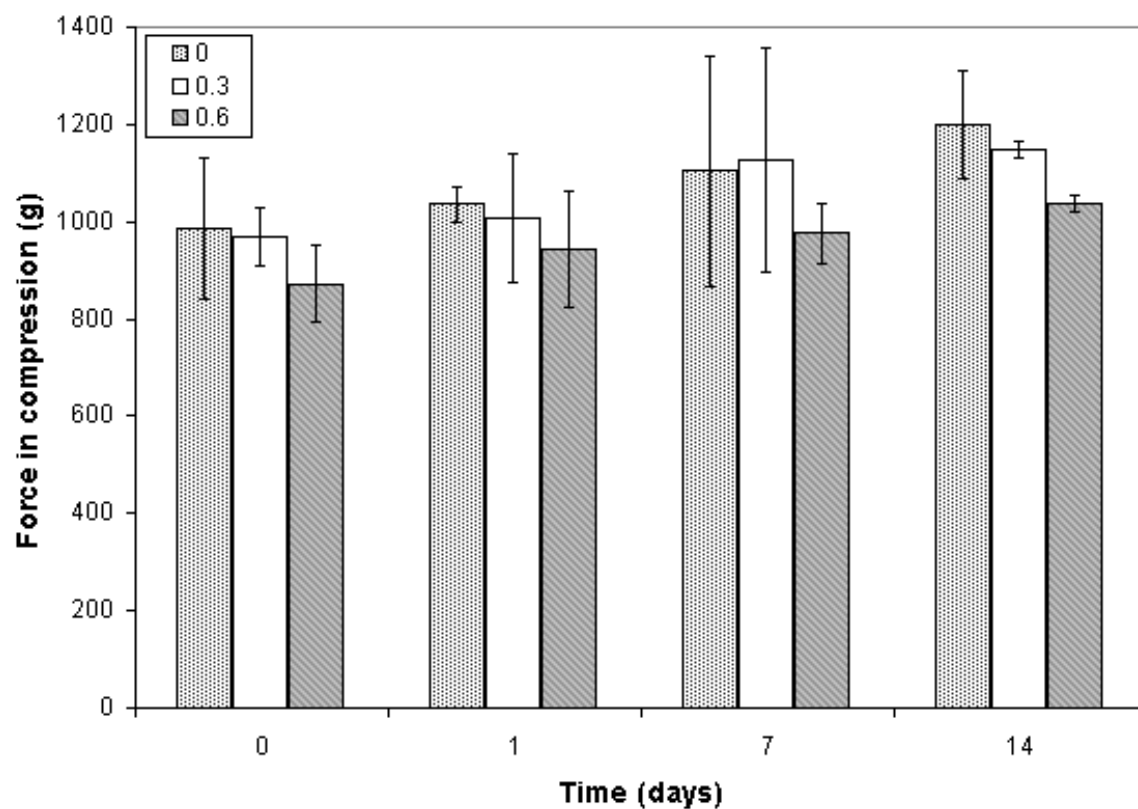


Figure 5: No significant difference is observed in the force required to rupture for alginate beads incubated over time with potassium concentrations comparable to that effluxed from immobilized cells.

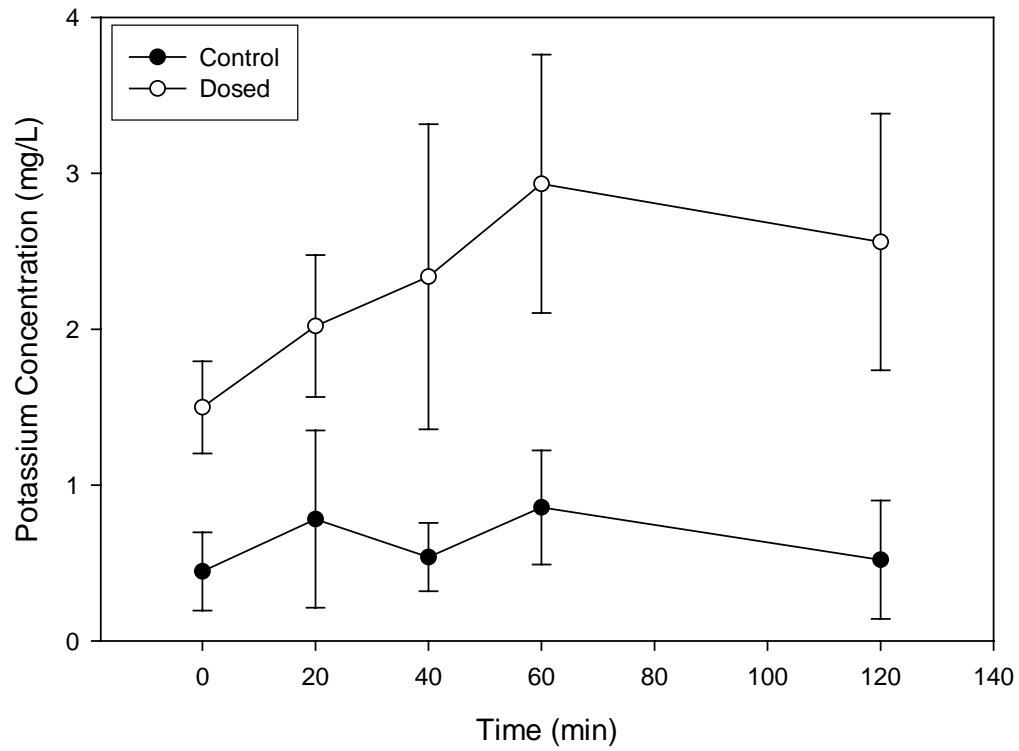


Figure 6.  $K^+$  efflux  $((1.3 \pm 0.1) \times 10^{-10} \text{ mg } K^+ \text{ per cell})$  at  $t=1$  day from *P. aeruginosa* immobilized in calcium alginate beads after exposure to 50 mg/L NEM versus an unstressed, immobilized control.

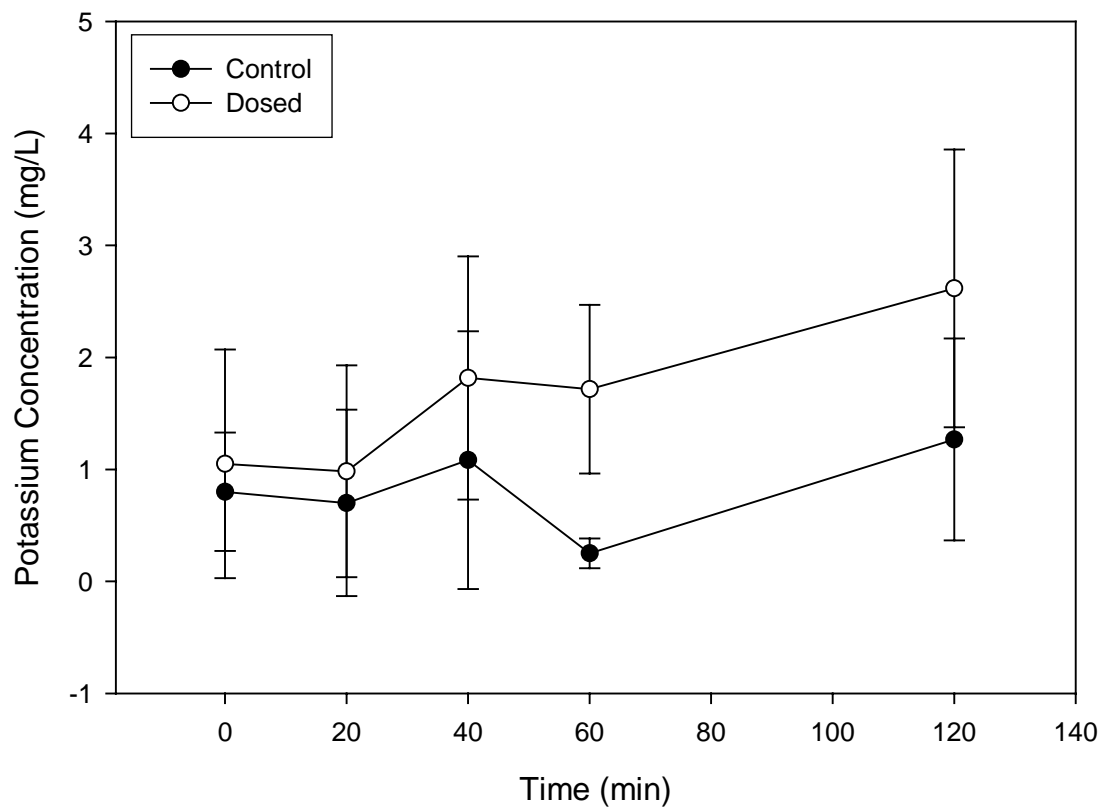


Figure 7:  $K^+$  efflux  $((1.3 \pm 0.1) \times 10^{-10} \text{ mg } K^+ \text{ per cell})$  at  $t=5$  days from *P. aeruginosa* immobilized in calcium alginate beads after exposure to 50 mg/L NEM versus an unstressed, immobilized control.

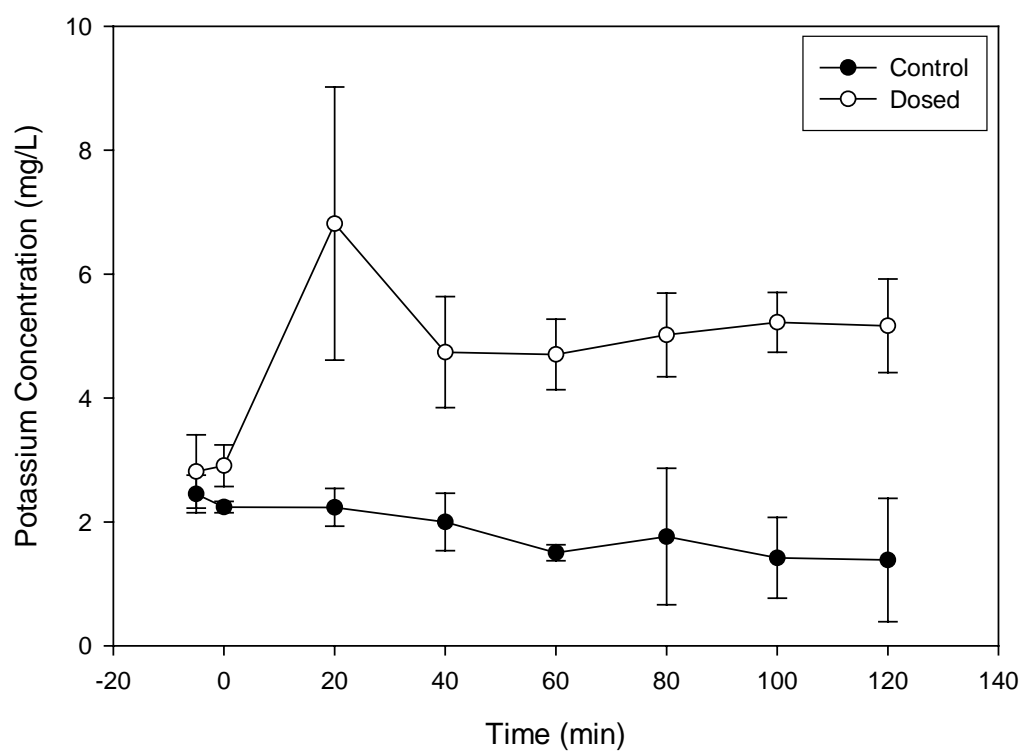


Figure 8.  $K^+$  efflux ( $(4.6 \pm 0.8) \times 10^{-10}$  mg  $K^+$ /cell ) at  $t=1$  day from *P. aeruginosa* immobilized in thermal polymer gels after exposure to 50 mg/L NEM versus an unstressed, immobilized control.

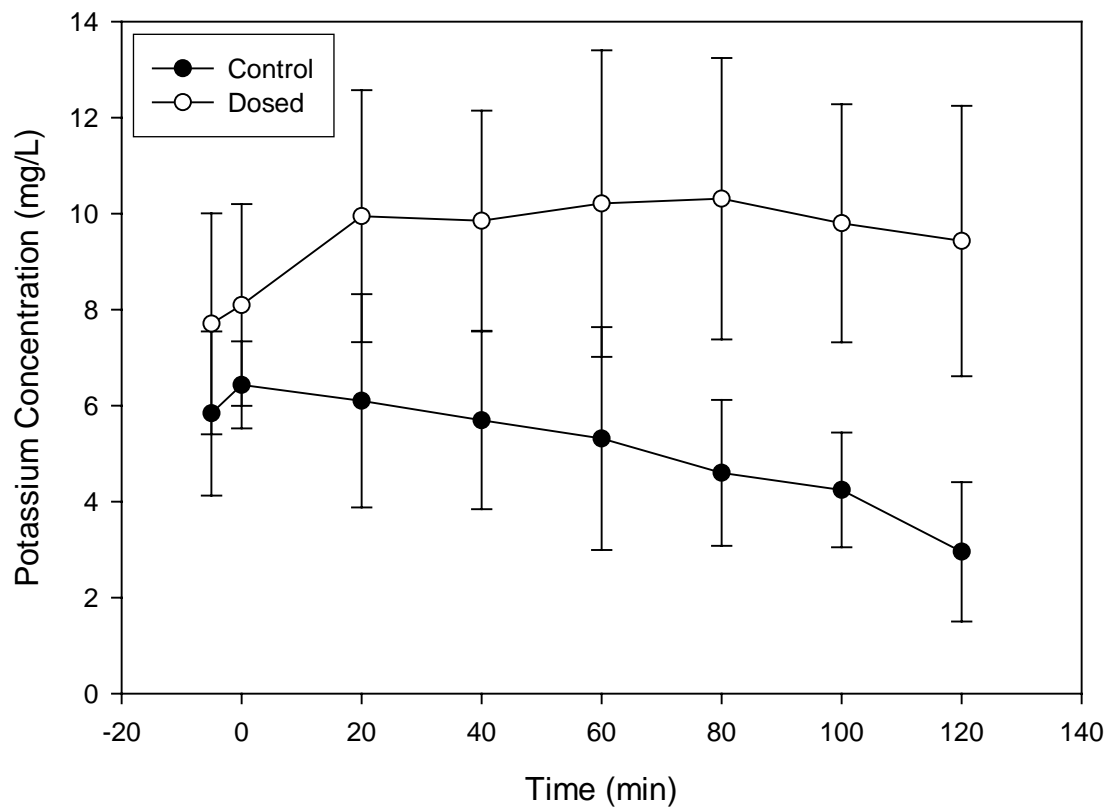


Figure 9:  $K^+$  efflux ( $(4.6 \pm 0.8) \times 10^{-10} \text{ mg } K^+/\text{cell}$ ) at  $t=5$  days from *P. aeruginosa* immobilized in thermal polymer gels after exposure to 50 mg/L NEM versus an unstressed, immobilized control.

## Chapter 4: Engineering Significance

### **Engineering Significance**

Properly functioning wastewater treatment plants are vital to human health and water quality. However, even the most efficient plant may have instances of process upset, characterized by deflocculation and poor nutrient and BOD removal, that result in the failure of the treatment train. During such an event, operators typically are unaware that upset has begun until the event is well underway and the damage to the biological treatment step has been done. Providing operators with advanced warning when an upset is about to occur would allow them to initiate protective measures to ensure the continued functioning of the treatment process. Such advance warning would be possible with the biosensor under development here.

This biosensor will be the first to harness the GGKE stress response mechanism to link the efflux of potassium from immobilized cells with the presence of an electrophile in the sample. The change in potassium concentration across the sensor caused by potassium efflux from immobilized cells will be monitored; and, at a certain threshold increase, activation of the GGKE system will be inferred. Because the system is activated by electrophiles, the sensor will not be useful for upset events caused by other classes of compounds, such as oil and grease. Since many upsets can be linked to electrophilic shock and potassium efflux and, thus, to deflocculation, the sensor will serve a vital role in improving the functionality of wastewater treatment plants under the influence of toxic chemical shocks.

Incorporating this sensor in the real-time analyses of plant influent will inform operators of potential upset due to electrophilic shock. However, it will not tell the whole

story of the potential for upset events because it is only useful for predicting electrophilic shock upset. Combining this sensor with other real-time sensors, such as sensors measuring the influent's effect on oxygen uptake rates within the bioreactor, would provide a more complete picture of the upset potential of the influent. Adding sensors for other effects on the biomass to create a sensor network that responds to plant influent in real time would significantly improve the operator's control over process operations by providing information on the types of effects the influent may cause in the biomass. Although such a sensor would provide limited information on the cause of the effect, the early warning allows operators time to reroute the suspect influent or initiate treatment steps to mitigate the toxic effects of the influent.

In addition to using an array of biosensors to monitor the plant influent, such sensors might be applied to test the effluent from industries that discharge to the sewer system. This testing could be conducted as a prerequisite for discharge to the sewer, to ensure the safety of the large quantities of wastewater generated from industrial activities. Alternately, daily samples of industrial wastewater could be collected and the testing could be performed on the stored samples after an upset event, or after the upset warning sensors at the plant were triggered, in an attempt to find the cause of the upset. Such a system would work well in an area containing a few high volume industrial contributions where the testing of stored samples would take minimal time. As the number of industries increases, the time to determine the source of the cause increases, as does the age of the sample tested, reducing the reliability of the results. Clearly, for such attempts to link the causative industry to an upset event, the results of the biosensor must be proven and reliable. Extensive tests to determine the response of the sensor against background shifts in pH and temperature must be

performed to rule out the possibility of false positive results. On the whole, an array of biosensors to monitor for process upset by electrophilic shock and by other modes of upset would improve the state of wastewater treatment by allowing operators time to respond to the threat, and by potentially enabling them to link the each upset with its cause.



## Appendix A: Data for Chapter 2

### A.1 Data for oxygen uptake rate experiments

Data averaged from Probe A and B

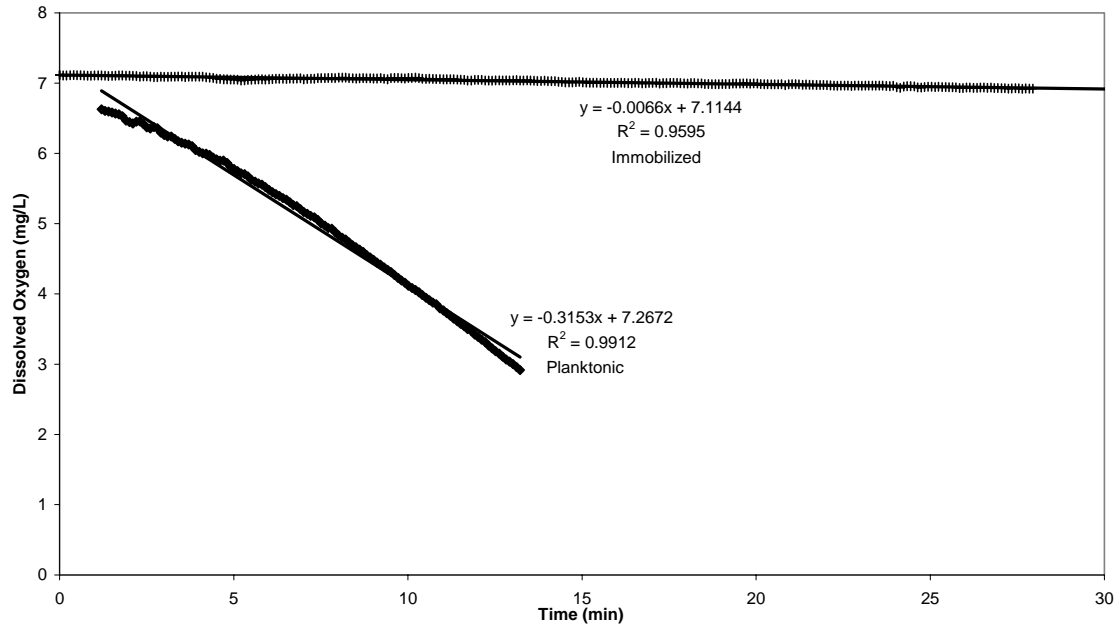
Presented in Chapter 2, Figure 2

#### A.1.1 Photopolymerizable polymer: Photo 3, 4-21-04, Book 2, Page 87

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
1.2	6.628	0	7.114	4.31	5.9795	3.01	7.0895	7.411	5.0525	6.109	7.058	10.52	3.9465	9.22	7.0725
1.3	6.604	0	7.115	4.41	5.939	3.11	7.0895	7.511	5.003	6.21	7.0625	10.62	3.9095	9.31	7.064
1.4	6.5955	0.1	7.108	4.51	5.9155	3.21	7.092	7.612	4.971	6.31	7.063	10.72	3.875	9.42	7.054
1.5	6.582	0.2	7.1095	4.61	5.894	3.31	7.0925	7.712	4.9385	6.41	7.0615	10.82	3.852	9.52	7.0715
1.6	6.568	0.3	7.1115	4.71	5.899	3.41	7.095	7.812	4.93	6.51	7.059	10.92	3.795	9.62	7.075
1.7	6.5565	0.4	7.1155	4.81	5.8635	3.51	7.0945	7.912	4.8805	6.61	7.0645	11.02	3.764	9.72	7.074
1.8	6.5285	0.5	7.113	4.91	5.805	3.61	7.0865	8.012	4.834	6.711	7.0635	11.12	3.7255	9.82	7.069
1.9	6.4665	0.6	7.1105	5.01	5.7755	3.71	7.0915	8.113	4.8	6.811	7.0645	11.22	3.688	9.92	7.0665
2	6.446	0.7	7.109	5.11	5.748	3.81	7.093	8.212	4.774	6.911	7.0675	11.32	3.6485	10	7.0735
2.1	6.4255	0.8	7.1065	5.21	5.716	3.91	7.092	8.313	4.7315	7.011	7.0535	11.42	3.6095	10.1	7.0745
2.2	6.4525	0.9	7.107	5.31	5.704	4.01	7.093	8.413	4.692	7.111	7.059	11.52	3.574	10.2	7.076
2.3	6.458	1	7.108	5.41	5.6715	4.11	7.0905	8.512	4.663	7.212	7.063	11.62	3.538	10.3	7.0705
2.4	6.4165	1.1	7.1095	5.51	5.6235	4.21	7.0825	8.613	4.6295	7.312	7.0635	11.72	3.498	10.4	7.064
2.5	6.37	1.2	7.108	5.61	5.5965	4.31	7.0785	8.713	4.596	7.412	7.07	11.82	3.4715	10.5	7.0605
2.6	6.354	1.3	7.1055	5.71	5.5705	4.41	7.074	8.814	4.564	7.512	7.07	11.92	3.421	10.6	7.0625
2.7	6.3725	1.4	7.1	5.81	5.5535	4.51	7.0615	8.913	4.518	7.612	7.07	12.02	3.3855	10.7	7.061
2.8	6.358	1.5	7.103	5.91	5.519	4.61	7.0605	9.014	4.485	7.712	7.073	12.12	3.3495	10.8	7.057
2.91	6.2965	1.6	7.1055	6.01	5.4805	4.71	7.054	9.114	4.4435	7.812	7.0745	12.22	3.314	10.9	7.056
3	6.2605	1.7	7.109	6.11	5.4485	4.81	7.053	9.214	4.416	7.913	7.0725	12.32	3.266	11	7.0555
3.1	6.2405	1.8	7.108	6.21	5.42	4.91	7.0515	9.314	4.377	8.013	7.0785	12.42	3.225	11.1	7.0555
3.21	6.241	1.9	7.1055	6.31	5.396	5.01	7.052	9.414	4.343	8.113	7.0775	12.52	3.185	11.2	7.0555
3.31	6.2055	2	7.106	6.41	5.363	5.11	7.0475	9.515	4.311	8.213	7.0785	12.62	3.148	11.3	7.0535
3.41	6.1725	2.1	7.1045	6.51	5.3405	5.21	7.037	9.615	4.269	8.313	7.071	12.72	3.105	11.4	7.0505
3.51	6.151	2.2	7.1005	6.61	5.3035	5.31	7.041	9.715	4.2265	8.414	7.069	12.82	3.0665	11.5	7.047
3.61	6.1375	2.3	7.092	6.71	5.264	5.41	7.0455	9.815	4.189	8.513	7.067	12.92	3.0355	11.6	7.0455
3.71	6.126	2.4	7.097	6.81	5.248	5.51	7.048	9.915	4.158	8.613	7.069	13.02	3.002	11.7	7.036
3.81	6.103	2.5	7.097	6.91	5.206	5.61	7.052	10.02	4.114	8.714	7.0705	13.12	2.9595	11.8	7.037
3.91	6.048	2.6	7.092	7.01	5.1645	5.71	7.054	10.12	4.0825	8.814	7.069	13.22	2.9145	11.9	7.0445
4.01	6.021	2.7	7.087	7.11	5.1385	5.81	7.0555	10.22	4.0535	8.914	7.069			12	7.0455
4.11	6.0005	2.81	7.0855	7.21	5.109	5.91	7.05	10.32	4.022	9.014	7.065			12.1	7.044
4.21	5.9955	2.91	7.093	7.31	5.0905	6.01	7.0535	10.42	3.982	9.114	7.0655			12.2	7.037

Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Average DO for Immobilized (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
12.32	7.037	15.42	7.0055	18.53	6.988	21.63	6.977	24.7	6.9365
12.42	7.0325	15.52	7.003	18.63	6.988	21.73	6.972	24.8	6.944
12.52	7.0385	15.62	7.004	18.73	6.9835	21.83	6.9725	24.9	6.9465
12.62	7.0385	15.72	7.0035	18.83	6.9845	21.93	6.973	25	6.946
12.72	7.037	15.83	7.0035	18.93	6.9835	22.03	6.971	25.1	6.9455
12.82	7.041	15.93	7.0025	19.03	6.988	22.13	6.968	25.2	6.9475
12.92	7.036	16.02	7.003	19.13	6.988	22.23	6.9635	25.3	6.944
13.02	7.0405	16.13	7.004	19.23	6.9865	22.33	6.9615	25.4	6.944
13.12	7.042	16.23	7.0015	19.33	6.994	22.43	6.966	25.5	6.9415
13.22	7.038	16.33	6.9995	19.43	6.994	22.54	6.9655	25.6	6.942
13.32	7.038	16.43	6.998	19.53	6.994	22.64	6.9655	25.7	6.9385
13.42	7.0385	16.53	7.005	19.63	6.9965	22.74	6.96	25.8	6.9295
13.52	7.0355	16.63	7.0035	19.73	6.996	22.84	6.9635	25.9	6.9305
13.62	7.033	16.73	6.996	19.83	6.9895	22.94	6.966	26	6.9365
13.72	7.031	16.83	7	19.93	6.9955	23.04	6.962	26.1	6.9365
13.82	7.032	16.93	7.0025	20.03	6.9925	23.14	6.9635	26.2	6.934
13.92	7.033	17.03	7.0025	20.13	6.987	23.24	6.9645	26.3	6.932
14.02	7.029	17.13	7.005	20.23	6.9855	23.34	6.966	26.4	6.9355
14.12	7.029	17.23	6.9935	20.33	6.9845	23.44	6.965	26.5	6.9345
14.22	7.0295	17.33	7.0005	20.43	6.982	23.54	6.966	26.6	6.9335
14.32	7.02	17.43	7.0005	20.53	6.983	23.64	6.964	26.7	6.935
14.42	7.016	17.53	7.0015	20.63	6.983	23.74	6.9575	26.8	6.9315
14.52	7.011	17.63	7.003	20.73	6.985	23.84	6.956	26.9	6.9305
14.62	7.0115	17.73	7.0035	20.83	6.9715	23.94	6.961	27	6.9265
14.72	7.011	17.83	7.0005	20.93	6.9815	24.04	6.9425	27.1	6.927
14.82	7.0125	17.93	6.9975	21.03	6.9855	24.14	6.934	27.2	6.921
14.92	7.0205	18.03	6.993	21.13	6.9845	24.24	6.9505	27.3	6.9255
15.02	7.0095	18.13	6.998	21.23	6.981	24.34	6.955	27.4	6.9265
15.12	7.0085	18.23	6.998	21.33	6.975	24.44	6.955	27.5	6.9235
15.22	7.0055	18.33	6.9975	21.43	6.979	24.54	6.952	27.6	6.918
15.32	7.006	18.43	6.995	21.53	6.9765	24.64	6.94	27.7	6.923

Oxygen Uptake Rates for Photopolymer Gel with New Initiator (Photo 3): 4-21-04

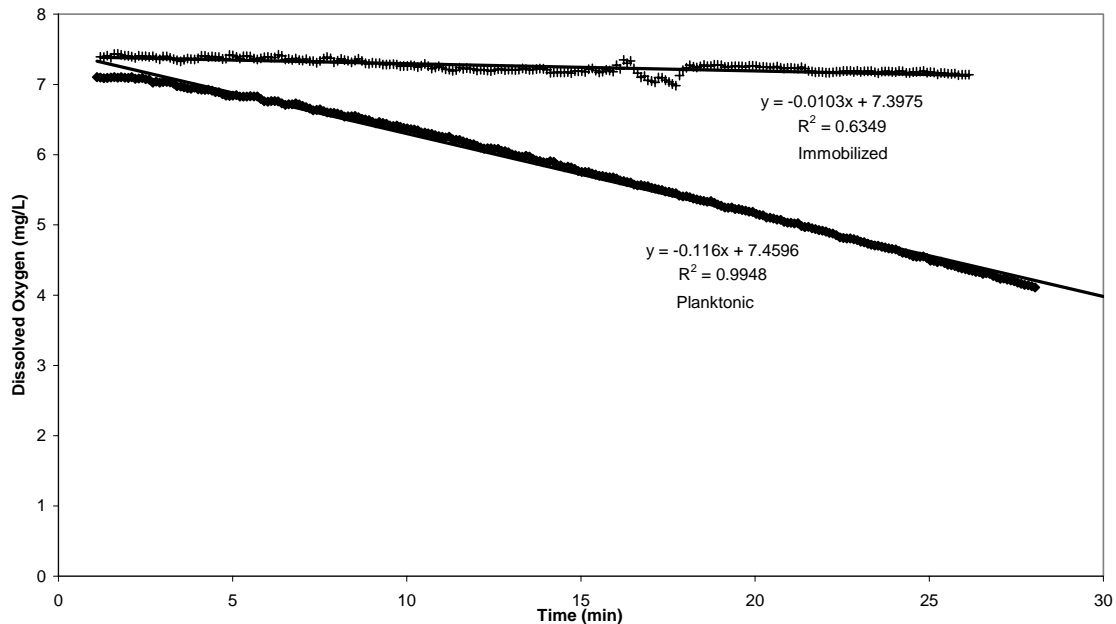


#### A.1.2 Photopolymerizable polymer: Photo 2, 3-18-04, Book 2, Page 77

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
1.102	7.1025	1.2	7.3925	4.21	6.9205	4.31	7.39	7.31	6.6295	8.312	7.336	10.42	6.3145	11.42	7.2035
1.202	7.097	1.3	7.3895	4.31	6.9255	4.41	7.398	7.41	6.637	8.413	7.3145	10.51	6.3125	11.52	7.24
1.302	7.0895	1.4	7.409	4.41	6.9085	4.51	7.3915	7.51	6.6445	8.512	7.3385	10.61	6.3005	11.62	7.2215
1.402	7.091	1.5	7.3795	4.51	6.8885	4.61	7.3885	7.61	6.62	8.613	7.363	10.72	6.2945	11.72	7.2315
1.502	7.096	1.6	7.431	4.61	6.888	4.71	7.3635	7.71	6.6005	8.713	7.333	10.82	6.2785	11.82	7.224
1.602	7.1025	1.7	7.4345	4.71	6.8605	5.71	7.354	7.81	6.5965	8.813	7.2985	10.92	6.265	11.92	7.218
1.703	7.0955	1.8	7.4195	4.81	6.841	5.81	7.3725	7.91	6.592	8.913	7.2935	11.02	6.2565	12.02	7.1975
1.803	7.1035	1.9	7.4075	4.91	6.835	5.91	7.3845	8.01	6.583	9.013	7.3085	11.12	6.2435	12.12	7.2095
1.903	7.0935	2	7.405	5.01	6.84	6.01	7.3915	8.11	6.5695	9.114	7.2985	11.22	6.254	12.22	7.2045
2.003	7.0925	2.1	7.394	5.11	6.846	6.11	7.38	8.21	6.5405	9.214	7.301	11.32	6.2175	12.32	7.1995
2.103	7.102	2.2	7.3765	5.21	6.825	6.21	7.384	8.31	6.5465	9.314	7.2825	11.42	6.211	12.42	7.189
2.203	7.0795	2.3	7.4045	5.31	6.8275	6.31	7.4195	8.41	6.5455	9.414	7.283	11.52	6.21	12.52	7.2045
2.303	7.083	2.4	7.3965	5.41	6.827	6.41	7.4065	8.51	6.548	9.514	7.284	11.62	6.1875	12.62	7.215
2.404	7.0915	2.5	7.4	5.51	6.8315	6.51	7.355	8.61	6.531	9.615	7.288	11.72	6.1715	12.72	7.2195
2.504	7.073	2.6	7.3915	5.61	6.8305	6.61	7.3635	8.71	6.51	9.714	7.283	11.82	6.1555	12.82	7.2025
2.603	7.0675	2.7	7.399	5.71	6.83	6.71	7.3485	8.81	6.499	9.814	7.26	11.92	6.148	12.92	7.2085
2.704	7.025	2.8	7.374	5.81	6.792	6.81	7.3695	8.91	6.4915	9.915	7.2605	12.02	6.1245	13.02	7.211
2.804	7.0385	2.91	7.356	5.91	6.759	6.91	7.346	9.01	6.4655	10.02	7.262	12.12	6.102	13.12	7.205
2.905	7.026	3	7.3985	6.01	6.7555	7.01	7.339	9.11	6.445	10.12	7.273	12.22	6.0865	13.22	7.2095
3.004	7.034	3.11	7.397	6.11	6.7625	7.11	7.3595	9.21	6.462	10.22	7.264	12.32	6.0905	13.32	7.226
3.104	7.0355	3.21	7.376	6.21	6.7635	7.21	7.3305	9.31	6.452	10.32	7.243	12.42	6.09	13.42	7.2175
3.205	7.0285	3.31	7.3585	6.31	6.756	7.31	7.332	9.41	6.441	10.42	7.2635	12.52	6.083	13.52	7.207
3.305	7.0095	3.41	7.343	6.41	6.7325	7.41	7.3065	9.51	6.413	10.52	7.291	12.62	6.0825	13.62	7.209
3.405	6.974	3.51	7.3275	6.51	6.7075	7.51	7.333	9.61	6.407	10.62	7.2595	12.72	6.052	13.72	7.218
3.505	6.9695	3.61	7.35	6.61	6.718	7.61	7.367	9.71	6.4135	10.72	7.224	12.82	6.0495	13.82	7.2245
3.605	6.9575	3.71	7.3685	6.71	6.718	7.71	7.389	9.81	6.396	10.82	7.241	12.92	6.0335	13.92	7.2205
3.706	6.9435	3.81	7.3595	6.81	6.732	7.81	7.371	9.91	6.38	10.92	7.259	13.02	6.0055	14.02	7.2075
3.805	6.9375	3.91	7.355	6.91	6.7145	7.91	7.313	10	6.3735	11.02	7.2375	13.12	5.994	14.12	7.167
3.905	6.954	4.01	7.3705	7.01	6.693	8.01	7.3365	10.1	6.361	11.12	7.2155	13.22	5.9795	14.22	7.169
4.006	6.93	4.11	7.406	7.11	6.6775	8.11	7.362	10.2	6.356	11.22	7.209	13.32	5.971	14.32	7.172
4.106	6.9255	4.21	7.407	7.21	6.6565	8.21	7.344	10.3	6.3435	11.32	7.1935	13.42	5.985	14.42	7.168

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
13.52	5.973	14.52	7.168	16.6	5.5645	19.93	7.2635	19.73	5.2015	23	7.1795
13.62	5.942	14.62	7.174	16.7	5.565	20.03	7.262	19.83	5.1875	23.1	7.187
13.72	5.9185	14.72	7.162	16.8	5.553	20.13	7.245	19.93	5.184	23.2	7.187
13.82	5.909	14.82	7.191	16.9	5.5525	20.23	7.249	20.03	5.157	23.3	7.1895
13.92	5.8925	14.92	7.186	17	5.5295	20.33	7.2445	20.13	5.1425	23.4	7.1735
14.02	5.8865	15.02	7.191	17.1	5.516	20.43	7.2395	20.23	5.135	23.5	7.159
14.12	5.9075	15.12	7.179	17.2	5.506	20.53	7.242	20.33	5.1045	23.6	7.181
14.22	5.898	15.22	7.215	17.3	5.4955	20.63	7.2525	20.43	5.103	23.7	7.1845
14.32	5.8475	15.32	7.228	17.4	5.4765	20.73	7.236	20.53	5.0895	23.8	7.1835
14.42	5.845	15.42	7.1965	17.5	5.4695	20.83	7.224	20.63	5.075	23.9	7.1775
14.52	5.821	15.52	7.168	17.6	5.4565	20.93	7.232	20.73	5.073	24	7.176
14.62	5.829	15.62	7.1815	17.7	5.452	21.03	7.236	20.83	5.0445	24.1	7.1895
14.72	5.817	18.03	7.236	17.8	5.4165	21.13	7.23	20.93	5.0325	24.2	7.1865
14.82	5.7975	18.13	7.274	17.9	5.4055	21.23	7.225	21.03	5.031	24.3	7.164
14.92	5.7685	18.23	7.249	18	5.406	21.33	7.243	21.13	5.0205	24.4	7.1625
15.02	5.7545	18.33	7.241	18.1	5.393	21.43	7.2255	21.23	5.0225	24.5	7.174
15.12	5.752	18.43	7.257	18.2	5.3745	21.53	7.1925	21.33	4.982	24.6	7.179
15.22	5.7505	18.53	7.275	18.3	5.3615	21.63	7.183	21.43	4.9685	24.7	7.181
15.32	5.731	18.63	7.2595	18.4	5.35	21.73	7.1735	21.53	4.971	24.8	7.191
15.42	5.715	18.73	7.2605	18.5	5.341	21.83	7.1785	21.63	4.9525	24.9	7.167
15.52	5.698	18.83	7.278	18.6	5.33	21.93	7.174	21.73	4.939	25	7.174
15.62	5.6965	18.93	7.2765	18.7	5.337	22.03	7.167	21.83	4.9265	25.1	7.17
15.72	5.683	19.03	7.273	18.8	5.316	22.13	7.1655	21.93	4.9165	25.2	7.1425
15.82	5.6785	19.13	7.248	18.9	5.2905	22.23	7.1725	22.03	4.906	25.3	7.165
15.92	5.676	19.23	7.251	19	5.273	22.33	7.181	22.13	4.8865	25.4	7.16
16.02	5.6615	19.33	7.2555	19.1	5.2475	22.43	7.1775	22.23	4.878	25.5	7.151
16.12	5.6335	19.43	7.258	19.2	5.244	22.53	7.1895	22.33	4.855	25.6	7.15
16.22	5.624	19.53	7.257	19.3	5.249	22.63	7.1895	22.43	4.8215	25.7	7.1545
16.32	5.61	19.63	7.255	19.4	5.226	22.73	7.1935	22.53	4.812	25.8	7.1325
16.42	5.604	19.73	7.248	19.5	5.2245	22.83	7.177	22.63	4.8085	25.9	7.1375
16.52	5.574	19.83	7.2645	19.6	5.21	22.93	7.1925	22.73	4.807	26	7.1375

Oxygen Uptake Rates for Photopolymer Gel, Photo 2, 3-18-04



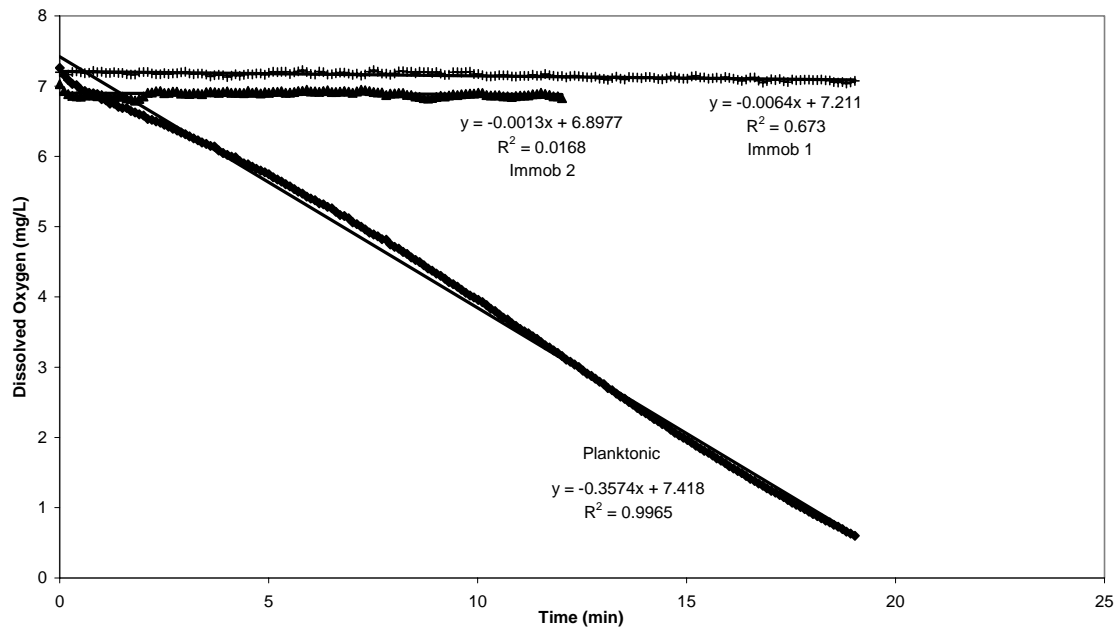
### A.1.3 Photopolymerizable polymer: Photo 1, 2-26-04, Book 2, Page 72

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
2.1	6.531	2.104	6.9035	5.208	5.67	5.208	6.918	8.312	4.612	8.312	6.875
2.2	6.52	2.203	6.911	5.307	5.64	5.307	6.9265	8.412	4.561	8.412	6.873
2.3	6.498	2.304	6.927	5.408	5.603	5.407	6.9045	8.512	4.524	8.512	6.8525
2.4	6.48	2.404	6.9295	5.508	5.572	5.508	6.9075	8.612	4.497	8.612	6.845
2.5	6.449	2.504	6.902	5.609	5.533	5.608	6.916	8.713	4.45	8.713	6.829
2.6	6.422	2.604	6.9045	5.708	5.496	5.708	6.929	8.813	4.404	8.813	6.822
2.7	6.395	2.704	6.922	5.808	5.472	5.808	6.934	8.913	4.372	8.913	6.8315
2.81	6.367	2.804	6.9225	5.909	5.428	5.908	6.946	9.013	4.331	9.013	6.8465
2.91	6.338	2.905	6.8935	6.009	5.398	6.009	6.923	9.113	4.299	9.113	6.861
3	6.316	3.004	6.898	6.109	5.376	6.109	6.924	9.214	4.259	9.213	6.851
3.11	6.285	3.105	6.89	6.209	5.332	6.209	6.9175	9.314	4.21	9.314	6.8655
3.21	6.255	3.205	6.9	6.309	5.317	6.309	6.9305	9.413	4.183	9.413	6.88
3.31	6.23	3.305	6.898	6.41	5.28	6.409	6.9425	9.514	4.144	9.514	6.873
3.41	6.198	3.405	6.886	6.51	5.259	6.51	6.9155	9.614	4.102	9.614	6.8835
3.51	6.177	3.505	6.913	6.609	5.212	6.609	6.9155	9.715	4.058	9.714	6.89
3.61	6.149	3.606	6.9195	6.71	5.165	6.71	6.921	9.814	4.02	9.814	6.894
3.71	6.14	3.706	6.912	6.81	5.15	6.81	6.9295	9.914	3.99	9.914	6.8915
3.81	6.081	3.805	6.9055	6.911	5.119	6.91	6.921	10.02	3.956	10.02	6.9055
3.91	6.049	3.906	6.917	7.01	5.06	7.01	6.904	10.12	3.926	10.12	6.901
4.01	6.023	4.006	6.923	7.11	5.035	7.11	6.9245	10.22	3.882	10.21	6.873
4.11	5.995	4.106	6.9035	7.211	4.999	7.211	6.9465	10.32	3.831	10.32	6.868
4.21	5.988	4.206	6.907	7.311	4.96	7.311	6.9415	10.42	3.799	10.42	6.869
4.31	5.932	4.306	6.9045	7.41	4.915	7.41	6.9295	10.52	3.748	10.52	6.8685
4.41	5.9	4.407	6.902	7.511	4.888	7.511	6.9145	10.62	3.704	10.62	6.855
4.51	5.885	4.506	6.933	7.611	4.861	7.611	6.91	10.72	3.676	10.72	6.8565
4.61	5.851	4.606	6.9055	7.712	4.823	7.712	6.909	10.82	3.622	10.82	6.846
4.71	5.824	4.707	6.9155	7.811	4.812	7.811	6.873	10.92	3.589	10.92	6.858
4.81	5.797	4.807	6.8965	7.911	4.747	7.911	6.8935	11.02	3.545	11.02	6.8635
4.91	5.775	4.907	6.9115	8.012	4.713	8.012	6.895	11.12	3.51	11.12	6.868
5.01	5.746	5.007	6.9055	8.111	4.686	8.111	6.9	11.22	3.48	11.22	6.869
5.11	5.702	5.107	6.9185	8.212	4.641	8.212	6.9025	11.32	3.439	11.32	6.884

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
11.42	3.402	11.42	6.8875
11.52	3.356	11.52	6.9045
11.62	3.312	11.62	6.89
11.72	3.28	11.72	6.8745
11.82	3.24	11.82	6.8555
11.92	3.201	11.92	6.8545
12.02	3.158	12.02	6.829

Oxygen Uptake Rates for Photopolymer Gel, Photo 1, 2-26-04



#### A.1.4 Alginate oxygen uptake rates

Alginate polymer: day zero, 4-18-04, Book 2, Page 84

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
1.203	7.8395	1.202	7.417	4.307	7.4315	4.307	7.252	7.412	7.284	7.411	7.02
1.303	7.8295	1.303	7.4145	4.408	7.398	4.407	7.2225	7.512	7.297	7.512	7.0165
1.403	7.7675	1.402	7.416	4.508	7.418	4.508	7.2235	7.613	7.2915	7.612	7.017
1.503	7.756	1.502	7.388	4.607	7.445	4.607	7.226	7.713	7.2785	7.712	6.9965
1.603	7.714	1.603	7.417	4.708	7.487	4.707	7.2285	7.812	7.2815	7.812	6.993
1.704	7.693	1.703	7.407	4.808	7.4765	4.808	7.222	7.913	7.2695	7.912	6.9765
1.803	7.684	1.803	7.397	4.909	7.477	4.907	7.226	8.013	7.262	8.013	6.9745
1.903	7.7265	1.903	7.4195	5.008	7.4725	5.008	7.208	8.113	7.246	8.113	6.982
2.004	7.688	2.003	7.373	5.109	7.461	5.108	7.1965	8.213	7.2385	8.213	6.977
2.104	7.623	2.104	7.3795	5.209	7.4595	5.208	7.1935	8.314	7.239	8.313	6.957
2.204	7.7085	2.203	7.3805	5.308	7.4565	5.308	7.1835	8.414	7.2165	8.413	6.942
2.304	7.7565	2.304	7.382	5.409	7.4555	5.408	7.188	8.514	7.193	8.513	6.944
2.405	7.6905	2.404	7.3855	5.509	7.4355	5.509	7.169	8.614	7.1855	8.613	6.9415
2.505	7.679	2.504	7.3695	5.61	7.457	5.609	7.156	8.714	7.173	8.714	6.9195
2.604	7.687	2.604	7.3475	5.709	7.404	5.708	7.154	8.815	7.1955	8.814	6.863
2.705	7.66	2.704	7.342	5.809	7.437	5.809	7.1515	8.915	7.157	8.913	6.7805
2.805	7.6205	2.805	7.334	5.91	7.418	5.909	7.144	9.014	7.1455	9.014	6.7545
2.905	7.601	2.905	7.3425	6.01	7.378	6.01	7.149	9.115	7.141	9.114	6.796
3.005	7.574	3.004	7.3335	6.11	7.3805	6.109	7.1295	9.215	7.091	9.215	6.784
3.105	7.5825	3.105	7.3255	6.21	7.4035	6.209	7.1125	9.315	7.1235	9.314	6.7915
3.206	7.5815	3.205	7.337	6.31	7.3765	6.31	7.1065	9.415	7.127	9.414	6.773
3.306	7.59	3.306	7.3205	6.411	7.3655	6.41	7.104	9.515	7.095	9.515	6.7595
3.406	7.554	3.405	7.313	6.51	7.357	6.51	7.1025	9.616	7.0815	9.615	6.762
3.506	7.562	3.505	7.285	6.611	7.3345	6.61	7.0885	9.715	7.0825	9.715	6.7485
3.606	7.5555	3.606	7.2595	6.711	7.3415	6.71	7.0785	9.816	7.0805	9.815	6.745
3.707	7.5545	3.705	7.2825	6.811	7.378	6.811	7.0635	9.916	7.084	9.915	6.7535
3.806	7.5545	3.806	7.3015	6.911	7.3565	6.911	7.055	10.02	7.0795	10.02	6.729
3.907	7.5265	3.906	7.2715	7.011	7.3195	7.011	7.061	10.12	7.0665	10.12	6.7265
4.007	7.48	4.007	7.2475	7.112	7.3125	7.111	7.0485	10.22	7.063	10.22	6.744
4.107	7.4575	4.107	7.2595	7.212	7.2875	7.212	7.0335	10.32	7.0345	10.32	6.7305
4.207	7.439	4.206	7.2605	7.312	7.297	7.312	7.022	10.42	7.0215	10.42	6.712

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
10.5	6.995	10.52	6.6945	13.62	6.6995	13.62	6.5985	16.7	6.4025	16.73	6.326
10.6	6.995	10.62	6.689	13.72	6.6815	13.72	6.593	16.8	6.3665	16.83	6.3075
10.7	7.001	10.72	6.69	13.82	6.6775	13.82	6.5775	16.9	6.363	16.93	6.294
10.8	6.976	10.82	6.6675	13.92	6.6945	13.92	6.5655	17	6.362	17.03	6.288
10.9	6.9835	10.92	6.664	14.02	6.67	14.02	6.557	17.1	6.352	17.13	6.2725
11	6.9595	11.02	6.6835	14.12	6.647	14.12	6.554	17.2	6.367	17.23	6.2665
11.1	6.944	11.12	6.719	14.22	6.6605	14.22	6.543	17.3	6.3435	17.33	6.259
11.2	6.948	11.22	6.6835	14.32	6.6595	14.32	6.5355	17.4	6.3445	17.43	6.2475
11.3	6.924	11.32	6.6435	14.42	6.64	14.42	6.514	17.5	6.323	17.53	6.2495
11.4	6.945	11.42	6.653	14.52	6.603	14.52	6.5025	17.6	6.3225	17.63	6.23
11.5	6.909	11.52	6.664	14.62	6.6185	14.62	6.5005	17.7	6.309	17.73	6.2295
11.6	6.891	11.62	6.6445	14.72	6.6125	14.72	6.491	17.8	6.274	17.83	6.22
11.7	6.906	11.72	6.643	14.82	6.5955	14.82	6.4775	17.9	6.2745	17.93	6.2215
11.8	6.918	11.82	6.648	14.92	6.6115	14.92	6.463	18	6.26	18.03	6.206
11.9	6.895	11.92	6.658	15.02	6.6025	15.02	6.465	18.1	6.264	18.13	6.198
12	6.874	12.02	6.646	15.12	6.586	15.12	6.455	18.2	6.2365	18.23	6.188
12.1	6.8755	12.12	6.63	15.22	6.565	15.22	6.445	18.3	6.2355	18.33	6.1765
12.2	6.8525	12.22	6.6505	15.32	6.5395	15.32	6.426	18.4	6.217	18.43	6.1765
12.3	6.8235	12.32	6.655	15.42	6.527	15.42	6.4155	18.5	6.196	18.53	6.172
12.4	6.799	12.42	6.6415	15.53	6.511	15.52	6.415	18.6	6.1825	18.63	6.1535
12.5	6.807	12.52	6.602	15.63	6.502	15.62	6.4065	18.7	6.165	18.73	6.151
12.6	6.808	12.62	6.592	15.73	6.4855	15.72	6.3775	18.8	6.174	18.83	6.141
12.7	6.804	12.72	6.6	15.83	6.4955	15.82	6.3905	18.9	6.166	18.93	6.141
12.8	6.78	12.82	6.5995	15.93	6.4955	15.93	6.3775	19	6.1585	19.03	6.1365
12.9	6.762	12.92	6.614	16.03	6.494	16.02	6.379	19.1	6.13	19.13	6.1155
13	6.784	13.02	6.6395	16.13	6.4805	16.13	6.364	19.2	6.112	19.23	6.1075
13.1	6.7685	13.12	6.6665	16.23	6.452	16.23	6.3435	19.3	6.085	19.33	6.1085
13.2	6.7485	13.22	6.669	16.33	6.4315	16.33	6.3485	19.4	6.1145	19.43	6.0955
13.3	6.7475	13.32	6.668	16.43	6.434	16.43	6.3465	19.5	6.1015	19.53	6.082
13.4	6.7325	13.42	6.641	16.53	6.4205	16.53	6.3205	19.6	6.114	19.63	6.062
13.5	6.7205	13.52	6.629	16.63	6.4085	16.63	6.324	19.7	6.0785	19.73	6.056

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)	Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Immobilized (mg/L)
19.8	6.057	19.83	6.057	23	5.812	26.14	5.554
19.9	6.0715	19.93	6.064	23.1	5.805	26.24	5.5345
20	6.065	20.03	6.051	23.2	5.785	26.34	5.5355
20.1	6.067	20.13	6.042	23.3	5.79	26.44	5.5265
20.2	6.035	20.23	6.037	23.4	5.779	26.54	5.5195
20.3	6.0015	20.33	6.0105	23.5	5.7785	26.64	5.5065
20.4	5.988	20.43	6.015	23.6	5.7715	26.74	5.4975
20.5	5.98	20.53	6.0125	23.7	5.757	26.84	5.483
20.6	5.9715	20.63	5.993	23.8	5.741	26.94	5.4695
20.7	5.9735	20.73	5.979	23.9	5.7385	27.04	5.4355
20.8	5.9675	20.83	5.976	24	5.718	27.14	5.3965
20.9	5.9625	20.93	5.9795	24.1	5.7065	27.24	5.3825
21	5.9575	21.03	5.953	24.2	5.713	27.34	5.3655
21.1	5.9265	21.13	5.921	24.3	5.675	27.44	5.349
21.2	5.91	21.23	5.944	24.4	5.613	27.54	5.3235
21.3	5.9135	21.33	5.941	24.5	5.6215	27.64	5.297
21.4	5.891	21.43	5.895	24.6	5.668	27.74	5.338
21.5	5.89	21.53	5.91	24.7	5.675	27.84	5.349
21.6	5.8795	21.63	5.905	24.8	5.671	27.94	5.3195
21.7	5.851	21.73	5.916	24.9	5.6655	28.04	5.2995
21.8	5.8665	21.83	5.906	25	5.6525		
21.9	5.856	21.93	5.8975	25.1	5.6395		
22	5.8495	22.03	5.881	25.2	5.612		
22.1	5.8265	22.13	5.884	25.3	5.6045		
22.2	5.818	22.23	5.872	25.4	5.605		
22.3	5.7965	22.33	5.846	25.5	5.5965		
22.4	5.802	22.43	5.831	25.6	5.587		
22.5	5.791	22.54	5.8435	25.7	5.5255		
22.6	5.781	22.64	5.8395	25.8	5.4855		
22.7	5.759	22.74	5.8365	25.9	5.5295		
22.8	5.744	22.84	5.829	26	5.55		

# Alginate polymer: days 1, 3, and 5

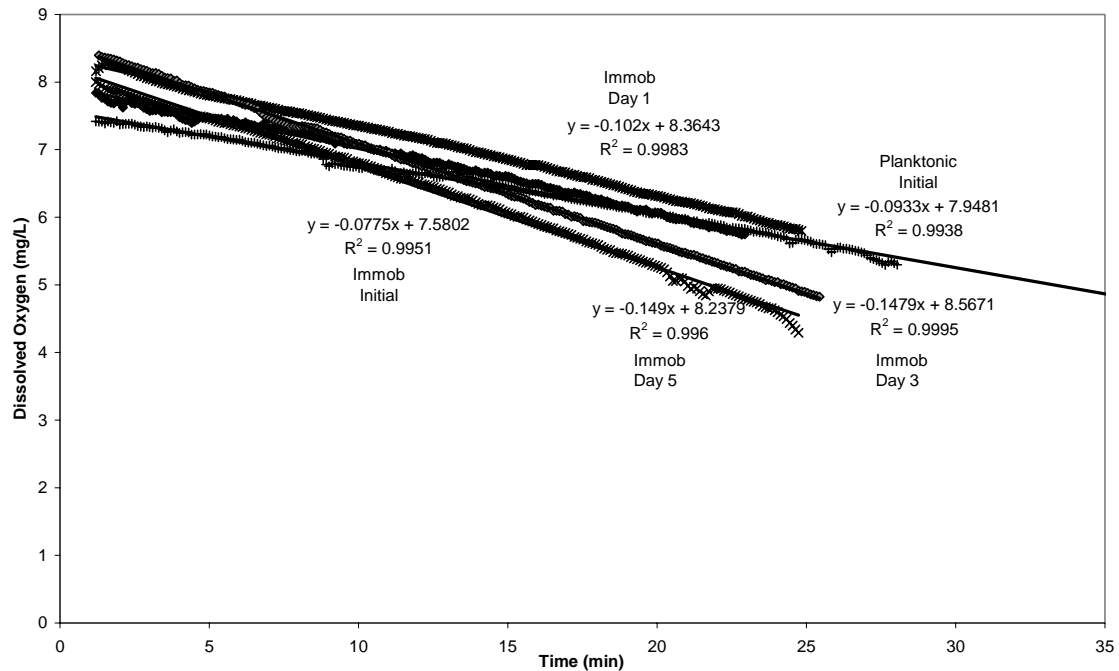
Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 5 (mg/L)
1.2	8.1605	1.303	8.395	1.202	7.9935
1.3	8.2055	1.403	8.37	1.302	7.973
1.4	8.2475	1.502	8.362	1.401	7.952
1.5	8.2805	1.603	8.353	1.502	7.91
1.6	8.287	1.703	8.343	1.602	7.8935
1.7	8.267	1.803	8.3305	1.703	7.885
1.8	8.251	1.903	8.3205	1.803	7.869
1.9	8.236	2.003	8.305	1.903	7.8665
2	8.2365	2.104	8.2905	2.003	7.8615
2.1	8.223	2.204	8.2635	2.103	7.8405
2.2	8.204	2.303	8.25	2.203	7.827
2.3	8.175	2.404	8.2325	2.303	7.811
2.4	8.1565	2.504	8.2185	2.404	7.8
2.51	8.1405	2.604	8.213	2.504	7.7785
2.61	8.118	2.704	8.191	2.603	7.7685
2.71	8.089	2.805	8.1785	2.704	7.746
2.81	8.0815	2.905	8.164	2.804	7.733
2.91	8.058	3.004	8.1435	2.905	7.722
3.01	8.0485	3.105	8.1305	3.004	7.712
3.11	8.0365	3.205	8.1325	3.104	7.6975
3.21	8.014	3.306	8.1175	3.205	7.6795
3.31	8.0085	3.405	8.0905	3.305	7.6655
3.41	7.9875	3.505	8.0635	3.405	7.653
3.51	7.9765	3.606	8.0575	3.505	7.646
3.61	7.9675	3.706	8.0535	3.606	7.629
3.71	7.957	3.806	8.0495	3.706	7.6135
3.81	7.9465	3.906	8.0215	3.805	7.5975
3.91	7.9325	4.006	7.988	3.906	7.587
4.01	7.924	4.107	7.9565	4.006	7.5705
4.11	7.9025	4.206	7.9525	4.107	7.563
4.21	7.888	4.307	7.949	4.206	7.553

Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 5 (mg/L)
4.307	7.8775	4.407	7.925	4.306	7.532
4.408	7.872	4.508	7.907	4.407	7.5005
4.508	7.8585	4.607	7.8845	4.507	7.492
4.607	7.847	4.707	7.869	4.607	7.492
4.708	7.8295	4.808	7.868	4.707	7.493
4.808	7.8175	4.908	7.8545	4.807	7.4845
4.909	7.81	5.008	7.847	4.907	7.4675
5.008	7.7985	5.108	7.8405	5.007	7.459
5.108	7.797	5.208	7.819	5.108	7.447
5.209	7.785	5.308	7.806	5.208	7.4335
5.309	7.778	5.408	7.7925	5.308	7.4125
5.409	7.767	5.509	7.786	5.408	7.4065
5.509	7.76	5.609	7.7435	5.508	7.3925
5.609	7.7545	5.709	7.7465	5.609	7.39
5.709	7.746	5.809	7.7385	5.708	7.377
5.809	7.7365	5.909	7.716	5.808	7.3575
5.91	7.7315	6.01	7.7025	5.909	7.356
6.01	7.7235	6.109	7.678	6.009	7.343
6.11	7.704	6.209	7.6645	6.109	7.333
6.21	7.6965	6.31	7.662	6.209	7.319
6.31	7.6905	6.41	7.638	6.309	7.3095
6.411	7.6815	6.51	7.615	6.41	7.296
6.51	7.663	6.61	7.5995	6.51	7.281
6.611	7.653	6.711	7.5855	6.609	7.2645
6.711	7.65	6.811	7.5125	6.71	7.2505
6.811	7.6425	6.911	7.4775	6.81	7.241
6.911	7.63	7.011	7.462	6.911	7.225
7.011	7.622	7.111	7.448	7.01	7.2185
7.112	7.613	7.211	7.4205	7.111	7.2095
7.212	7.6025	7.312	7.4085	7.211	7.198
7.312	7.592	7.411	7.3905	7.311	7.173

Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 5 (mg/L)
7.412	7.577	7.512	7.3755	7.41	7.163
7.512	7.5675	7.612	7.3595	7.51	7.1515
7.613	7.568	7.712	7.339	7.61	7.14
7.713	7.5635	7.812	7.344	7.71	7.1275
7.812	7.5535	7.912	7.3365	7.81	7.103
7.913	7.5405	8.013	7.337	7.91	7.0935
8.013	7.54	8.113	7.3495	8.01	7.086
8.113	7.5325	8.212	7.3435	8.11	7.079
8.213	7.52	8.313	7.3315	8.21	7.049
8.313	7.5115	8.413	7.3265	8.31	7.037
8.414	7.498	8.514	7.3195	8.41	7.0185
8.514	7.492	8.613	7.3155	8.51	7.0125
8.614	7.48	8.713	7.2915	8.61	6.994
8.714	7.4715	8.814	7.2615	8.71	6.9825
8.814	7.4605	8.913	7.252	8.81	6.96
8.915	7.447	9.014	7.232	8.91	6.95
9.014	7.4365	9.114	7.205	9.01	6.938
9.115	7.4245	9.214	7.193	9.11	6.917
9.215	7.4195	9.314	7.1825	9.21	6.902
9.315	7.412	9.414	7.1805	9.31	6.8925
9.415	7.4025	9.515	7.159	9.41	6.8865
9.515	7.3955	9.615	7.136	9.51	6.8815
9.616	7.3845	9.715	7.1335	9.61	6.863
9.715	7.376	9.815	7.1055	9.71	6.831
9.816	7.3645	9.915	7.085	9.81	6.8245
9.916	7.3585	10.02	7.0855	9.91	6.81
10.02	7.354	10.12	7.0605	10	6.799
10.12	7.344	10.22	7.0555	10.1	6.7925
10.22	7.3345	10.32	7.0245	10.2	6.784
10.32	7.3265	10.42	7.0085	10.3	6.762
10.42	7.313	10.52	7.003	10.4	6.751

Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 5 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 5 (mg/L)
19.83	6.33	19.93	5.6195	19.8	5.295	22.94	6.011	23.04	5.1735	22.93	4.799
19.93	6.319	20.03	5.61	19.9	5.2845	23.04	6.0115	23.14	5.1495	23.04	4.78
20.03	6.3145	20.13	5.581	20	5.266	23.14	5.9945	23.24	5.1435	23.14	4.7645
20.13	6.3065	20.23	5.5655	20.1	5.2515	23.24	5.975	23.34	5.1285	23.23	4.751
20.23	6.29	20.33	5.5555	20.2	5.231	23.34	5.96	23.44	5.112	23.34	4.7405
20.33	6.277	20.43	5.544	20.3	5.1835	23.44	5.9525	23.54	5.094	23.44	4.7175
20.43	6.2675	20.53	5.53	20.4	5.1245	23.54	5.9335	23.64	5.072	23.54	4.6845
20.53	6.253	20.63	5.515	20.5	5.058	23.64	5.922	23.74	5.0775	23.64	4.6725
20.63	6.2405	20.73	5.4945	20.6	5.06	23.74	5.9195	23.84	5.0585	23.74	4.655
20.73	6.233	20.83	5.48	20.7	5.1035	23.84	5.8975	23.94	5.0395	23.84	4.653
20.83	6.2315	20.93	5.476	20.8	5.095	23.94	5.89	24.04	5.042	23.94	4.6255
20.93	6.2205	21.03	5.4535	20.9	5.0505	24.04	5.887	24.14	5.012	24.04	4.597
21.03	6.212	21.13	5.445	21	4.9845	24.14	5.877	24.24	5.01	24.14	4.5585
21.13	6.2085	21.23	5.4415	21.1	4.9415	24.24	5.865	24.34	4.9915	24.24	4.535
21.23	6.1955	21.33	5.4275	21.2	4.9695	24.34	5.8475	24.44	4.975	24.34	4.496
21.33	6.188	21.43	5.403	21.3	4.9455	24.44	5.8355	24.54	4.96	24.44	4.436
21.43	6.1735	21.53	5.3945	21.4	4.905	24.54	5.8275	24.64	4.9475	24.54	4.3965
21.53	6.1635	21.63	5.375	21.5	4.8645	24.64	5.83	24.74	4.913	24.64	4.3405
21.63	6.149	21.73	5.3655	21.6	4.8445	24.74	5.8145	24.84	4.9035	24.74	4.293
21.73	6.133	21.83	5.345	21.7	4.902	24.84	5.799	24.94	4.898		
21.83	6.1235	21.93	5.3355	21.8	4.953			25.04	4.878		
21.93	6.1205	22.03	5.3185	21.9	4.9485			25.14	4.859		
22.03	6.105	22.13	5.297	22	4.9455			25.24	4.8495		
22.13	6.0975	22.23	5.287	22.1	4.9355			25.34	4.835		
22.24	6.088	22.33	5.27	22.2	4.9165			25.44	4.8265		
22.33	6.0805	22.43	5.2635	22.3	4.903						
22.44	6.071	22.53	5.2415	22.4	4.8885						
22.54	6.0705	22.63	5.235	22.5	4.8635						
22.64	6.069	22.74	5.1995	22.6	4.8475						
22.74	6.0465	22.83	5.1955	22.7	4.8305						
22.84	6.02	22.94	5.1925	22.8	4.81						

Oxygen Uptake Rates for Alginate Gels: Experiment Begun 4-18-04





Sample	Date	Gel Age (days)	DO Uptake Rate (mg/L/min)
Plank Control	4/18/04	0	0.0933
Gel	4/18/04	0	0.0775
Gel	4/19/04	1	0.1020
Gel	4/21/04	3	0.1479
Gel	4/23/04	5	0.149

#### A.1.5 Thermal polymer oxygen uptake rates

Thermal polymer: planktonic control, and polymer on days 0, 1, 5, 8, 10, and 14  
4-18-04, Book 2, Page 84

cells counts 4.00E+09 2.90E+09 3.80E+09  
ave 3.57E+09 cells per mL  
tot vol 12 mL  
cells per batch 7.13E+09

Time (min)	Av DO for Planktonic (mg/L)	Time (min)	Av DO for Day 0 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 10 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
2.303	6.3045	2.303	5.823	3.505	4.8945	2.504	2.6735	3.104	6.559	2.505	5.0645	2.504	4.8605
2.404	6.2575	2.404	5.7615	3.605	4.874	2.603	2.633	3.204	6.5205	2.604	5.0725	2.604	4.799
2.504	6.2195	2.504	5.8605	3.706	4.894	2.704	2.6765	3.305	6.642	2.704	5.085	2.704	4.833
2.604	6.187	2.603	5.7265	3.805	4.886	2.804	2.651	3.405	6.645	2.805	5.0785	2.804	4.8
2.704	6.1245	2.704	5.781	3.906	4.902	2.904	2.663	3.504	6.671	2.905	5.0395	2.905	4.8115
2.804	6.0875	2.804	5.8545	4.006	4.917	3.004	2.641	3.605	6.705	3.005	5.0405	3.004	4.7955
2.905	6.034	2.905	5.959	4.106	4.835	3.104	2.586	3.705	6.628	3.105	5.027	3.105	4.778
3.004	5.9995	3.004	5.839	4.206	4.843	3.205	2.544	3.806	6.6005	3.205	5.085	3.205	4.8155
3.104	5.9535	3.104	5.761	4.306	4.84	3.305	2.544	3.905	6.646	3.306	5.0605	3.306	4.791
3.205	5.895	3.205	5.8145	4.407	4.846	3.405	2.5545	4.005	6.685	3.405	5.097	3.405	4.816
3.305	5.835	3.305	5.8915	4.506	4.8055	3.505	2.509	4.106	6.689	3.506	5.038	3.505	4.7885
3.405	5.7815	3.405	5.823	4.607	4.8	3.605	2.4655	4.206	6.651	3.606	5.035	3.606	4.768
3.505	5.7395	3.505	5.7565	4.707	4.8345	3.706	2.477	4.306	6.67	3.706	5.0735	3.706	4.775
3.605	5.6625	3.605	5.6575	4.807	4.751	3.805	2.433	4.406	6.5825	3.806	5.038	3.806	4.7685
3.706	5.606	3.706	5.545	4.907	4.772	3.905	2.4245	4.506	6.666	3.906	5.0665	3.906	4.795
3.805	5.554	3.805	5.61	5.007	4.81	4.006	2.4045	4.607	6.589	4.007	5.0345	4.006	4.7725
3.906	5.523	3.905	5.68	5.107	4.764	4.106	2.373	4.706	6.6225	4.107	5.064	4.107	4.7575
4.006	5.477	4.006	5.641	5.208	4.7445	4.206	2.3475	4.806	6.607	4.207	5.021	4.206	4.753
4.106	5.414	4.106	5.5465	5.307	4.715	4.306	2.3245	4.907	6.6995	4.307	5.067	4.307	4.8105
4.206	5.3455	4.206	5.5795	5.408	4.774	4.406	2.2895	5.006	6.695	4.407	5.033	4.407	4.753
4.306	5.298	4.306	5.6695	5.508	4.7495	4.507	2.308	5.107	6.6495	4.508	5.066	4.508	4.7765
4.407	5.2435	4.406	5.491	5.608	4.692	4.606	2.253	5.207	6.6605	4.607	4.957	4.607	4.7615
4.507	5.1755	4.507	5.492	5.708	4.633	4.707	2.245	5.308	6.683	4.708	4.9805	4.707	4.7515
4.606	5.1	4.606	5.5205	5.808	4.6255	4.807	2.2485	5.407	6.707	4.808	4.988	4.808	4.709
4.707	5.047	4.707	5.413	5.909	4.6905	4.907	2.1955	5.507	6.6765	4.908	4.968	4.907	4.6745
4.807	5.0125	4.807	5.383	6.009	4.7555	5.007	2.1685	5.608	6.6095	5.008	4.9015	5.008	4.6965
4.907	4.9525	4.907	5.443	6.109	4.624	5.107	2.1675	5.708	6.6295	5.108	4.82	5.108	4.674
5.007	4.911	5.007	5.3545	6.209	4.655	5.208	2.15	5.807	6.712	5.209	4.81	5.208	4.6985
5.107	4.8145	5.107	5.2985	6.309	4.6635	5.307	2.1215	5.908	6.6445	5.308	4.793	5.308	4.643
5.208	4.756	5.208	5.315	6.41	4.5915	5.407	2.0635	6.008	6.6095	5.408	4.8205	5.408	4.6665
5.308	4.7075	5.308	5.3785	6.51	4.651	5.508	2.073	6.109	6.6335	5.509	4.802	5.509	4.679

Time (min)	Av DO for Plankto	Time (min)	Av DO for Day 0 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 10 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
5.408	4.629	5.407	5.2425	6.609	4.6575	5.608	2.049	6.208	6.567	5.609	4.822	5.609	4.662
5.508	4.551	5.508	5.3435	6.71	4.617	5.708	1.9835	6.308	6.5895	5.709	4.8225	5.708	4.607
5.608	4.4845	5.608	5.2595	6.81	4.5615	5.808	1.962	6.409	6.6405	5.809	4.777	5.809	4.5935
5.708	4.4535	5.708	5.226	6.911	4.4995	5.908	1.92	6.509	6.6115	5.909	4.8145	5.909	4.571
5.808	4.3745	5.808	5.2505	7.01	4.5055	6.009	1.937	6.609	6.4795	6.01	4.7745	6.01	4.568
5.909	4.303	5.908	5.2455	7.11	4.525	6.109	1.9325	6.709	6.5255	6.109	4.7325	6.109	4.627
6.009	4.24	6.009	5.1945	7.211	4.4885	6.209	1.882	6.809	6.5405	6.21	4.742	6.209	4.5925
6.109	4.1705	6.109	5.237	7.311	4.55	6.309	1.8665	6.91	6.5235	6.31	4.711	6.31	4.602
6.209	4.0935	6.208	5.1765	7.411	4.4615	6.41	1.834	7.01	6.5745	6.411	4.7465	6.41	4.612
6.309	4.0115	6.309	5.081	7.511	4.4375	6.51	1.8085	7.11	6.5995	6.51	4.744	6.51	4.5395
6.41	3.935	6.409	4.983	7.612	4.525	6.609	1.8145	7.21	6.651	6.61	4.735	6.61	4.5965
6.51	3.8655	6.51	5.0075	7.712	4.409	6.71	1.7475	7.31	6.5315	6.711	4.7115	6.711	4.5535
6.609	3.8105	6.609	5.0185	7.811	4.464	6.81	1.7315	7.41	6.6905	6.811	4.71	6.811	4.5815
6.71	3.731	6.709	4.9545	7.912	4.3785	6.911	1.7205	7.51	6.6135	6.911	4.698	6.911	4.5775
6.81	3.6645	6.81	5.0705	8.012	4.3735	7.01	1.6715	7.611	6.5645	7.011	4.6655	7.011	4.5395
6.911	3.577	6.91	5.0445	8.113	4.399	7.11	1.666	7.711	6.6005	7.111	4.7015	7.111	4.531
7.01	3.5165	7.01	4.9875	8.212	4.3195	7.211	1.652	7.811	6.5885	7.212	4.7215	7.212	4.538
7.11	3.448	7.11	4.889	8.312	4.3905	7.311	1.6285	7.911	6.6295	7.312	4.675	7.312	4.5395
7.211	3.367	7.21	4.9545	8.413	4.3	7.411	1.592	8.011	6.603	7.412	4.627	7.411	4.4765
7.311	3.297	7.311	4.9005	8.512	4.2915	7.511	1.559	8.111	6.548	7.512	4.662	7.512	4.519
7.411	3.221	7.41	4.8595	8.613	4.2225	7.611	1.534	8.211	6.5075	7.612	4.6605	7.612	4.5065
7.511	3.1675	7.511	4.749	8.713	4.2695	7.712	1.5395	8.311	6.583	7.713	4.6945	7.713	4.5215
7.611	3.072	7.611	4.7695	8.813	4.307	7.811	1.486	8.412	6.559	7.812	4.6695	7.812	4.5065
7.712	2.991	7.711	4.8325	8.913	4.249	7.912	1.4565	8.512	6.461	7.913	4.672	7.912	4.5175
7.811	2.903	7.811	4.759	9.013	4.234	8.012	1.4405	8.612	6.541	8.013	4.6745	8.013	4.486
7.912	2.854	7.911	4.666	9.114	4.211	8.111	1.411	8.712	6.5265	8.113	4.659	8.113	4.492
8.012	2.7635	8.012	4.7235	9.214	4.1285	8.212	1.4005	8.812	6.491	8.213	4.6345	8.213	4.4615
8.111	2.6635	8.111	4.637	9.314	4.2435	8.312	1.391	8.913	6.521	8.313	4.62	8.313	4.4145
8.212	2.598	8.211	4.6145	9.414	4.159	8.412	1.319	9.012	6.5175	8.414	4.561	8.414	4.459
8.312	2.5305	8.312	4.628	9.514	4.1555	8.512	1.329	9.113	6.572	8.514	4.5565	8.514	4.467
8.413	2.4615	8.412	4.6205	9.615	4.216	8.612	1.305	9.213	6.565	8.614	4.571	8.613	4.4

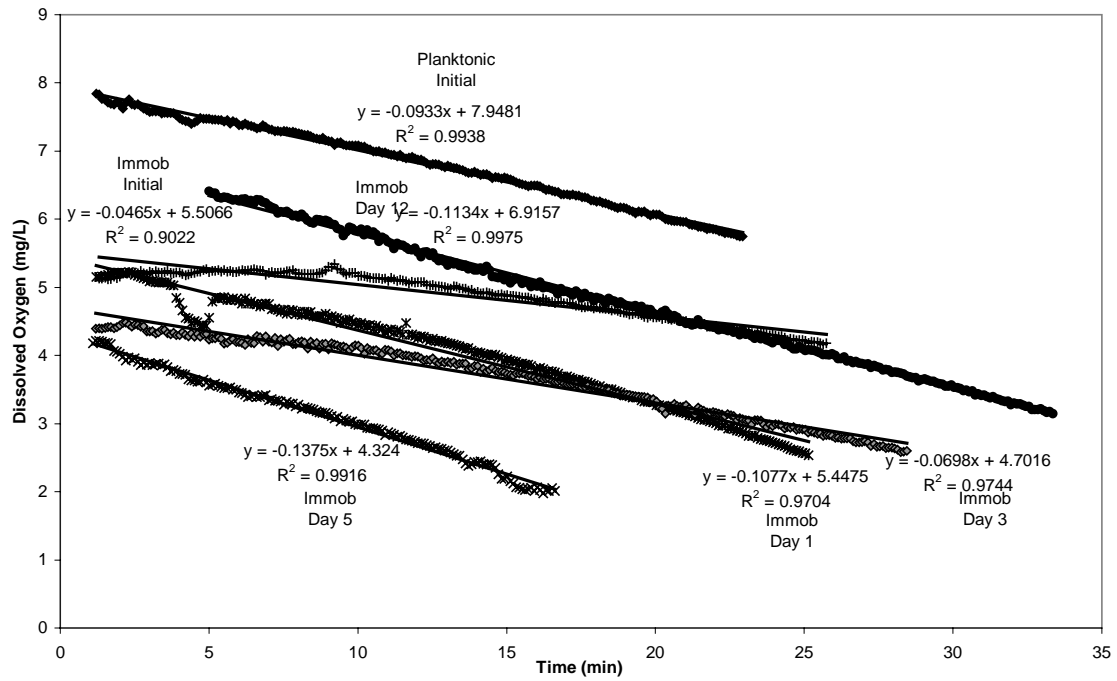
Time (min)	Av DO for Plankto	Time (min)	Av DO for Day 0 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 3 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 10 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
8.512	2.41	8.512	4.5735	9.715	4.1485	8.713	1.2725	9.313	6.5955	8.714	4.578	8.714	4.425
8.612	2.306	8.612	4.559	9.815	4.0635	8.813	1.2375	9.413	6.5455	8.814	4.5865	8.814	4.415
8.713	2.237	8.712	4.4665	9.915	4.1085	8.913	1.2255	9.513	6.507	8.915	4.544	8.914	4.431
8.813	2.1585	8.813	4.5165	10.015	4.058	9.013	1.202	9.613	6.5845	9.014	4.513	9.014	4.3955
8.913	2.096	8.913	4.4285	10.115	4.0845	9.113	1.1745	9.714	6.5625	9.115	4.487	9.114	4.4125
9.013	1.9935	9.012	4.398	10.215	4.027	9.214	1.135	9.813	6.6375	9.215	4.462	9.215	4.37
9.113	1.9365	9.113	4.4385	10.315	4.042	9.314	1.0875	9.914	6.495	9.314	4.512	9.314	4.362
9.214	1.8505	9.213	4.432	10.416	3.994	9.413	1.0885	10.014	6.51	9.415	4.505	9.415	4.4085
9.314	1.7755	9.314	4.401	10.516	3.992			10.114	6.435	9.515	4.4745	9.515	4.383
9.414	1.6715	9.413	4.4085	10.616	4.0125			10.214	6.49	9.616	4.4795	9.616	4.351
9.514	1.636	9.513	4.295	10.716	4.0035			10.314	6.55	9.715	4.496	9.715	4.32
9.614	1.553	9.614	4.2415	10.816	3.972			10.415	6.5185	9.816	4.502	9.815	4.348
9.715	1.4855	9.714	4.2525	10.916	3.9425			10.515	6.533	9.916	4.448	9.916	4.345
9.814	1.385	9.814	4.1935	11.016	3.8685			10.614	6.549	10.016	4.4695	10.016	4.3095
9.915	1.301	9.914	4.191	11.117	3.9115			10.715	6.523	10.116	4.468	10.116	4.342
10.015	1.2475	10.014	4.223	11.217	3.891			10.815	6.502	10.216	4.4685	10.216	4.33
10.115	1.156	10.115	4.102	11.316	3.881			10.915	6.5035	10.317	4.4545	10.316	4.2945
10.215	1.073	10.214	4.06	11.417	3.8825			11.015	6.521	10.417	4.3805	10.417	4.3225
		10.315	4.0035	11.517	3.8275			11.115	6.5365	10.517	4.408	10.516	4.2775
		10.415	3.973	11.618	3.8575			11.216	6.5895	10.617	4.3665	10.617	4.252
		10.514	4.0855	11.717	3.8385			11.316	6.46	10.717	4.3615	10.717	4.284
		10.615	3.994	11.818	3.8185			11.416	6.453	10.818	4.3135	10.817	4.3105
		10.715	3.8445	11.918	3.8165			11.516	6.5395	10.917	4.295	10.917	4.2345
		10.816	3.953	12.018	3.7885			11.616	6.4355	11.017	4.289	11.017	4.258
		10.915	3.9	12.118	3.7705			11.717	6.542	11.118	4.2595	11.118	4.234
		11.015	3.9155	12.218	3.8105			11.816	6.5655	11.218	4.251	11.218	4.2465
		11.116	3.871	12.319	3.775			11.917	6.5665	11.318	4.24	11.317	4.1785
		11.216	3.879	12.419	3.737			12.017	6.487	11.418	4.23	11.418	4.1945
		11.316	3.7305	12.518	3.7145			12.117	6.471	11.518	4.2205	11.518	4.206
		11.416	3.7695	12.619	3.689			12.217	6.568	11.619	4.226	11.618	4.2285
		11.516	3.7295	12.719	3.6725			12.317	6.4975	11.718	4.1605	11.718	4.2255

Time (min)	Av DO for Day 0 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 10 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
11.617	3.7955	12.819	3.6855	12.418	6.4925	11.819	4.214	11.818	4.2395
11.717	3.748	12.919	3.6945	12.517	6.462	11.919	4.213	11.919	4.2175
11.817	3.635	13.019	3.6595	12.617	6.485	12.019	4.1885	12.019	4.1605
11.917	3.523	13.12	3.624	12.718	6.4675	12.119	4.168	12.119	4.151
12.017	3.6535	13.22	3.554	12.818	6.5395	12.219	4.175	12.219	4.17
12.118	3.5295	13.32	3.573	12.918	6.567	12.32	4.191	12.319	4.1965
12.217	3.52	13.42	3.547	13.018	6.4785	12.42	4.1485	12.42	4.1295
12.318	3.5215	13.521	3.5775	13.118	6.4195	12.52	4.191	12.519	4.1645
12.418	3.4855	13.62	3.573	13.219	6.519	12.62	4.202	12.62	4.148
12.517	3.5455	13.72	3.529	13.318	6.4855	12.72	4.1625	12.72	4.0995
12.618	3.4955	13.821	3.5055	13.418	6.5255	12.821	4.1735	12.821	4.1335
12.718	3.419	13.921	3.512	13.519	6.489	12.92	4.1595	12.92	4.125
12.818	3.4905	14.021	3.4625	13.619	6.4035	13.021	4.167	13.02	4.0895
12.918	3.4025	14.121	3.4235	13.719	6.4645	13.121	4.1905	13.121	4.0735
13.018	3.329	14.221	3.366	13.819	6.4695	13.221	4.17	13.22	4.0955
13.119	3.279	14.322	3.35	13.919	6.4255	13.321	4.1675	13.321	4.1015
13.219	3.2875	14.422	3.3205	14.02	6.4825	13.421	4.1695	13.421	4.0825
13.318	3.316	14.521	3.349	14.12	6.4125	13.522	4.134	13.521	4.1075
13.419	3.223	14.622	3.372	14.22	6.4555	13.622	4.1445	13.622	4.033
13.519	3.1245	14.722	3.338	14.32	6.3935	13.722	4.1595	13.721	4.0445
13.62	3.1625	14.823	3.3205	14.42	6.4825	13.822	4.104	13.822	4.037
13.719	3.165	14.922	3.278	14.521	6.4645	13.922	4.122	13.922	4.0645
13.819	3.1495	15.022	3.2855	14.62	6.5405	14.023	4.106	14.021	4.077
13.92	3.056	15.123	3.309	14.72	6.4595	14.122	4.0985	14.122	4.053
14.02	3.126	15.222	3.264	14.821	6.4005	14.223	4.12	14.222	4.0175
14.12	3.055	15.323	3.23	14.92	6.397	14.323	4.098	14.323	4.074
14.22	2.9595	15.423	3.243	15.021	6.45	14.422	4.0925	14.422	4.0705
14.32	2.9745	15.524	3.225	15.121	6.401	14.523	4.0625	14.522	4.0505
14.421	2.8985	15.623	3.2105	15.222	6.483	14.623	4.061	14.623	4.001
14.521	2.9455	15.723	3.149	15.321	6.42	14.724	4.0565	14.723	4.041
14.621	2.923	15.824	3.076	15.421	6.4385	14.823	4.064	14.823	3.9905

Time (min)	Av DO for Day 0 (mg/L)	Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 10 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
14.721	2.875	15.924	3.103	15.522	6.4355	14.923	4.066	14.923	3.9845
14.821	2.7995	16.024	3.026	15.622	6.374	15.024	4.0555	15.024	4.0195
14.921	2.8815	16.124	3.057	15.722	6.4445	15.124	4.017	15.124	4.0025
15.021	2.722	16.224	3.012	15.822	6.446	15.224	4.044	15.224	3.98
15.122	2.7285	16.325	3.0075	15.922	6.449	15.324	4.015	15.324	3.972
15.222	2.709	16.424	2.9985	16.023	6.4315	15.424	4.0345	15.424	3.977
15.321	2.708	16.525	3.008	16.122	6.3525	15.525	4.03	15.525	3.9875
15.422	2.68	16.625	2.966	16.223	6.4155	15.625	4.0025	15.625	3.9425
15.522	2.641	16.725	2.9475	16.323	6.5035			15.724	3.976
15.622	2.666	16.826	2.9625	16.423	6.4585			15.825	3.961
15.722	2.558	16.925	2.9795	16.524	6.49			15.925	3.9535
		17.026	2.964	16.623	6.4355			16.025	3.9325
		17.126	2.9455	16.723	6.4635			16.125	3.907
		17.226	2.918	16.824	6.4905			16.225	3.896
		17.326	2.949	16.924	6.4035			16.326	3.9085
		17.426	2.9505	17.024	6.397			16.426	3.924
		17.527	2.936	17.124	6.316			16.526	3.8975
		17.626	2.904	17.225	6.499			16.626	3.877
		17.727	2.9015	17.324	6.401			16.726	3.8985
		17.827	2.898	17.424	6.447			16.826	3.8555
		17.927	2.8735	17.525	6.44			16.926	3.8765
		18.027	2.8435	17.625	6.4805			17.027	3.9105
		18.127	2.8725	17.726	6.38			17.127	3.8655
		18.228	2.8685	17.825	6.39			17.227	3.846
		18.328	2.8775	17.925	6.433			17.327	3.856
		18.427	2.862	18.026	6.386			17.427	3.847
		18.528	2.8205	18.125	6.38			17.528	3.8075
		18.628	2.7765	18.226	6.48			17.627	3.836
		18.729	2.7785	18.326	6.414			17.728	3.821
		18.828	2.82	18.426	6.4765			17.828	3.841
		18.928	2.778	18.527	6.3605			17.928	3.8005

Time (min)	Av DO for Day 1 (mg/L)	Time (min)	Av DO for Day 8 (mg/L)	Time (min)	Av DO for Day 14 (mg/L)
19.029	2.799	18.626	6.444	18.028	3.7955
19.129	2.7695	18.727	6.3315	18.128	3.82
19.229	2.768	18.827	6.341	18.229	3.754
19.329	2.771	18.927	6.4305	18.329	3.76
19.429	2.7705	19.027	6.314	18.429	3.7575
19.53	2.7515	19.127	6.3955	18.529	3.7355
19.629	2.706	19.228	6.3575	18.629	3.7435
19.73	2.738	19.327	6.2725	18.729	3.7675
19.83	2.727	19.427	6.403	18.829	3.743
19.931	2.734	19.528	6.3755	18.93	3.7305
20.03	2.691	19.628	6.409	19.03	3.73
20.13	2.663	19.728	6.3595	19.13	3.7015
20.231	2.6505	19.828	6.281	19.23	3.7005
20.331	2.67	19.928	6.3115	19.33	3.7195
20.431	2.641	20.029	6.342	19.431	3.7095
20.531	2.6365	20.128	6.3705	19.531	3.711
20.631	2.616	20.228	6.315	19.63	3.6765
20.732	2.6425	20.329	6.303	19.731	3.655
20.831	2.5925	20.429	6.3405	19.831	3.661
20.932	2.592	20.529	6.3225	19.931	3.687

# Oxygen Uptake Rates for Thermal Polymer Gels: Experiment Begun 4-18-04



Sample	Date	Gel Age (days)	DO Uptake Rate (mg/L/min)
Plank Control	4/18/04	0	0.0933
Gel	4/18/04	0	0.0465
Gel	4/19/04	1	0.1077
Gel	4/21/04	3	0.0698
Gel	4/23/04	5	0.1375
Gel	4/30/04	12	0.1134

## Planktonic control with HAC

Time (min)	Average
0.6	4.0265
0.701	3.8775
0.801	3.7255
0.902	3.569
1.002	3.403
1.101	3.267
1.202	3.1185
1.302	2.979
1.403	2.8415
1.502	2.6805
1.602	2.542
1.703	2.394
1.803	2.252
1.903	2.096
2.003	1.953
2.103	1.814
2.204	1.6725
2.303	1.531
2.404	1.369
2.504	1.228
2.604	1.091
2.704	0.948
2.804	0.797
2.905	0.6625

## Planktonic control without HAC

Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average
1:02	7.395	4:207	7.115	7.312	6.9505	10.416	6.7315	13.521	6.645	16.625	6.504	19.73	6.3655	22.834	6.225
1:202	7.3725	4:307	7.11	7.411	6.9395	10.517	6.7905	13.621	6.641	16.726	6.494	19.83	6.355	22.935	6.221
1:302	7.2525	4:407	7.1075	7.512	6.9335	10.616	6.789	13.72	6.635	16.826	6.501	19.931	6.3485	23.035	6.222
1:403	7.3325	4:507	7.1035	7.612	6.9335	10.717	6.779	13.821	6.6325	16.926	6.489	20.031	6.3475	23.136	6.216
1:502	7.317	4:607	7.0945	7.712	6.9332	10.817	6.770	13.921	6.6325	17.026	6.484	20.131	6.345	23.235	6.2065
2:003	7.2055	4:707	7.0915	7.812	6.9325	10.917	6.7605	14.022	6.632	17.126	6.479	20.231	6.3425	23.335	6.202
1:702	7.235	4:808	7.084	7.912	6.9313	11.017	6.7505	14.121	6.619	17.226	6.483	20.331	6.3325	23.435	6.2
1:803	7.2815	4:908	7.077	8.012	6.9308	11.117	6.7595	14.221	6.614	17.326	6.4695	20.431	6.33	23.535	6.2065
1:903	7.2655	5:008	7.0665	8.113	6.9055	11.218	6.7545	14.322	6.6115	17.426	6.465	20.531	6.3285	23.635	6.192
2:003	7.2635	5:108	7.0635	8.212	6.9012	11.318	6.7545	14.422	6.6085	17.527	6.464	20.631	6.3225	23.736	6.1845
2:104	7.2655	5:208	7.0595	8.313	6.8965	11.417	6.7415	14.522	6.603	17.627	6.453	20.732	6.315	23.836	6.181
2:204	7.2455	5:309	7.0474	8.413	6.8945	11.518	6.7315	14.622	6.6005	17.727	6.4555	20.832	6.3035	23.937	6.177
2:305	7.2349	5:409	7.0348	8.513	6.8905	11.618	6.7215	14.722	6.603	17.827	6.4525	20.932	6.2915	24.037	6.173
2:404	7.223	5:508	7.044	8.613	6.8815	11.717	6.713	14.822	6.5795	17.927	6.4455	21.032	6.3055	24.137	6.167
2:504	7.2225	5:609	7.038	8.713	6.8755	11.818	6.7275	14.922	6.5825	18.027	6.443	21.132	6.296	24.237	6.164
2:605	7.2105	5:709	7.0295	8.814	6.8765	11.918	6.718	15.023	6.5795	18.127	6.4405	21.233	6.2945	24.337	6.167
2:704	7.208	5:809	7.027	8.913	6.8854	12.019	6.713	15.123	6.575	18.228	6.429	21.332	6.2885	24.437	6.16
2:805	7.2035	5:909	7.024	9.014	6.8625	12.118	6.714	15.224	6.556	18.328	6.4215	21.433	6.2905	24.537	6.153
2:905	7.1885	6:009	7.0195	9.114	6.8565	12.218	6.703	15.323	6.552	18.428	6.4245	21.533	6.28	24.638	6.1475
3:004	7.1935	6:101	6.9965	9.214	6.852	12.319	6.6745	15.423	6.5525	18.528	6.418	21.632	6.2775	24.738	6.146
3:105	7.175	6:202	6.9875	9.314	6.8375	12.419	6.6564	15.523	6.554	18.628	6.4125	21.732	6.2645	24.838	6.141
3:205	7.1715	6.31	6.9905	9.414	6.8385	12.519	6.6945	15.624	6.5535	18.729	6.4045	21.832	6.2475	24.938	6.1325
3:306	7.17	6.41	6.996	9.515	6.8335	12.619	6.6935	15.724	6.544	18.829	6.3995	21.934	6.2685	25.038	6.131
3:405	7.1545	6.51	6.988	9.615	6.8305	12.719	6.682	15.824	6.533	18.929	6.401	22.034	6.2565	25.139	6.125
3:505	7.153	6.61	6.9855	9.715	6.8275	12.82	6.671	15.924	6.5355	19.029	6.395	22.133	6.2545	25.238	6.126
3:606	7.147	6.71	6.9845	9.815	6.8245	12.92	6.6775	16.024	6.533	19.129	6.3875	22.234	6.2525	25.339	6.1195
3:706	7.1525	6.81	6.97	9.915	6.8195	13.022	6.6765	16.124	6.527	19.229	6.3875	22.334	6.2465	25.439	6.1105
3:806	7.1455	6.91	6.965	10.015	6.8165	13.122	6.671	16.224	6.5225	19.329	6.3825	22.434	6.2405	25.539	6.1035
3:906	7.123	7.01	6.965	10.115	6.8135	13.222	6.654	16.325	6.517	19.43	6.379	22.534	6.2365	25.639	6.101
4:007	7.1235	7.11	6.9625	10.216	6.8096	13.322	6.6535	16.425	6.503	19.53	6.376	22.635	6.2355	25.739	6.0985
4:107	7.1215	7.21	6.946	10.316	6.804	13.422	6.652	16.525	6.499	19.629	6.3685	22.735	6.225	25.84	6.095

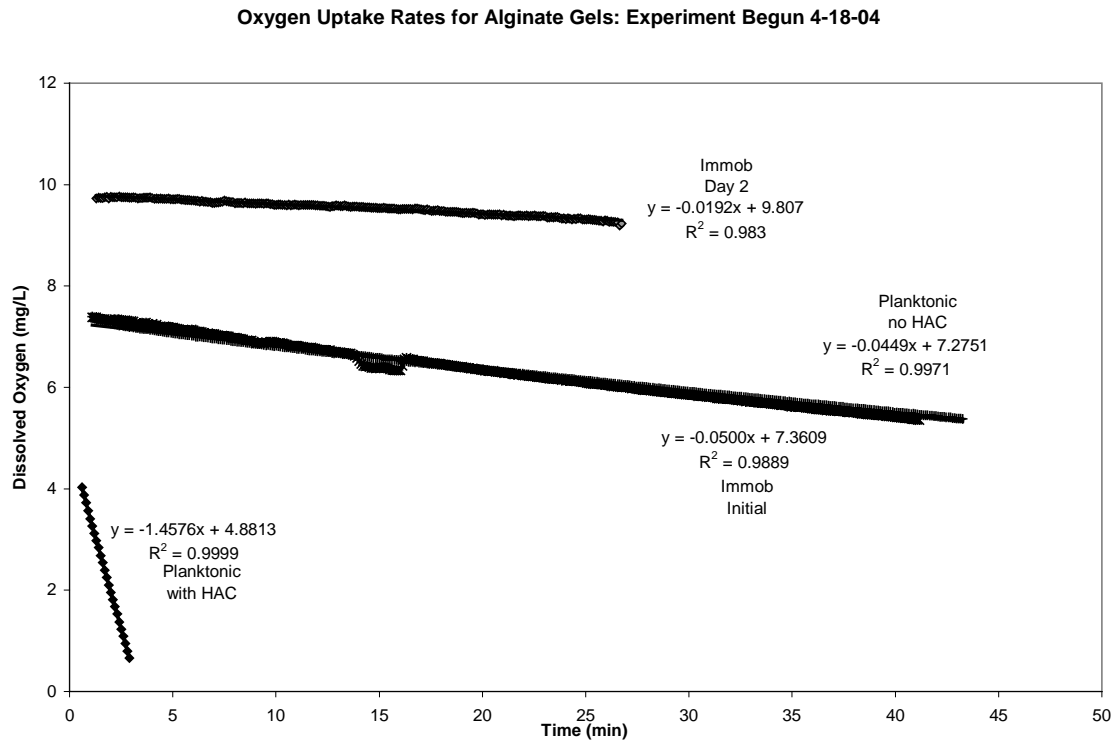


Time	Average	Time	Average
34.154	5.675	37.458	5.5265
34.253	5.6645	37.559	5.519
34.354	5.655	37.659	5.5155
34.454	5.6525	37.759	5.506
34.554	5.653	37.859	5.5095
34.654	5.6505	37.959	5.507
34.754	5.6415	38.06	5.506
34.855	5.632	38.16	5.5
34.955	5.6195	38.26	5.4875
35.054	5.6235	38.36	5.4755
35.155	5.616	38.461	5.4815
35.255	5.6135	38.561	5.473
35.355	5.6125	38.66	5.4655
35.455	5.617	38.761	5.465
35.555	5.6065	38.861	5.468
35.656	5.594	38.961	5.4675
35.756	5.5945	39.061	5.457
35.856	5.596	39.161	5.448
35.956	5.58	39.262	5.446
36.057	5.5745	39.361	5.445
36.157	5.5685	39.462	5.4455
36.256	5.5615	39.562	5.433
36.357	5.5605	39.662	5.425
36.457	5.5575	39.763	5.424
36.557	5.5585	39.862	5.4245
36.657	5.548	39.963	5.4145
36.757	5.5575	40.063	5.4105
36.858	5.5435	40.163	5.4065
36.958	5.5365	40.263	5.4045
37.058	5.5385	40.363	5.3995
37.158	5.5355	40.464	5.394
37.259	5.533	40.563	5.391
37.359	5.534	40.664	5.384

## Alginate immobilized cells, no HAC, day 2

Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average	Time	Average
1.301	9.7275	4.506	9.721	7.71	9.6645	10.916	9.6025	14.12	9.555	17.325	9.509	20.53	9.4065	23.734	9.3405
1.401	9.7395	4.606	9.7215	7.811	9.656	11.015	9.5965	14.22	9.5585	17.425	9.497	20.63	9.4075	23.835	9.3265
1.5	9.7345	4.705	9.72	7.91	9.6535	11.116	9.593	14.321	9.5535	17.526	9.4815	20.731	9.4105	23.935	9.3345
1.601	9.7325	4.806	9.73	8.011	9.6335	11.216	9.6	14.421	9.551	17.626	9.4895	20.83	9.4125	24.035	9.32
1.701	9.7475	4.906	9.7125	8.111	9.6355	11.316	9.599	14.521	9.5475	17.726	9.486	20.93	9.3905	24.135	9.3355
1.802	9.76	5.006	9.7115	8.21	9.6375	11.416	9.6015	14.621	9.54	17.826	9.491	21.031	9.404	24.235	9.3285
1.901	9.7265	5.106	9.709	8.311	9.639	11.516	9.5955	14.721	9.5465	17.926	9.4765	21.131	9.392	24.336	9.309
2.002	9.758	5.206	9.716	8.411	9.632	11.617	9.598	14.822	9.545	18.027	9.481	21.232	9.3835	24.435	9.3295
2.102	9.753	5.307	9.715	8.512	9.643	11.717	9.6	14.922	9.5355	18.126	9.4765	21.331	9.387	24.536	9.322
2.202	9.7475	5.406	9.7005	8.611	9.627	11.817	9.6	15.021	9.5355	18.227	9.4605	21.431	9.38	24.636	9.3315
2.302	9.75	5.507	9.6995	8.712	9.63	11.917	9.5915	15.122	9.5315	18.327	9.4665	21.532	9.3775	24.736	9.3315
2.402	9.766	5.607	9.6955	8.812	9.6285	12.017	9.589	15.222	9.5425	18.427	9.4645	21.632	9.381	24.837	9.31
2.503	9.7535	5.707	9.693	8.912	9.6285	12.118	9.5795	15.323	9.5385	18.527	9.462	21.732	9.3895	24.936	9.312
2.603	9.753	5.807	9.6965	9.012	9.6245	12.217	9.5815	15.422	9.524	18.627	9.4605	21.832	9.387	25.037	9.313
2.702	9.7515	5.907	9.6895	9.112	9.632	12.318	9.5795	15.522	9.5305	18.728	9.462	21.932	9.3795	25.137	9.3185
2.803	9.747	6.008	9.6845	9.213	9.627	12.418	9.5745	15.623	9.5245	18.828	9.4545	22.032	9.3835	25.236	9.3135
2.903	9.7445	6.108	9.6775	9.313	9.6275	12.518	9.57	15.722	9.526	18.927	9.4435	22.132	9.3895	25.337	9.3015
3.003	9.746	6.207	9.681	9.413	9.622	12.618	9.562	15.823	9.5205	19.028	9.44	22.233	9.377	25.437	9.3025
3.103	9.748	6.308	9.6605	9.513	9.627	12.718	9.571	15.923	9.513	19.128	9.441	22.333	9.3845	25.538	9.294
3.203	9.74	6.408	9.6785	9.613	9.6295	12.819	9.577	16.023	9.511	19.229	9.443	22.433	9.379	25.638	9.2905
3.304	9.7275	6.509	9.6625	9.714	9.617	12.918	9.594	16.124	9.5155	19.328	9.44	22.533	9.3875	25.737	9.2845
3.404	9.738	6.609	9.661	9.814	9.6115	13.018	9.579	16.223	9.519	19.428	9.4375	22.633	9.377	25.838	9.275
3.504	9.7375	6.708	9.6515	9.913	9.6	13.119	9.571	16.324	9.5165	19.529	9.445	22.733	9.375	25.938	9.2965
3.604	9.74	6.809	9.6505	10.014	9.5995	13.219	9.5745	16.424	9.5165	19.629	9.4395	22.833	9.3785	26.038	9.288
3.705	9.746	6.909	9.642	10.114	9.61	13.319	9.5865	16.524	9.519	19.729	9.43	22.933	9.3835	26.138	9.264
3.805	9.7385	7.01	9.6405	10.214	9.606	13.419	9.5775	16.624	9.5115	19.829	9.4105	23.034	9.3785	26.238	9.271
3.904	9.7495	7.109	9.649	10.314	9.597	13.519	9.569	16.724	9.525	19.929	9.4155	23.134	9.364	26.339	9.264
4.005	9.7355	7.209	9.65	10.414	9.5975	13.62	9.558	16.825	9.523	20.029	9.418	23.233	9.3545	26.438	9.2645
4.105	9.715	7.31	9.652	10.515	9.5925	13.719	9.566	16.924	9.5195	20.129	9.4025	23.334	9.358	26.539	9.262
4.206	9.7245	7.41	9.6605	10.615	9.607	13.82	9.5645	17.025	9.5145	20.23	9.4085	23.434	9.354	26.639	9.195
4.305	9.7205	7.51	9.685	10.715	9.5895	13.92	9.567	17.125	9.501	20.33	9.416	23.535	9.3565	26.74	9.2305
4.405	9.726	7.61	9.6675	10.816	9.5955	14.02	9.561	17.225	9.4955	20.43	9.4105	23.635	9.3565		

## Summary plot from alginate degradation experiment



Sample	Date	DO Uptake Rate (mg/L/min)
Plank with HAC	5/22/04	1.4576
Plank no HAC	5/22/04	0.0449
Gel Initial no HAC	5/22/04	0.0500
Gel Day 2 no HAC	5/24/04	0.0192



### A.3 t-tests to determine statistical difference

t tests for planktonic potassium efflux experiments: (units = mg K<sup>+</sup>/cell):

Referenced in Chapter 3

Data:

late log PA	mid log PA
2.13E-10	5.09E-10
5.46E-10	5.61E-10
2.52E-11	3.89E-10
2.06E-10	3.42E-10
4.89E-10	
3.63E-10	

late log EC	mid log EC
4.16E-10	4.51327E-10
1.87E-10	6.87023E-10
6.43E-10	4.78676E-10
	5.93559E-10
	5.58081E-10

Compare late log PA to mid log PA

t-Test: Two-Sample Assuming Unequal Variances

	Variable 1	Variable 2
Mean	3.07151E-10	4.49969E-10
Variance	3.83649E-20	1.04178E-20
Observations	6	4
Hypothesized Mean D	0	
df	8	
t Stat	-1.505553529	
P(T<=t) one-tail	0.085300189	
t Critical one-tail	1.85954832	
P(T<=t) two-tail	0.170600377	
t Critical two-tail	2.306005626	

tcalc < t crit, so accept null hypothesis. No difference exists.

Compare late log PA to late log EC

t-Test: Two-Sample Assuming Unequal Variances

	Variable 1	Variable 2
Mean	3.07151E-10	4.15329E-10
Variance	3.83649E-20	5.19538E-20
Observations	6	3
Hypothesized Mean D	0	
df	4	
t Stat	-0.702517739	
P(T<=t) one-tail	0.260543522	
t Critical one-tail	2.131846486	
P(T<=t) two-tail	0.521087044	
t Critical two-tail	2.776450856	

tcalc < t crit, so accept null hypothesis. No difference exists.

Compare late log EC to mid log EC

t-Test: Two-Sample Assuming Unequal Variances

	Variable 1	Variable 2
Mean	4.15329E-10	5.53733E-10
Variance	5.19538E-20	8.87291E-21
Observations	3	5
Hypothesized Mean D	0	
df	2	
t Stat	-1.001652612	
P(T<=t) one-tail	0.211007083	
t Critical one-tail	2.91998731	
P(T<=t) two-tail	0.422014166	
t Critical two-tail	4.302655725	

tcalc < t crit, so accept null hypothesis. No difference exists.

Compare mid log PA to mid log EC

t-Test: Two-Sample Assuming Unequal Variances

	Variable 1	Variable 2
Mean	4.49969E-10	5.53733E-10
Variance	1.04178E-20	8.87291E-21
Observations	4	5
Hypothesized Mean D	0	
df	6	
t Stat	-1.568050427	
P(T<=t) one-tail	0.083958121	
t Critical one-tail	1.943180905	
P(T<=t) two-tail	0.167916242	
t Critical two-tail	2.446913641	

tcalc < t crit, so accept null hypothesis. No difference exists.

## Appendix B: Data for Chapter 3

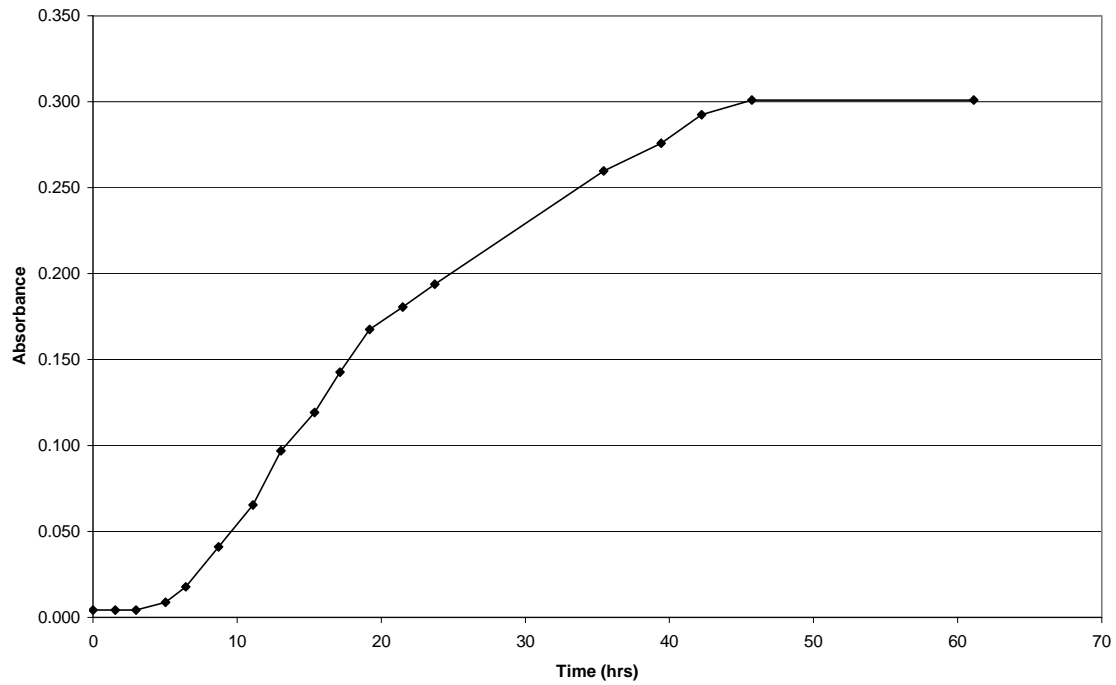
### B.1 Growth Curve Data

#### B.1.1 *Psuedomonas aeruginosa*

7-22-03, Book 2, Page 12

Time	Trans 1	Abs 1
0.0	99	0.004
1.5	99	0.004
3.0	99	0.004
5.0	98	0.009
6.4	96	0.018
8.7	91	0.041
11.1	86	0.066
13.0	80	0.097
15.4	76	0.119
17.1	72	0.143
19.2	68	0.167
21.5	66	0.180
23.7	64	0.194
35.4	55	0.260
39.4	53	0.276
42.2	51	0.292
45.7	50	0.301
61.1	50	0.301

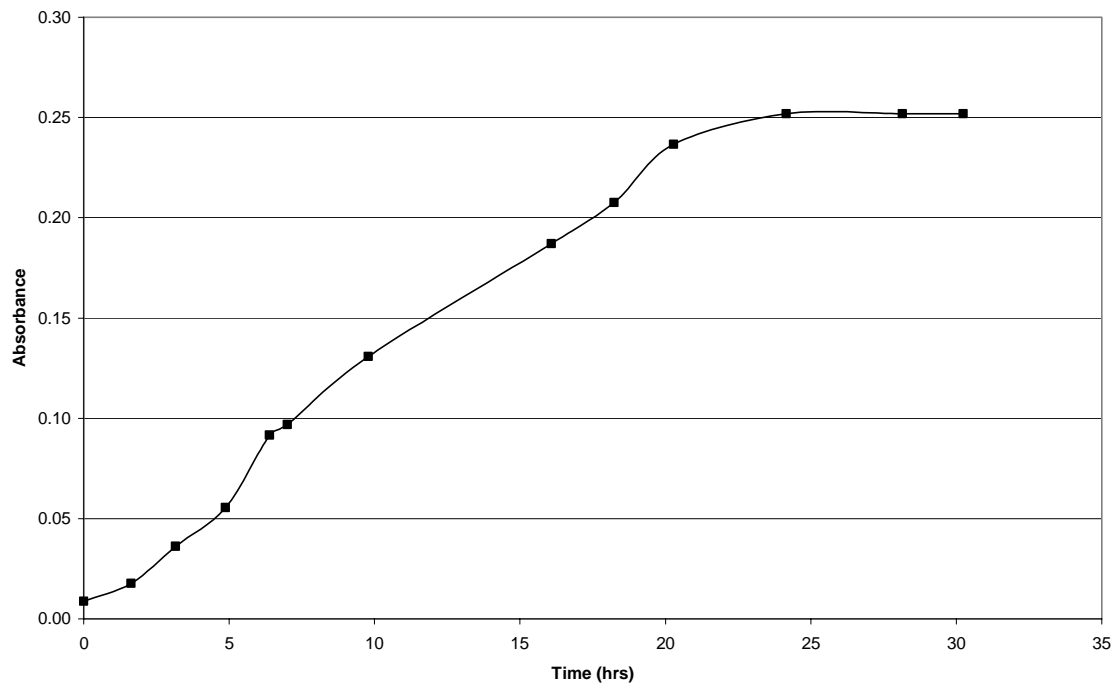
*P. aeruginosa* Growth Curve in 5L Jug



B.1.2 *Escherchia coli*  
8-14-03, Book 2, Page 16

Time	Transmittance	Absorbance
0.0	98	0.0088
1.6	96	0.0177
3.2	92	0.0362
4.9	88	0.0555
6.4	81	0.0915
7.0	80	0.0969
9.8	74	0.1308
16.1	65	0.1871
18.2	62	0.2076
20.3	58	0.2366
24.2	56	0.2518
28.2	56	0.2518
30.2	56	0.2518

*E. coli* Growth Curve in 5 L Jug



## B.2 Data for potassium efflux per cell for planktonic cultures

### B.2.1 Planktonic efflux from *P. aeruginosa*

Summary table of efflux data for planktonic *P. aeruginosa*

Trans	Abs	Cell Counts			Av cell count	StdDev cell count	delta K			av delta K	Std Dev delta K	delta K / cell	Error on Efflux
61	0.2147	1.7E+09	1.2E+09	1.4E+09	1.4E+09	2.5E+08	3.2	2.8	3.3	3.07	0.284	2.13E-10	4.1E-11
72	0.1427	1.3E+09	1.1E+09	1.1E+09	1.2E+09	8.1E+07	5.5	6.5	5.7	5.88	0.501	5.09E-10	5.6E-11
60	0.2218	1.2E+09	1.3E+09	1.2E+09	1.2E+09	4.2E+07	7.0	6.6	6.7	6.73	0.202	5.46E-10	2.5E-11
50	0.3010	9.0E+09	7.2E+09	8.4E+09	8.2E+09	9.2E+08	2.2	2.3	1.7	2.07	0.321	2.52E-11	4.8E-12
55	0.2596	1.3E+09	1.1E+09	1.2E+09	1.2E+09	7.6E+07	2.5	2.6	2.5	2.48	0.058	2.06E-10	1.4E-11
91	0.0410	2.7E+08	3.3E+08	3.2E+08	3.1E+08	3.2E+07	1.7	1.7	1.9	1.73	0.104	5.61E-10	6.7E-11
79	0.1024	7.30E+08	6.20E+08	6.70E+08	6.7E+08	5.5E+07	2.6	3.1	2.2	2.62	0.425	3.89E-10	7.1E-11
75	0.1249	7.70E+08	7.70E+08	8.60E+08	8.0E+08	5.2E+07	1.8	2.7	3.7	2.73	0.950	3.42E-10	1.2E-10
66	0.1805	1.84E+09	1.72E+09	1.23E+09	1.6E+09	3.2E+08	6.8	7.0	9.7	7.81	1.644	4.89E-10	1.4E-10
62	0.2076	1.78E+09	1.82E+09	1.86E+09	1.8E+09	4.0E+07	6.4	6.8	6.7	6.61	0.190	3.63E-10	1.3E-11

The following sets of data were obtained by acidifying the samples with nitric acid, diluting, and analyzing on the AA. Data shown has been corrected for dilution and for machine drift during analysis. Control flasks are indicated by "C", and dosed flasks by "F." Potassium concentration is reported in mg/L.

Potassium efflux from transmittance = 61, 6-20-03, Book 1, Page 99

Time	C1	C2	C3	F1	F2	F3	av control	av dose
0	0.15	0.05	0.15	0.15	0.40	--	0.12	0.28
5	0.15	0.30	0.35	1.85	1.60	1.60	0.27	1.68
15	0.10	0.25	0.20	2.80	2.55	2.70	0.18	2.68
30	0.25	0.10	0.10	3.40	3.00	3.00	0.15	3.13
60	0.35	0.20	0.15	3.30	3.15	3.50	0.23	3.32

Potassium efflux from transmittance = 72, 7-18-03, Book 2, Page 9

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	2.30	2.35	2.65	2.90	3.10	2.70	2.43	2.90	0.189	0.200
5	1.75	1.85	1.60	6.05	5.70	7.25	1.73	6.33	0.126	0.813
15	2.15	1.85	1.65	7.70	8.00	8.80	1.88	8.17	0.252	0.569
30	1.70	1.35	1.70	8.75	8.60	7.95	1.58	8.43	0.202	0.425
60	1.55	1.60	1.60	8.40	9.55	8.40	1.58	8.78	0.029	0.664

Potassium efflux from transmittance = 60, 7-19-03, Book 2, Page 10

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	1.40	2.05	1.15	1.60	1.70	1.80	1.53	1.70	0.465	0.100
15	3.00	1.80	2.85	7.80	7.75	8.65	2.55	8.07	0.654	0.506
30	2.30	2.25	2.05	8.10	7.70	7.85	2.20	7.88	0.132	0.202

Initial 1.15

Potassium efflux from transmittance = 50, 7-24-04, Book 2, Page 11

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	0.05	0.05	0.20	0.55	0.15	0.55	0.10	0.42	0.087	0.231
20	0.10	0.15	0.10	1.50	1.30	1.50	0.12	1.43	0.029	0.115
40	0.05	0.05	0.10	2.15	2.40	2.20	0.07	2.25	0.029	0.132
60	0.05	0.05	0.05	2.75	2.45	2.25	0.05	2.48	0.000	0.252

Initial 3.15

Potassium efflux from transmittance = 55, 7-29-03, Book 2, Page 14

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	0.20	0.30	0.15	0.25	0.20	0.20	0.22	0.22	0.076	0.029
20	0.25	0.30	0.15	1.60	1.40	1.55	0.23	1.52	0.076	0.104
40	0.20	0.30	0.20	2.25	2.45	2.25	0.23	2.32	0.058	0.115
60	0.20	0.15	0.15	2.70	2.75	2.65	0.17	2.70	0.029	0.050

Initial 3.15

Potassium efflux from transmittance = 91, 7-31-03, Book 2, Page 15

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	2.10	1.85	2.05	2.10	2.00	1.90	2.00	2.00	0.132	0.100
20	1.75	2.00	1.65	2.10	1.95	2.15	1.80	2.07	0.180	0.104
40	1.35	1.50	1.40	2.20	2.75	2.50	1.42	2.48	0.076	0.275
60	1.65	0.80	0.65	2.30	2.35	2.50	1.03	2.38	0.539	0.104

Initial 3.15

Potassium efflux from transmittance = 79, 11-23-03, Book 2, Page 53

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	2.30	0.60	3.25	1.55	0.95	1.25	2.05	1.25	1.343	0.300
5	0.90	0.95	1.40	1.55	1.95	2.35	1.08	1.95	0.275	0.400
15	0.65	0.80	0.75	3.45	3.05	3.20	0.73	3.23	0.076	0.202
30	0.75	0.65	0.70	3.25	4.00	3.85	0.70	3.70	0.050	0.397

Potassium efflux from transmittance = 75, 11-23-03, Book 2, Page 54

Time	C1	C2	C3	F1	F2	F3	av control	av dose	std dev cont	std dev dose
0	0.95	0.70	1.35	1.80	1.20	0.85	1.00	1.28	0.328	0.480
5	3.80	0.95	2.00	2.95	2.95	1.95	2.25	2.62	1.441	0.577
15	1.80	0.85	0.45	4.30	3.55	3.65	1.03	3.83	0.693	0.407
30	2.20	1.10	1.05	3.60	3.90	4.55	1.45	4.02	0.650	0.486

Potassium efflux from transmittance = 66, 1-2-04, Book 2, Page 59

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	1.90	1.95	1.29	1.80	2.54	1.51	1.71	1.95	0.369	0.530
20	1.34	1.90	1.59	5.08	5.62	5.18	1.61	5.30	0.281	0.287
40	1.80	2.77	2.72	8.17	8.71	9.01	2.43	8.63	0.546	0.423
60	7.00	2.10	3.13	8.56	9.50	11.21	4.08	9.76	2.584	1.343

Initial 2.36

Potassium efflux from transmittance = 62, 1-17-04, Book 2, Page 63

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.51	0.85	1.43	0.89	0.95	0.55	0.93	0.80	0.466	0.214
20	0.58	1.89	1.58	1.79	3.72	3.92	1.35	3.14	0.684	1.178
40	3.47	0.55	0.62	5.35	4.82	6.42	1.55	5.53	1.666	0.815
60	2.01	0.93	1.70	7.29	7.72	8.82	1.55	7.94	0.555	0.790

Initial 2.15

## B.2.2 Planktonic efflux from *E. coli*

Summary table of efflux data for planktonic *E. coli*

Trans	Abs	Cell Counts			Av cell count	StdDev cell count	delta K			av delta K	Std Dev delta K	delta K / cell	Error on Efflux
56	0.252	1.0E+09	1.1E+09	1.1E+09	1.1E+09	4.0E+07	4.6	4.3	4.4	4.38	0.153	4.16E-10	2.16E-11
56	0.252	1.9E+09	2.1E+09	2.1E+09	2.1E+09	9.6E+07	3.6	4.1	3.9	3.83	0.275	1.870E-10	1.61E-11
78	0.108	1.1E+09	1.3E+09	1.0E+09	1.1E+09	1.4E+08	4.9	5.0	5.5	5.10	0.304	4.513E-10	6.27E-11
70	0.155	9.1E+08	8.2E+08	8.9E+08	8.7E+08	4.7E+07	5.7	5.8	6.6	6.00	0.477	6.870E-10	6.61E-11
55	0.260	1.68E+09	1.44E+09	1.43E+09	1.5E+09	1.4E+08	9.4	9.8	10.1	9.75	0.377	6.429E-10	6.50E-11
76	0.119	4.20E+08	4.40E+08	5.00E+08	4.5E+08	4.2E+07	2.1	2.2	2.3	2.17	0.092	4.787E-10	4.84E-11
86	0.066	1.10E+09	8.00E+08	1.05E+09	9.8E+08	1.6E+08	5.8	6.1	5.7	5.84	0.201	5.936E-10	9.91E-11
89	0.051	1.28E+09	1.32E+09	1.42E+09	1.3E+09	7.2E+07	6.2	6.5	9.7	7.48	1.970	5.581E-10	1.50E-10

The following sets of data were obtained by acidifying the samples with nitric acid, diluting, and analyzing on the AA. Data shown has been corrected for dilution and for machine drift during analysis. Control flasks are indicated by "C", and dosed flasks by "F." Potassium concentration is reported in mg/L.

Potassium efflux from transmittance = 56, 8-15-03, Book 2, Page 17

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.40	0.30	0.25	0.25	0.35	0.30	0.32	0.30	0.466	0.214
20	0.35	0.10	0.40	3.40	3.20	2.80	0.28	3.13	0.684	1.178
40	0.20	0.35	0.25	4.25	4.20	4.55	0.27	4.33	1.666	0.815
60	0.25	0.30	0.20	4.70	4.60	4.90	0.25	4.73	0.555	0.79

Initial 0.35

Potassium efflux from transmittance = 56, 8-20-03, Book 2, Page 18

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.35	0.30	0.25	0.45	0.35	0.75	0.30	0.52	0.466	0.214
20	0.50	0.25	0.30	1.35	1.45	1.80	0.35	1.53	0.684	1.178
40	0.40	0.45	0.45	3.70	3.50	3.80	0.43	3.67	1.666	0.815
60	0.40	0.40	0.25	4.25	4.50	3.95	0.35	4.23	0.555	0.79

Initial 0.40

Potassium efflux from transmittance = 78, 8-22-03, Book 2, Page 20

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.20	0.15	0.15	0.40	2.95	1.70	0.17	1.68	0.466	0.214
20	0.30	0.25	0.15	4.75	4.25	4.55	0.23	4.52	0.684	1.178
40	0.30	0.40	0.30	5.05	5.10	4.65	0.33	4.93	1.666	0.815
60	0.20	0.30	0.40	4.55	4.70	5.60	0.30	4.95	0.555	0.79

Initial 0.15

Potassium efflux from transmittance = 70, 8-23-03, Book 2, Page 21

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.55	0.55	0.50	0.45	1.25	0.70	0.53	0.80	0.466	0.214
20	0.60	0.80	0.45	4.75	5.55	5.10	0.62	5.13	0.684	1.178
40	0.50	0.60	0.30	6.05	6.65	7.45	0.47	6.72	1.666	0.815
60	0.65	0.45	0.35	6.60	6.40	9.25	0.48	7.42	0.555	0.79

Initial 0.90

Potassium efflux from transmittance = 55, 9-25-03, Book 2, Page 33

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	1.10	1.90	0.70	0.85	1.60	1.85	1.23	1.43	0.466	0.214
20	0.35	0.90	0.75	4.50	4.55	4.75	0.67	4.60	0.684	1.178
40	0.85	1.15	1.25	10.15	8.60	8.40	1.08	9.05	1.666	0.815
60	0.65	0.55	0.75	10.10	10.55	10.85	0.65	10.50	0.555	0.79

Potassium efflux from transmittance = 76, 12-10-03, Book 2, Page 56

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.17	0.47	1.16	0.27	0.74	0.79	0.60	0.60	0.466	0.214
20	0.52	0.93	1.22	1.43	1.55	1.55	0.89	1.51	0.684	1.178
40	0.76	0.64	0.35	2.42	2.07	2.36	0.58	2.29	1.666	0.815
60	1.28	0.93	1.10	3.18	2.48	2.60	1.10	2.75	0.555	0.79

Init 0.33

Potassium efflux from transmittance = 86, 12-12-03, Book 2, Page 57

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	3.24	0.50	0.68	0.76	0.37	0.65	1.47	0.59	0.466	0.214
20	3.58	1.38	1.96	4.48	4.15	4.42	2.31	4.35	0.684	1.178
40	1.61	1.08	1.61	5.04	5.92	5.31	1.43	5.42	1.666	0.815
60	1.03	0.85	0.91	6.09	6.37	5.98	0.93	6.15	0.555	0.79

Initial 0.70

Potassium efflux from transmittance = 89, 1-6-04, Book 2, Page 60

Time	C1	C2	C3	F1	F2	F3	av control	av dose	st dev cont	st dev dose
0	0.77	0.77	0.82	0.97	0.61	0.72	0.79	0.77	0.466	0.214
20	0.68	1.07	1.75	5.36	5.36	4.95	1.17	5.22	0.684	1.178
40	0.73	1.02	0.77	6.23	6.58	6.33	0.84	6.38	1.666	0.815
60	0.73	0.87	0.68	7.14	7.55	10.46	0.76	8.39	0.555	0.79

Initial 1.04

### B.3 Data for efflux from alginate-immobilized *P. aeruginosa*

The following data were obtained by acidifying the samples with nitric acid, diluting, and analyzing on the AA. Data shown has been corrected for dilution and for machine drift during analysis. Control flasks are indicated by "C", and dosed flasks by "F." Potassium concentration is reported in mg/L. Days after immobilization are given (e.g., day 0 = immediately after immobilization and day 1 = 24 hours after immobilization). Cell counts were performed by serial dilutions and plating. Volumes shown with cell counts indicate total volume of culture after resuspension. Total cells = average cell count x resuspension volume. This total was divided equally into six flasks to give cells per flask.

Efflux 2, Day 1

2-4-04, Book 2, Page 69

Presented in Chapter 3, Table 1 and Figure 6

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.56	0.62	0.16	1.16	1.72	1.61	0.45	1.50	0.251	0.296
20	0.17	1.29	0.88	1.50	2.22	2.34	0.78	2.02	0.569	0.455
40	0.51	0.34	0.77	1.33	2.39	3.29	0.54	2.34	0.219	0.979
60	0.51	1.24	0.83	2.73	2.22	3.84	0.86	2.93	0.366	0.829
120	0.84	0.62	0.10	2.39	1.83	3.45	0.52	2.56	0.380	0.823

Cell Counts      2.46E+10   2.37E+10   2.87E+10   cells per mL  
Average            2.57E+10   cells per mL                      38 ml total  
Total cells        9.75E+11   total cells

Cells per flask    1.63E+11

Efflux 3, Day 5

1-27-04, Book 2, Page 67

Presented in Chapter 3, Figure 7

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.63	0.43	1.34	0.66	0.24	2.19	0.80	1.03	0.4764	1.0258
20	0.12	1.70	0.33	0.62	0.24	2.04	0.72	0.97	0.8602	0.9497
40	0.84	0.12	2.25	0.62	1.99	2.79	1.07	1.80	1.0828	1.1001
60	0.22	0.17	0.37	2.01	0.84	2.19	0.26	1.68	0.1048	0.7328
120	2.26	0.43	1.14	2.30	1.49	3.94	1.28	2.58	0.9258	1.2485

Data not included in thesis:

1-26-04, Book 2, Page 66

Efflux 1, Day 0

Time	C1	C2	C3	F1	F2	F3	PD	Av Cont	Av Dose	st dev cont	st dev dose
0	4.55	1.85	5.69	2.11	1.09	1.83	1.16	4.03	1.68	1.9730	0.5289
20	2.39	3.41	8.80	3.60	3.52	1.63	2.85	4.87	2.92	3.4451	1.1154
40	2.19	5.10	2.52	2.86	2.44	2.03	4.06	3.27	2.44	1.5913	0.4104
60	3.41	4.42	4.14	3.87	1.90	2.17	3.72	3.99	2.65	0.5234	1.0676
120	2.32	1.85	2.25	3.80	4.80	3.32	3.79	2.14	3.97	0.2537	0.7583

Cell Counts      2.12E+10   2.41E+10   2.01E+10   cells per mL  
Average            2.18E+10   cells per mL                      18.8 ml total  
Total cells        4.10E+11   total cells

Cells per flask    6.83E+10



### Efflux 2, Day 4

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.91	0.96	0.55	0.08	0.79	0.48	0.81	0.45	0.2220	0.3526
20	0.50	0.65	0.08	0.92	0.89	1.04	0.41	0.95	0.2951	0.0815
40	1.57	0.75	0.19	2.01	0.73	0.89	0.84	1.21	0.6959	0.6961
60	0.40	0.55	0.66	0.86	0.99	0.79	0.53	0.88	0.1297	0.1030
120	0.50	0.70	0.97	1.91	0.99	4.76	0.72	2.55	0.2348	1.9694

1-27-04, Book 2, Page 67

### Efflux 1, Day 0

Time	C1	C2	C3	F1	F2	F3	PD	Av Cont	Av Dose	st dev cont	st dev dose
0	5.80	5.44	5.45	3.85	4.85	5.32	1.85	5.56	4.68	0.2027	0.7499
20	7.30	4.37	4.19	7.65	5.45	7.59	2.59	5.28	6.90	1.7460	1.2511
40	8.51	3.87	3.65	7.92	5.39	6.52	4.45	5.34	6.61	2.7451	1.2685
60	6.87	5.30	3.72	5.65	6.05	7.65	1.39	5.29	6.45	1.5748	1.0587
120	10.01	5.73	5.79	7.85	9.99	8.59	1.59	7.17	8.81	2.4572	1.0843

Cell Counts 9.40E+10 1.07E+11 8.90E+10 cells per mL  
 Average 9.67E+10 cells per mL 38 ml total  
 Total cells 3.67E+12 total cells

Cells per flask 6.12E+11

### Efflux 2, Day 3

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.84	0.43	1.01	0.11	0.22	1.91	0.76	0.75	0.2987	1.0066
20	1.19	0.07	0.16	1.11	1.35	2.57	0.47	1.68	0.6239	0.7842
40	0.28	0.33	0.46	1.56	1.45	3.08	0.35	2.03	0.0955	0.9121
60	0.38	0.07	0.31	1.96	1.30	1.86	0.25	1.70	0.1609	0.3576
120	0.38	0.22	1.01	1.81	1.30	2.52	0.54	1.88	0.4167	0.6148

2-4-04, Book 2, Page 69

### Efflux 1, Day 0

Time	C1	C2	C3	F1	F2	F3	PD	Av Cont	Av Dose	st dev cont	st dev dose
0	0.13	0.44	1.45	0.57	1.12	2.81	1.25	0.67	1.50	0.6394	1.168
20	0.18	1.49	0.79	1.18	3.71	2.92	13.25	0.82	2.60	0.658	1.295
40	1.34	0.07	2.34	2.18	6.57	3.93	25.5	1.25	4.23	1.138	2.213
60	2.60	0.39	1.62	3.79	5.39	3.15	12.75	1.54	4.11	1.108	1.158
120	0.65	0.86	0.23	2.84	3.43	3.71	14.25	0.58	3.33	0.321	0.441

Cell Counts 2.46E+10 2.37E+10 2.87E+10 cells per mL  
 Average 2.57E+10 cells per mL 15 ml total  
 Total cells 3.85E+11 total cells

Cells per flask 6.42E+10

### Efflux 2, Day 2

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.56	0.62	0.16	1.16	1.72	1.61	0.45	1.50	0.251	0.296
20	0.17	1.29	0.88	1.50	2.22	2.34	0.78	2.02	0.569	0.455
40	0.51	0.34	0.77	1.33	2.39	3.29	0.54	2.34	0.219	0.979
60	0.51	1.24	0.83	2.73	2.22	3.84	0.86	2.93	0.366	0.829
120	0.84	0.62	0.10	2.39	1.83	3.45	0.52	2.56	0.380	0.823

### Efflux 3, Day 5

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.49	0.38	1.33	1.16	1.05	0.33	0.73	0.85	0.519	0.455
20	1.27	0.72	0.88	1.39	1.67	1.89	0.96	1.65	0.287	0.252
40	1.27	0.21	0.66	0.83	2.84	1.22	0.72	1.63	0.533	1.066
60	0.72	0.16	0.55	1.44	5.19	2.06	0.47	2.90	0.287	2.007
120	2.39	0.94	--	1.22	4.24	1.67	1.67	2.37	--	1.628

#### B.4 Data for thermally reversible gel-immobilized *P. aeruginosa*

The following data were obtained by acidifying the samples with nitric acid, diluting, and analyzing on the AA. Data shown has been corrected for dilution and for machine drift during analysis. Control flasks are indicated by "C", and dosed flasks by "F." Potassium concentration is reported in mg/L. Days after immobilization are given (e.g., day 0 = immediately after immobilization and day 1 = 24 hours after immobilization). Cell counts were performed by serial dilutions and plating. Volumes shown with cell counts indicate total volume of culture after resuspension. Total cells = average cell count x resuspension volume. This total was divided equally into six flasks to give cells per flask.

Efflux 1, Day One, 4-19-04, Book 2, Page 86

Presented in Chapter 3, Table 1 and Figure 8

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	2.27	2.80	2.28	2.45	3.50	2.50	2.45	2.81	0.3026	0.5909
0	2.21	2.16	2.34	2.95	2.55	3.22	2.24	2.91	0.0914	0.3355
20	2.05	2.59	2.06	9.34	5.27	5.83	2.23	6.81	0.3052	2.2044
40	1.74	2.53	1.73	5.67	3.88	4.66	2.00	4.74	0.4628	0.8964
60	1.36	1.52	1.62	5.12	4.05	4.94	1.50	4.70	0.1282	0.5711
80	0.94	3.01	1.34	5.73	4.38	4.94	1.76	5.02	1.1003	0.6750
100	0.99	1.10	2.17	5.01	5.77	4.88	1.42	5.22	0.6536	0.4821
120	0.78	2.53	0.84	5.95	4.44	5.11	1.38	5.17	0.9963	0.7567

Cell Counts      3.19E+09   3.54E+09   3.42E+09   cells per mL  
Average          3.38E+09   cells per mL                      6.0 ml total  
Total cells        2.03E+10   total cells

Cells per flask    3.38E+09

5-24-04, Book 2, Page 92

Presented in Chapter 3, Figure 9

Efflux 1, Day 3

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	6.83	7.31	6.66	10.51	6.04	5.16	6.93	7.23	0.3331	2.8708
0	7.67	7.15	7.10	11.55	9.95	7.36	7.31	9.62	0.3177	2.1163
20	5.31	5.99	6.06	11.94	9.62	8.49	5.78	10.02	0.4163	1.7581
40	4.15	6.31	6.11	9.19	9.57	8.33	5.52	9.03	1.1943	0.6368
60	4.46	6.06	5.29	8.21	9.46	8.43	5.27	8.70	0.7978	0.6639
80	4.46	6.33	5.18	7.88	9.29	8.86	5.33	8.68	0.9435	0.7227
100	2.88	5.40	4.85	8.43	9.13	8.06	4.38	8.54	1.3222	0.5463
120	2.25	5.12	4.30	8.43	9.46	8.76	3.89	8.88	1.4786	0.5249

Cell Counts      4.60E+10   4.00E+10   4.30E+10   cells per mL  
Average          4.30E+10   cells per mL

16 ml total divided into 8 batches  
Cells per flask    8.60E+10

Data not included in thesis:

3-31-04, Book 2, Page 82

### Efflux 1, Day 1

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
0	0.62	1.19	1.59	2.37	2.20	1.98	1.13	2.18	0.4905	0.1945
20	0.88	0.46	4.87	3.42	2.63	3.77	2.07	3.28	2.4348	0.5847
40	0.30	0.46	1.87	3.31	2.85	2.90	0.88	3.02	0.8628	0.2530
60	0.20	0.30	1.37	3.31	3.07	2.96	0.62	3.11	0.6478	0.1815
80	0.20	0.20	1.48	3.37	3.18	3.67	0.63	3.40	0.7400	0.2464
100	0.41	0.25	0.76	3.81	3.34	3.56	0.47	3.57	0.2598	0.2372
120	0.51	0.25	0.48	4.59	3.29	3.56	0.41	3.81	0.1423	0.6890

Cell Counts 6.90E+10 5.30E+10 6.10E+10 cells per mL

Average 6.10E+10 cells per mL

Total cells 2.32E+12 total cells

11.5 ml total, 8 batches

Cells per flask 3.33E+12

### Efflux 2, Day 3

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	0.08	0.55	0.12	0.35	0.17	0.23	0.25	0.25	0.2613	0.0907
0	0.08	0.97	0.07	1.13	0.85	1.02	0.37	1.00	0.5186	0.1439
20	0.40	0.97	0.57	1.30	1.02	1.64	0.65	1.32	0.2952	0.3111
40	0.34	1.71	0.40	1.02	1.86	1.02	0.82	1.30	0.7694	0.4880
60	0.08	0.55	0.07	1.58	1.19	1.13	0.23	1.30	0.2768	0.2469
80	0.13	0.97	0.12	1.13	1.58	1.24	0.41	1.32	0.4872	0.2338
100	0.19	0.61	0.63	1.30	1.30	1.58	0.47	1.39	0.2484	0.1623
120	0.19	0.08	0.29	1.36	1.47	1.41	0.19	1.41	0.1043	0.0553

### Efflux 3, Day 7

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	0.34	0.51	0.94	0.33	0.36	0.13	0.60	0.28	0.3095	0.1239
0	1.53	0.45	1.66	0.22	1.39	1.16	1.21	0.93	0.6612	0.6204
20	2.03	1.19	0.55	0.55	0.82	0.53	1.26	0.64	0.7433	0.1600
40	0.40	0.28	0.28	2.60	1.96	2.42	0.32	2.33	0.0671	0.3271
60	0.34	0.45	1.27	0.61	0.42	0.42	0.63	0.48	0.5085	0.1084
80	0.56	0.40	0.77	0.61	0.76	0.65	0.58	0.67	0.1893	0.0804
100	1.36	0.40	0.17	0.50	0.36	0.53	0.64	0.46	0.6314	0.0902
120	0.23	0.11	0.06	0.50	0.65	0.65	0.13	0.60	0.0868	0.0874

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### Efflux 2, Day 3

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	5.43	5.64	3.36	3.30	8.43	8.93	4.81	6.88	1.2600	3.1182
0	8.14	5.47	3.26	3.39	8.14	8.71	5.62	6.75	2.4401	2.9237
20	6.64	5.51	2.80	3.92	8.64	10.64	4.98	7.74	1.9750	3.4521
40	6.05	5.26	2.92	4.11	8.71	8.57	4.75	7.13	1.6293	2.6195
60	5.22	5.22	2.83	4.08	8.57	12.00	4.42	8.22	1.3820	3.9738
80	4.60	7.39	2.58	5.23	9.43	9.93	4.85	8.20	2.4155	2.5791
100	4.18	4.76	2.64	4.45	8.71	15.14	3.86	9.44	1.0968	5.3822
120	4.60	4.30	2.42	4.20	8.79	9.14	3.77	7.38	1.1806	2.7557

# Efflux 3, Day 5

Time	C1	C2	C3	F1	F2	F3	Av Cont	Av Dose	st dev cont	st dev dose
-5	5.93	7.50	4.08	5.15	8.33	9.63	5.84	7.70	1.7111	2.3032
0	6.64	7.21	5.44	5.72	8.83	9.73	6.43	8.09	0.9065	2.1016
20	6.93	7.79	3.58	7.08	10.53	12.23	6.10	9.95	2.2216	2.6233
40	5.29	7.71	4.08	7.30	10.53	11.73	5.69	9.85	1.8505	2.2936
60	5.14	7.71	3.08	6.87	10.53	13.23	5.31	10.21	2.3211	3.1935
80	5.21	5.71	2.87	7.37	10.33	13.23	4.60	10.31	1.5202	2.9315
100	4.50	5.29	2.94	6.94	11.13	11.33	4.24	9.80	1.1947	2.4797
120	3.29	4.21	1.37	6.22	10.53	11.53	2.96	9.43	1.4520	2.8193