

**IN-PLANT TESTING OF THE HYDROFLOAT
SEPARATOR FOR COARSE PHOSPHATE RECOVERY**

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by

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ABSTRACT

The HydroFloat technology was specifically developed to upgrade phosphate sands that are too coarse to be efficiently recovered by conventional flotation methods. In this novel process, classified feed is suspended in a fluidized-bed and then aerated. The reagentized phosphate particles become buoyant and report to the product launder after encountering and attaching to the rising air bubbles. Simultaneously, the hydrophilic particles are rejected as a high solids content (65-70%) underflow. The fluidized bed acts as a “resistant” layer through which no bubble/particle aggregates can penetrate. As a result, the HydroFloat also acts as a density separator that is capable of treating much coarser particles as compared to traditional flotation processes. In addition, the high solids content of the teeter bed promotes bubble-particle attachment and reduces the cell volume required to achieve a given capacity. To fully evaluate the potential advantages of the HydroFloat technology, a 5-tph test circuit was installed and evaluated in an industrial phosphate beneficiation plant. Feed to the test circuit was continuously classified, conditioned and upgraded using the HydroFloat technology. The test results indicated that the HydroFloat could produce a high-grade phosphate product in a single stage of separation. Product quality ranged between 70-72% BPL (bone phosphate of lime = $2.185 \times \%P_2O_5$) and 5-10% insols (acid insoluble solids). BPL recoveries exceeded 98% at feed rates greater than 2.0 tph per ft² of separator cross-sectional area. These results were superior to traditional column flotation, which recovered less than 90% of the valuable product at a capacity of less than 1 tph per ft².

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EXECUTIVE SUMMARY

The Eriez HydroFloat technology was specifically developed to upgrade phosphate sands that are too coarse to be efficiently recovered by existing flotation methods. In this novel process, classified feed is suspended in a fluidized-bed and aerated using an external sparging system. Air bubbles selectively attach to particles that have been made hydrophobic through the addition of a flotation collector. The teetering effect of the fluidized-bed forces the low-density bubble-particle aggregates into the overflow, while hydrophilic particles are rejected as a high solids content underflow. Since the HydroFloat is essentially a density separator, the process can treat much coarser particles than traditional flotation systems. In addition, the high solids content of the teeter-bed promotes bubble-particle attachment and reduces the cell volume required to achieve a given capacity.

Initial laboratory- and pilot-scale test data indicated that the HydroFloat cell is capable of achieving superior recoveries of BPL (bone phosphate of lime) as compared to traditional mechanical and column flotation cells. This was particularly evident with particle sizes greater than 35 mesh. Recovery of the coarse, high-grade particles led to greatly improved product quality. These coarse phosphate particles are often lost when using traditional flotation processes due to detachment and buoyancy limitations.

In any flotation process, recovery is improved when particle retention time is lengthened, mixing is reduced, and the probability of bubble-particle collision is increased. The HydroFloat cell has the advantage of simultaneously improving each of these factors. The counter-current flow of particles settling in a hindered state against an upward rising current of water increases particle retention time. The presence of the teeter

bed reduces turbulence (i.e., mixing) and increases the plug-flow characteristics of the separator. The high solids content of the teeter-bed greatly also increases the probability of bubble-particle contacting. In addition, the HydroFloat utilizes less energy per ton of feed since no mechanical agitator is required. The increase in unit capacity also results in reduced capital and installation costs.

To demonstrate the benefits of the HydroFloat separator, a pilot-scale HydroFloat circuit was installed and evaluated at an industrial phosphate plant. The primary objective of the pilot-scale test program was to quantify the effects of key design and operating parameters on the performance of the HydroFloat separator. Tests were also conducted to evaluate the effectiveness of an alternative rotary drum system for conditioning the coarse feed stream.

The pilot-scale test circuit was installed at PCS Phosphate (Swift Creek Plant, White Springs, Florida). The circuit was designed to handle a dry solids feed rate of 4-6 tph and included all unit operations for classification, conditioning, and flotation. Classification was carried out using an Eriez CrossFlow hindered-bed separator. Feed preparation was accomplished using either a four-cell bank of stirred-tanks or a rotating drum conditioner.

The test data obtained during the course of this project showed that the rotary conditioner performed significantly better than the stirred tank conditioner. In fact, the overall BPL recovery increased more than 20% when using the rotary conditioner. The poorer separation results obtained with the stirred-tank conditioner are attributed to the creation of excess fines. The high-energy input per unit volume that was required to maintain the coarse sand in suspension resulted in unwanted attrition of the phosphate

ore. Consequently, the required reagent addition rate increased and selectivity decreased when using the stirred-tank conditioning cells. This increased generation of ultrafine particles and decrease in selectivity was verified through comparative testing of the products from each conditioning system.

The HydroFloat separator was able to achieve excellent results when operated with the rotary drum conditioner. The test results (including long-term testing) indicate that the HydroFloat unit is capable of achieving BPL recoveries greater than 98% with a product BPL and insols grade of 71% and 6%, respectively. These results were achieved at dry solids feed rates surpassing 2 tph/ft² and reagent addition rates between 0.60 and 0.75 lbs/ton of feed solids. These impressive results demonstrate that the HydroFloat separator is a practical and technologically sound solution to the long-standing problems encountered when processing coarse phosphate ore.

INTRODUCTION

BACKGROUND

Hindered-bed separators are commonly used in the minerals industry as gravity concentration devices. These units can be used for mineral concentration if the particle size range and density difference between mineral types are within acceptable limits. However, these separators often suffer from misplacement of low-density, coarse particles to the high-density underflow. This shortcoming is due to the accumulation of coarse, low-density particles at the top of the teeter-bed. These particles are too light to penetrate the teeter-bed, but are too heavy to be carried by the rising water into the overflow launder. Ultimately, these particles are forced to the underflow by mass action as more particles accumulate at the top of the teeter-bed. This inherent inefficiency can be partially corrected by increasing the teeter-water velocity to convey the coarse, low-density solids to the overflow. Unfortunately, the higher water rates will cause fine, high-density solids to be misplaced to the overflow, thereby reducing the separation efficiency.

To overcome the shortcomings of traditional hindered-bed separators, a novel device known as the HydroFloat was developed. As shown in Figure 1, the HydroFloat consists of a tank subdivided into an upper separation chamber and a lower dewatering cone. The device operates much like a traditional hindered-bed separator with the feed settling against an upward current of fluidization water. The fluidization (teeter) water is supplied through a network of pipes that extend across the bottom of the separator. However, in the case of the HydroFloat separator, the teeter-bed is continuously aerated by injecting compressed air and a small amount of frothing agent into the fluidization water. The air bubbles become attached to the hydrophobic particles within the teeter-

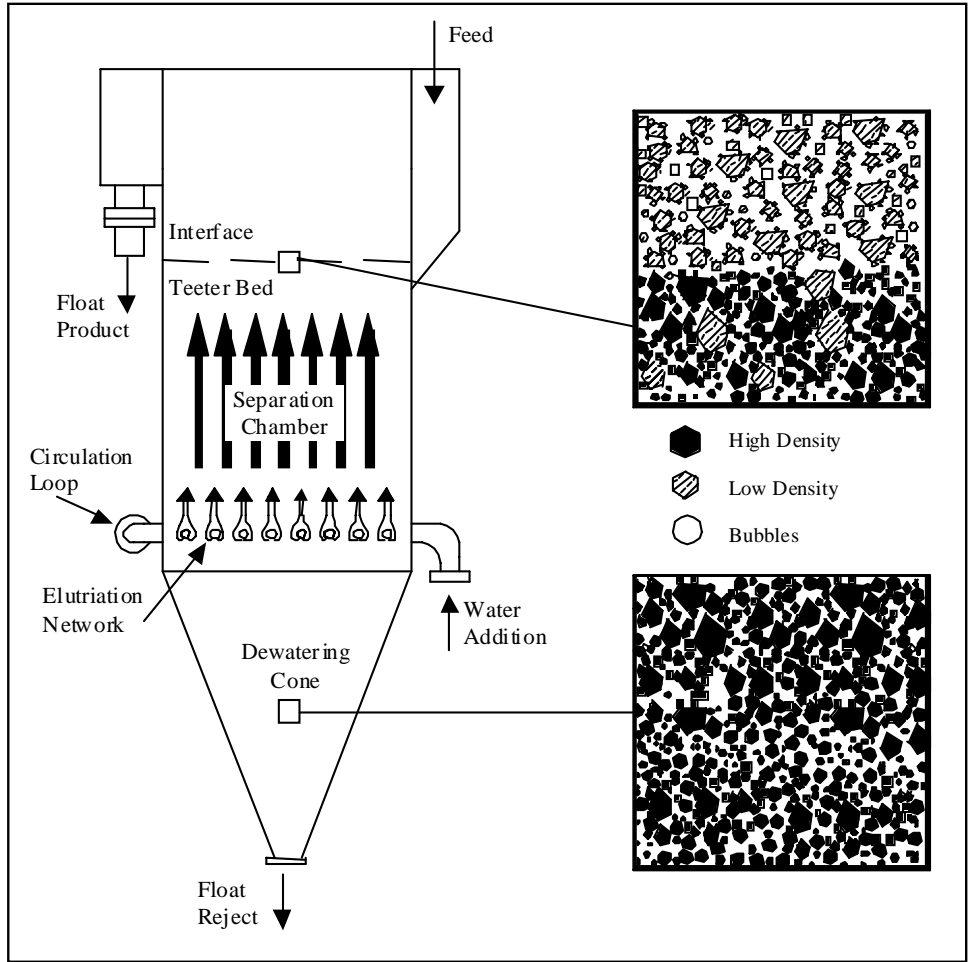


Figure 1. Conceptual Illustration of the HydroFloat Separator.

bed, thereby reducing their effective density. The lighter bubble-particle aggregates rise to the top of the denser teeter-bed and overflow the top of the separation chamber.

Unlike flotation, the bubble-particle aggregates do not need to have sufficient buoyancy to rise to the top of the cell. Instead, the teetering effect of the hindered-bed forces the low-density agglomerates to overflow into the product launder. Hydrophilic particles that do not attach to the air bubbles continue to move down through the teeter-bed and eventually settle into the dewatering cone. These particles are discharged as a high solids stream (e.g., 75% solids) through a control valve at the bottom of the

separator. The valve is actuated in response to a control signal provided by a pressure transducer mounted on the side of the separation chamber. This configuration allows a constant effective density to be maintained within the teeter-bed.

The HydroFloat can be theoretically applied to any system where differences in apparent density can be created by the selective attachment of air bubbles. Although not a requirement, the preferred mode of operation would be to make the low-density component hydrophobic so that the greatest difference in specific gravity is achieved. Compared to traditional flotation processes, the HydroFloat offers important advantages for treating coarser material including enhanced bubble-particle contacting, increased residence time, lower axial mixing/cell turbulence, and reduced air consumption.

LITERATURE REVIEW

The improved recovery of coarse particles has long been a goal in the minerals processing industry. Several studies have been conducted in an effort to overcome the inefficiencies associated with existing processes and equipment. The studies range in scope from fundamental investigations of bubble-particle interactions to the development of novel equipment. Advancements in chemistry and conditioning practices have also been employed at a number of industrial installations.

Froth Flotation Technology

Research on the relationship between particle size and floatability began as early as 1931 with work conducted by Gaudin, *et al.* (1931) showing that coarse and extremely fine particles are more difficult to recover as compared to intermediate size particles. Twenty years after this original work, Morris (1952) arrived at the same conclusion that

particle size is one of the most important factors in the recovery of ores by flotation. Generally, recovery is low for the finest particles ($d_p < 10 \mu\text{m}$) and is at a maximum for intermediate size particles. A sharp decrease in recovery occurs as the particle diameter continues to increase. This reduction in recovery on the fine and coarse ends is indicative of a reduction in the flotation rate of the particles (Jameson *et al.*, 1977). It can be seen that the efficiency of the froth flotation process deteriorates rapidly when operating in the extremely fine or coarse particle size ranges, i.e., below $10 \mu\text{m}$ and above $250 \mu\text{m}$. These findings suggest that current conventional flotation practices are optimal only for the recovery of particles in the size range of about 65 to 100 mesh.

According to Soto and Barbery (1991), conventional flotation cells operate with two contradictory goals. A conventional cell has to provide enough agitation to maintain particles in suspension, shear and disperse air bubbles, and promote bubble-particle collision. However, for optimal recovery, a quiescent system is required to reduce detachment and minimize entrainment. As a result, coarse particle flotation is more difficult since increased agitation is required to maintain particles in suspension. Furthermore, coarse particles are more likely to detach under turbulent conditions. To compensate for the lack of recovery, some installations are using relatively small flotation devices operated at low feed rates (Lawver *et al.*, 1984).

The stability of bubble-particle aggregates was also examined in theoretical and experimental studies conducted by Schulze (1977). This work showed that the upper particle size limit for flotation is dictated by the resultant of forces acting on a bubble and particle aggregate. These forces include gravity, buoyancy, hydrostatic pressure, capillary compression, tension, and shear forces induced by the system. According to Schulze,

particles with a diameter of several millimeters should float (in the absence of turbulence) provided the contact angle is greater than 50°. Later work by Schulze (1984) shows that turbulent conditions, similar to those found in mechanical flotation cells, drastically reduce the upper size limit of floatable material. Several other investigations support these findings (Bensley and Nicol, 1985; Soto, 1988). In fact, it has been demonstrated that turbulent conditions can reduce the maximum floatable size to one tenth of that found in non-turbulent conditions (Ives, 1984; Ahmed and Jameson, 1989).

Another theory is that small particles have a higher rate of flotation and, therefore, crowd out coarse particles from the surfaces of the air bubbles. Soto and Barbery (1991) disagree with this assessment, speculating that the poor recovery of coarse material is strictly a result of detachment. They further advocate the use of separate circuits for fine and coarse processing in an effort to optimize the conditions necessary for increased recovery.

Several new devices have been produced and tested for the sole purpose of improving the recovery of coarse particles. For example, Harris, *et al.*, (1992) tested a hybrid mechanical flotation column, which is essentially a cross between a conventional cell and a column flotation cell. In this device, a column is mounted above an impeller agitator. The column component offers the advantage of an upper quiescent section optimal for coarse particle flotation, while the mechanical impeller offers the opportunity for reattachment and increased collection of any non-attached coarse material in the lower zone. However, when compared to a release analysis curve, this hybrid mechanical column out-performed a conventional flotation cell, but was equivalent to a traditional flotation column.

Improvements in coarse particle recovery have also been seen with the advent of non-mechanical flotation cells. For example, success in floating coarser particles has been reported when using column flotation cells, Lang launders, skin flotation systems, and the negative-bias flotation columns. Column flotation offers several advantages that can be useful in any application. Barbery (1984) advocates that columns have no mechanical parts, are easy to automate and control, and provide a high capacity. In addition, columns are low turbulence machines that have well-defined hydrodynamic conditions. These advantages translate to ease of maintenance, scale-up, modeling, and a reduction of short-circuiting usually observed in conventional flotation machines.

Phosphate Flotation Technology

The United States is the world's largest producer of phosphate rock. In 1999, this industry accounted for approximately 45 million tons of marketable product valued at more than \$1.1 billion annually (United States Geological Survey, Mineral Commodity Summaries, January 1999). Approximately 83% of this production can be attributed to mines located in Florida and North Carolina. In subsequent reports it is stated that "U.S. phosphate rock production and use dropped to 40 year lows in 2006." This contracting market requires ever more efficient operations to remain competitive.

Prior to marketing, the run-of-mine phosphate matrix must be upgraded to separate the valuable phosphate grains from other impurities. The first stage of processing involves screening to recover a coarse (plus 14 mesh) high-grade pebble product. The screen underflow is subsequently deslimed at 150 mesh to remove fine clays. Although 20-30% of the phosphate contained in the matrix is present in the fine fraction, technologies currently do not exist that permit this material to be recovered in a

cost-effective manner. The remaining 14 x 150 mesh fraction is classified into coarse (e.g., 14 x 35 mesh) and fine (e.g., 35 x 150 mesh) fractions that are upgraded using conventional flotation machines, column flotation cells, or other novel techniques such as belt flotation (Moudgil and Gupta, 1989). The fine fraction (35 x 150 mesh) generally responds well to froth flotation. In most cases, conventional (mechanical) flotation cells can be used to produce acceptable concentrate grades with recoveries in excess of 90%. On the other hand, high recoveries are often difficult to maintain for the coarser (14 x 35 mesh) fraction.

Prior work has shown that the recovery of coarse particles (e.g., larger than 30 mesh) can be less than 50% in many industrial operations (Davis and Hood, 1992). For example, Figure 2 illustrates the sharp reduction in recovery as particle size increases from 0.1 mm (150 mesh) to 1 mm (16 mesh) for a Florida phosphate operation. In many cases, attempts by plant operators to improve coarse particle recovery often produce an undesirable side effect of diminishing flotation selectivity.

The findings presented in Figure 2 are consistent with historical data from other flotation applications, which show coarse particles are more difficult to recover using traditional flotation machines. Current research indicates that coarser material is lost due to unfavorable hydrodynamic conditions and/or competition with the fines for the available bubble surface area. For this reason, split-feed circuit arrangements are often recommended when treating a wide feed particle size distribution. In addition, new and/or improved technologies need to be developed that are more efficient in treating coarser feeds.

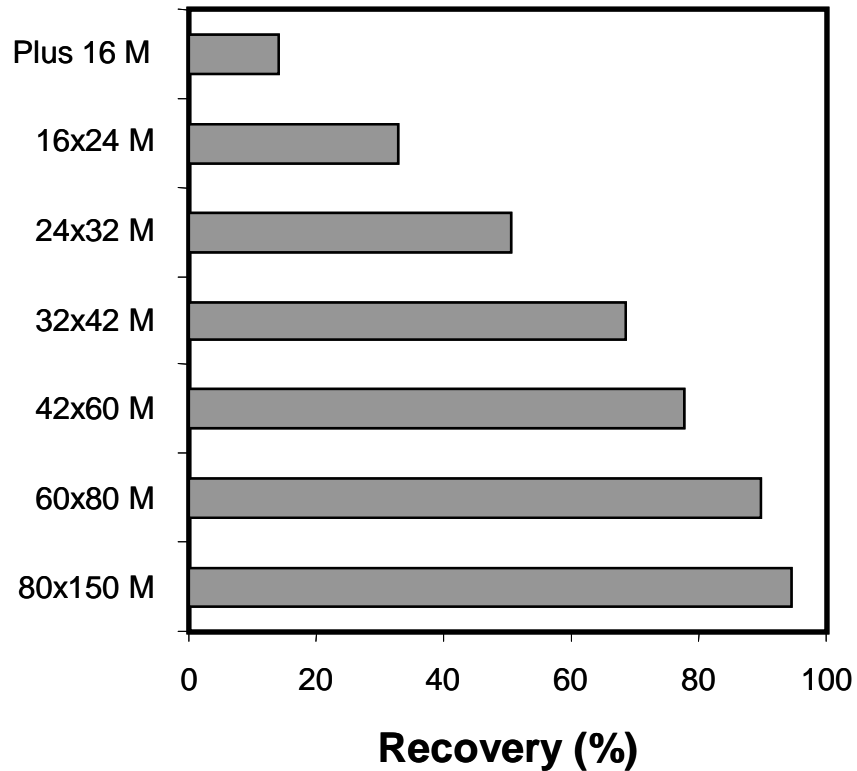


Figure 2. BPL Recovery by Particle Size Class.

Existing column cells used in the phosphate industry have performance limitations due to their mechanical design. In most cases, air is introduced using venturi-type aspirators that require a great deal of water. The majority of this aeration water reports to the column overflow product. This aeration water carries undesired gangue material into the froth product. Additionally, the column aeration rate is intrinsically dependent upon the aspirator water flow rate. As a result, an increase in aeration rate requires an increase in water flow rate that, in turn, can have a detrimental effect on performance. Based on these limitations, it is apparent that a flotation system is required that incorporates quiescent hydrodynamic conditions and provides for a de-coupling of the aeration system from external water supplies.

One well-known method of improving flotation performance is to classify the feed into narrow size fractions and to float each size class separately. This technique, which is commonly referred to as split-feed flotation, has several potential advantages. These advantages include higher throughput capacity, lower reagent requirements, and improved separation efficiency. Split-feed flotation has been successfully applied to a wide variety of flotation systems including coal, phosphate, potash, and industrial minerals (Soto and Barbery, 1991).

The United States Bureau of Mines (USBM) conducted one of the most comprehensive studies of the coarse particle recovery problem in the phosphate industry (Davis and Hood, 1993). This investigation involved the sampling of seven Florida phosphate operations to identify sources of phosphate losses that occur during beneficiation. According to this field survey, approximately 50 million tons of flotation tailings are discarded each year in the phosphate industry. Although the tailings contain only 4% of the matrix phosphate, more than half of the potentially recoverable phosphate in the tailings is concentrated in the plus 28 mesh fraction. In all seven plants, the coarse fraction was higher in grade than overall feed to the flotation circuits. In some cases, the grade of the plus 28 mesh fraction in the tailings approached 57% BPL. The USBM study indicated that the flotation recovery of the plus 35 mesh fraction averaged only 60% for the seven sites included in the survey. Furthermore, the study concluded that of the seven phosphate operations, none have been successful in efficiently recovering the coarse phosphate particles.

There have been several attempts to improve the poor recovery of coarse (16 x 35 mesh) phosphate grains using improved flotation reagents. The University of Florida,

under the sponsorship of the Florida Institute of Phosphate Research (FIPR Project 02-067-099), completed one such investigation in early 1992. This study showed that the flotation of coarse phosphate is very difficult and recoveries of only 60% or less are normally achievable. The goal of the FIPR study was to determine whether the recovery of coarse phosphate particles could be enhanced via collector emulsification and froth modification achieved by frothers and fines addition. Plant tests conducted as part of this project showed that the appropriate selection of reagents could improve the recovery of coarse phosphate (16 x 35 mesh) by up to 6 percentage points. Furthermore, plant tests conducted with emulsified collector provided recovery gains as large as 10 percent in select cases. Unfortunately, reports of follow-up work by industry that support these findings are not available.

In 1988, FIPR also provided financial support (FIPR Project 02-070-098) to Laval University to determine the mechanisms involved in coarse particle flotation and to explain the low recoveries of such particles when treated by conventional froth flotation. In light of this study, these investigators proposed the development of a modified low turbulence device for the flotation of coarse phosphate particles. Laboratory tests indicated that this approach was capable of achieving recoveries of greater than 99% for coarse phosphate feeds. In addition, the investigators noted that this approach did not suffer from high reagent costs associated with other strategies designed to overcome the coarse particle recovery problem. Although the preliminary data was extremely promising, this work was never carried through to industrial plant trials due to problems with the sparging and tailings discharge systems.

Building on these early findings, Soto and Barbery (1991) developed a negative bias flotation column that improved coarse particle recovery. It was surmised that the only factors preventing conventional columns from being ideally suited for coarse particle recovery were wash water flow and a thick froth layer. Wash water is used in column flotation to “wash” fine gangue (i.e., clays) from the product froth. However, wash water also forced some of the coarser particles back into the pulp resulting in a reduction in recovery. Soto and Barbery removed the wash water, which resulted in a net upward flow through the column (i.e., negative bias flow). In addition, they added an upward flow of elutriation water to assist in the transport of coarse particles-bubble aggregates into the overflow launder. As a result of these modifications, Barbery (1989) was able to achieve a four-fold improvement in coarse particle recovery when utilizing this negative bias column. Essentially, this device is operated in a flooded manner and in the absence of a froth zone. Several similar devices have also been introduced that make use of this same principle to improve coarse particle flotation (e.g., Laskowski, 1995).

Several other alternative processes have been used by industry in an attempt to improve the recovery of the coarser particles. These techniques include gravity-based devices such as heavy media cyclones, tables, and spirals, as well as belt conveyors that have been modified to perform skin-flotation (Moudgil and Barnett, 1979). Although some of these units have been successfully used in industry, they normally must be supplemented with scavenging flotation cells to maintain acceptable levels of performance (Moudgil and Barnett, 1979; Lawver *et al.*, 1984). Furthermore, these units typically require excessive maintenance, have low throughput capacities, and suffer from high operating costs.

PROJECT OBJECTIVES

One of the most obvious advantages of improved coarse particle recovery is the increased production of phosphate rock from reserves currently being mined. For example, a survey of one Florida plant indicated that 7-15% of the plant feed was present in the plus 35 mesh fraction. At a 2,000 tph feed rate, this fraction represents 140-300 tph of flotation feed. An improvement in coarse particle recovery from 60% to 90% would represent an additional 50-100 tph of phosphate concentrate. This tonnage corresponds to an additional \$7.5-15 million of revenues. This incremental tonnage and income could be produced without additional mining or reserve depletion. Past attempts to improve the recovery of coarse phosphate particles have been unsuccessful for technical or cost reasons. In addition, many of the proposed solutions could not be transferred to a plant scale operation. As a result, it is apparent that a new low-cost technology is needed to improve the recovery of coarse phosphate particles (>35 mesh).

The objective of this study is to conduct an in-plant pilot-scale evaluation of a new separator known as the HydroFloat concentrator. This technology is specifically designed to improve the recovery of coarse phosphate particles that are currently lost in industrial processing plants. The study includes (i) a technical evaluation that examines the capabilities of the new technology in terms of product recovery, quality and throughput capacity and (ii) an economic analysis that examines the financial feasibility of implementing the system in the Florida phosphate industry.

EXPERIMENTAL

WORK PLAN PREPARATION

A project work plan was prepared and submitted to FIPR and PCS Phosphate for approval. This work plan provided plant personnel the opportunity to modify the proposed work and to incorporate any ideas or new information that may have become available between the project award date and the initiation of activities. The work plan provided a description of the on-site testing strategy as well as experimental procedures, analytical methods, and reporting guidelines for the proposed work. The original schedule for the proposed work is presented in Figure 3. According to this chart, the work was scheduled for completion in 12 months. However, a downturn of the phosphate

Work Element	Work Element Description	Duration (Month)											
		1	2	3	4	5	6	7	8	9	10	11	12
Task 1	Work Plan Preparation	█											
Task 2	HydroFloat Testing												
Subtask 2.1	Equipment Setup		█										
Subtask 2.2	Shakedown Testing			█									
Subtask 2.3	Detailed Testing				█	█	█	█	█	█	█	█	█
Subtask 2.4	Comparison Testing				█	█	█	█	█	█	█	█	█
Task 3	Conditioner Testing												
Subtask 3.1	Equipment Setup		█										
Subtask 3.2	Shakedown Testing			█									
Subtask 3.3	Detailed Testing				█	█	█	█	█	█	█	█	█
Task 4	Long-Duration Testing											█	█
Task 5	Process Evaluation												
Subtask 5.1	Technical Evaluation				█	█	█	█	█	█	█	█	█
Subtask 5.2	Modeling/Simulation				█	█	█	█	█	█	█	█	█
Task 6	Sample Analysis				█	█	█	█	█	█	█	█	█
Task 7	Final Report Preparation												█

Figure 3. Project Tasks and Schedule.

industry resulted in on-site manpower reduction. As a result, the industrial participants extended the length of the project to 18 months to accommodate changes in staffing levels and production schedules. This extension was also used to accommodate additional pilot-scale testing of a novel flotation reagent in conjunction with the University of Utah.

HYDROFLOAT TESTING

Equipment Setup

A schematic of the pilot-scale test circuit used to evaluate the performance of the HydroFloat separator is shown in Figure 4. The test circuit consisted of three primary unit operations, i.e., pilot-scale classifier, slurry conditioner, and HydroFloat separator. In this circuit, the coarse underflow from an existing bank of classifying cyclones was fed to a 5 ft x 5 ft Eriez CrossFlow classifier (see Figure 5). The preliminary tests showed that the classifier was capable of handling solid flows in excess of 150 ton/hr (6 ton/hr/ft²) despite

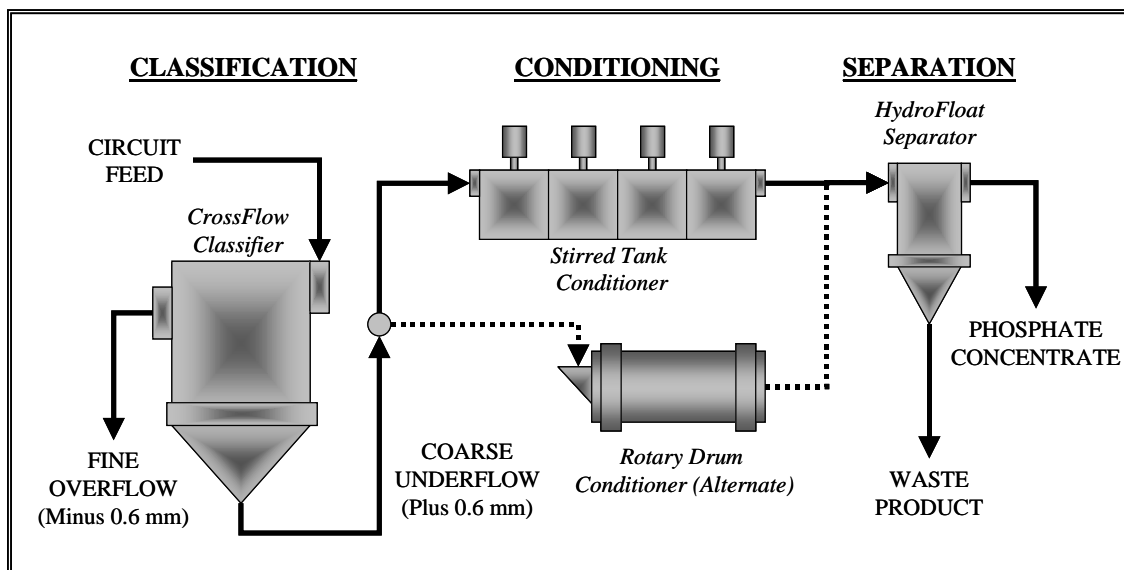


Figure 4. Pilot-Scale Test Circuit Used to Evaluate the HydroFloat Separator.

significant variations in the feed solids content from 15% to 60%. This ability was attributed to the tangential feed presentation system that allows for a consistent underflow stream regardless of plant operating conditions (i.e., feed tonnage, percent solids). The underflow from the classifier was passed to the conditioning unit (see Figure 6). Appropriate reagents were added ahead of the conditioner to control pH (ammonia) and particle hydrophobicity (fatty acid/fuel oil blend).

The test circuit was configured so that feed



Figure 5. Photograph of the 5 ft x 5 ft CrossFlow Classifier.



Figure 6. Photograph of the Stirred-Tank Conditioner.

conditioning could be performed using either a stirred-tank (four stage) or a single-stage rotary drum (30-inch diameter) conditioner. The conditioner circuit was able to operate reliably at approximately 40-75% solids at a maximum mass flow rate of 4-6 ton/hr (dry solids). This corresponds to a range in retention time from 1-3 minutes.

The conditioned slurry flowed by gravity to the feed inlet for either the HydroFloat separator (see Figure 7) or a 20-inch diameter flotation column (not shown). This arrangement made it possible to directly compare the effectiveness of the HydroFloat separator with existing column technology. The test circuit was installed with all necessary components (i.e., feeder, conditioner, reagent pumps, etc.) required to operate the separator in continuous mode at a maximum capacity of 4-6 tph.



Figure 7. Photograph of the Pilot-Scale HydroFloat Separator.

ROTARY CONDITIONER TESTING

Equipment Setup

Laboratory test data indicate that a significant increase in BPL recovery can be achieved by improving the conditioning of the coarse phosphate matrix. In particular, a rotary drum conditioner has been shown to be capable of improving the separation

performance compared to a traditional multi-cell, stirred-tank conditioner. The tumbling nature of the rotary conditioner minimizes the creation of slimes and allows conditioning to be conducted at higher feed percent solids (>75% solids) without sanding.

The evaluation of the rotary conditioning system was carried out in this project using a 30-inch diameter drum conditioner. A conceptual drawing of the assembled rotary conditioner is presented in Figure 8. The pilot-scale unit was fabricated and installed at the test site using field personnel from Eriez and staff from PCS Phosphates. Jacobs Engineering designed the conditioner as part of their subcontract for this project. After the design was completed, Eriez was responsible for preparing the detailed manufacturing drawings and for fabricating and assembling the equipment. As shown, the conditioning drum was mounted on rollers and powered by an electric drive.

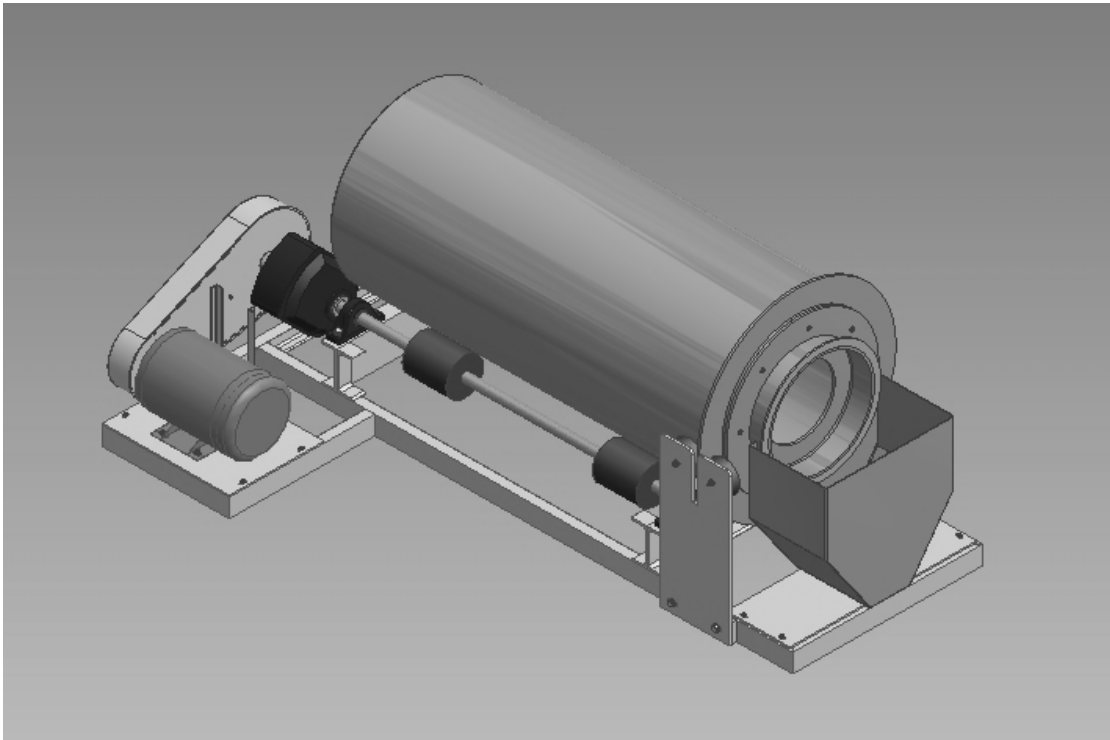


Figure 8. Rotary Drum Conditioner (30-Inch Diameter).

DATA RECONCILIATION

To ensure that the test data are reliable and self-consistent, all test data was be analyzed and adjusted using a mass balance program. For the testing of the HydroFloat, samples of the feed, concentrate and tailings streams were collected for each test. A head sample was taken from each stream and the remainder was screened into four different size fractions (+16, 16x28, 28x35 and -35) and weight percentages were determined. Chemical analysis (%BPL and %insoluble) of each of the five fractions was then performed. The results from the chemical analysis of those streams were used to determine performance characteristics such as BPL recovery, insoluble rejection, etc.

The mass balance was conducted based on the conservation of total mass and phosphate throughout the circuit. This balance provides three independent linear equations for steady-state operation:

$$\sum_1^i \%inclass_i = 100 \quad [1]$$

$$\sum_1^i (PercentMass)_i \times (ComponentContent)_i - HeadComponent = 0 \quad [2]$$

$$Feed = Concentrate + Tailings \quad [3]$$

In many cases, the experimental data from the test circuits were over-defined. This occurs when redundant streams are sampled or when multiple independent assays (e.g., % BPL and %Insoluble) are available for each stream. Assays for different components in each stream may result in different (but equally valid) estimates of the concentrate mass yield (Y). The yield may be calculated using the well-known two-product formula given by:

$$Y = \frac{f - t}{c - t} \quad [4]$$

where f , c and t are experimental assays for the feed, concentrate and tailing streams, respectively. For example, Table 1 summarizes the mass yields calculated for the unit. The yields calculated using the two assays are very close in some cases regardless of whether it was based on % BPL or % insols. The yields determined for the +16 and 16x28 mesh material are in this group. On the other hand, the yields calculated using the two different assays varied in some cases. The yields determined for the head sample, 28x35 and -35 mesh material fall into this category for this particular example. These discrepancies are due to experimental errors associated with process fluctuations, sampling techniques and laboratory analysis procedures.

One method of resolving this dilemma is to construct a “self-consistent” data set which satisfies the mass balance criteria given by Equations [1] - [3]. This procedure must be performed such that the minimum total adjustment is made to the measured data. This can be achieved by minimizing the weighted sum-of-squares ($WSSQ$) given by:

$$WSSQ = \sum_{k=1}^c \sum_{i=1}^m \frac{(A_i^{k*} - A_i^k)^2}{(S_i^k)^2} + \sum_{i=1}^m \frac{(M_i^* - M_i)^2}{(S_i)^2} = 0 \quad [5]$$

where S_i^k and S_i are the standard deviations of the measured assay values and measured flow rates, respectively. The superscript * is used to distinguish estimated values from

Table 1. Comparison of Yield Calculations.

Size Class	BPL Yield	Insol Yield
Head	22%	26%
+16	22%	22%
16x28	18%	18%
28x35	27%	28%
-35	68%	70%

experimental values. In most cases S_i^k and S_i are assumed to be proportional to the value of the measured assay and are calculated by:

$$S_i^k = e_i^k A_i^k \quad [6]$$

$$S_i = e_i M_i \quad [7]$$

where e_i^k and e_i are the respective relative errors in the measurements of the k-th component assays and mass rates for stream i.

Several mathematical techniques can be used to perform the minimization. These include the use of Lagrangian Multipliers (Wiegel, 1979) and direct search techniques (Mular, 1979). Several commercial software packages have also been developed for this purpose. In the current study, the balancing was done using an Excel spreadsheet that made use of the Solver program to converge upon a solution that satisfied the constraints. An example spreadsheet can be found in Table 2. The user-entered values are all in the

Table 2. Example Mass Balance Spreadsheet.

Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)		
	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow
Unbalanced Sample Data															
Head	--	--	--	100.0	50.0	50.0	27.8	72.8	15.0	59.8	2.8	79.6	100.0	50.0	50.0
+16	47.1	39.4	40.4	15.7	13.1	13.5	42.7	72.7	34.2	42.1	2.9	53.2	15.7	6.5	6.7
16x28	165.4	133.6	188.7	55.0	44.4	62.9	22.4	72.1	11.4	69.5	3.2	83.9	55.0	22.2	31.5
28x35	74.6	92.5	65.7	24.8	21.9	27.3	74.0	10.2	62.9	2.1	82.7	24.8	15.4	11.0	
-35	13.4	35.4	5.0	4.5	11.8	1.7	62.7	72.7	41.2	15.2	3.1	44.2	4.5	5.9	0.8
Balanced Sample Data															
Head	n/a	n/a	n/a	100.0	23.9	76.1	28.5	71.9	14.9	61.1	2.9	79.3	100.0	23.9	76.1
+16	n/a	n/a	n/a	14.1	13.4	14.4	42.8	72.6	34.1	41.9	2.9	53.3	14.1	3.2	10.9
16x28	n/a	n/a	n/a	57.2	44.1	61.3	22.5	71.8	11.4	68.8	3.2	83.7	57.2	10.5	46.7
28x35	n/a	n/a	n/a	24.8	32.2	22.6	28.3	71.6	10.1	61.8	2.4	86.8	24.8	7.2	17.2
-35	n/a	n/a	n/a	4.2	12.3	1.7	65.0	71.9	41.2	15.4	3.1	43.7	4.2	2.9	1.3
	head assay check			head assay constraint			0.0	0.0	0.0	0.0	0.0	0.0			
Relative Error															
Head	n/a	n/a	n/a	1.0	99.0	99.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
Relative Change															
Head	n/a	n/a	n/a	0.0	-52.2	52.2	2.6	-1.2	-0.7	2.2	2.7	-0.3	n/a	n/a	n/a
+16	n/a	n/a	n/a	-9.9	2.0	6.7	0.3	-0.2	-0.3	-0.3	-0.4	0.1	n/a	n/a	n/a
16x28	n/a	n/a	n/a	3.9	-0.8	-2.6	0.7	-0.5	-0.5	-0.9	-1.4	-0.3	n/a	n/a	n/a
28x35	n/a	n/a	n/a	-1.4	-1.4	3.3	3.8	-3.2	-1.1	-1.7	-0.7	1.1	n/a	n/a	n/a
-35	n/a	n/a	n/a	-5.5	4.3	0.9	0.4	-0.4	-0.1	1.3	-0.6	-1.2	n/a	n/a	n/a
Weighted Sum of Squares															
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	Mass Rate Constraints		
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	(Mass)	BPL	Insol
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

blue font. These include the unbalanced sample data and the relative errors. The yield of the unit is unknown so it is estimated that there is a 50/50 split and then a low confidence is given to those numbers by giving those values high relative errors of 99%. Once this information has been entered, the Solver routine is used to balance the data (Luttrell, 1996). Examples of some of the mass balances are provided in APPENDIX B.

RESULTS AND DISCUSSION

HYDROFLOAT RESULTS

Shakedown Testing

Shakedown was completed without any considerable difficulties. The shakedown tests confirmed that the 5 ft x 5 ft CrossFlow could supply sufficient feed to the conditioner and the 2 ft x 2 ft HydroFloat. Several minor operational problems were resolved on site. These included replacement of the original pneumatically powered, stirred-tank conditioner with electric agitators since the plant air system could not deliver the required air flow and pressure. The electric mixers easily maintained the coarse phosphate matrix in suspension up to approximately 65% solids. In addition, rectangular inserts were placed into the conditioner cells to produce an octagonal shape. This configuration increased efficiency by minimizing the “sanding” in the corners.

The HydroFloat aeration system also required minor alterations to the piping manifold to ensure consistent distribution of air throughout the teeter-bed. Poor distribution resulted in channeling through the teeter-bed in localized areas. The air/water distribution manifold was redesigned (with fewer holes) to resolve this problem.

Detailed Testing

Tests were conducted to evaluate the effect of key operating and design parameters on the performance of the HydroFloat separator. Variables investigated included feed injection depth, teeter-water injection spacing, mass feed rate, feed solids content, water rate, bed depth, aeration rate, and reagent dosage. All tests were conducted on a classified feed that was nominally 10 x 35 mesh.

Feed Injection Depth. Figure 9 shows the effect of changing the feed injection point was studied by varying the position of the feed pipe inside the separator. Feed insertion depth is reported as the vertical distance above the water injection pipes. The tests were performed while maintaining a constant bed height of 18 inches above the teeter pipes. The data indicate that the feed insertion point had a strong impact on the overall BPL recovery. As the feed slurry was introduced closer to the overflow lip, the recovery of valuable phosphate increased. Likewise, the recovery decreased as the feed introduction point was lowered deeper into the cell. This finding suggests that particles introduced deeper into the teeter-bed are more difficult to recover. The lower recovery

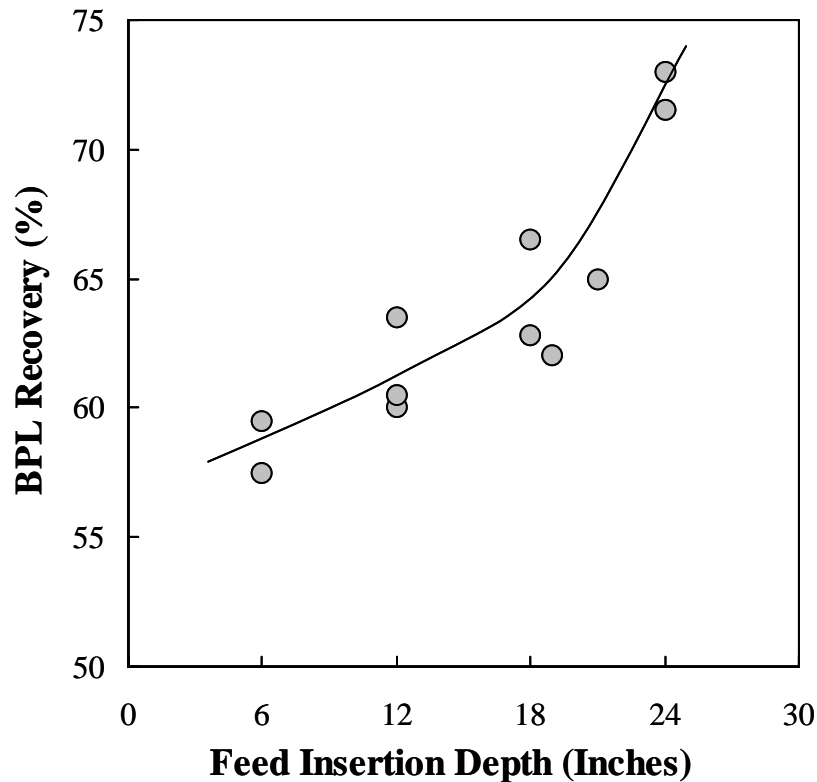


Figure 9. Effect of Feed Injection Point on HydroFloat Performance.

can be attributed to the fact that particles introduced deeper into the bed have a higher probability of becoming detached or misplaced as they travel through the high solids teeter-bed.

Water Injection Spacing. The number of injection pipes and the spacing between the water injection holes were found to be very important. For example, the data given in Figure 10 show that the performance of the cell can be improved by reducing the original number of water injection pipes (and number of injection holes) by half. When using too many holes, the system pressure was too low, thus allowing the air bubbles to coalesce before entering the teeter-bed. These “burps” create turbulence that is

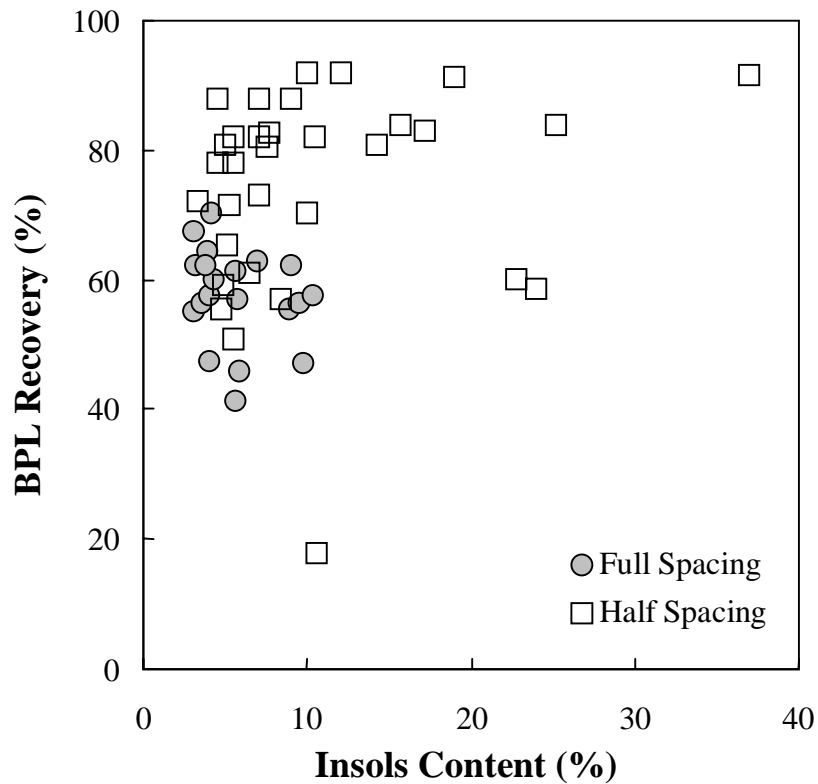


Figure 10. Effect of Water Pipe Spacing on HydroFloat Performance.

detrimental to separation performance. The higher pressure allowed for a greater number of smaller individual bubbles to form and rise, sustaining the teeter bed separation zone.

Fluidization Water Rate. Figure 11 shows the effect of increasing fluidization water rate on product quality. The data show that the product insols content increased from approximately 5% to 10% as the fluidization rate increased. In fact, the data collected to date suggest that this relationship is nearly linear. The increased water velocity through the teeter bed helps lift bubble-particle aggregates out of the bed and, hence, provides a slight increase in BPL recovery. Unfortunately, the increased water velocity also tends to carry silica into the overflow product, thereby reducing the quality

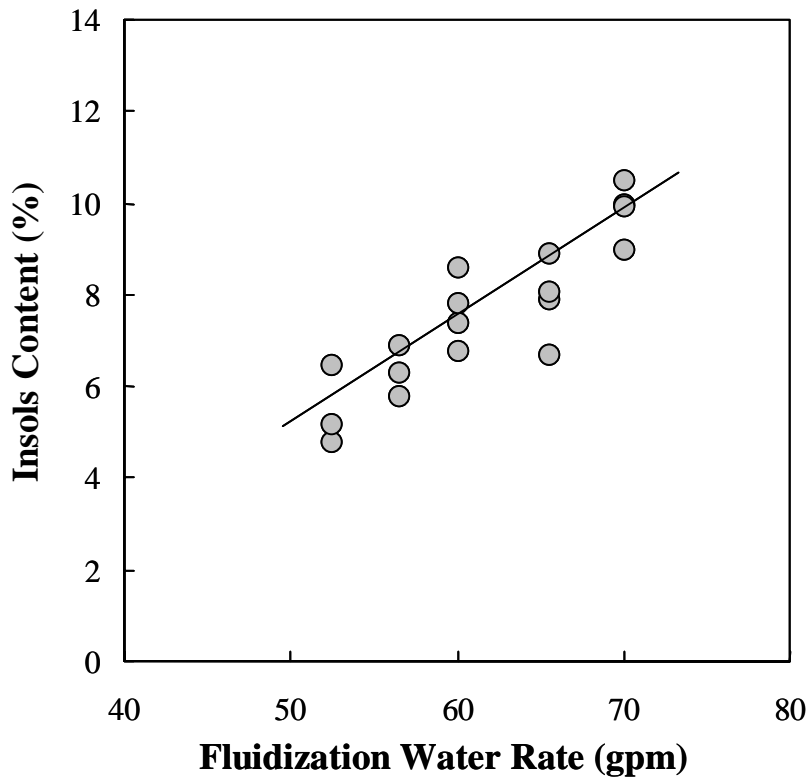


Figure 11. Effect of Fluidization Water Rate on HydroFloat Performance.

of the overflow product. Therefore, an optimum water rate must be selected in each case that balances the loss in recovery against the decrease in selectivity.

Teeter-Bed Depth. The data presented in Figure 12 show that the depth of the teeter-bed had a significant impact on product insols content. Bed level is reported as the vertical distance between the top of the teeter bed and the water injection pipes. As the bed level approaches the overflow lip, more silica is short-circuited into the overflow and the insols content of the product increases. Likewise, as the bed level is dropped away from the overflow lip, the product grade improves as less material is misplaced into the product launder. Despite the significant amount of scatter in the test data, the relationship

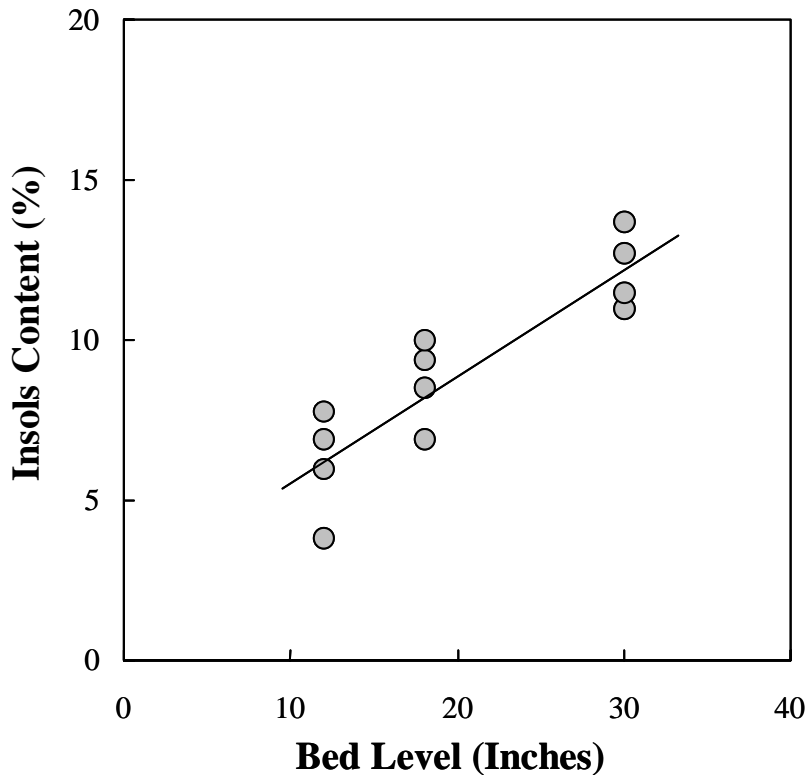


Figure 12. Effect of Teeter-Bed Level on HydroFloat Performance.

between bed depth and insoluble content appears to be nearly linear. Also, although not shown in this plot, the bed depth had minimal influence on BPL recovery.

Mass Feed Rate. Figure 13 shows the effect of dry solids feed rate on the performance of the HydroFloat. As shown, the BPL recovery remains relatively constant up to a feed rate of approximately 6 tph of dry solids. This value corresponds to a specific unit capacity of approximately 1.5 tph/ft². Phosphate recovery decreases substantially at solids feed rates in excess of 1.5 tph/ft². However, as discussed later, the limitation on throughput capacity appears to be a result of insufficient capacity in the stirred tank conditioning system as opposed to an inherent limitation associated with the HydroFloat.

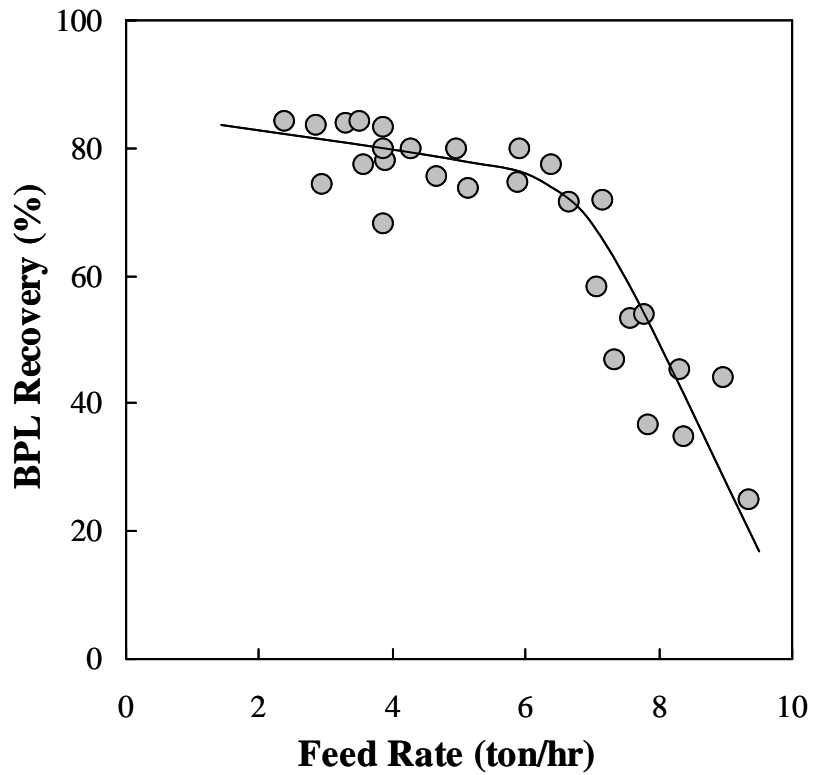


Figure 13. Effect of Dry Feed Rate on HydroFloat Performance.

Feed Solids Content. The percent solids used during conditioning and separation was found to have a large impact on flotation recovery. As shown in Figure 14, the BPL recovery increased from 50% to over 80% as the conditioning percent solids increased from 45% to 65%. This improvement is attributed to several factors. First, the reduction in water content as feed solids increases results in a higher chemical concentration within the conditioner. The higher solids content enhances the contacting between reagents and solids. Secondly, an increase in the percent solids (at the same solids throughput) results in a lower mass flow and, consequently, a longer retention time within the conditioner. As with any process, an increase in retention time typically provides a higher product

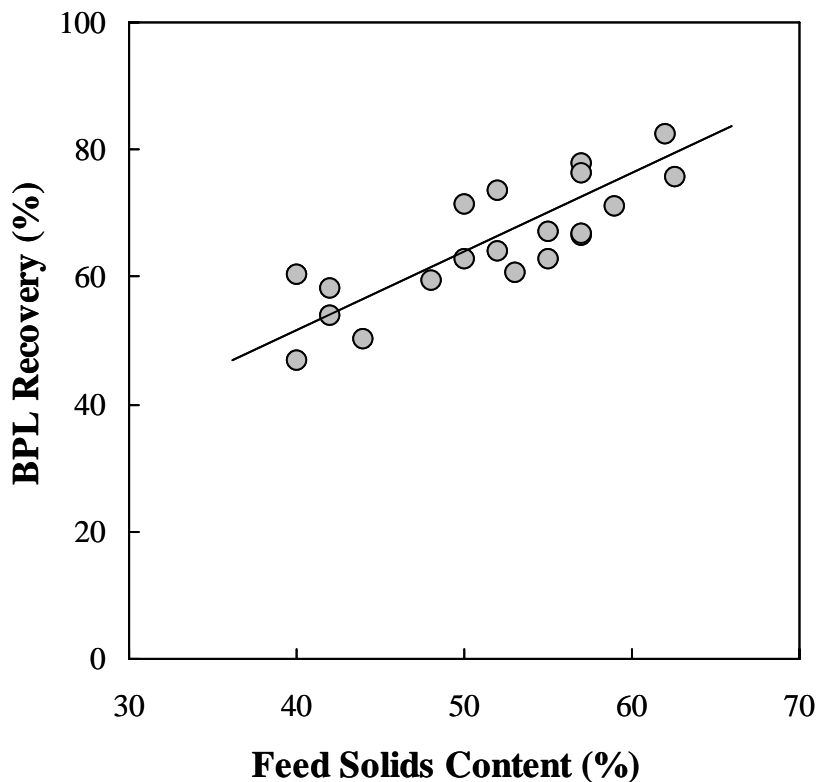


Figure 14. Effect of Feed Solids Content on HydroFloat Performance.

recovery. Unfortunately, tests could not be performed at solids contents higher than 65% due to particle sanding in the conditioners.

In conventional conditioning practices, the presence of finer particles (35 x 150 mesh) increases slurry viscosity, thus reducing the free-settling characteristics of the particles. The absence of fines in this test program required more vigorous mixing to maintain the particles in suspension during the conditioning stage. The action has the unwanted side effect of generating additional slimes that are detrimental to flotation.

Aeration Rate. Detailed tests were conducted to determine the effect of aeration rate on the performance of the HydroFloat cell. As shown in Figure 15, an increase in air

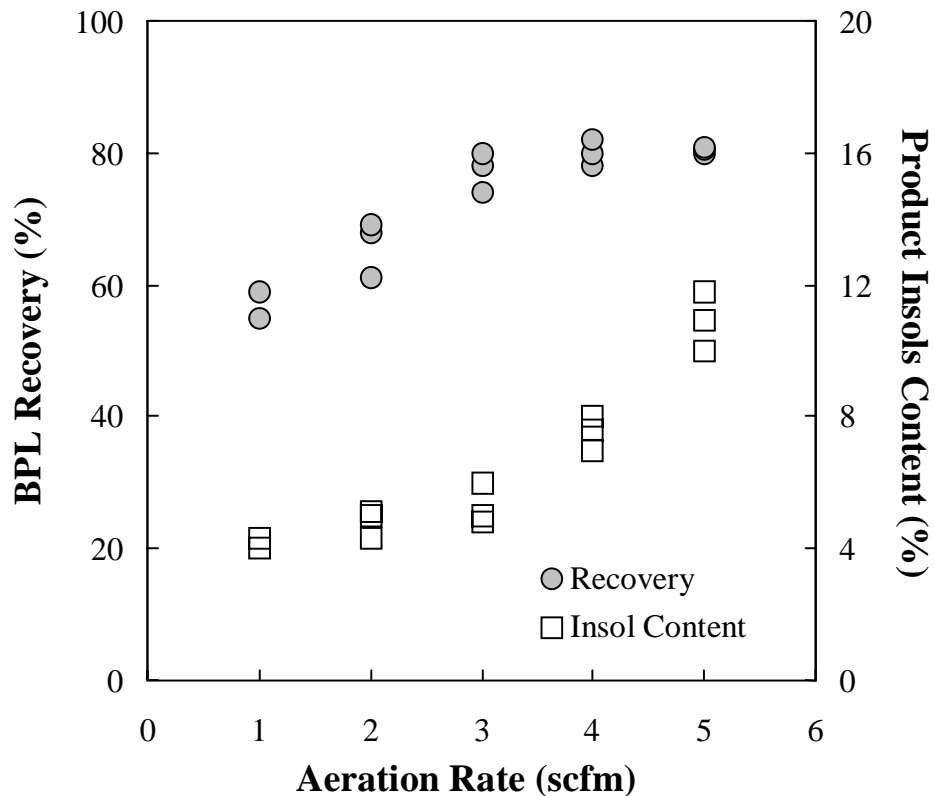


Figure 15. Effect of Air Rate on HydroFloat Performance.

rate from 1 scfm to 5 scfm resulted in an increase in BPL recovery and product insols content. (Note that all air flow values were converted to standard conditions prior for reporting purposes.) The increase in recovery can be attributed to an increase in the flotation rate. The increase in flotation rate with gas flow rate is well documented in the technical literature. An increase in gas flow rate (at the same bubble size) results in a greater gas flux through the column and, consequently, a greater probability of floatable solids encountering an air bubble (Schulze, 1984).

The increase in product insols content is attributed to several factors. The first is simple hydraulic entrainment. The increased gas flow rate results in greater turbulence within the cell that carries hydrophilic gangue particles into the overflow concentrate. In addition, some of the phosphate particles at the test site were locked with silica (insols). Therefore, an increase in phosphate recovery will naturally produce a higher insols content in the concentrate product. The optimum aeration rate is between 3 and 4 SCFM, which would maximize the recovery while not largely increasing silica contamination ct.

Frother Dosage. A glycol-type frother (F-507) was used during the HydroFloat evaluation. According to the data presented in Figure 16, the BPL recovery dropped as the frother addition rate increased. At 0.35 lbs/ton of frother, the BPL recovery ranged from 75% to 80%. At 0.80 lbs/ton, however, the BPL recovery was only 67%. The reduction in recovery is attributed to a decrease in bubble size as frother concentration increased. Smaller bubbles (<0.5 mm) create bubble/particle aggregates with less buoyancy when compared to larger bubbles (~1mm). In contrast to conventional flotation processes, it is believed that the bubble-particle aggregates formed with larger bubbles

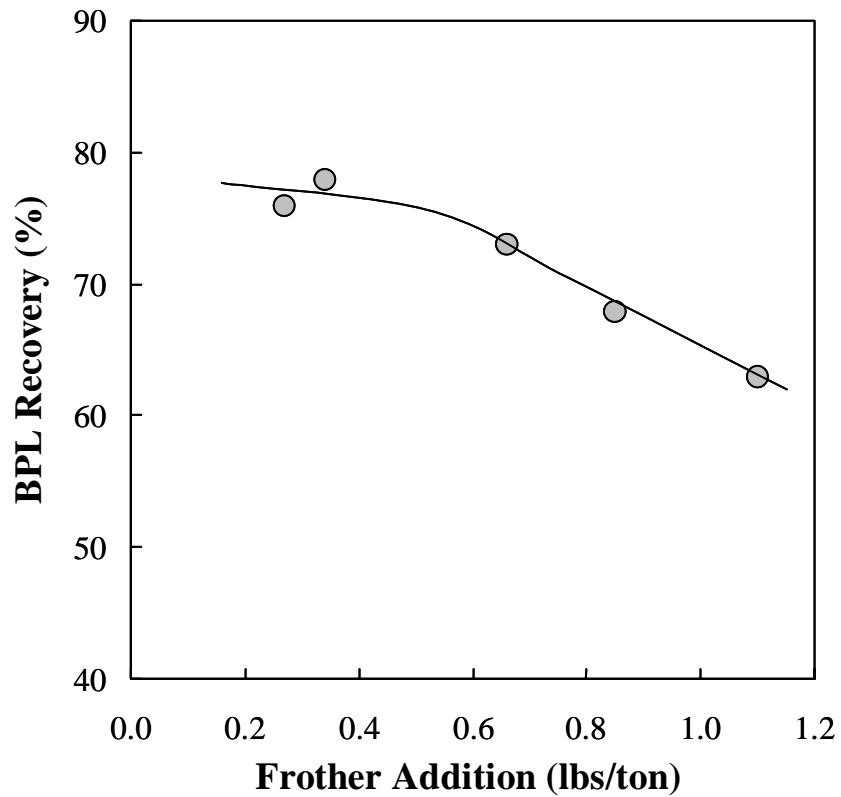


Figure 16. Effect of Frother Dosage on HydroFloat Performance.

have a lower apparent density and are recovered more readily using the HydroFloat system.

Collector Dosage. The collector used in the HydroFloat evaluation was supplied as a 70/30 mixture of fatty acid (FA) and fuel oil (FO). The data presented in Figure 17 suggests that the collector addition rate plays a significant role in determining the recovery of coarse phosphate. As the dosage of the fatty acid/fuel oil mixture increased from 0.2 lbs/ton to 0.5 lbs/ton, the recovery of coarse phosphate improved from 30% to 75%. In this example, the maximum BPL recovery was achieved at a collector dosage between 0.8-1.0 lbs/ton. It should be noted that this optimum addition rate is less than

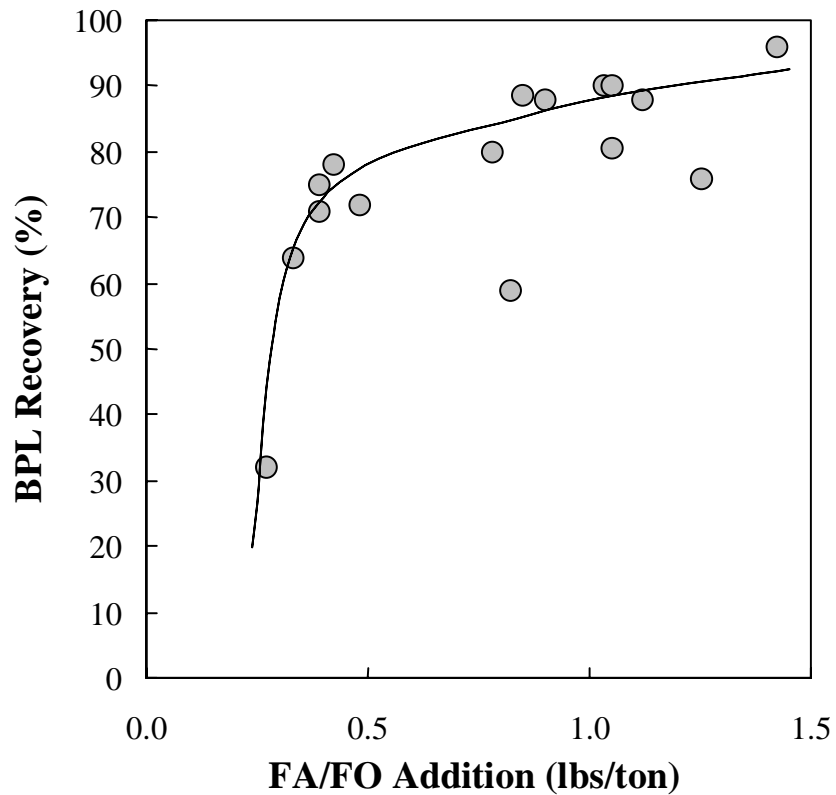


Figure 17. Effect of Fatty Acid to Fuel Oil Dosage on Performance.

that currently used in plant operations. However, a lower collector dosage should be expected due to the reduced surface area of the coarser feed used in the HydroFloat tests.

Column Comparison Tests

To compare the HydroFloat with current state-of-the-art column technology, comparison tests were conducted using a 20-inch diameter open-column flotation cell. The results from the column comparison tests are presented in Figure 18 and 19. A Canadian Process Technologies (CPT) column flotation cell was selected for this application. The CPT column utilizes the patented SlamJet sparging technology that incorporates an automatic, self-regulating, gas injection system. The column was

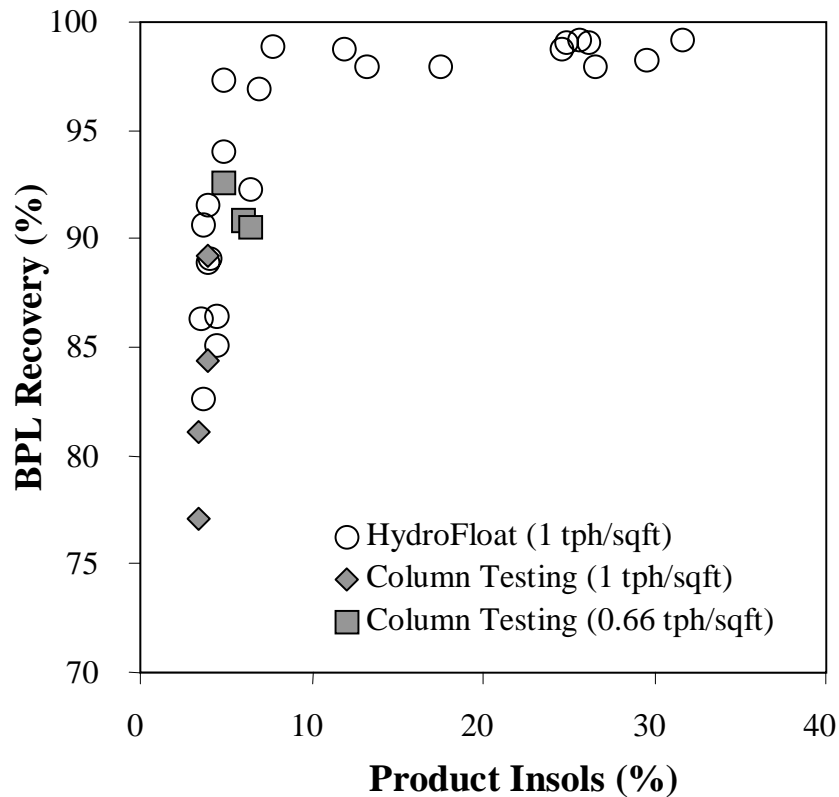


Figure 18. BPL Recovery Comparison for Column and HydroFloat Systems.

supplied with instrumentation to maintain level and monitor air and water flow rates and was installed beside the existing HydroFloat cell so that feed could be easily diverted from one cell to the other. Comparison tests were conducted on each cell as a function of various operating conditions. The objective of the test program was to collect sufficient data using each separator to generate comparable product grade versus recovery curves.

Tests conducted with the CPT column flotation cell were conducted using the rotary drum-type conditioner. The potential benefits of this particular conditioning system are discussed in greater detail in the next section of this report. A representative from Jacobs Engineering was present during the column evaluation. Jacobs Engineering

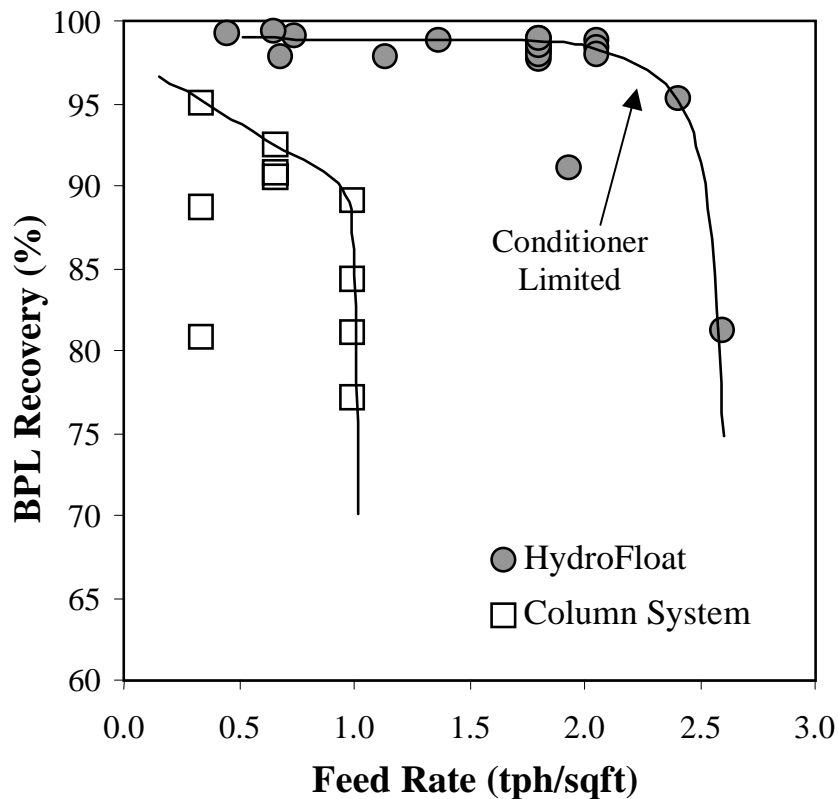


Figure 19. Feed Rate Comparison for Column and HydroFloat Systems.

was responsible for ensuring that the column cell was operated in a manner consistent with current standards employed in the phosphate industry.

The data shown in Figure 18 indicate that both the HydroFloat and open column operated on the same product grade versus recovery curve. The BPL recovery, however, was substantially higher for the HydroFloat system. The result is particularly impressive considering that the open column was operated at a substantially lower feed rate than the HydroFloat. The open column was able to achieve BPL recoveries exceeding 90% at a feed rate of 0.66 tph/ft². However, as the feed rate increased to a higher value of 1.0 tph/ft², the BPL recovery dropped significantly.

As illustrated in Figure 19, the HydroFloat was able to maintain a BPL recovery averaging 98% at a feed rate exceeding 2.0 tph/ft². It should be noted that at a feed rate of 2.5 tph/ft², the capacity of the conditioner (not the HydroFloat) was exceeded. At this capacity, the poor conditioning caused a decrease in the downstream performance of the HydroFloat separator. Thus, the maximum capacity of the HydroFloat cell could not be fully established in the current test program. Nevertheless, the data clearly demonstrate that the capacity of this new technology is far in excess of that achieved using the flotation column cells currently used by the phosphate industry.

ROTARY CONDITIONER RESULTS

Shakedown Testing

Figure 20 compares the initial separation results obtained using the rotary and stirred-tank conditioners for a 10 x 35 mesh feed. The data show that an acceptable product grade (i.e., <10% insols content) can be obtained using either conditioning system. The overall recovery, however, was nearly 20% higher for the tests conducted using the rotary conditioner. The difference in recovery can be attributed to the presence of slimes generated by the stirred-tank conditioner.

It is important to note that in current plant practice, the conditioner feed size distribution typically ranges from 10 mesh to 150 mesh. The presence of the fines fraction (35 x 150 mesh) contributes to an increase in viscosity that helps maintain coarser solids in suspension. After classification to remove the 10 x 150 mesh material, however, the 10 x 35 mesh fraction is highly prone to “sanding.” As such, high mixing speeds are required to maintain the plus 35 mesh solids in suspension when using the

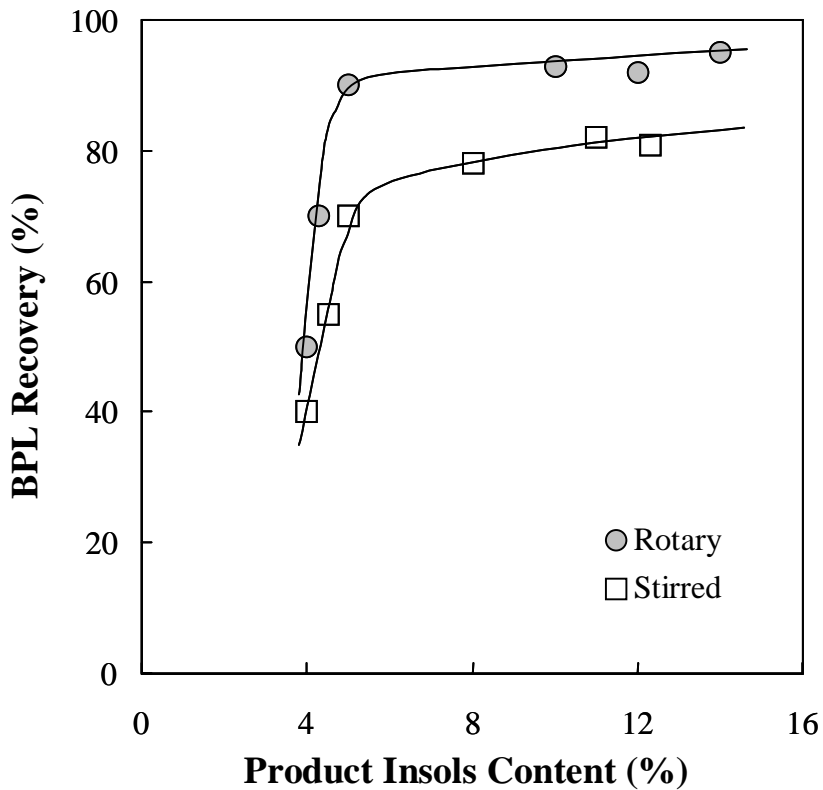


Figure 20. Effect of Conditioner Type on HydroFloat Performance.

stirred-tank conditioner. The high mixing speeds and absence of fines resulted in the attrition of solids and subsequent slimes generation.

Several field tests were conducted to verify that the stirred tank conditioners produced more slimes than the rotary conditioner. These experiments were conducted by collecting samples of the discharge from both conditioners as a function of time. The proportion of slimes generated was determined by screening the conditioned solids at 100 mesh and 325 mesh. The test data from these evaluations are summarized in Figure 21. As shown, no measurable increase in slimes content was found to exist for the rotary conditioning system. In contrast, the results obtained using the stirred-tank conditioner indicates a twenty-fold increase in the amount of minus 325 mesh slimes. The large

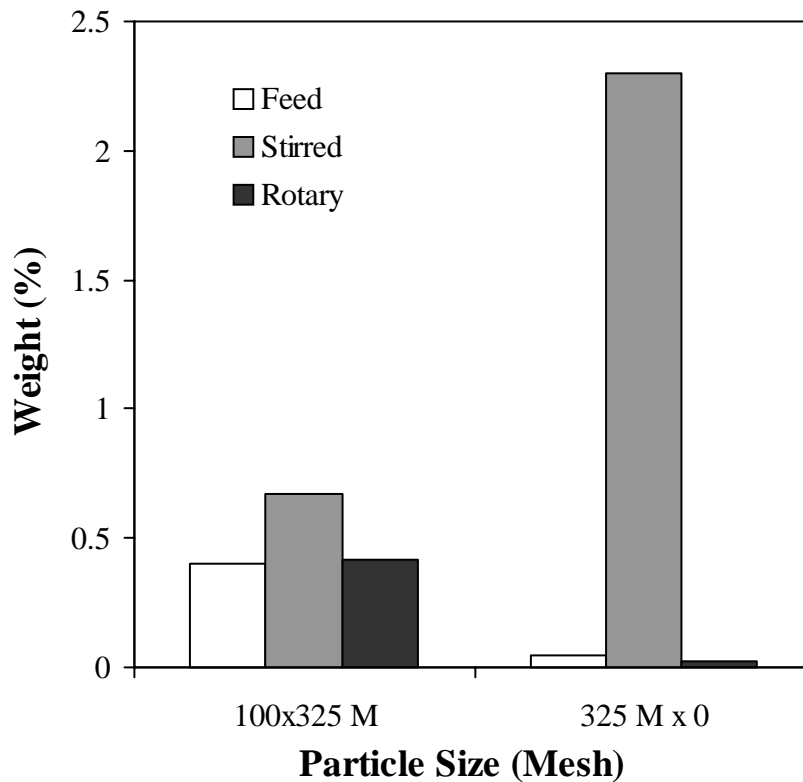


Figure 21. Slimes Generation by Stirred and Rotary Conditioners.

increase in the proportion of ultrafines is responsible for the lower recovery and poorer selectivity of the results obtained using the stirred tank conditioner.

Detailed Testing

A wide variety of field tests were conducted to evaluate the overall performance of the rotary conditioner. The operating conditions for these tests were set as follows. The rotary conditioner was designed to operate at a feed rate of 4-6 tph of dry solids at a pulp density of 65% solids by weight. This volume flow of slurry provides a mean retention (conditioning) time of approximately 3 minutes. However, the unit was configured so that significantly higher solids contents could be evaluated (i.e., >70%). Based on preliminary

laboratory testing, the optimum feed density and drum speed were determined to be 72% solids and 60 rpm, respectively.

Figure 22 provides a summary of the test data obtained using both the rotary drum conditioner and stirred tank conditioner. The improved flotation response for the drum conditioner, which was demonstrated in an earlier laboratory evaluation, was verified through the pilot-scale testing. As shown, the rotary conditioner improved BPL recovery by approximately 20 percentage points. In fact, the BPL recovery approached 98% at a product insols grade between 5% and 12%. The very high separation efficiency afforded by the rotary conditioner is also evident in the BPL recovery versus insols rejection curve

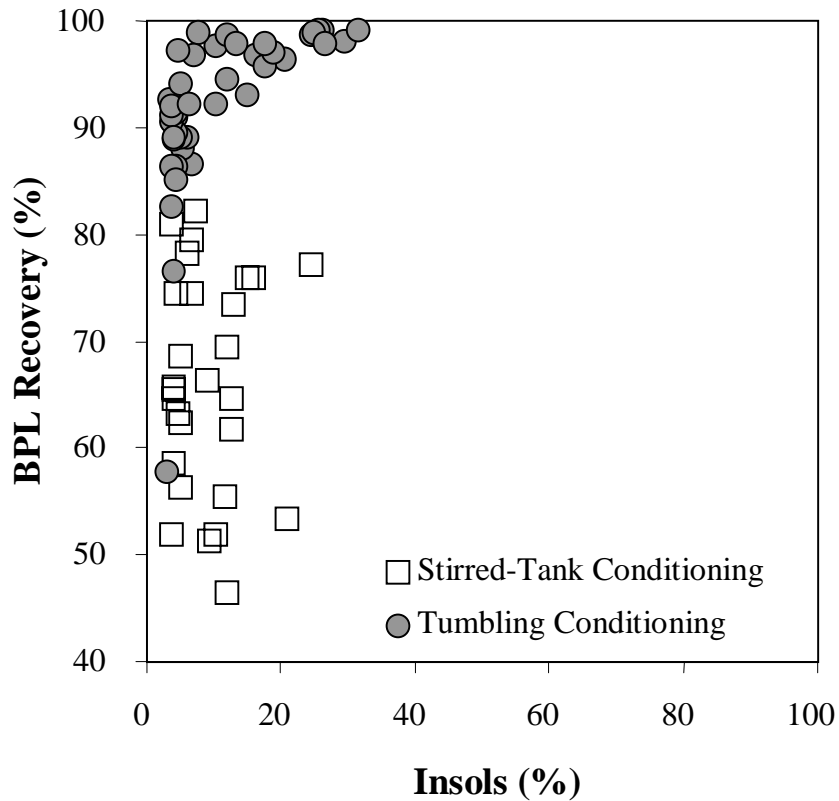


Figure 22. Recovery vs. Grade for Stirred and Rotary Conditioners.

presented in Figure 23. The high concentrate grade is due to the improved recovery of the coarse, high-grade particles normally lost in traditional mechanical flotation. When using the HydroFloat system, over 80% of the coarsest phosphate particles (+10 mesh) were recovered.

Figure 24 shows the typical size-by-size BPL recoveries and insols rejections obtained using the HydroFloat separator. As shown, the HydroFloat was able to maintain a high BPL recovery and insols rejection for all size classes. In fact, the comparison data indicate that the conditioning system has a greater impact on separator performance than most of the other operating variables examined in this investigation. Thus, greater

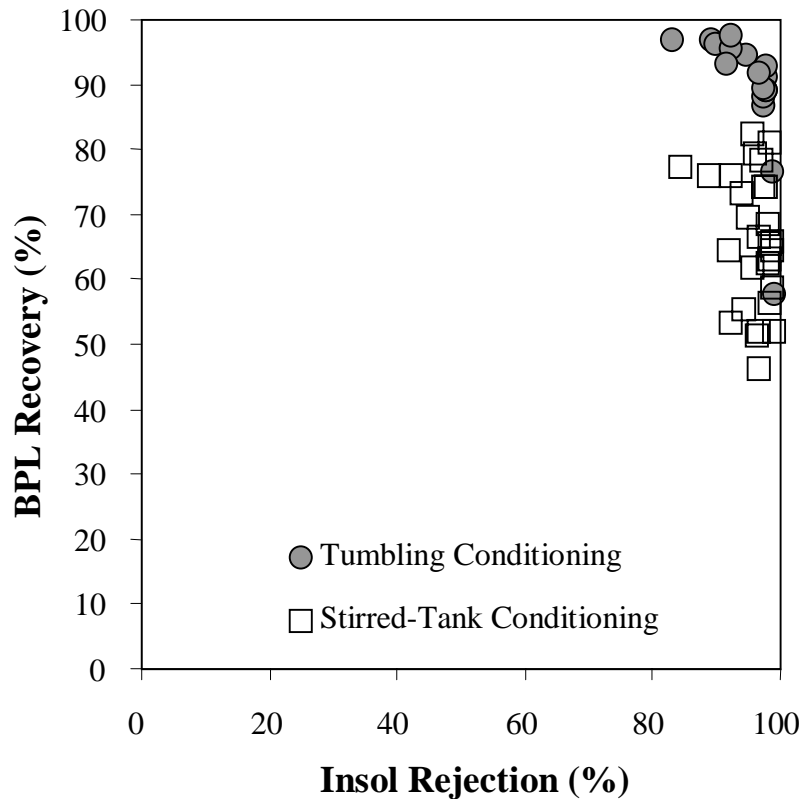


Figure 23. Recovery vs. Rejection - Stirred and Rotary Conditioners.

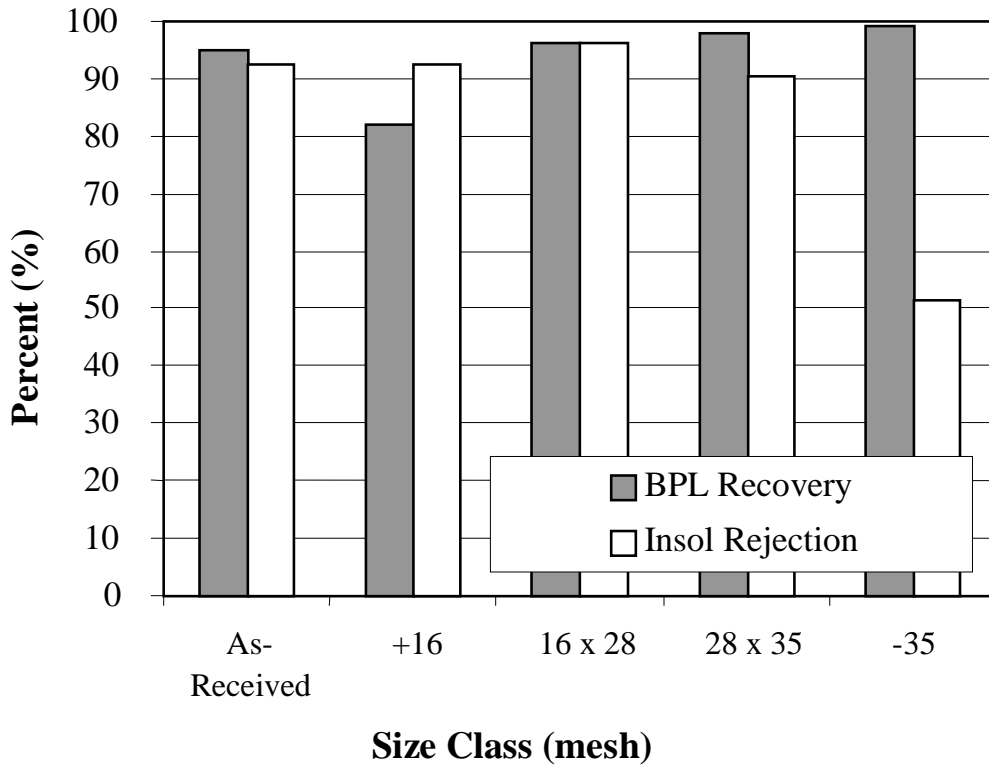


Figure 24. Size-by-Size BPL Recovery and Insols Rejection.

attention to conditioning is probably warranted at industrial sites where poor coarse particle recoveries are achieved.

The high efficiency of the HydroFloat separator can also be demonstrated by the reduced reagent addition required to maintain a high BPL recovery. The low turbulence, long retention time, and high probability of bubble/particle collision improve flotation kinetics and provide a higher overall recovery. As a result, the HydroFloat required only 0.75 lbs/ton of the fatty-acid/fuel-oil collector as shown in Figure 25. Conventional mechanical and column flotation generally requires collector addition rates between 1.0 and 1.4 lbs/ton. The reduction in reagent requirements should represent a significant cost savings for industrial users of the HydroFloat separator.

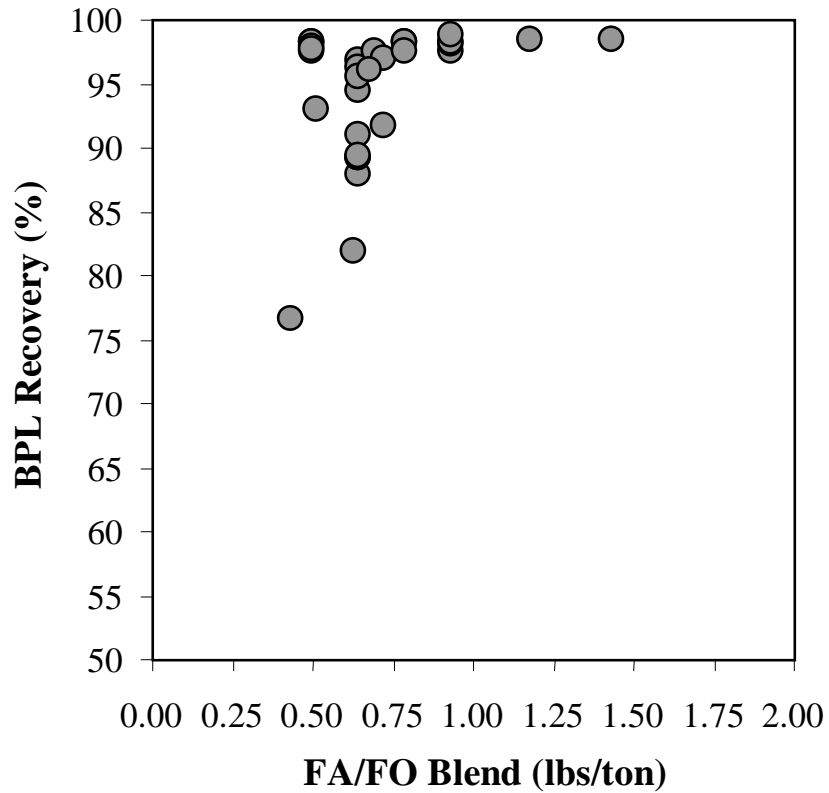


Figure 25. BPL Recovery as a Function of Collector Addition Rate.

LONG-DURATION RESULTS

As a summary to the overall pilot-scale test program, a long-term test was completed under optimized conditions to evaluate the operational stability of the HydroFloat system. A long duration test was conducted over a period of approximately 8 hours (one operational shift). In these tests, samples were collected at regular intervals and analyzed for BPL and insols content.

The results of the long duration tests are summarized in Figure 26. As shown, the HydroFloat separator achieved an extremely high BPL recovery on the coarse phosphate matrix. Over the duration of the long-term test, BPL recovery averaged 98.5%. The corresponding product BPL and insols content was maintained at 71.1% and 5.1%, respectively. It should be noted that the standard deviation for product grade and recovery was less than 1% in all cases.

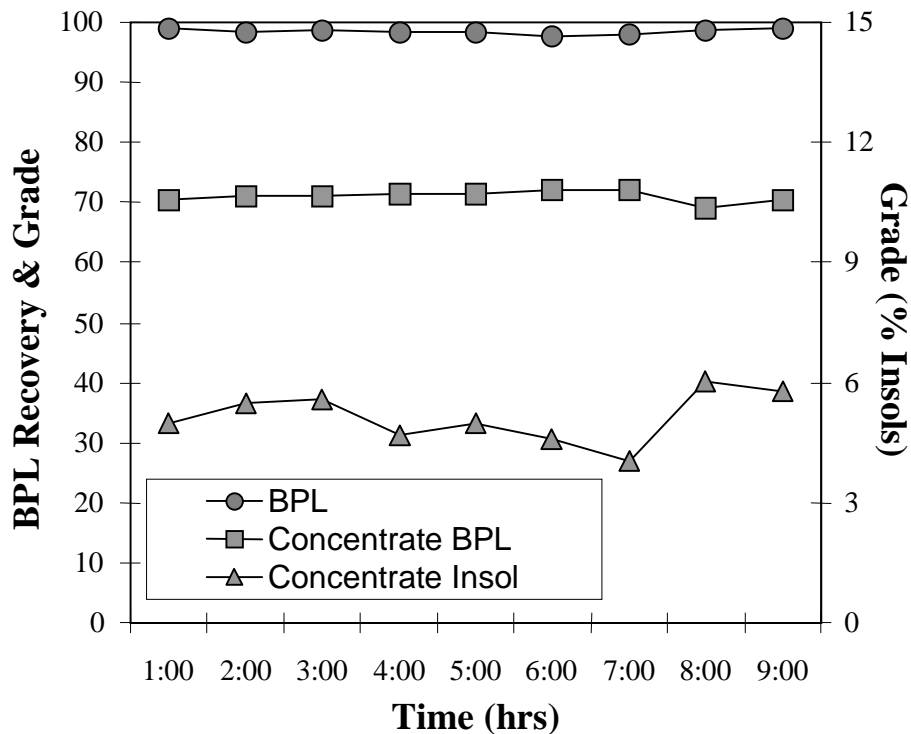


Figure 26. BPL and Insols Grade and BPL Recovery for Long Duration Testing.

PROCESS EVALUATION

A technical evaluation was conducted to examine the potential benefits of improving phosphate recovery from coarse feed to the concentrate. Concentrate production was estimated for three flotation scenarios; unsized feed (Low), sized feed with conventional cells (Medium), and sized feed utilizing the HydroFloat for coarse flotation (High). Operating costs for the three scenarios were estimated based on a “phosphate” cost model for a hypothetical mine (see 0).

Two assumed ore types were examined; Ore “1” yields all concentrate, while Ore “2” yields a 50:50 mix of pebble and concentrate. Concentrate recovery was estimated by applying standardized recovery coefficients (by size) for classification and flotation to assumed particle size analyses for each ore type (see 0). The particle size analyses are compared in Table 3.

The margins for each case were estimated from the difference between selling

Table 3. Ore 1 and Ore 2 Size Characteristics.

Mesh	Ore 1			Ore 2		
	Unsize	Coarse	Fine	Unsize	Coarse	Fine
>14	2.0%	10.9%	0.0%	2.4%	14.4%	0.0%
14/20	3.0%	15.2%	0.3%	2.5%	13.9%	0.2%
20/28	7.0%	25.5%	2.9%	4.8%	19.4%	1.9%
28/35	10.0%	20.3%	7.7%	9.1%	20.3%	6.9%
35/48	13.0%	12.5%	13.1%	13.3%	14.2%	13.1%
48/65	23.0%	9.8%	26.0%	23.7%	11.2%	26.1%
65/100	26.0%	4.8%	30.7%	26.8%	5.4%	31.0%
100/150	13.0%	1.0%	15.7%	14.4%	1.2%	17.0%
<150	3.0%	0.1%	3.6%	3.0%	0.1%	3.7%
Total	100.0%	99.9%	100.0%	100.0%	100.0%	100.0%
%Wt. Distribution	100.0	18.3	81.7	100.0	16.5	83.5
%BPL	18.6	27.8	16.5	15.9	33.3	12.4
%BPL Distribution	100.0	27.3	72.7	100.0	34.7	65.3

price (\$24/ton) and estimated operating costs, multiplied by the concentrate tonnage. Pebble tonnage, which remained constant, was not considered in the margin. The Net Present Values (NPV) of the margins were then calculated.

Ore 1. The cost model simulations for Ore 1 were based on the following annual production statistics as presented in Table 4. The production values are based on the year 2000 phosphate mine average statistics for the Fertilizer Industry (TFI). The results of the three flotation scenarios and corresponding cost estimates are summarized in Table 5.

The simulated production cost (concentrate production only) appears low compared to the industry average. The underestimation is due to estimation accuracy and

Table 4. Annual Product Statistics for Ore 1.

Operating schedule	7 days / week
No. of draglines	3
Acres mined	528*
Overburden stripped	21,100,000 bcy*
Ore recovered	15,100,000 bcy*
Ore density	1.188 dry t/bcy
Flotation feed	12,917,000 t/y
Feed %BPL	18.6

**Based on 2000 TFI Report*

Table 5. Summary of Results for Ore 1.

	Recovery Scenario		
	Low	Medium	High
%BPL Recoveries			
Coarse Flotation	na	68	92
Fine Flotation	na	86	86
Combined Flotation	76.1	81.4	88.1
Concentrate t/y	2,689,000	2,876,000	3,113,000
Production cost/ton	\$23.52	\$22.17	\$20.70

cost escalation factors such as longer pumping distances and higher labor rates, which were not updated for this exercise. Nevertheless, the simulated costs are acceptable for the following incremental analysis.

The margins, assuming \$24/ton selling price, for the scenarios are tabulated in Table 6. Also shown are the net margins and net present values. The net margins are the incremental improvement between adjacent scenarios. For example, converting from unsized feed flotation (Low) to sized feed flotation with conventional cells (Medium) increases the annual margin by \$3,972,360 (from \$1,290,720 to \$5,263,080). Similarly, converting from sized feed flotation with conventional cells (Medium) to sized feed flotation with HydroFloat (High) increases the annual margin by \$5,009,820 (from \$5,263,080 to \$10,272,900).

The net present values of the net margins over 10 years are based on a 20% discount rate. Another way of looking at the net present values is that an investment of \$16.6 million to convert from unsized feed flotation (Low) to sized feed flotation (Medium) would have a 20% internal rate of return if the plant operated for 10 years. An investment of less than \$16.6 million would have a higher return. Similarly, an

Table 6. Tabulated Values of Recovery Scenarios for Ore 1.

	Recovery Scenario		
	Low	Medium	High
Concentrate t/y	2,689,000	2,876,000	3,113,000
Revenues (tons x \$24)	\$64,536,000	\$69,024,000	\$74,712,000
Costs (tons x \$cost)	\$63,245,280	\$63,760,920	\$64,439,100
Margin	\$1,290,720	\$5,263,080	\$10,272,900
Net Margin	\$0	\$3,972,360	\$5,009,820
Net Present Value	\$0	\$16,654,008	\$21,003,531

investment of \$21 million to convert from sized feed flotation (Medium) to sized feed flotation (High) would have a 20% internal rate of return for 10 years of operation.

Ore 2. The cost model simulations for Ore 2 were based on the following annual production statistics presented in Table 7. The same phosphate mine average statistics as described for the Ore 1 simulations were used in the Ore 2 investigations. The results of the three flotation scenarios and corresponding production cost estimates are summarized in Table 8.

The margins, assuming \$24/t selling price, for the scenarios are tabulated below in Table 9. Also shown are the net margins and net present values. The net margins are the

Table 7. Annual Production Statistics for Ore 2.

Operating schedule	7 days / week
No. of draglines	3
Acres mined	528
Overburden stripped	21,100,000 bcy*
Ore recovered	15,100,000 bcy*
Ore density	1.188 dry t/bcy
Pebble	1,812,000 t/y
Flotation feed	11,105,000 t/y
Feed %BPL	15.9

**Based on 2000 TFI Report*

Table 8. Summary of Results for Ore 2.

	Recovery Scenario		
	Low	Medium	High
%BPL Recoveries			
Coarse Flotation	na	68	92
Fine Flotation	na	86	86
Combined Flotation	70.3	77.6	87.6
Concentrate t/y	1,793,000	1,979,000	2,234,000
Production cost/ton	\$16.95	\$16.29	\$15.47

Table 9. Tabulated Values of Recovery Scenarios for Ore 2.

	Recovery Scenario		
	Low	Medium	High
Concentrate t/y	1,793,000	1,979,000	2,234,000
Revenues (tons x \$24)	\$43,032,000	\$47,496,000	\$53,616,000
Costs (tons x \$cost)	\$30,391,350	\$32,237,910	\$34,559,980
Margin	\$12,640,650	\$15,258,090	\$19,056,020
Net Margin	\$0	\$2,617,440	\$3,797,930
Net Present Value	\$0	\$10,973,544	\$16,244,572

incremental improvement between adjacent scenarios. For example, converting from unsized feed flotation (Low) to sized feed flotation with conventional cells (Medium) increases the annual margin by \$2,617,440 (from \$12,640,650 to \$15,258,090). Similarly, converting from sized feed flotation with conventional cells (Medium) to sized feed flotation with HydroFloat (High) increases the annual margin by \$3,797,930 (from \$15,258,090 to \$19,056,020).

The net present values of the net margins over 10 years are based on a 20% discount rate. Another way of looking at the net present values is that an investment of \$10.9 million to convert from unsized feed flotation (Low) to sized feed flotation (Medium) would have a 20% internal rate of return if the plant operated for 10 years. An investment of less than \$10.9 million would have a higher return. Similarly, an investment of \$16.2 million to convert from sized feed flotation (Medium) to sized feed flotation (High) would have a 20% internal rate of return if the plant operated for 10 years.

The benefits of sized feed flotation are clear given the assumptions of the study. The assumptions are considered reasonable; however, they may not accurately represent

current conditions at any given plant. Clearly, if a plant feed BPL distribution is finer than the feed in this study, the benefits of improved coarse feed flotation are diminished. However, in comparing Ores 1 and 2, it is apparent that improving flotation has more significance as the relative amount of concentrate increases. In general, the remaining ore reserves are such that the Florida Phosphate Industry will see a decline in pebble production and an increase in concentrate production.

SUMMARY

A detailed test program to evaluate the Eriez HydroFloat separator for coarse phosphate flotation was completed at PCS Phosphate in White Springs, Florida. The primary objectives of this program were:

- to evaluate the principal operating parameters of the HydroFloat,
- to conduct comparison tests with an open-column flotation cell, and
- to compare a rotary, drum-type conditioner to conventional stirred-tanks for coarse phosphate (plus 35 mesh) conditioning.

To meet these objectives, nine different controllable variables were examined in the pilot-scale test program. The following generic observations can be made based on this test work:

- Increased recovery and product insols were obtained at shallower feed injection depths.
- Distribution of air/water was improved with increased spacing of water injector holes and distribution pipes.
- Increased recovery and insols were obtained with increases in the fluidization (teeter bed) water rate.
- Increased product insols were observed with increasing bed level, while bed level had little impact on recovery.
- Improved recovery was observed with higher conditioning percent solids, while no influence on product grade was noted (up to the conditioner capacity limit).
- Increased recovery and product insols were observed with increasing aeration rate.
- Decreased recovery was observed with an increase in frother addition rate.
- Increased recovery was observed with collector dosage up to an optimum plateau at 0.7 lbs/ton.

In each case, theoretical explanations can be provided to account for the observed trends in grade and/or recovery.

Comparison tests were also conducted with a standard open-column cell. The results indicate that the HydroFloat achieved a higher product recovery at a similar quality as compared to the open column. Furthermore, the HydroFloat was able to maintain performance at feed rates in excess of twice that of the standard column. A summary of results from the comparison testing is provided in Table 10. The most notable findings are the very high recovery (>98%) and high capacity (>2.5 tph/ft²) of the HydroFloat cell.

The final objective of the test program was to evaluate a rotary drum-type conditioner as compared to conventional stirred-tanks for coarse particle conditioning. These tests were conducted using a 30-inch diameter drum designed by Jacobs Engineering. Comparison tests were conducted using the HydroFloat separator in conjunction with the two conditioners. The results from these tests, which are summarized in Table 11, showed that the rotary drum design dramatically outperformed the standard stirred-tank conditioner. The drum-type conditioner provided a substantially higher BPL recovery at an identical product quality. This improvement is attributed to minimal slimes production in the drum conditioner. Conversely, the stirred-tank style tends to generate phosphate slimes (minus 325 mesh) that result in a lower recovery and increased reagent consumption. The increase in phosphate slimes results from the excessive energy required to maintain the “ultracoarse” feed in suspension without the fines fraction (35 x 150 mesh).

Table 10. HydroFloat/Column Metallurgical Comparison.

Parameter	HydroFloat	Open Column
BPL Recovery (%)	98.5	90
BPL Grade (%)	71.1	70.8
Insols Grade (%)	5.1	5.0
Max. Feed Rate (tph/ft ²)	2.5	0.6

Table 11. Conditioner Test Metallurgical Comparison.

Conditioner Type	Product Insols (%)	BPL Recovery (%)
Stirred-Tanks-in-Series	4.0-6.0	82.1
Rotary Drum	4.0-6.0	98.5

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APPENDIX A - COST SIMULATION DATA

Performance Coefficients

Microns	Sizing			Flotation			
	IP Sizer	Sizer	X-Flow	U/S Feed	C Feed	C' Feed	F Feed
1118	0.422	0.994	0.998	0.02	0.10	0.75	0.02
850	0.199	0.927	0.945	0.10	0.65	0.94	0.10
600	0.068	0.665	0.678	0.65	0.85	0.98	0.65
425	0.022	0.370	0.360	0.85	0.90	0.99	0.85
300	0.007	0.176	0.160	0.89	0.95	0.96	0.89
212	0.002	0.078	0.066	0.91	0.90	0.91	0.91
150	0.001	0.034	0.026	0.89	0.89	0.90	0.89
105	0.000	0.014	0.010	0.85	0.80	0.91	0.85
74	0.000	0.006	0.004	0.75	0.75	0.96	0.75

Identification Code: No Pebble Case (unsized feed)
 Data File Dated: 25-Feb-02

PRODUCTION DATA & RATES

Operating Schedule:	7	Days per Week
Number of Draglines:	3	Operating
Area Mined:	528	Acres per Year
Volume Stripped:	21.1	Million bcy/y
Ore Recovered:	15.1	Million bcy/y
Ore Density:	88	Dry pcf

Process	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	10.228	28.127
Pebble	0.000	0.000
Concentrate	2.689	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	4.62
2	Reagents_____	1.88
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.88
5	Dam Building_____	0.90
6	Operating Labor_____	2.39
7	Contract Maintenance_____	0.73
8	Maintenance Labor_____	1.56
9	Maintenance Materials_____	2.84
10	Operating Supplies_____	0.76
11	Operating Services_____	0.90
12	Autos & Trucks_____	0.10
13	Insurance_____	0.07
14	Taxes_____	0.61
15	Mine Overhead_____	1.18
16	Other_____	0.06
17	Subtotal Cost	21.09
18	Depreciation_____	1.65
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	23.52

Identification Code: No Pebble Case (Base)
 Data File Dated: 25-Feb-02

PRODUCTION DATA & RATES

Operating Schedule:	7	Days per Week
Number of Draglines:	3	Operating
Area Mined:	528	Acres per Year
Volume Stripped:	21.1	Million bcy/y
Ore Recovered:	15.1	Million bcy/y
Ore Density:	88	Dry pcf

Process	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	10.041	27.612
Pebble	0.000	0.000
Concentrate	2.876	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	4.31
2	Reagents_____	1.78
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.83
5	Dam Building_____	0.84
6	Operating Labor_____	2.24
7	Contract Maintenance_____	0.68
8	Maintenance Labor_____	1.45
9	Maintenance Materials_____	2.66
10	Operating Supplies_____	0.71
11	Operating Services_____	0.84
12	Autos & Trucks_____	0.10
13	Insurance_____	0.07
14	Taxes_____	0.57
15	Mine Overhead_____	1.10
16	Other_____	0.06
17	Subtotal Cost	19.86
18	Depreciation_____	1.55
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	22.17

Identification Code: No Pebble Case (Hydraflot)
 Data File Dated: 25-Feb-02

PRODUCTION DATA & RATES

Operating Schedule: 7 Days per Week
 Number of Draglines: 3 Operating
 Area Mined: 528 Acres per Year
 Volume Stripped: 21.1 Million bcy/y
 Ore Recovered: 15.1 Million bcy/y
 Ore Density: 88 Dry pcf

Process	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	9.804	26.961
Pebble	0.000	0.000
Concentrate	3.113	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	3.98
2	Reagents_____	1.68
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.76
5	Dam Building_____	0.78
6	Operating Labor_____	2.07
7	Contract Maintenance_____	0.63
8	Maintenance Labor_____	1.34
9	Maintenance Materials_____	2.47
10	Operating Supplies_____	0.65
11	Operating Services_____	0.77
12	Autos & Trucks_____	0.10
13	Insurance_____	0.06
14	Taxes_____	0.52
15	Mine Overhead_____	1.02
16	Other_____	0.05
17	Subtotal Cost	18.51
18	Depreciation_____	1.43
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	20.70

Identification Code: Pebble Case (unsized feed)
 Data File Dated: 26-Feb-02

PRODUCTION DATA & RATES

Operating Schedule: 7 Days per Week
 Number of Draglines: 3 Operating
 Area Mined: 528 Acres per Year
 Volume Stripped: 21.1 Million bcy/y
 Ore Recovered: 15.1 Million bcy/y
 Ore Density: 88 Dry pcf

Process <u>Stream</u>	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	9.150	25.163
Pebble	1.973	0.000
Concentrate	1.793	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	3.11
2	Reagents_____	1.08
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.63
5	Dam Building_____	0.64
6	Operating Labor_____	1.71
7	Contract Maintenance_____	0.52
8	Maintenance Labor_____	1.11
9	Maintenance Materials_____	1.95
10	Operating Supplies_____	0.53
11	Operating Services_____	0.63
12	Autos & Trucks_____	0.10
13	Insurance_____	0.05
14	Taxes_____	0.43
15	Mine Overhead_____	0.84
16	Other_____	0.04
17	Subtotal Cost	15.00
18	Depreciation_____	1.18
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	16.95

Identification Code: Pebble Case (Base)
 Data File Dated: 26-Feb-02

PRODUCTION DATA & RATES

Operating Schedule:	7	Days per Week
Number of Draglines:	3	Operating
Area Mined:	528	Acres per Year
Volume Stripped:	21.1	Million bcy/y
Ore Recovered:	15.1	Million bcy/y
Ore Density:	88	Dry pcf

Process	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	8.964	24.651
Pebble	1.973	0.000
Concentrate	1.979	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	2.95
2	Reagents_____	1.05
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.60
5	Dam Building_____	0.61
6	Operating Labor_____	1.63
7	Contract Maintenance_____	0.49
8	Maintenance Labor_____	1.06
9	Maintenance Materials_____	1.87
10	Operating Supplies_____	0.50
11	Operating Services_____	0.60
12	Autos & Trucks_____	0.10
13	Insurance_____	0.05
14	Taxes_____	0.41
15	Mine Overhead_____	0.80
16	Other_____	0.04
17	Subtotal Cost	14.39
18	Depreciation_____	1.13
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	16.29

Identification Code: Pebble Case (Hydraflot)
 Data File Dated: 27-Feb-02

PRODUCTION DATA & RATES

Operating Schedule:	7	Days per Week
Number of Draglines:	3	Operating
Area Mined:	528	Acres per Year
Volume Stripped:	21.1	Million bcy/y
Ore Recovered:	15.1	Million bcy/y
Ore Density:	88	Dry pcf

Process <u>Stream</u>	Million <u>Tons/Year</u>	Million <u>Ton-Miles</u>
Mud Balls	0.179	0.045
Clays	4.844	7.266
Tailings	8.709	23.950
Pebble	1.973	0.000
Concentrate	2.234	0.000
Ore	17.940	53.820

Phosphate Rock Production Cost

	<u>COST ELEMENT</u>	<u>\$/PRODUCT TON</u>
1	Electricity_____	2.77
2	Reagents_____	1.01
3	Severance Tax_____	1.62
4	Land Reclamation_____	0.56
5	Dam Building_____	0.58
6	Operating Labor_____	1.53
7	Contract Maintenance_____	0.46
8	Maintenance Labor_____	0.99
9	Maintenance Materials_____	1.76
10	Operating Supplies_____	0.47
11	Operating Services_____	0.56
12	Autos & Trucks_____	0.10
13	Insurance_____	0.04
14	Taxes_____	0.39
15	Mine Overhead_____	0.75
16	Other_____	0.04
17	Subtotal Cost	13.65
18	Depreciation_____	1.06
19	Depletion & Royalties_____	0.77
20	Production Cost FOB Mine	15.47

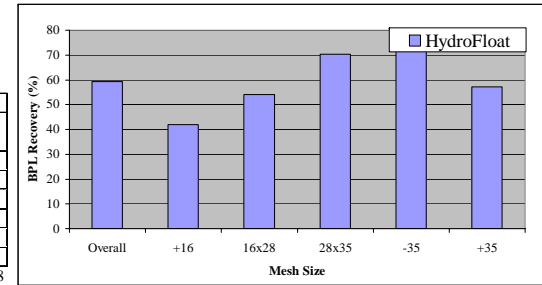
APPENDIX B – TEST RESULTS

Operating Conditions	Data
Test No. 7	13-Oct-00
CrossFlow	
Level (#):	85
Elutriation Rate (gpm):	460
Elutriation Rate (gpm/sqft):	18.4
Underflow Solids (%)	75
Conditioner	
Feed Rate (tph):	4.0
Percent Solids (%):	?
HydroFloat	
Feed Rate (tph/sqft):	1.0
Feed System:	V-Notch
No. of Baffles:	1
Level (s.p.):	74
Level (#):	4
Elutriation Rate (gpm):	80
Elutriation Rate (gpm/sqft):	20.0
Air Meter Reading (No.):	1.05
Aeration Rate (lpm):	n/a
Aeriation Rate (cfm):	n/a
Chemicals	
Frother Stroke:	26
Frother Frequency:	75
Frother Addition Rate (lb/ton):	insert eqn.
Fatty-Acid Stroke:	20
Fatty-Acid Frequency:	18
Fatty-Acid Addition Rate (lb/ton):	0.68
Ammonia Stroke:	20
Ammonia Frequency:	46
Ammonia Addition Rate (lb/ton):	insert eqn.
Test pH:	>9
**Notes	
High Bed Level	
Extremely low air	
FA Freq increased	

At the end of the test, i.e. after the samples were taken The feed rate went up to 23 sec/5 gal, It may have jumped up at the end of the test or been a gradual increase through the test. This is another instance where a better feed control valve would help the project. The unit sanded out as a result of the feed increase and the %solids reading was not able to be taken.

Mass Balance																
Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)			
	Feed	Underflow	Underflow	Feed	Underflow	Underflow	Feed	Underflow	Underflow	Feed	Underflow	Underflow	Feed	Underflow	Underflow	
Unbalanced Sample Data																
Head	--	--	--	100.0	50.0	50.0	28.7	68.2	17.0	47.7	6.0	75.7	100.0	50.0	50.0	
+16	87.9	93	87.1	14.9	13.4	14.3	37.8	70.0	30.5	47.6	4.4	56.9	14.9	6.7	7.2	
16x28	316.5	226	315.5	53.5	32.6	51.9	19.7	69.8	12.0	71.4	4.3	82.6	53.5	16.3	25.9	
28x35	152.9	256.9	177.8	25.8	37.1	29.2	31.1	67.4	13.7	57.6	7.3	79.7	25.8	18.5	14.6	
-35	34.2	116.8	27.6	5.8	16.9	4.5	67.1	70.0	47.6	9.4	5.9	33.8	5.8	8.4	2.3	
Balanced Sample Data																
Head	n/a	n/a	n/a	100.0	25.5	74.5	29.4	68.5	16.1	56.0	5.7	73.2	100.0	25.5	74.5	
+16	n/a	n/a	n/a	14.5	13.5	14.8	39.1	68.6	29.9	45.2	4.4	58.0	14.5	3.5	11.0	
16x28	n/a	n/a	n/a	49.8	32.8	55.6	21.1	67.9	11.6	66.5	4.4	79.1	49.8	8.4	41.4	
28x35	n/a	n/a	n/a	28.9	36.7	26.3	31.0	67.2	13.6	53.6	7.5	75.7	28.9	9.4	19.6	
-35	n/a	n/a	n/a	6.8	17.0	3.4	63.5	72.5	48.0	11.9	5.4	23.1	6.8	4.3	2.5	
				head assay check:				100				100				
				head assay constraint:				0.0				0.0				
Relative Error																
Head	n/a	n/a	n/a	1.0	5.0	5.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
Relative Change																
Head	n/a	n/a	n/a	0.0	-49.0	49.0	2.6	0.5	-5.3	17.3	-5.6	-3.4	0.0	-49.0	49.0	
+16	n/a	n/a	n/a	-2.8	0.8	3.1	3.5	-2.0	-2.0	-5.0	0.6	1.9	-2.8	-48.6	53.6	
16x28	n/a	n/a	n/a	-7.0	0.5	7.1	7.2	-2.7	-2.9	-6.8	1.3	-4.3	-7.0	-48.7	59.6	
28x35	n/a	n/a	n/a	12.0	-1.1	-10.1	-0.3	-0.2	-0.6	-6.9	2.1	-5.0	12.0	-49.5	34.0	
-35	n/a	n/a	n/a	18.1	0.7	-26.1	-5.3	3.6	0.9	25.7	-9.0	-31.6	18.1	-48.6	10.2	
Weighted Sum of Squares																
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
-35	n/a	n/a	n/a	0.0	0.0	0.1	0.0	0.0	0.0	0.1	0.0	0.1	0.0	0.0	0.0	
											Sum:		0.4			
											Mass Rate Constraints					
											(Mass)			BPL	Insol	
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
-35	n/a	n/a	n/a	0.0	0.0	0.1	0.0	0.0	0.0	0.1	0.0	0.1	0.0	0.0	0.0	

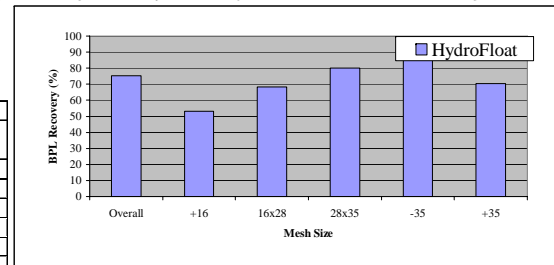
HydroFloat Performance Results										
Size (mesh)	Feed Grade (%) BPL	Feed Grade (%) Insol	Con Grade (%) BPL	Con Grade (%) Insol	Tail Grade (%) BPL	Tail Grade (%) Insol	BPL Rec. (%)	Insol Rej. (%)		
Overall	29.4	56.0	68.5	5.7	16.1	73.2	59.4	97.4		
+16	39.1	45.2	68.6	4.4	29.9	58.0	41.9	97.7		
16x28	21.1	66.5	67.9	4.4	11.6	79.1	54.1	98.9		
28x35	31.0	53.6	67.2	7.5	13.6	75.7	70.2	95.5		
-35	63.5	11.9	72.5	5.4	48.0	23.1	72.4	71.2		
+35	26.9	59.2	67.7	5.7	14.9	74.9	57.1	97.8		
HydroFloat Feed > 35 Mesh (%)				93.2			22.725448	22.725448		



Operating Conditions	Data
Test No. 1	13-Oct-00
CrossFlow	
Level (#):	85
Elutriation Rate (gpm):	460
Elutriation Rate (gpm/sqft):	18.4
Underflow Solids (%):	75
Conditioner	
Feed Rate (tph):	4.0
Percent Solids (%):	55
HydroFloat	
Feed Rate (tph/sqft):	1.0
Feed System:	V-Notch
No. of Baffles:	0
Level (s.p.):	74
Level (#):	4
Elutriation Rate (gpm):	100
Elutriation Rate (gpm/sqft):	20.0
Air Meter Reading (No.):	1.00
Aeration Rate (lpm):	n/a
Aeration Rate (cfm):	n/a
Chemicals	
Frother Stroke:	19
Frother Frequency:	50
Frother Addition Rate (lb/ton):	insert eqn.
Fatty-Acid Stroke:	20
Fatty-Acid Frequency:	40
Fatty-Acid Addition Rate (lb/ton):	1.37
Ammonia Stroke:	20
Ammonia Frequency:	46
Ammonia Addition Rate (lb/ton):	insert eqn.
Test pH:	>9
**Notes	
High Bed Level	

Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)			
	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	
Unbalanced Sample Data																
Head	--	--	--	100.0	50.0	50.0	27.1	71.2	9.8	62.4	4.2	85.7	100.0	50.0	50.0	
+16	50.9	68.5	40.3	8.2	9.8	8.0	39.5	69.7	29.5	44.4	3.8	57.9	8.2	4.9	4.0	
16x28	256.8	177	237.5	41.1	25.3	47.2	20.7	70.6	7.6	71.1	3.9	89.0	41.1	12.6	23.6	
28x35	225.2	231.8	191.7	36.1	33.1	38.1	21.4	70.6	5.9	70.1	4.5	91.3	36.1	16.5	19.1	
-35	91.6	223.1	33.4	14.7	31.9	6.6	54.4	71.4	20.2	25.9	4.1	72.0	14.7	15.9	3.3	
Balanced Sample Data																
Head	n/a	n/a	n/a	100.0	29.3	70.7	27.4	70.5	9.6	62.1	4.2	86.1	100.0	29.3	70.7	
+16	n/a	n/a	n/a	8.4	9.4	8.1	41.5	67.6	28.9	42.1	3.8	60.6	8.4	2.8	5.7	
16x28	n/a	n/a	n/a	40.6	25.8	46.8	19.8	72.5	7.7	72.1	3.9	87.8	40.6	7.6	33.1	
28x35	n/a	n/a	n/a	36.6	32.2	38.5	22.1	68.7	5.9	69.5	4.5	92.0	36.6	9.4	27.2	
-35	n/a	n/a	n/a	14.3	32.6	6.7	54.5	71.4	20.2	26.2	4.1	71.1	14.3	9.6	4.7	
				head assay check:			100	100	27.4	70.5	9.6	62.1	4.2	86.1		
				head assay constraint:			0.0	0.0	0.0	0.0	0.0	0.0	0.0			
Relative Error																
Head	n/a	n/a	n/a	1.0	5.0	5.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
Relative Change																
Head	n/a	n/a	n/a	0.0	-41.4	41.4	1.0	-1.1	-2.5	-0.6	-0.8	0.4	0.0	-41.4	41.4	
+16	n/a	n/a	n/a	3.6	-4.1	0.5	5.2	-3.0	-2.1	-5.3	0.2	4.6	3.6	-43.8	42.1	
16x28	n/a	n/a	n/a	-1.2	2.3	-0.9	-4.3	2.8	2.1	1.5	0.2	-1.4	-1.2	-40.0	40.0	
28x35	n/a	n/a	n/a	1.6	-2.7	1.0	3.2	-2.7	-0.1	-0.8	0.3	0.8	1.6	-43.0	42.7	
-35	n/a	n/a	n/a	-2.8	2.3	0.4	0.1	0.0	0.3	1.4	0.1	-1.2	-2.8	-40.0	41.9	
Weighted Sum of Squares																
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
												Mass Rate Constraints				
												Sum:	0.0	(Mass)	BPL	Insol
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	

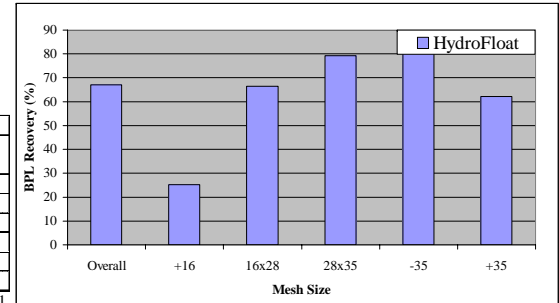
HydroFloat Performance Results									
Size (mesh)	Feed Grade (%) BPL	Feed Grade (%) Insol	Con Grade (%) BPL	Con Grade (%) Insol	Tail Grade (%) BPL	Tail Grade (%) Insol	BPL Rec. (%)	Insol Rej. (%)	
Overall	27.4	62.1	70.5	4.2	9.6	86.1	75.3	98.0	
+16	41.5	42.1	67.6	3.8	28.9	60.6	53.1	97.1	
16x28	19.8	72.1	72.5	3.9	7.7	87.8	68.3	99.0	
28x35	22.1	69.5	68.7	4.5	5.9	92.0	80.1	98.3	
-35	54.5	26.2	71.4	4.1	20.2	71.1	87.7	89.5	
+35	22.9	68.0	70.0	4.2	8.8	87.2	70.45	98.6	
HydroFloat Feed > 35 Mesh (%)					85.7	23.054535 23.054535			



Operating Conditions	Data
Test No. 2	13-Oct-00
CrossFlow	
Level (#):	85
Elutriation Rate (gpm):	460
Elutriation Rate (gpm/sqft):	18.4
Underflow Solids (%):	75
Conditioner	
Feed Rate (tph):	3.8
Percent Solids (%):	65
HydroFloat	
Feed Rate (tph/sqft):	1.0
Feed System:	V-Notch
No. of Baffles:	0
Level (s.p.):	72
Level (#):	3
Elutriation Rate (gpm):	100
Elutriation Rate (gpm/sqft):	20.0
Air Meter Reading (No.):	1.00
Aeration Rate (lpm):	n/a
Aeration Rate (cfm):	n/a
Chemicals	
Frother Stroke:	19
Frother Frequency:	50
Frother Addition Rate (lb/ton):	insert eqn.
Fatty-Acid Stroke:	20
Fatty-Acid Frequency:	40
Fatty-Acid Addition Rate (lb/ton):	1.45
Ammonia Stroke:	20
Ammonia Frequency:	46
Ammonia Addition Rate (lb/ton):	insert eqn.
Test pH:	>9
**Notes	
Recirculation valve craked open	

Mass Balance																
Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)			
	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	
Unbalanced Sample Data																
Head	--	--	--	100.0	50.0	50.0	29.0	71.2	16.2	59.5	3.9	76.3	100.0	50.0	50.0	
+16	116	37.9	54.5	15.8	5.9	15.6	38.9	70.9	34.3	44.8	2.9	52.2	15.8	3.0	7.8	
16x28	342.3	240.1	168	46.7	37.6	48.0	20.9	70.9	11.0	70.8	3.0	84.0	46.7	18.8	24.0	
28x35	183.2	228.1	109.9	25.0	35.7	31.4	29.8	71.1	10.0	58.4	3.3	85.6	25.0	17.9	15.7	
-35	91.6	132.5	17.6	12.5	20.7	5.0	63.3	70.3	31.9	13.1	5.5	55.4	12.5	10.4	2.5	
Balanced Sample Data																
Head	n/a	n/a	n/a	100.0	31.6	68.4	31.9	67.5	15.4	55.7	3.7	79.7	100.0	31.6	68.4	
+16	n/a	n/a	n/a	13.6	6.1	17.1	39.3	70.6	34.2	45.1	2.9	52.0	13.6	1.9	11.7	
16x28	n/a	n/a	n/a	46.3	36.1	51.0	23.5	63.1	10.5	67.2	3.0	88.2	46.3	11.4	34.9	
28x35	n/a	n/a	n/a	29.2	33.1	27.4	30.9	68.3	10.0	57.4	3.4	87.4	29.2	10.5	18.8	
-35	n/a	n/a	n/a	10.9	24.7	4.5	60.8	72.2	32.1	15.7	5.2	42.1	10.9	7.8	3.1	
				head assay check:		100	100	31.9	67.5	15.4	55.7	3.7	79.7			
				head assay constraint:		0.0	0.0	0.0	0.0	0.0	0.0	0.0				
Relative Error																
Head	n/a	n/a	n/a	1.0	5.0	5.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a	
Relative Change																
Head	n/a	n/a	n/a	0.0	-36.8	36.8	9.7	-5.2	-5.3	-6.4	-4.5	4.5	0.0	-36.8	36.8	
+16	n/a	n/a	n/a	-14.2	2.1	9.6	1.0	-0.4	-0.2	0.6	0.2	-0.5	-14.2	-35.5	49.9	
16x28	n/a	n/a	n/a	-0.9	-3.9	6.2	12.1	-10.9	-4.2	-5.0	1.3	5.1	-0.9	-39.2	45.2	
28x35	n/a	n/a	n/a	17.0	-7.3	-12.6	3.7	-3.9	-0.5	-1.8	1.4	2.2	17.0	-41.4	19.6	
-35	n/a	n/a	n/a	-12.8	18.9	-9.8	-4.0	2.7	0.7	20.0	-4.3	-24.0	-12.8	-24.8	23.4	
Weighted Sum of Squares																
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.1	0.0	0.0	0.0	
												Mass Rate Constraints				
												Sum:	0.3	(Mass)	BPL	Insol
												0.0	0.0	0.0	0.0	
												0.0	0.0	0.0	0.0	
												0.0	0.0	0.0	0.0	
												0.0	0.0	0.0	0.0	

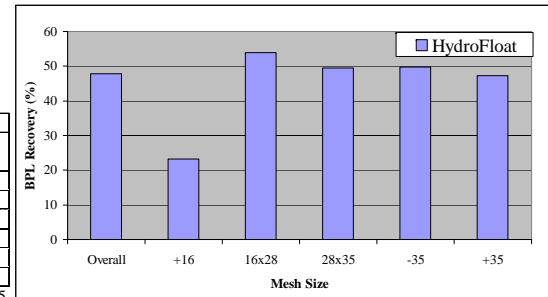
HydroFloat Performance Results								
Size (mesh)	Feed Grade (%) BPL	Feed Grade (%) Insol	Con Grade (%) BPL	Con Grade (%) Insol	Tail Grade (%) BPL	Tail Grade (%) Insol	BPL Rec. (%)	Insol Rej. (%)
Overall	31.9	55.7	67.5	3.7	15.4	79.7	67.0	97.9
+16	39.3	45.1	70.6	2.9	34.2	52.0	25.3	99.1
16x28	23.5	67.2	63.1	3.0	10.5	88.2	66.4	98.9
28x35	30.9	57.4	68.3	3.4	10.0	87.4	79.2	97.9
-35	60.8	15.7	72.2	5.2	32.1	42.1	85.0	76.3
+35	28.3	60.6	66.0	3.2	14.6	81.5	62.3	98.6
HydroFloat Feed > 35 Mesh (%)				89.1			26.71791	26.71791



Operating Conditions	Data
Test No. 3	13-Oct-00
CrossFlow	
Level (#):	85
Elutriation Rate (gpm):	460
Elutriation Rate (gpm/sqft):	18.4
Underflow Solids (%)	75
Conditioner	
Feed Rate (tph):	4.1
Percent Solids (%):	62
HydroFloat	
Feed Rate (tph/sqft):	1.0
Feed System:	V-Notch
No. of Baffles:	0
Level (s.p.):	75
Level (#):	4
Elutriation Rate (gpm):	80
Elutriation Rate (gpm/sqft):	20.0
Air Meter Reading (No.):	1.05
Aeration Rate (lpm):	n/a
Aeriation Rate (cfm):	n/a
Chemicals	
Frother Stroke:	24
Frother Frequency:	75
Frother Addition Rate (lb/ton):	insert eqn.
Fatty-Acid Stroke:	20
Fatty-Acid Frequency:	15
Fatty-Acid Addition Rate (lb/ton):	0.55
Ammonia Stroke:	20
Ammonia Frequency:	46
Ammonia Addition Rate (lb/ton):	insert eqn.
Test pH:	>9
**Notes	
High Bed Level	
Extremely low air	

Mass Balance															
Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)		
	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow
Unbalanced Sample Data															
Head	--	--	--	100.0	50.0	50.0	28.2	66.8	18.7	60.4	9.6	73.5	100.0	50.0	50.0
+16	37	32.9	61.9	9.0	5.2	9.6	39.3	70.2	32.4	45.6	3.9	54.6	9.0	2.6	4.8
16x28	158.2	240.1	273.4	38.5	37.9	42.5	18.7	69.3	12.9	75.5	6.2	81.4	38.5	18.9	21.2
28x35	164.3	228.1	265.2	40.0	36.0	41.2	24.8	63.8	15.6	65.5	13.8	78.0	40.0	18.0	20.6
-35	51.5	132.5	43.3	12.5	20.9	6.7	61.9	67.6	56.9	14.5	7.9	22.0	12.5	10.5	3.4
Balanced Sample Data															
Head	n/a	n/a	n/a	100.0	20.8	79.2	28.4	65.2	18.7	60.7	9.3	74.3	100.0	20.8	79.2
+16	n/a	n/a	n/a	8.8	5.3	9.7	37.9	70.9	33.2	46.9	3.9	53.0	8.8	1.1	7.7
16x28	n/a	n/a	n/a	40.9	35.4	42.3	21.2	63.5	11.9	70.7	6.3	84.9	40.9	7.4	33.5
28x35	n/a	n/a	n/a	40.0	36.8	40.8	24.9	64.3	15.5	65.4	14.0	77.6	40.0	7.7	32.3
-35	n/a	n/a	n/a	10.4	22.6	7.2	61.9	68.0	56.9	15.1	7.8	21.2	10.4	4.7	5.7
				head assay check:			100	100	100	head assay constraint:			0.0	0.0	0.0
Relative Error															
Head	n/a	n/a	n/a	1.0	5.0	5.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
Relative Change															
Head	n/a	n/a	n/a	0.0	-58.4	58.4	0.6	-2.4	-0.2	0.6	-2.8	1.0	0.0	-58.4	58.4
+16	n/a	n/a	n/a	-2.4	1.2	1.1	-3.6	1.0	2.6	2.7	0.0	-3.0	-2.4	-57.9	60.1
16x28	n/a	n/a	n/a	6.2	-6.6	-0.3	13.6	-8.3	-7.8	-6.3	0.7	4.3	6.2	-61.1	57.9
28x35	n/a	n/a	n/a	0.0	2.2	-1.0	0.4	0.8	-0.2	-0.2	1.4	-0.6	0.0	-57.4	56.8
-35	n/a	n/a	n/a	-17.3	7.9	6.3	0.0	0.6	-0.1	4.2	-0.5	-3.6	-17.3	-55.1	68.3
Weighted Sum of Squares															
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
											Sum:		0.1	Mass Rate Constraints	
											(Mass)		BPL	Insol	
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0

HydroFloat Performance Results								
Size (mesh)	Feed Grade (%) BPL	Feed Grade (%) Insol	Con Grade (%) BPL	Con Grade (%) Insol	Tail Grade (%) BPL	Tail Grade (%) Insol	BPL Rec. (%)	Insol Rej. (%)
Overall	28.4	60.7	65.2	9.3	18.7	74.3	47.9	96.8
+16	37.9	46.9	70.9	3.9	33.2	53.0	23.3	99.0
16x28	21.2	70.7	63.5	6.3	11.9	84.9	53.9	98.4
28x35	24.9	65.4	64.3	14.0	15.5	77.6	49.6	95.9
-35	61.9	15.1	68.0	7.8	56.9	21.2	49.8	76.5
+35	24.5	66.0	64.4	9.8	15.7	78.4	47.3	97.3
HydroFloat Feed > 35 Mesh (%)				89.6	17.989445 17.989445			



Operating Conditions	Data
Test No. 4	13-Oct-00
CrossFlow	
Level (#):	85
Elutriation Rate (gpm):	460
Elutriation Rate (gpm/sqft):	18.4
Underflow Solids (%):	75
Conditioner	
Feed Rate (tph):	4.0
Percent Solids (%):	62
HydroFloat	
Feed Rate (tph/sqft):	1.0
Feed System:	V-Notch
No. of Baffles:	1
Level (s.p.):	75
Level (#):	4
Elutriation Rate (gpm):	80
Elutriation Rate (gpm/sqft):	20.0
Air Meter Reading (No.):	1.05
Aeration Rate (lpm):	n/a
Aeration Rate (cfm):	n/a
Chemicals	
Frother Stroke:	24
Frother Frequency:	75
Frother Addition Rate (lb/ton):	insert eqn.
Fatty-Acid Stroke:	20
Fatty-Acid Frequency:	15
Fatty-Acid Addition Rate (lb/ton):	0.55
Ammonia Stroke:	20
Ammonia Frequency:	46
Ammonia Addition Rate (lb/ton):	insert eqn.
Test pH:	>9
**Notes	
High Bed Level	
Extremely low air	
Baffle hung 1 3/4' from surface	

Mass Balance															
Size (mesh)	Mass (g)			Percent Mass (%)			BPL Content (%)			Insol Content (%)			Mass Rate (tph)		
	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow	Feed	Overflow	Underflow
Unbalanced Sample Data															
Head	--	--	--	100.0	50.0	50.0	29.7	69.5	19.2	24.1	6.0	72.9	100.0	50.0	50.0
+16	74.9	28.4	73.5	11.0	8.1	9.6	37.8	69.9	32.9	46.9	4.1	53.9	11.0	4.1	4.8
16x28	299.6	81.5	351.7	44.2	23.3	45.9	20.0	70.1	13.5	72.0	4.5	81.1	44.2	11.7	22.9
28x35	236	130.3	287.1	34.8	37.3	37.5	28.4	68.8	16.3	11.6	7.2	76.9	34.8	18.6	18.7
-35	67.6	109.2	54	10.0	31.3	7.0	65.0	69.6	55.9	60.2	6.8	23.5	10.0	15.6	3.5
Balanced Sample Data															
Head	n/a	n/a	n/a	100.0	20.8	79.2	29.9	69.7	19.4	35.3	6.1	42.9	100.0	20.8	79.2
+16	n/a	n/a	n/a	9.9	8.3	10.3	38.7	69.3	32.2	44.7	4.1	53.4	9.9	1.7	8.1
16x28	n/a	n/a	n/a	40.7	24.1	45.1	20.2	69.5	13.3	59.3	4.5	67.0	40.7	5.0	35.7
28x35	n/a	n/a	n/a	38.1	39.5	37.7	27.9	69.3	16.4	12.7	6.9	14.3	38.1	8.2	29.8
-35	n/a	n/a	n/a	11.4	28.1	7.0	63.5	70.4	56.2	16.4	7.0	26.4	11.4	5.9	5.5
head assay check:				100	100	100	29.9	69.7	19.4	35.3	6.1	42.9			
head assay constraint:							0.0	0.0	0.0	0.0	0.0	0.0			
Relative Error															
Head	n/a	n/a	n/a	1.0	5.0	5.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
+16	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
16x28	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
28x35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
-35	n/a	n/a	n/a	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	n/a	n/a	n/a
Relative Change															
Head	n/a	n/a	n/a	0.0	-58.3	58.3	0.5	0.3	1.3	46.2	1.6	-41.1	0.0	-58.3	58.3
+16	n/a	n/a	n/a	-10.6	2.2	7.2	2.5	-0.9	-2.1	-4.5	-0.2	-1.0	-10.6	-57.4	69.7
16x28	n/a	n/a	n/a	-7.9	3.2	-1.8	1.4	-0.8	-1.4	-17.7	-0.6	-17.4	-7.9	-57.0	55.5
28x35	n/a	n/a	n/a	9.3	6.0	0.5	-2.0	0.8	0.4	10.3	-3.3	-81.3	9.3	-55.8	59.1
-35	n/a	n/a	n/a	14.0	-10.2	-1.2	-2.2	1.1	0.6	-72.7	3.0	12.2	14.0	-62.6	56.5
Weighted Sum of Squares															
Head	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.2	0.0	0.2	0.0	0.0	0.0
+16	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
16x28	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
28x35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0
-35	n/a	n/a	n/a	0.0	0.0	0.0	0.0	0.0	0.0	0.5	0.0	0.0	0.0	0.0	0.0
										Mass Rate Constraints					
										Sum:	1.8	(Mass)	BPL	Insol	

HydroFloat Performance Results								
Size (mesh)	Feed Grade (%) BPL	Feed Grade (%) Insol	Con Grade (%) BPL	Con Grade (%) Insol	Tail Grade (%) BPL	Tail Grade (%) Insol	BPL Rec. (%)	Insol Rej. (%)
Overall	29.9	35.3	69.7	6.1	19.4	42.9	48.6	96.4
+16	38.7	44.7	69.3	4.1	32.2	53.4	31.4	98.4
16x28	20.2	59.3	69.5	4.5	13.3	67.0	42.3	99.1
28x35	27.9	12.7	69.3	6.9	16.4	14.3	53.9	88.2
-35	63.5	16.4	70.4	7.0	56.2	26.4	57.0	78.0
+35	25.6	37.7	69.4	5.8	16.6	44.2	45.9	97.4
HydroFloat Feed > 35 Mesh (%)				88.6			16.910678	16.910678

