

Evaluation of cocoa (*Theobroma cacao*) bean processing strategies to enhance α -glucosidase inhibitory activity of dietary cocoa

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ABSTRACT

Cocoa beans (*Theobroma cacao*) are a highly concentrated source of dietary flavanols- bioactive compounds associated with the health protective properties of cocoa. Cocoa beans undergo processing steps, such as fermentation, roasting, winnowing, grinding, pressing, etc., to produce a final product with specific desirable sensory attributes. It is well established that these processing steps, specifically fermentation and roasting, result in dramatic degradation of cocoa's native flavanols, but it is possible that these processing steps may generate compounds with novel activities, potentially preserving or enhancing bioactivity. Raw unfermented cocoa beans were processed by way of a partial factorial approach to produce cocoa powders from the same batch of raw beans using various combinations of fermentation [unfermented, cool fermented (maximum 46°C), hot fermented (maximum 60°C)] and roasting [unroasted, cool roasted (120°C), hot roasted (170°C)]. To simulate cocoa fermentation in a highly controlled environment, a pilot-scale fermentation model system was employed to eliminate many external unknowns and ensure that the differences between our cocoa powders were due to our various treatments, rather than unknown factors occurring during fermentation and roasting. Low and high molecular weight fractions (8-10 kDa cutoff) were produced from cocoa powder extracts (CPE) of each treatment to quantify Maillard reaction products (MRP). A HILIC-UPLC MS/MS method was developed to more efficiently and sensitively quantify cocoa flavanols with high degrees of polymerization (DP) produced during processing. Overall, cocoa processing significantly ($p < 0.05$) decreased the total phenolic and total flavanol concentrations of CPEs. Hot roasting had the greatest impact on native flavanol degradation yet produced CPEs with the highest mean degree of polymerization (mDP). All CPEs dose-dependently inhibited α -glucosidase enzyme activity, with cool fermented/cool roasted cocoa powder exhibiting the best inhibition (IC_{50} of 62.2 $\mu\text{g/mL}$). Increasing flavanol mDP was correlated with decreasing IC_{50} values, suggesting that the complex flavanols produced during processing enhance cocoa's bioactivity (or their production is associated with other products that enhance bioactivity). Alternatively, high molecular weight CPE fractions were correlated with increasing IC_{50} values, suggesting that MRPs interfere with enzyme inhibition or are associated with other products (polyphenols, macronutrients, etc.) that interfere with enzyme inhibition. Overall, the data presented within this work indicate that the components of processed cocoa powders are promising inhibitors of α -glucosidase, despite a significant reduction in native flavanol composition induced by processing, and moreover that fermentation and roasting conditions can positively influence the bioactivity of cocoa despite losses of native flavanols.

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GENERAL AUDIENCE ABSTRACT

According to the Centers for Disease Control and Prevention, obesity-related chronic conditions such as cardiovascular disease and type 2 diabetes mellitus (T2D) are the leading cause of preventable and/or premature death, with 51% of the American population predicted to be obese by 2030. Cocoa (*Theobroma cacao*) is a highly concentrated source of polyphenols, and these compounds have been shown to interact with and inhibit digestive enzymes responsible for carbohydrate breakdown. By inhibiting the activity of these digestive enzymes, it is possible to slow down carbohydrate absorption after a meal and ultimately reduce large spikes in blood glucose levels, being a promising strategy in the prevention and maintenance of T2D. Cocoa beans undergo processing steps to produce a final product, such as cocoa powder, and it is known that these processing steps reduce the levels of beneficial polyphenols. Yet, how this processing-induced degradation effects the health protective activities of cocoa is still widely unknown and is the focus of this work. Through highly controlled cocoa bean processing, cocoa powders of different processing conditions were produced and used to assess how various processing parameters impacted digestive enzyme activity. Overall, processing steps did reduce levels of native polyphenols. However, these losses did not demonstrate a reduction in enzyme inhibition and certain processing conditions actually enhanced digestive enzyme inhibition. This research shows promise for the potential use of processed cocoa powder as an effective strategy in the prevention and maintenance of T2D and further work must be done to understand the mechanisms behind this relationship.

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Table of Contents

Acknowledgements.....	iv
Table of Contents.....	v
List of Figures.....	vii
List of Tables.....	xii
List of Abbreviations.....	xiii
Attributions.....	xiv
Chapter 1. Introduction and Justification.....	1
References.....	3
Chapter 2. Review of Literature.....	5
2.1 Theobroma Cacao.....	5
2.2 Polyphenols.....	8
2.3 Flavanols and Bioavailability.....	9
2.4 Cocoa Processing and Impact on Flavanol Composition.....	12
2.5 Maillard Reaction Products.....	15
2.6 Digestive Enzyme Inhibition.....	18
2.7 Characterization of Polyphenols by Mass Spectrometry.....	21
2.8 Conclusions.....	24
References.....	25
Chapter 3. Development of a Rapid HILIC UPLC-MS/MS Method for Procyanidins with Enhanced Ionization Efficiency.....	31
3.1 Introduction.....	32
3.2 Materials and Methods.....	35
3.3 Results and Discussion.....	38
3.4 Conclusions.....	52
References.....	53
Chapter 4. Development and Characterization of a Pilot-Scale Model Cocoa Fermentation System Suitable for Studying the Impact of Fermentation on Putative Bioactive Compounds and Bioactivity of Cocoa.....	55
4.1 Introduction.....	56
4.2 Materials and Methods.....	58
4.3 Results.....	65
4.4 Discussion.....	72
References.....	78

Chapter 5. Modulation of α -glucosidase activity results from changes in flavanol mean degree of polymerization imparted through controlled fermentation and roasting	83
5.1 Introduction.....	84
5.2 Materials and Methods.....	86
5.3 Results.....	93
5.4 Discussion.....	103
5.5 Conclusion	109
References.....	110
Chapter 6. Conclusions and Future Work	114
Appendix A: Supplementary Information for Chapter 5	116
A1. Supplementary Materials and Methods.....	116
A2. Supplementary Results.....	120
Appendix B: Copyright Release.....	126

List of Figures

Figure 2.1 Cocoa processing flow diagram ⁷	7
Figure 2.2 Basic skeletal structures of polyphenols.....	8
Figure 2.3 Select monomeric and oligomeric procyanidins.....	10
Figure 2.4 Proposed MRP formation.....	16
Figure 2.5 Chemical structure of acarbose.....	19
Figure 2.6 Scheme of tandem mass spectrometry, where two or more mass analyzers are in sequence to analyze components of a mixture. Starting at the inlet, analytes are ionized in the ion source and the subject ion then moves through MS1 for a precursor ion mass selection. The collision cell is the site of fragmentation before the product ion is then analyzed in MS2, followed by detection.....	23
Figure 3.1. Structures of monomeric cocoa flavanols (C, EC), and select representative flavanol oligomers (dimer, heptamer). Note that raw cocoa beans contain primarily (-)-C, but epimerization during processing results in (+)-C being the predominant epimer in finished cocoa products and cocoa powder.....	32
Figure 3.2. Peak areas of cocoa flavanols resulting from post-column infusion of potential ESI enhancer compounds. ESI enhancers (1 M) were infused at 10 μ L/min into the flow path after column elution but before ionization, through the built-in syringe pump of the LC-MS/MS instrument: no infusion, water (LC-MS grade), ammonium formate (1M), sodium carbonate (1M), sodium acetate (1M), sodium citrate (1M), ammonium bicarbonate (1M). A 40 mg/mL cocoa extract was injected into the column at a volume of 1 μ L. Each bar represents the peak areas of a different analyte, progressing from EGC, DP1 – DP10. Samples were analyzed in triplicate and values are presented as the mean \pm SEM.....	40
Figure 3.3. Optimization of ammonium formate infusion rate. 1.0 M ammonium formate was infused at various rates from 0-30 μ L/min. Injections were performed using a highly concentrated 40 mg/mL CE at an injection volume of 1 μ L/min. All values have been normalized to 100% using a no infusion baseline (0 μ L). Samples were analyzed in triplicate and values are presented as the mean \pm SEM. Significance between time points within each compound was determined by one-way ANOVA and Tukey's HSD post-hoc test (P<0.05) Time points with superscripts are significantly different and those with no superscripts indicate no significant difference between treatments.....	42
Figure 3.4. Optimization of ammonium formate infusion concentrations. Ammonium formate was infused at various concentrations from 0-2.0 M at 5 μ L/min. Injections were performed during analysis of a highly concentrated 40 mg/mL CE at an injection volume of 1 μ L. All values have been normalized to 100% using a no infusion baseline (0 μ L). Note broken x-axis for ease of interpretation. Samples were analyzed in triplicate and values are presented as the mean \pm SEM. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test (P<0.05) Time points with superscripts are significantly different and those with no superscripts indicate no significant difference between treatments.....	43

Figure 3.5. Net effect of optimized infusion and MS tune (i.e. source) settings. Samples were run with and without the infusion solution (.04 M ammonium formate infused at 5 μ L/min) at original (org) and optimized (opt) tune settings. Injections were performed using a 5 mg/mL CE at an injection volume of 2 μ L. Samples were analyzed in triplicate and values are presented as the mean \pm SEM.....45

Figure 3.6. (A) MRM chromatograms of flavanol monomers, representing the impact of injection volume on peak intensity. A 5 mg/mL CE was injected at (A) 0.5 μ L, (B) 1 μ L, (C) 2 μ L, (D) 5 μ L, (E) 10 μ L, (F) 20 μ L, (G) 30 μ L, (H) 40 μ L, and (I) 50 μ L. A 40 mg/mL CE was injected at 1 μ L (J), 20 mg/mL CE at 2 μ L (K), 10 mg/mL CE at 4 μ L (L), 5 mg/mL at 8 μ L (M), 2.5 mg/mL CE at 16 μ L (N), and 1 mg/mL CE at 40 μ L (O). (B) Decamer MRM chromatograms representing the impact of injection volume on peak intensity. A 5 mg/mL CE was injected at (A) 0.5 μ L, (B) 1 μ L, (C) 2 μ L, (D) 5 μ L, (E) 10 μ L, (F) 20 μ L, (G) 30 μ L, (H) 40 μ L, and (I) 50 μ L. A 40 mg/mL CE was injected at 1 μ L (J), 20 mg/mL CE at 2 μ L (K), 10 mg/mL CE at 4 μ L (L), 5 mg/mL at 8 μ L (M), 2.5 mg/mL CE at 16 μ L (N), and 1 mg/mL CE at 40 μ L (O).....47

Figure 3.7. LC-MS/MS overlay chromatogram of non-smoothed peaks of each compound analyzed from cocoa extract (left), as well as hexamer and nonamer chromatograms, obtained from analysis of the respective authentic standards separately.....52

Figure 4.1. (A) pH measurements for both simulated pulp media and bean nib. It is important to note that, for bean nib measurements, these values do not quantify the pH of the cocoa bean itself, but rather of the acidity derived when bean acids are diluted in water. These nib values are useful for comparison between the pH of the solution produced by beans at different time points. Dissolved oxygen (DO) measurements within the simulated pulp media are expressed in mg/L. (B) Fermentation index (FI) expressed as a ratio of absorbance at 460 and 530 nm. (C) Cut test of six randomly selected beans per each timepoint. Beans were selected from both fermentation treatments to form one composite representation. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points for each value was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. 66

Figure 4.2. Enumeration of (A) yeast, (B) lactic acid bacteria (LAB) and (C) acetic acid bacteria (AAB) in simulated pulp media, expressed in log colony-forming units (CFU)/mL. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. 67

Figure 4.3. Concentration of fermentation substrates and metabolites in simulated pulp media across 168 h. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. 68

Figure 4.4. Concentration of fermentation substrates and metabolites in cocoa beans across 168 h. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different values. 69

Figure 4.5. **(A)** Concentration of total polyphenols over the 168-h fermentation, as quantified by the Folin–Ciocalteu colorimetric assay, expressed in mg GAE/g cocoa bean. **(B)** Concentration of total flavanols over the 168-h fermentation, as quantified by the 4-dimethylaminocinnamaldehyde (DMAC) colorimetric assay, expressed in mg PCB2/g bean. **(C–G)** Individual polyphenol concentrations (C, EC, PCB2, PCC1, CinA2) over the 168-h fermentation, as quantified by reversed phase UPLC-MS, and expressed as mg/g cocoa bean. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey’s HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. 70

Figure 4.6. Individual polyphenol concentrations by mean degree of polymerization (mDP) over the 168-h fermentation as quantified by HILIC UPLC-MS/MS and expressed as mg/g cocoa bean. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey’s HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values..... 72

Figure 4.7. Polyphenol-rich cocoa extracts (CE) prepared at each point throughout the 168-h fermentation. See Section 2.8 for methodology. It is important to note the change in color and texture towards the final hours of fermentation. 75

Figure 5.1. Multivariate approach to evaluating the impact of combined fermentation and roasting parameters, producing 7 total cocoa powders: unfermented/unroasted (UF/UR), unfermented/cool roast (UF/CR), unfermented/hot roast (UF/HR), cool fermentation/unroasted (CF/UR), cool fermentation/cool roast (CF/CR), hot fermentation/unroasted (HF/UR), hot fermentation/hot roast (HF/HR)..... 87

Figure 5.2. **A.** pH of simulated pulp media/bean nib and dissolved oxygen (DO). It is important to note that for bean nib measurements, these values do not quantify the pH of the cocoa bean itself, but rather the acidity derived from bean acids diluted in water. These nib values are useful for comparison between the pH of the solution produced by beans at different time points. **B.** Cut test for all fermentations performed. **C.** Fermentation index as a ratio of 460 nm:530 nm, with values ≥ 1 indicating a complete fermentation. Note broken axes for ease of interpretation on select graphs. Values are presented as the mean \pm SEM of fermentation replicates within treatments. Significant between time points for each value was determined by one-way ANOVA and Tukey’s HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. No letters indicate no statistical difference within values. 94

Figure 5.3. Total polyphenols in each cocoa powder **(A)** and cocoa bean **(B)** expressed in gallic acid equivalents. Total flavanols from cocoa powder **(C)** and cocoa bean **(D)** expressed in procyanidin B2 equivalents. **(E)** Overall mean flavanol degree of polymerization for the total flavanols in cocoa powder- native monomers were accounted for in calculation. **(F)** Mean flavanol degree of polymerization for oligomers and polymers in cocoa powder (not including native monomers); Note broken axes (B,D,E) for ease of interpretation. Raw bean (B,D) indicates the extract prepared from the cocoa beans as received from the supplier and is different from UF/UR (-/-) as these beans were rehydrated and dried. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey’s HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. 96

Figure 5.4. Levels of individual procyanidin compounds in cocoa powders. Values are normalized to the fat-free mass of each treatment to account to varying fat content. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. 97

Figure 5.5. Total procyanidins (DP 1-10) per cocoa powder treatment as measured by HILIC UPLC-MS/MS. Each segment represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. 98

Figure 5.6. Analysis of LMW and HMW CPE fractions and the starting 40 mg/mL CPE for early, intermediate, and late MRP. Early MRP were quantified at 0.15625 mg/mL at 280 nm , intermediate MRP were quantified at 2.5-1.25 mg/mL at 360 nm, and late MRP were quantified at 5 mg/mL (<8-10 kDa), 2.5 mg/mL (>8-10 kDa), and 10 mg/mL (unfractionated CPE) at 420. Due to the lack of standard response at 420 nm, absolute absorbance of these compounds is reported, but this absorbance is relative to concentration. Each bar represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. No letters indicate no statistical difference within values. 99

Figure 5.7. α -glucosidase activity (%A compared to no inhibitor) for cocoa powder extracts (A) and soluble digesta fractions (B) with Acarbose positive control (extracts only). IC_{50} values are representative of cocoa powder extract inhibitory activity (C) with R^2 values for each treatment as follows: 0.9625 (UF/UR), 0.9539 (UF/CR), 0.9593 (UF/HR), 0.9511 (CF/UR), 0.9543 (CF/CR), 0.9702 (HF/UR), 0.9777 (HF/HR), 0.9476 (Acarbose (A)). Specific cocoa powder extract concentrations (62.5-500 μ g/mL) at %A above and below IC_{50} value (D-G). Note that IC_{50} values do not have error bars, as values were interpolated from inhibition curves. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. 101

Figure 5.8. Correlations between cocoa powder extract composition and enzyme IC_{50} values. Note the x-axis for mDP (All) and mDP (O+P) has a minimum value of 1 mDP because there cannot be a mDP value of zero. Note that late MRP are presented as absolute absorbance. Individual points represent mean composition values and calculated IC_{50} values for each treatment. Lines represent the least-squares regression line for each plot. Note that composition values are for the cocoa extract, not powders, since the extract was evaluated for enzyme activity..... 103

Figure A1. Progression of one cool fermentation batch from 0 h-168 h, followed by bean oven drying. Fermentation started at 25°C and concluded at 46°C, increasing 3.5°C/24 h.....122

Figure A2. Levels of individual procyanidin compounds in cocoa beans, as quantified by HILIC UPLC-MS/MS. Raw bean indicates the extract prepared from the cocoa beans as received from the supplier and is different from UF/UR (-/-) as these beans were rehydrated and dried. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.....123

Figure A3. Levels of individual procyanidin compounds in cocoa powders, as quantified by HILIC UPLC-MS/MS. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.....124

Figure A4. Analysis of LMW and HMW CPE fractions and the starting 40 mg/mL CPE for early, intermediate, and late MRP. Early MRP were quantified at 0.15625 mg/mL at 280 nm, intermediate MRP were quantified at 2.5 mg/mL at 360 nm, and late MRP were quantified at 5 mg/mL (<8-10 kDa), 2.5 mg/mL (>8-10 kDa), and 10 mg/mL (unfractionated CPE) at 420. Note that absolute absorbance of these compounds is reported, but this absorbance is relative to concentration. Each bar represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.....125

List of Tables

Table 1.1. Metabolic syndrome risk factors.....	1
Table 3.1. MS/MS settings for MRM detection of monomer-decamer.....	36
Table 3.2. Calibration curve slope and intercept, coefficient of determination (R^2), lower limit of detection (LLOD), and lower limit of quantification (LLOQ). Standards were run in triplicate and values were determined from the mean of those triplicates.....	48
Table 3.3. Coefficient of variation (CV) of retention time (RT) and peak areas for intraday and interday replication of compounds. Nine injections of a 5 mg/mL CE at 5 μ L were run each day for three consecutive days. A fresh aliquot of CE was used each day.....	50
Table 4.1. MS settings for individual polyphenol analysis by reverse-phase (RP)-UPLC-MS...	63
Table 4.2. Tandem MS/MS settings for multi-reaction monitoring (MRM) detection of monomeric-decameric flavanols.....	64
Table 5.1. Specifications for cocoa liquors and cakes of each treatment.....	89
Table 5.2. Total and soluble digesta yields from three-stage in vitro digestion.....	100
Table A1. MS/MS settings for MRM detection of monomer-decamer flavanols.....	121
Table A2. Preliminary melanoidin identification.....	121

List of Abbreviations

T2D; type 2 diabetes, MS; mass spectrometry, ESI; electrospray ionization, MALDI; matrix-assisted laser desorption/ionization, LC; liquid chromatography, TOF; time of flight, DC; direct current; rf; radio-frequency, MS/MS; tandem mass spectrometry, QqQ; triple quadrupole, HPLC; high performance liquid chromatography, RP; reversed phase, NP; normal phase, FLD; fluorescence detector, HILIC; hydrophilic interaction liquid chromatography, DP; degree of polymerization, TNF- α ; tumor necrosis factor-alpha, IL-6; interleukin-6, HOMA-IR; homeostasis model assessment of insulin resistance, QUICKI; quantitative insulin sensitivity check index, MR; Maillard reaction, UPLC; ultra performance liquid chromatography, C; catechin, E; epicatechin, PCB2; procyanidin B2, PCC1; procyanidin C1, CinA2; cinnamtannin A2, CE; cocoa extract, MRM; multi-reaction monitoring, EGCG; epigallocatechin-3-gallate, EGC; epigallocatechin, LLOD; lower limit of detection, LLOQ; lower limit of quantification, CV; coefficient of variation, RT; retention time, LAB; lactic acid bacteria, AAB; acetic acid bacteria, MRS; de Man-Rogosa-Sharpe agar, FI; fermentation index, DMAC; 4-dimethylaminocinnamaldehyde, DO; dissolved oxygen, GAE; gallic acid equivalent, MRP; Maillard reaction products, CF; cool fermentation, HF; hot fermentation, UF; unfermented, CR; cool roast, HR; hot roast, UR; unroasted, CBE; cocoa bean extract, CPE; cocoa powder extract, HMW; high molecular weight, LMW; low molecular weight

Attributions

Several colleagues contributed to Chapters 3-5 of this thesis. A brief explanation of their contributions is listed below.

Chapter 3: Development of a Rapid HILIC UPLC-MS/MS Method for Procyanidins with Enhanced Ionization Efficiency

Andrew H. Lee, PhD, a formal doctoral student in the Department of Food Science and Technology at Virginia Tech assisted with the sample preparation and data collection of individual procyanidins.

Amanda C. Stewart, PhD, a current faculty member in the Department of Food Science and Technology at Virginia Tech assisted in the design of the method and compilation of the manuscript.

Kenneth W. Blakeslee, PhD, an employee at Waters Corporation, provided the authentic standards used in the method and assisted with the completion of the manuscript.

Andrew P. Neilson, PhD, a current faculty member at the Plants for Human Health Institute in the Department of Food, Bioprocessing, and Nutrition Sciences at North Carolina State University assisted with the study design, data collection, compilation, and completion of the manuscript.

Chapter 4: Development and Characterization of a Pilot-Scale Model Cocoa Fermentation System Suitable for Studying the Impact of Fermentation and Putative Bioactive Compounds and Bioactivity of Cocoa

Andrew H. Lee, PhD, a formal doctoral student in the Department of Food Science and Technology at Virginia Tech assisted with the model fermentation system, sample preparation, data collection, and data interpretation of fermentation products and metabolites.

Brian D. Wiersema, MS, the pilot plant manager in the Department of Food Science and Technology at Virginia Tech assisted with the model fermentation system preparation and equipment needed to complete the study.

Haibo Huang, PhD, a current faculty member in the Department of Food Science and Technology at Virginia Tech assisted with the data collection and interpretation of the fermentation metabolites via HPLC.

Joshua D. Lambert, PhD, a current faculty member in the Department of Food Science at Pennsylvania State University contributed to the study design, compilation, and completion of the manuscript.

Amanda C. Stewart, PhD, a current faculty member in the Department of Food Science at Virginia Tech contributed to the study design, fermentation model system, compilation, and completion of the manuscript.

Andrew P. Neilson, PhD, a current faculty member at the Plants for Human Health Institute in the Department of Food, Bioprocessing, and Nutrition Sciences at North Carolina State University contributed to the study design, compilation, and completion of the manuscript.

Chapter 5: Controlled Fermentation and Roasting of Cocoa Beans Suggests that Flavanol Degree of Polymerization is the Key Parameter Dictating the α -glucosidase Inhibitory Activity of Cocoa

Brian D. Wiersema, MS, the pilot plant manager in the Department of Food Science and Technology at Virginia Tech assisted with the model fermentation system, processing of cocoa beans, and supplied necessary equipment needed.

Laura E. Griffin, PhD, a post-doctoral scholar at the Plants for Human Health Institute of North Carolina State University assisted with sample preparation and conduction of thiolysis and digestive enzyme assays.

Lauren A. Essenmacher, a current graduate student in the Department of Food Science and Technology at Virginia Tech assisted with the extraction of cocoa powder and cocoa beans.

Amy N. Moore, a current graduate student in the Department of Food Science and Technology at Virginia Tech assisted with the preparation of simulated pulp media and conduction of fermentation model systems.

Andrew H. Lee, PhD, a former doctoral student in the Department of Food Science and Technology at Virginia Tech assisted with the design of the model fermentation system.

Joshua D. Lambert, PhD, a current faculty member in the Department of Food Science at Pennsylvania State University contributed to the study design, compilation, and completion of the manuscript.

Amanda C. Stewart, PhD, a current faculty member in the Department of Food Science and Technology at Virginia Tech contributed to the study design and completion of the manuscript.

Andrew P. Neilson, PhD, a current faculty member at the Plants for Human Health Institute in the Department of Food, Bioprocessing, and Nutrition Sciences at North Carolina State University contributed to the study design, data interpretation, compilation and completion of the manuscript.

CHAPTER 1. INTRODUCTION AND JUSTIFICATION

Diabetes mellitus is a chronic metabolic disorder that is characterized by abnormally high concentrations of blood glucose. It is estimated that in 2017 approximately 451 million adults (≥ 18 years) were living with diabetes, a number that has increased over fourfold since 1980.¹ More specifically, Type 2 diabetes mellitus (T2D) accounts for 90-95% of all diabetic cases and is a condition thought to be preventable as obesity is one of the most prominent contributing causes of development.² Obesity and excessive amounts of adipose tissue contribute to substantially increased risks of associated health complications such as cardiovascular disease, high blood pressure, diabetes mellitus, as well as other chronic health conditions. Collectively, the metabolic syndrome (MetS) is a modern diagnosis that is used to classify this increased risk, with a positive diagnosis when patients exhibit at least three of the characteristic symptoms (**Table 1.1**).³

Table 1.1 Metabolic syndrome risk factors

Risk Factor	Criteria
Abdominal Waist Circumference	≥ 88 cm (women) ≥ 102 cm (men)
Blood Triglycerides	> 150 mg/dL
HDL Blood Cholesterol	< 50 mg/dL (women) < 40 mg/dL (men)
Blood Pressure	$> 130/80$ mmHg
Fasting Blood Glucose	≥ 100 mg/dL

Obesity can have a chronic impact if not controlled. The presence of excess lipids dysregulates vital tissues such as adipose tissue, liver, muscle, and pancreatic tissue. Additionally, these tissues act as direct inflammation sites and become saturated with macrophages which ultimately interfere with crucial internal functions, such as insulin signaling.⁴ Diet and exercise are important lifestyle choices that can help control and reduce the risk for obesity and MetS development without medical intervention. With approximately \$850 billion in annual global healthcare expenditures on diabetes related costs alone, there is an increasing need of reliable nutrition interventions consisting of foods easily and readily available to consumers.¹ It has been shown that consumption of polyphenol-rich foods such as green tea, berries, apples, grapes, and cocoa is beneficial to overall health and may even delay or prevent

the onset of obesity and MetS, as well as associated chronic conditions.⁵⁻⁸ Furthermore, digestive enzymes like α -glucosidase play a key role in the breakdown of carbohydrates. α -glucosidase is located on the brush border of the small intestines and influences the rate of post-prandial hyperglycemia, thus serving as a potential target in the management of T2D.

Per weight, cocoa (*Theobroma cacao*) is the most concentrated source of dietary flavanols, a flavonoid subclass, and contains other putative bioactives. Fermentation, drying, roasting, and other further processing steps (winnowing, grinding, pressing, etc.) are performed to achieve desirable cocoa flavors and characteristics. Although it is understood that these processing steps can negatively impact the overall total flavanol composition of cocoa beans, the impact of processing on cocoa's health-protective activities, and ultimately bioactivity, is yet to be elucidated, though it is generally accepted that these losses are likely to reduce the potential bioactivities and health benefits of cocoa.⁸⁻¹⁰ Despite this flavanol reduction, it is possible that the chemical reactions occurring during cocoa processing result in the formation of new bioactives, which may potentially preserve or enhance the bioactivity of cocoa. Heat-induced high molecular weight compounds like melanoidins have potential health protective activities, with melanoidins exerting prebiotic activity and enhancing the antioxidant capacity of cocoa.^{11,12} Additionally, α -glucosidase inhibition has been associated with flavanols within processed cocoa (fermented/roasted liquor).⁸ By targeting enzyme inhibition through dietary interventions such as cocoa consumption, undesirable side effects and costs associated with available pharmaceuticals that possess similar activities are mitigated.

The overall objective of this research is to determine how processing impacts the chemical composition and α -glucosidase inhibitory activity of cocoa, and to identify optimal processing approaches that maximize the α -glucosidase inhibitory activities of cocoa. The central hypothesis is that cocoa bean fermentation and roasting parameters can be tailored to specifically enhance cocoa's chemical composition and α -glucosidase inhibitory activity. In order to test the central hypothesis and achieve the overall objective, the following specific aims were proposed:

1. Conduct a model cocoa production under a range of processing parameters (fermentation, roasting).
2. Characterize potentially bioactive components (including native polyphenols and melanoidins) in each cocoa powder following processing.

3. Determine the impact of cocoa fermentation and roasting on cocoa's capability to inhibit α -glucosidase activity.
4. Correlate α -glucosidase inhibitory activity with various compositional factors and processing conditions to identify processes and predictors that can be used to develop cocoa with enhanced activity.

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CHAPTER 2. REVIEW OF LITERATURE

2.1 *Theobroma Cacao*

Cocoa beans are the seeds of *Theobroma cacao*, an evergreen tree endemic to tropical areas, growing at approximately 20° N and 20° S of the equator. The trees grow best in areas of high humidity, dense shade, and prolonged rain. Cocoa cultivation is believed to have originated as early as 1500 BC in Mesoamerica by the ancient Aztec and Mayan populations.¹ Historically regarded to guarantee health and power, beans were most commonly roasted and consumed as a beverage, mixed with water and chili peppers, and served during religious ceremonies or times of celebration. It was not until the early 15th century that the modern chocolate industry began to flourish, exchanging bitterness and astringency for a well-known delicacy. Mexico remained the predominant cocoa market until the 17th century where the growth of trade expanded cocoa planting to areas of South America, the Caribbean, as well as across the Pacific to the Philippines where it is thought to have reached parts of Sri Lanka and India.² Following the independence of Brazil in the mid-1800s, cocoa established a presence in Ghana and Nigeria to begin its cultivation in West Africa.²

The three main varieties of cocoa, Criollo, Forastero, and Trinitario, each have unique flavor and cultivation characteristics. Criollo beans of Central and South America are characterized by their pale color and mild flavor. These beans are typically used to produce the finest chocolate but have a high susceptibility to disease and thus comprise only 5-10% of the world's cocoa production.³ Forastero beans are known for their dark purple color and originated in the Amazonian region. Due to their high disease and pest resistance, as well as their traditional cocoa flavors, these beans make up about 80% of the world's cocoa production.³ Trinitario beans are the hybrid of Criollo and Forastero plants. Their variable flavor and color are highly dependent upon the regions in which they grow and make up 10-15% of the world's chocolate production.³

Cocoa pods contain 30-40 beans encapsulated in a viscous pulp. Within each bean there are two main parts, the testa and the embryo/cotyledon, and are approximately 55% lipid, 16% fiber, 10% protein, and 3% ash.⁴ Cocoa pulp consists of 82-87% water, 10-15% sugar, 2-3% pentosans, 1-3% citric acid, and 1-1.5% pectin and is essential during fermentation, providing the substrate for microbial growth.⁵ The modern processing chain for cocoa beans is a complex

and lacks traceability (**Figure 2.1**). From farm to processed cocoa powder/butter, beans from various farmers, areas, and countries are comingled into large batch sizes, with one batch often containing beans from over 70 different farmers.⁶ According to the World Cocoa Foundation, 634,000 tons of cocoa is consumed in the United States each year, with 2014 global production rising to 4.3 million tons.¹ Further understanding of bean composition before and after the fermentation process could potentially enhance dietary attributes of beans without sacrificing desirable sensory characteristics.

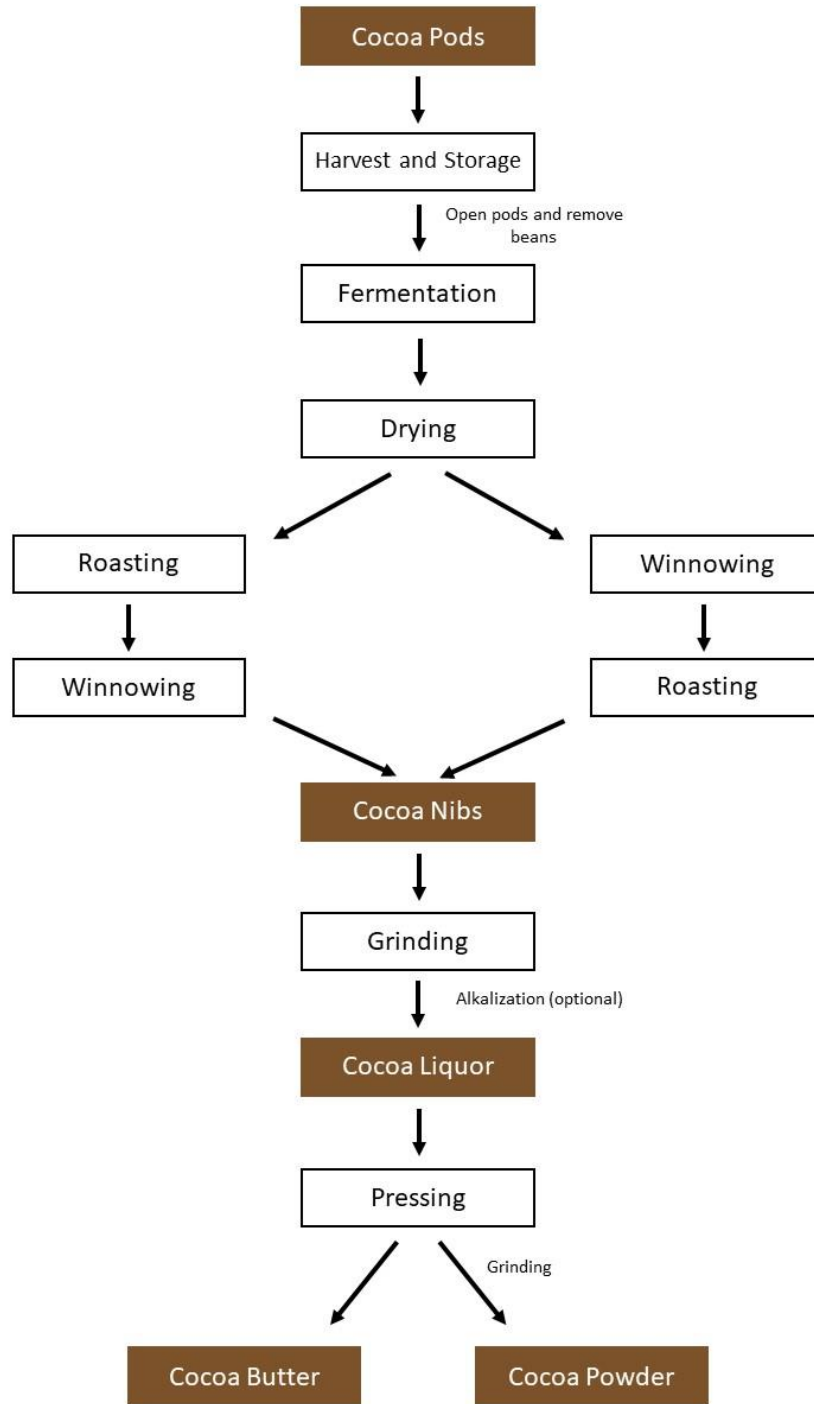


Figure 2.1 Cocoa processing flow diagram⁷

2.2 Polyphenols

Polyphenols are plant-based secondary metabolites that are comprised of multiple phenol structures, the largest classification of phytochemicals.⁸ These strong antioxidants have gained significant interest among researchers due to their positive implications on human health with potential preventative role in chronic diseases, especially those associated with oxidative stress like cancer, cardiovascular disease, and neurodegenerative diseases, as well as other biological characteristics that have yet to be elucidated.^{9,10} Polyphenols are extremely abundant in the human diet, with over 8,000 structural variations, most commonly present in fruits, coffee, tea, wine, and cocoa products.⁸⁻¹⁰

There are over 15 sub-groups of polyphenols, including phenolic acids, stilbenes, flavonoids, and lignins. Due to their diversity, polyphenols are most commonly classified by their chemical structure, specifically the number of phenolic rings and the functional groups that link them together (**Figure 2.2**).⁸ Of these classifications, flavonoids are the most abundant polyphenol in the human diet, with over 4000 different compounds identified to date. Within flavonoids, further division can be made into anthocyanins, flavanols (commonly flavan-3-ols), flavonols, flavones, and flavanones.^{8,9} Flavanols exist as monomers, such as catechin and epicatechin, and larger oligomers and polymers, known as proanthocyanidins. When these proanthocyanidins are composed exclusively of linked catechin and epicatechin residues, they are referred to as procyanidins and are the most abundant flavonoids found in plants.¹¹ Procyanidins play a key role in the health benefits of cocoa and their absorption and metabolism will be further address in the remaining sections.

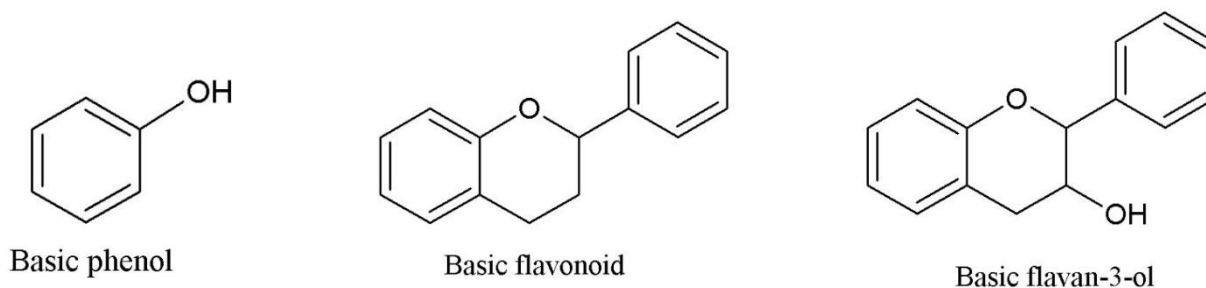


Figure 2.2 Basic skeletal structures of polyphenols

2.3 Flavanols and Bioavailability

Procyanidins from nuts, fruits, wine, and cocoa have been shown to possess beneficial physiological activities like anti-carcinogenic, cardioprotective, antimicrobial, and neuro-protective.¹² The mechanisms of these activities have attracted attention in recent investigations as the majority of ingested flavanols are not absorbed by the small intestine. Degree of polymerization (DP) has a major influence on the absorption and bioavailability of flavanols.¹²⁻¹⁴ Additionally, the composition of the food matrix in which these compounds are present can impact their absorption and pharmacokinetics. Macronutrients and physical state (solid vs. liquid) can also influence flavanol absorption and bioavailability.¹⁴

Flavanol absorption occurs in four major steps. First, immediately after ingestion, compounds must be released from their food or beverage matrix before being solubilized in the gut lumen. These stable solubilized compounds are then transported by the intestinal epithelial cells where they are diffused across the unstirred water layer, absorbed, and metabolized.¹⁴ To be absorbed, these compounds must endure a variety of gastrointestinal conditions and extreme pH changes. Despite these physiological obstacles, monomeric and oligomeric flavanols appear to be stable through the oral and gastric phases of digestion. Of the flavan-3-ols, monomeric (+)-catechin and (-)-epicatechin have the highest rates of absorption, while dimers, trimers, and tetramers undergo limited absorption and those with DP>4 are not absorbable (**Figure 2.3**).¹³ Monomers are readily absorbed by the small intestine where they are metabolized by phase II enzymes. Larger compounds must pass intact through the GI tract and ultimately reach the colon where they are broken down to microbial metabolites by colonic microbiota.¹² The production of these metabolites have led researchers to believe that they may be responsible for the health effects of flavanol consumption.

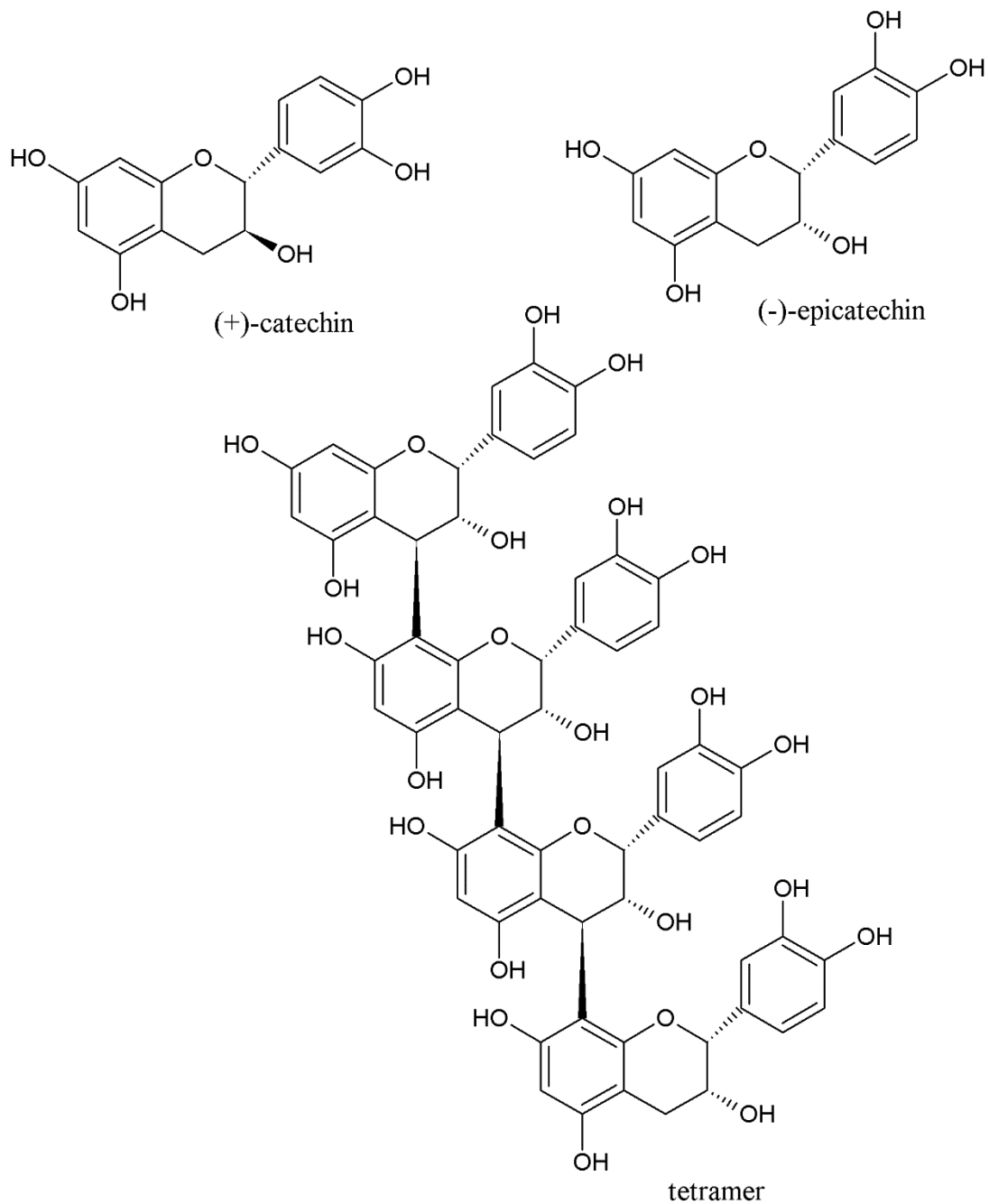


Figure 2.3 Select monomeric and oligomeric procyanidins

As previously mentioned, the majority of ingested procyanidins are not absorbed in the small intestine, but arrive at the colon in their native form where they are then extensively degraded into microbial metabolites.¹⁴ In the colon, procyanidin dimer B2 was degraded 2X

faster than monomeric (-)-epicatechin, supporting the notion that the bioavailability of procyanidins decrease as molecular weight (and therefore DP) increases.¹³ With expanding research on the gut microbiota and bacterial populations, it has been hypothesized that absorption may not be a prerequisite to bioactivity and is thus not necessarily a determinant of the health protective activities of flavanols against many chronic conditions.

As mentioned in Chapter 1, metabolic syndrome diagnosis involves many metabolic abnormalities (**Table 1.1**). Chronic low-grade inflammation is often associated with the development and consequences of these abnormalities, originating as dysfunctional visceral adipose tissue. The overconsumption of macronutrients often leads to the growing size of adipocytes and increased recruitment of macrophages, ultimately triggering the secretion of free fatty acids and pro-inflammatory cytokines such as tumor necrosis factor-alpha (TNF- α) and interleukin-6 (IL-6).^{15,16} In an *in vitro* study performed with cocoa procyanidins of differing degrees of polymerization, polymeric fractions exhibited the highest inhibitory effect of pro-inflammatory cytokine release (TNF- α) when stimulating macrophages compared to oligomeric fractions.¹⁷ Animal studies have demonstrated similar results, that in a high fat diet long-term cocoa supplementation alleviates adipose tissue inflammation. High fat fed mice had significantly increased levels of pro-inflammatory cytokines compared to low fat lean mice, and when supplemented with cocoa, mice exhibited a 40-60% decrease in adipose tissue DNA levels of pro-inflammatory cytokines, a 40% decrease in plasma endotoxin levels, improved gut barrier function, and decreased plasma levels of IL-6 with increased adiponectin levels when compared to high fat fed mice.^{16,18} Furthermore, long term supplementation of dietary cocoa also reduced the presence of pro-inflammatory genes in white adipose tissue.¹⁸

Additionally, suppression of low-grade inflammation through consumption of dietary cocoa flavanols can also protect against insulin resistance. In parallel with decreased levels of many pro-inflammatory cytokines in animal models with cocoa supplemented high fat diets, this 18 w supplementation was also effective at reducing fasting plasma insulin levels by 14.8%, reducing fasting plasma triglycerides, and also reducing fasting plasma free fatty acid levels when compared to high fat fed animals.¹⁶ In a shorter feeding model, cocoa extract supplementation was dose-dependently effective at significantly lowering serum glucose levels and total cholesterol levels in diabetic rats.¹⁹ At all dietary doses, cocoa extract was effective at

decreasing total triglyceride levels. *In vitro* studies have also examined the impact that cocoa flavanols have on glucose tolerance and insulin sensitivity. Specifically, epicatechin and a total cocoa powder extract were used on glucose treated human HepG2 cells and findings suggest that the supplementation of these compounds improve insulin sensitivity.²⁰ Finally, a human clinical trial examined the implications of dark vs. white chocolate supplementation on healthy subjects for 15 d. Although this study did not look at the mechanisms underlying their reported results, there was significantly lower homeostasis model assessment of insulin resistance (HOMA-IR) values and significantly higher quantitative insulin sensitivity check index (QUICKI) values after supplementation with dark vs. white chocolate.²¹ In addition to improved insulin sensitivity, dark chocolate supplementation was also effective at reducing blood pressure.

Although it is clear that cocoa flavanols have the potential to reduce the risk for chronic inflammation and metabolic syndrome diagnosis, the mechanisms underlying these beneficial implications remain uncertain. The association between cocoa processing, mDP, and subsequent health benefits is an area where more research is needed to fully understand the link between dietary cocoa flavanols and bioactivity.

2.4 Cocoa Processing and Impact on Flavanol Composition

The polyphenolic content of cocoa is highly dependent on fermentation and subsequent processing steps, as various biochemical reactions and high roasting temperatures degrade native polyphenols to limit astringent flavors in final cocoa products.²²⁻²⁵ By better understanding the polyphenolic changes that are taking place within the bean during cocoa processing, the health protective activities and bioactive potential of dietary cocoa can be better characterized.

Complete cocoa processing steps are shown in **Figure 2.1**.

Fermentation is the chemical breakdown of a substrate involving microorganisms such as bacteria and yeasts. Historically, fermentation was regarded as an easy and inexpensive method of removing the viscous pulp from beans to facilitate drying, but only in the last century has the relationship between these processing conditions and cocoa flavor development been established. Desirable flavor and aroma precursors are generated through a series of biochemical transformations during cocoa fermentation. On farm there is a great amount of variability between fermentations as the environment, climate, ambient microorganisms, as well as tools

and surfaces used can influence the native microbial composition of a fermentation, and the fermentation conditions (e.g. temperature, dissolved oxygen, substrate availability).

Cocoa fermentation traditionally occurs in 25-2000 kg batches over 5-7 days in large heaps on the ground or in wooden boxes covered with banana leaves.⁵ During the initial hours of fermentation, low pH creates a suitable environment for anaerobic yeast proliferation. Yeasts use the high sugar content of pulp (sucrose, glucose, fructose) as fuel to facilitate the production of alcohols and to metabolize citric acid. This results in a rise in pH and oxygen levels, favoring lactic acid bacteria. At this stage, pulp begins to lose viscosity and drain off, introducing oxygen into the heap and raising the temperature to 45-50°C, creating the optimal environment for the oxidation of ethanol into acetic acid, and dominating the remainder of the fermentation.²⁶⁻²⁸ Towards the final hours of fermentation, heat and acids penetrate through the bean testa, stimulating enzymatic reactions as cellular components freely mix within the seed.² Ultimately, this results in bean death where endogenous chemical reactions allow for the development of flavor, aromatic, and color precursors.²⁹ As oxygen infiltrates the dead seed, polyphenol oxidase reactions utilize monomeric flavanols, like (-)-epicatechin, to initiate the browning of the cotyledon, a visual representation that fermentation is complete.

Drying is considered the second phase of fermentation, as enzymatic and non-enzymatic reactions continue with sufficient moisture. On farm, drying takes place in the sun over the span of one to four weeks with regular rotation until the moisture falls below 8%.³⁰ In the case of artificial drying, extreme care must be exercised in that the bean temperature does not exceed 60°C, as at these high temperatures enzymatic reactions can be deactivated and cause harsh off flavors, lowering the quality of the beans. After fermentation is complete, the dead seed loses membrane integrity which allows for increased aeration into the cotyledon. The presence of oxygen then drives polyphenol oxidation reactions, ultimately resulting in brown color formation and volatile aroma precursors.³¹ Although they involve relatively minor chemical constituents, these reactions are crucial to the avoidance of off-flavors and spoilage organisms. When done slowly and under appropriate conditions, drying will produce desirable sensory characteristics at safe moisture levels that will limit the risk of spoilage during subsequent transport and further processing of cocoa.

Before fermentation, polyphenol content of cocoa beans is made up of approximately 58% procyanidins.³² Fermentation can cause anywhere from 0-80% loss of native polyphenols, likely influenced by a variety of factors including pod storage and pre-harvest conditions, the diffusion of soluble polyphenols into the fermentation ‘sweating’ (pulp draining), the enzymatic oxidation and non-enzymatic oxidation occurring during drying, and even the season and weather conditions during the fermentation time frame.³³⁻³⁵ These losses are ultimately responsible for the reduction in bitterness and astringency following fermentation. Bitterness and stringency are characteristics associated with raw unfermented beans. The most significant losses occur in the first 48-72 h of fermentation, as polyphenols diffuse out of the bean cotyledon and bean death is initiated during this time.³⁶ Bean variety is an important factor to consider when accounting for total polyphenol losses. Criollo beans contain few or no anthocyanins and are known to have about 2/3 the total polyphenol content of Forastero beans, yet other studies have reported consistent total polyphenol quantities among Criollo, Forastero, Trinitario, and other hybrid bean species.^{37,38} However, Criollo beans have demonstrated a much faster polyphenol degradation than other varieties. This early and rapid loss of polyphenols could possibly lead to misinterpretation of distinct cultivar identification, and contribute to the wide range of reported Criollo bean polyphenol content.³⁸ Regardless, this extreme degradation of native polyphenols has often been assumed to result in a subsequent reduction in bioactivity. This widely accepted paradigm has come under scrutiny as more recent investigations have suggested that reactions occurring throughout cocoa processing may produce compounds with novel activities, potentially preserving or enhancing bioactivity compared to raw unfermented beans.³⁹⁻⁴¹

After beans have been fermented and dried, they undergo a roasting process, essential for flavor and aroma development. Depending on the desired characteristics of the final product, beans are often roasted at 120°C-150°C for 5-120 min.⁵ Polyphenols that are still within the nib, specifically flavanols, are heat sensitive, and thus roasting will result in further losses. Roasting has become a processing step of increased research interest, as it is hypothesized that large procyanidins have increased biological activities and this flavan-3-ol polymerization is time and temperature dependent.^{42,43} Roasting, although causing further degradation of native polyphenols, defines the sensory characteristics of the finished cocoa product. Roasting introduces the beans to elevated temperatures and increased oxygen flow, readily degrading and/or binding flavanols to polymer structures like proteins, polysaccharides, and Maillard

reaction products (MRP), ultimately leading to the possible formation of insoluble complexes.^{25,44} Roasting with increased air humidity and lower temperature has shown to decrease the intensity of phenolic degradation within roasted beans, but the sensory implications of this process have yet to be determined.⁴⁵ Development and potential activities of roasting-induced high molecular weight compounds, such as melanoidins, will be further discussed in the next section.

To be further processed, beans are first winnowed, which is simply the removal of husks to expose the nib. Beans can be winnowed prior to roasting (nib roasting) or roasted whole and then winnowed. Because the husk contains trace amounts of fermented pulp, it must be removed to prevent off flavors in the final product. The cocoa nibs are then milled and refined into a homogenous fluid paste, or cocoa liquor, and then pressed at elevated temperatures and under high pressure so that the cocoa butter drains off and a solid cocoa cake is left behind. This cake is finally ground into a fine powder, cocoa powder, and sold for confectionary use.

2.5 Maillard Reaction Products

The Maillard reaction (MR) is arguably the most important reaction that takes place during roasting. This non-enzymatic chemical reaction takes place within a food matrix and involves the interaction between carbonyl groups of reducing sugars and amino groups of peptides, proteins, or amino acids.⁴⁶ It is the reaction that takes place under high temperatures and is responsible for the development of flavor, aroma, and color precursors. There are different steps to the MR, each producing unique compounds. Stage one is the formation of early compounds, or Amadori products, then intermediate products such as hydroxymethylfurfural are formed, and finally melanoidins, or the final products of the MR, are formed (**Figure 2.4**).⁴⁷

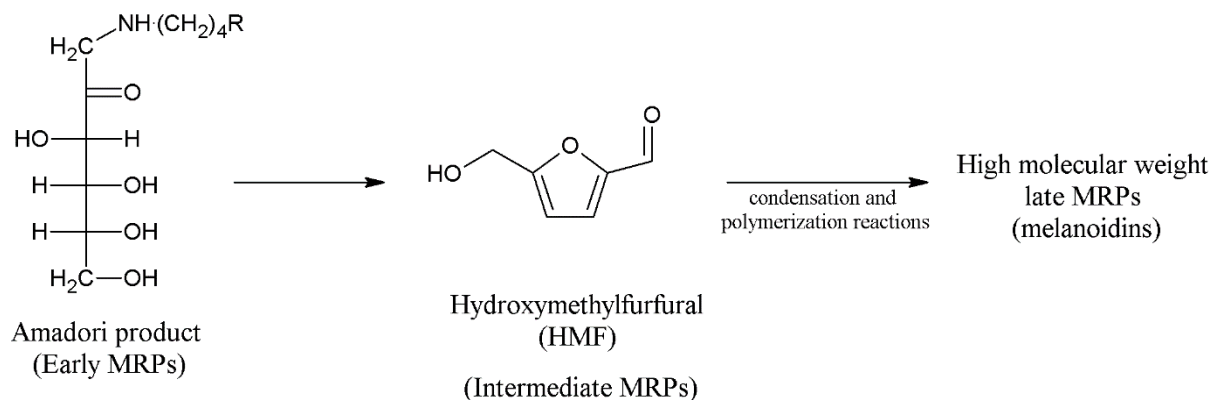


Figure 2.4 Proposed MRP formation^{46,48}

It is hypothesized that earlier MRPs and intermediates polymerize and crosslink with one another to ultimately form high molecular weight melanoidins in the later stages of the reaction.^{4,46} These large melanoidins are suspected of having health promoting benefits, such as chemopreventive, antioxidant, and antimicrobial activities, but their exact structure and compositional properties is dependent upon the food matrix they are formed within and the processing conditions they are subjected to.^{4,46,47,49}

Melanoidins have been the topic of increased investigation over the past two decades, yet the exact structure and biological activities of these compounds is still largely ambiguous.^{46,47} It has been reported, though, that these compounds are hydrophilic, heterogenous, nitrogen-containing polymers.^{46,47} There are different classes of melanoidins that have been differentiated depending on the nature of the food matrix. Melanoproteins are very large insoluble MRPs that form within protein-rich foods where these proteins are crosslinked with carbohydrates and carbohydrate-derived compounds.⁴⁷ On the other hand, smaller low molecular weight compounds (monosaccharides, amino acids, etc.) can play in the formation of melanoidins by polymerizing together into high molecular weight soluble compounds.⁴⁷ If poly- and oligo-saccharides are involved in these reactions, a wider range of melanoidin structures can be formed with variable solubility. Finally, polyphenols can be involved in the formation of melanoidins as they polymerize and be non-covalently linked to the base structure.^{46,47} It is hypothesized that these bound fractions, especially polyphenol and low molecular weight compounds, significantly contribute to the biological activities of melanoidins but this activity can vary due to structural changes that occur during thermal processing.⁴⁶ Several foods, including roasted coffee, malt, barley, baked goods, honey, balsamic vinegar, and roasted cocoa have been looked at for their

melanoidin and MRP contents.⁴⁷ The quantification and molecular weight determination in different food matrices, although growing within the literature, is widely under investigated, primarily due to the analytical challenges these compounds present and the lack of standards and reference materials available.

The bioavailability of melanoidins is suggested to be very limited but there is increasing evidence that these compounds possess health protective activities. Absorption of high molecular weight fractions has been suggested, but only after modification within the small intestine. On the other hand, approximately 30% of lower molecular weight products, dependent upon structure and dose, have been reportedly absorbed.⁵⁰ In an early animal study with a 2% high molecular weight melanoidin diet, there was limited fecal detection of small compounds, suggesting that the ingested compounds were broken down by intestinal enzymes and/or microorganisms, and then absorbed.⁵¹ Yet, the indigestible compounds are predicted to have more beneficial effects, given that they survive the harsh conditions of the gastrointestinal tract. As they pass through the intestine, they can exert powerful antioxidant and prebiotic effects, often acting like dietary fiber.⁴⁶ Depending on the structure, polysaccharide-rich or protein-rich, these compounds can be metabolized by *Bifidobacteria* spp. and enhance the growth of beneficial bacteria in the upper intestinal tract, or serve as a substrate for harmful bacteria in the colon.^{4,47} Regardless, there is a need to optimize food processing techniques to maximize the production of beneficial melanoidin structures.

Food products like coffee and baked goods have been the subject of more thorough investigation regarding MRPs, with cocoa compounds growing in interest across researchers. Unlike these products, though, cocoa beans contain limited reducing sugars and polysaccharides, but have high concentrations of lipids (50-57%) and proteins (10-15%).⁴ There are other sources of reactive carbonyl compounds necessary for the MR and thermally processed foods, such as cocoa, contain these compounds through lipid oxidation reactions that will ultimately interact with amino acids and proteins. During cocoa processing, compounds other than MRPs contribute to the characteristic brown color formation after roasting.⁵² These compounds include brown procyanidins that naturally occur or are produced as a result of oxidation reactions throughout fermentation and roasting. Color intensity is a common method for the quantification of MRPs, but because of these additional color contributors, color intensity of roasted cocoa is not

necessarily the best indication of MRP concentration. There has been some evidence showing cocoa processing, particularly roasting, increases bioactivity due to the formation of MRPs and melanoidins. Specifically, separate studies have reported a decrease in phenolic activity and antioxidant activity at shorter, cooler roasting parameters yet as roasting temperature increases and time lengthens, the antioxidant activity of cocoa increases, with the MR favored under higher temperatures.^{40,49,53} This observed decrease in MRPs after short roasting times could potentially result from macromolecule (i.e. proteins, polysaccharides, proteins, polyphenols) structural changes that can be induced by higher temperatures. Additionally epicatechin has been shown to potentially inhibit the early products of the MR.⁴ Yet, increases in MRPs after prolonged high temperature roasting is most likely from the polymerization and condensation reactions that take place among MR intermediates in the final stages of the MR.⁴ By roasting for longer times, further oxidation is occurring between intermediates and therefore forming more complex products. In addition to composition, factors such as pH, water activity, variety, and processing techniques can influence the rate of the MR and ultimately the amount of high molecular weight MRPs within cocoa beans.⁵² Through increased investigation and understanding of cocoa melanoidin structural characteristics and biological activities, processing techniques and parameters can be optimized to maximize the health protective activities of dietary cocoa.

2.6 Digestive Enzyme Inhibition

In the past century, most industrialized countries have seen an elimination of undernutrition and various micro and macronutrient deficiencies due to nutrient fortification and enrichment of foods, increased food supply, and more targeted medical interventions such as vitamins and nutritional supplements.^{54,55} Within recent decades, though, macronutrient overnutrition has emerged and does not show the same trends of decline as undernutrition. Overnutrition is often a precursor to obesity and the chronic conditions that result from excessive adipose tissue, like T2D, cardiovascular disease, and some cancers. Due to this public health concern, prevention and management strategies to reduce macronutrient digestion and absorption are being explored as possible solutions to mitigate the rising BMI of the global population.

With rising rates of obesity and obesity-related chronic conditions (i.e. T2D), prevention strategies have started focusing on vehicles that can interfere with the breakdown and absorption of dietary carbohydrates and lipids. α -glucosidase is a digestive enzyme located on the brush

border of the small intestine. Primarily responsible for the catalytic cleavage of oligosaccharides into simple sugars, α -glucosidase is a key factor determining postprandial blood glucose levels.⁵⁶ Through the inhibition of this enzyme, carbohydrate digestion is delayed and post-prandial hyperglycemia is decreased, thus α -glucosidase inhibition by pharmaceutical intervention is proving to be an effective prevention strategy in the management of T2D. Although there are various pharmaceuticals available, such as acarbose (**Figure 2.5**), to act on digestive enzymes, achieving this activity through diet is a more desirable approach with fewer undesirable side effects, specifically gastrointestinal intolerance, and high costs.⁵⁷

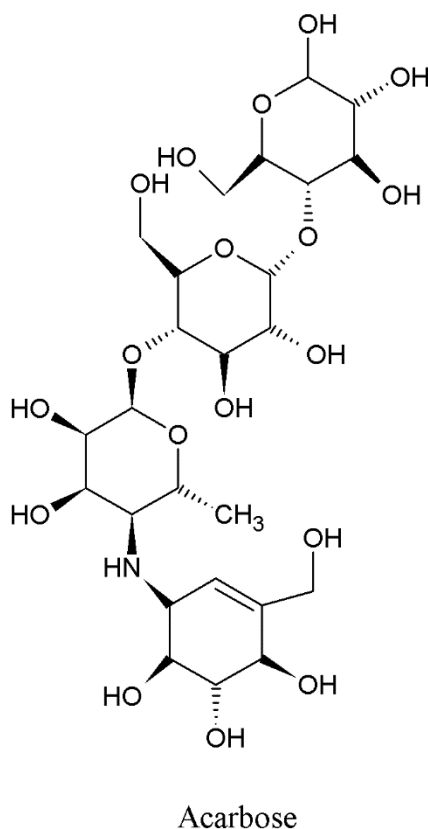


Figure 2.5 Chemical structure of acarbose⁵⁸

Dietary polyphenols from berries, tea, cocoa, and other plants/plant-derived products have been shown to possess digestive enzyme inhibitory capacity *in vitro* and *in vivo*. Gu et al⁴¹ first reported evidence that cocoa procyanidins in polyphenol-rich cocoa extracts exhibited potent digestive enzyme inhibitory activities. This inhibition was shown to be a function of polyphenol content, and furthermore inhibitory activity increased with increasing procyanidin mDP. Yamashita et al⁵⁹ reported similar findings *in vitro* upon examination of cocoa liquor

extract and α -glucosidase inhibition. Compared to a low DP extract fraction, the high DP fraction had a stronger α -glucosidase inhibitory effect. A recent animal study examined the impact of a diet supplemented with low and high grape seed procyanidins and concluded that procyanidins with high mDP had a greater effect on digestive enzyme inhibition.⁶⁰ On the other hand, others have reported that procyanidin content and mDP may not influence cocoa inhibitory activity as strongly as previously suggested, and that procyanidins with a lower mDP have stronger inhibitory potential.^{39,61,62} Although these results are often conflicting and the mechanism behind procyanidin activity on digestive enzyme inhibition has yet to be elucidated, Ryan et al³⁹ is one of the only studies to examine the impact of cocoa processing on digestive enzyme inhibition. At physiologically relevant doses, cocoa extract was shown to effectively inhibit α -glucosidase and furthermore, that unfermented cocoa liquor (cocoa mass resulting from roasting and grinding of beans) had a great inhibitory effect on α -glucosidase compared to unfermented and fermented cocoa beans (unroasted), and ultimately acarbose. These findings are especially novel in that they suggest that cocoa processing strategies may be used to maximize α -glucosidase inhibition. Other studies have looked at the implications of roasting time and temperature on enzymatic inhibition- with longer roasting times increasing the inhibitory activity of pancreatic lipase, the digestive enzyme that hydrolyzed triglycerides into glycerol and free fatty acids, but few have examined subsequent cocoa processing steps (fermentation, roasting).⁴²

Additionally, the contribution of MRPs to α -glucosidase inhibition has been under minimal investigation. As described above, cocoa processing exposes beans to a series of high temperatures, ultimately initiating the formation of complex high molecular weight compounds, such as melanoidins. These large heterogenous polymers, as previously discussed, have the potential to resemble lignin and fiber and when in the gut, can bind proteins and improve enzyme inhibition imparted by cocoa flavanols.^{26,39,57} It has been reported that intermediate and high molecular weight MRPs are more effective at inhibiting α -glucosidase than low molecular weight compounds (<10 kDa).⁵⁷ Cocoa's ability to inhibit digestive enzymes, and α -glucosidase specifically, cannot be attributed to one single compound but rather the interactions and activities between many compounds of various sizes and complexities. In summary, the current state of research in this area points to the great health-promoting potential of the as-yet largely unexplored chemical complexity of fermented and/or thermally processed cocoas. These reported data further support the hypothesis that the remaining native cocoa compounds, when

exposed to long duration of high heat, undergo complex reactions that result in large, intricate bioactive structures.

2.7 Characterization of Polyphenols by Mass Spectrometry

Mass spectrometry (MS) is a technique used to determine the mass of a molecule and can provide essential information about a selected analyte, such as structure, purity, and composition.^{63,64} The term MS in itself is often misleading, as mass is not what is analyzed. MS bases its analysis on the mass to charge ratio (m/z), or the mass of an ion divided by its charge, of a positively or negatively charged gas phase ion.⁶³ Simply put, if an ion is singly charged, the m/z is equivalent to the mass itself, whereas if an ion is doubly charged with a mass of 56, the m/z ratio would be 28. This analysis is a sequence of basic, but essential, components- the ionization source, mass analyzer, and detector.

Ionization is the first step in MS, where the analytes of interest are converted into gas phase ions. These charged particles can then make their way through the remaining components of analysis. There are many different ionization techniques, and selection will depend on the nature of the analyte. Early ionization approaches limited analytes to small, thermally stable compounds, but more recent advances have extended that to a variety of large biomolecules and thermally labile organic and inorganic compounds.⁶⁵ The primary ionization techniques used today include electrospray ionization (ESI) and matrix-assisted laser desorption/ionization (MALDI). In ESI, a solution is passed through a capillary to produce a continuous stream of ions at atmospheric pressure.⁶⁵ This technique often appeals to multi-disciplinary researchers as it overcomes the problems of analyzing biomacromolecules and is easily paired with liquid chromatography (LC). MALDI involves ion production via pulsed-laser irradiation from the co-crystallization of a sample with a solid matrix.⁶⁵ The main difference between these ionization techniques is the state in which the sample is introduced to the MS. ESI utilizes a solvated sample that must be infused into the instrument whereas MALDI samples are introduced in the solid state. Additionally, MALDI often provides singly charged ions while ESI generates multiply charged ions. Depending on the intended analysis and coupled mass analyzer, singly charged ions can provide information regarding multiple ions but if working with a limited m/z range, multiple charges can facilitate the analysis of higher molecular-weight compounds.^{63,65}

After passing through the gate of ionization, ions move into the mass analyzer to be separated. There are two groups of mass analyzers, beam and trapping, but they share similar characteristics regardless of classification, including mass range, resolution, ion transmission to the detector, and sensitivity.⁶⁴ During beam analysis, ions exit the ion source in a beam and travel through the mass analyzer on their way to the detector. On the other hand, trapping analysis hold or “trap” ions within the mass analyzer before being pushed to the detector.⁶⁵ For simplicity, two of the more common mass analyzers, quadrupole and time-of-flight (TOF), will be briefly discussed. Quadrupoles consist of four parallel rods surrounding a circular cross section. At one end, the ions arrive via ion source and move through to the detector at the opposing end. These four rods are paired and mass separation is directly dependent on the m/z of the ion.⁶⁵ Two of rods are applied with direct current (DC) voltages while the remaining two link radio-frequency (rf) voltages. Through a combination of these forces, ions of a specified mass are able to move through the rods while those outside of the given mass will collide with rods of opposing polarity and discharge, ultimately having the rods serve as a mass filter.⁶⁴ TOF, on the other hand, is conceptually simple as ions are separated based on their velocity.⁶⁵ TOF employs a 1-2 m tube that allows the free flow of ions from one end to the other, before reaching the detector. Unlike quadrupoles, all ions reach the detector through TOF and two ions with the same nominal mass can be distinguished by their kinetic energy, ultimately determining the m/z of each ion. These kinetic energy differences between ions result in poor resolution because of mass dispersion, but this limitation has been overcome by changing the ionic path through the development of an electrostatic ion mirror, or a reflectron-type TOF.⁶³

Tandem mass spectrometry (MS/MS) describes the concept of connecting two or more mass analyzers in sequence to analyze components of a mixture (**Figure 2.6**). In phase one (MS₁), ions from the ion source are filtered to a specific m/z to eliminate any residual chemical noise. These parent ions are then subjected to fragmentation in the collision cell and move on to MS₂, where daughter ions are then analyzed by their m/z .^{63,65} Advantages of MS/MS include the reduction of residual chemical noise, ultimately enhancing sensitivity, and potentially gaining more structural information on the targeted analyte by utilizing its fragmentation pattern.

Common MS/MS instruments include the triple quadrupole (QqQ) and the hybrid quadrupole orthogonal time-of-flight, of Q-TOF.⁶³

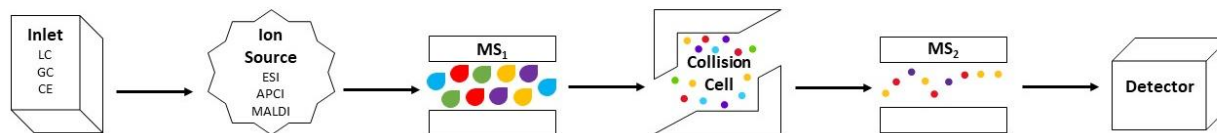


Figure 2.6 Scheme of tandem mass spectrometry, where two or more mass analyzers are in sequence to analyze components of a mixture. Starting at the inlet, analytes are ionized in the ion source and the subject ion then moves through MS_1 for a precursor ion mass selection. The collision cell is the site of fragmentation before the product ion is then analyzed in MS_2 , followed by detection.

For quantification of cocoa procyanidins, reversed-phase (RP) or normal-phase (NP) high performance liquid chromatography (HPLC) is coupled with ESI-MS. RP is the most common form of HPLC ESI-MS due to its powerful separation ability, ease of operation, and wide commercial availability of authentic standards. It operates on the principle that the flow path is moving in increasing polarity, as the stationary phase is non-polar and the mobile phases are polar (i.e. water, methanol, acetonitrile). Yet RP-HPLC has its limitations including the limited retention of hydrophilic, ionic, and polar molecules, including but not limited to, high molecular weight cocoa procyanidins.⁶⁶ NP, although similar to RP in that there is a wide commercial availability of authentic standards and its ease of operation, is the exact opposite of RP with the flow path moving from more polar to less polar, as the stationary phase is polar and the mobile phase is non-polar (i.e. hexane, diethyl ether). In NP-HPLC, analyte retention is inversely related to the mobile phase polarity, with increased analyte retention as polarity decreases therefore causing more polar analytes to have a higher degree of retention than non-polar analytes.⁶⁷ Although NP-HPLC can overcome many of the limitations associated with RP, it is difficult to interface with ESI-MS because of the non-polar solvents required.⁶⁶

The quantification of high molecular weight procyanidins has proven to be difficult due to their structural complexity.⁶⁸ NP-HPLC coupled with fluorescence detectors (FLD) has been the gold standard in the quantification of complex, high molecular weight cocoa procyanidins despite long run times and limited sensitivity.⁶⁸⁻⁷³ Recent advancements in column technologies and hydrophobic interaction liquid chromatography (HILIC) applications extend promise in the

improved quantification of these large procyanidins while coupling with MS/MS for mass confirmation and fragmentation lost in HPLC-FLD. HILIC employs aspects of both RP and NP chromatography, using a polar stationary phase and organic polar solvents, similar to those in RP, along with the addition of water to serve as a stronger eluting solvent.⁶⁶ HILIC eluent gradients increase in polarity- beginning with low-polarity organic solvents and increasing as compounds begin to elute.^{67,74} Mobile phase additives or post-column infusion are often utilized to manipulate the solution pH and increase ion strength.⁶⁷ Although complex, HILIC runs with many advantages including up to a 10-fold increase in sensitivity compared to RP, improved on-column retention, affluent pairing with MS/MS, and higher sample throughput/shorter run times.⁶⁷

2.8 Conclusions

Cocoa fermentation is a well investigated phenomenon but the relationship between fermentation, further processing, and cocoa's bioactive properties are not well understood. Although it is widely known that fermentation and roasting significantly decrease the levels of native polyphenols within cocoa beans, how this degradation impacts (or possibly preserves and enhances) cocoa bioactivity is still under investigation. Furthermore, the mechanisms driving these health protective activities are largely unknown and can depend on a variety of factors, such as bean variety and composition, processing environment and harvest practices, as well as processing parameters. The purpose of the work in the following chapters was to process raw unfermented beans in a controlled environment so that a relationship between processing techniques, chemical composition, and biological activity could be established. To effectively and efficiently quantify the influential procyanidins within cocoa beans, a HILIC UPLC-MS/MS method was developed. Cocoa beans were then fermented and dried on a large pilot-scale in a fermentation model system to effectively determine the fermentation kinetics and success of our model system. Finally, using this fermentation model system, cocoa beans of seven different treatments were fermented, roasted, and further processed into powder to assess the α -glucosidase inhibitory activity of cocoas produced under different processing parameters.

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CHAPTER 3. Development of a Rapid HILIC UPLC-MS/MS Method for Procyanidins with Enhanced Ionization Efficiency

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ABSTRACT

Cocoa flavanols (catechins and procyanidins) can exist in various polymerization states and are commonly classified by their degree of polymerization (DP). There is increasing evidence that flavanols of distinct DP possess different biological activities, but separation and quantification of the higher DP procyanidins is challenging and has thus created the need for new methodologies that utilize advancements in columns and LC-MS/MS systems. An aqueous normal phase (hydrophilic interaction liquid chromatography, HILIC), UPLC method with post-column ESI adjuvant infusion was developed to reduce the total analysis time, increase peak separation, and increase detection specificity (compared to traditional fluorescence methods) by coupling with mass spectrometry detection. The total elution time was reduced from 70-90 min (typically used for normal phase and HILIC HPLC separation of procyanidins) down to 9 min by employing UPLC. Results indicate that by using a post-column 0.04 M ammonium formate infusion (5 $\mu\text{L}/\text{min}$), ionization of procyanidins was significantly enhanced. Lower limits of detection ranged from 3.19×10^{-2} -4.56 pmol-on-column, and lower limits of quantification ranged from 2.79×10^{-2} - 1.17×10^2 pmol-on-column across compounds DP 1-9. This method builds upon the foundation set by existing analytical methods and employs new technologies to dramatically increase sample throughput and enhance detection limits and specificity, facilitating improved analysis for procyanidins.

3.1 INTRODUCTION

Cocoa is one of the most abundant sources of dietary flavanols, a subclass of flavonoids. Flavanols can exist as monomers ((±)-catechin (C), (-)-epicatechin (EC), etc.) or in various polymerization states (oligomers and polymers known as procyanidins, proanthocyanidins or condensed tannins) (**Figure 3.1**). These compounds are commonly classified by their degree of polymerization (DP), and products such as cocoa contain high amounts of flavanols with DP 1-10 [1–3]. Cocoa flavanols have drawn significant interest due to their apparent health promoting effects, and there is increasing evidence that procyanidins with different DP possess structurally distinct biological activities [4–6]. Thus, qualitative and quantitative analysis of procyanidins by DP is important for understanding the biological activities of procyanidins.

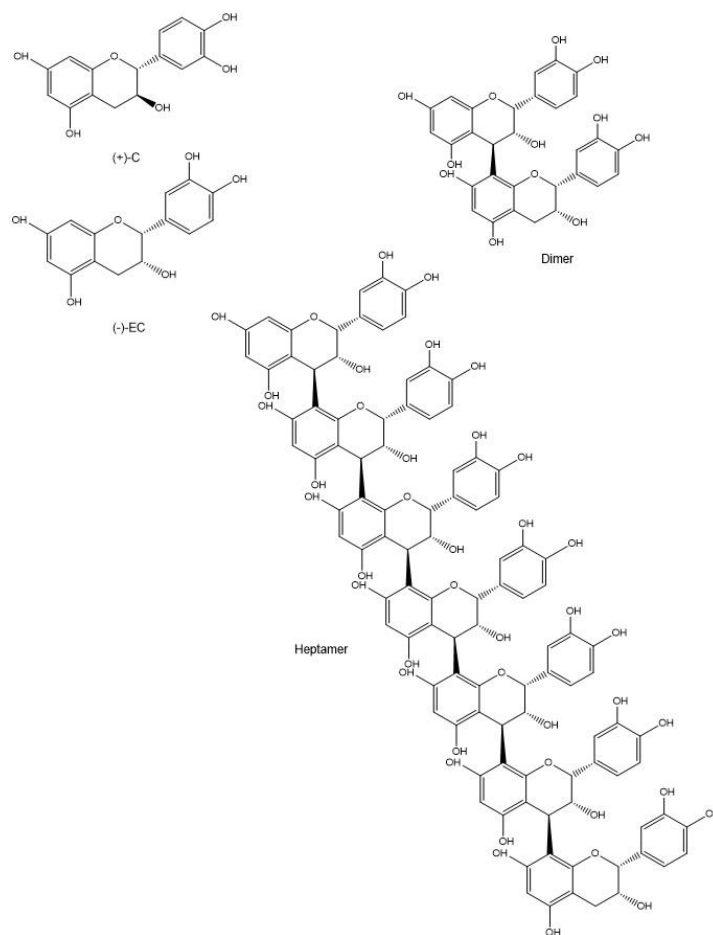


Figure 3.1. Structures of monomeric cocoa flavanols (C, EC), and select representative flavanol oligomers (dimer, heptamer). Note that raw cocoa beans contain primarily (-)-C, but epimerization during processing results in (+)-C being the predominant epimer in finished cocoa products and cocoa powder.

Due to factors such as ease of analysis by and more widespread use of reverse-phase (RP) LC (which typically cannot resolve the large procyanidins adequately), wide commercial availability of standards and comparatively high bioavailability, much of the literature focuses on the food content and biological action of flavanol monomers, C and EC. However, the larger species (oligomeric and polymeric flavanols) are widely distributed in the diet, and recent evidence suggests that despite their limited bioavailability, these complex flavanols are effective at mediating the onset of obesity and insulin resistance as well as protecting against gut inflammation activity when compared to smaller flavanol fractions [5–7]. Although the relationship between DP and biological activity remains the subject of investigation, these complex flavanols are the subject of increasing investigation as potentially potent and novel complementary approaches to chronic disease prevention. Due to this interest, it is critical to develop analytical methods that can provide rapid, sensitive and specific detection and quantification of these individual procyanidins in order to more thoroughly understand their underlying mechanisms of action, plant distribution and consumption patterns.

Because of the structural complexity these high molecular weight procyanidins possess, their analysis is challenging [1]. There is generally an inverse relationship between flavanol DP and detector response (for various detection modalities), and thus limits of detection, limits of quantification, and analytical sensitivity [8]. Normal-phase (NP) or HILIC HPLC coupled to fluorescence detection (FLD) typically provide the best resolution of large flavanols, but efficiency and sensitivity remain the primary challenge of using these methods [1,8–12]. With run times typically ranging between 70-90 min, these methods are severely limited by low sample throughput and place high demand on analytical resources. Machonis et al [10] was able to significantly optimize the robust, widely-used NP method proposed by Robbins et al [9], reducing the elution time to 15 min as opposed to 86 min. Additionally, Hollands et al [8] adapted the method proposed by Robbins et al [9] but with a HILIC HPLC application to quantify large procyanidins extracted from apples. Although this method is able to quantify similar procyanidins, it has a lengthy 45 min run time. Recently, advances in UPLC column technology and the improvement of HILIC UPLC columns suggests that the speed of these methods may be optimized even further. However, despite reduced analysis time and increased throughput, sensitivity of high DP compounds remains low. This is due to the fact that NP methods typically rely on FLD [9–11]. While FLD is useful for procyanidins, use of FLD does not provide the specificity of definitive

mass confirmation and fragmentation achieved by MS/MS. Therefore, coupling the NP or HILIC resolution power with the specificity of mass spectrometry (MS) is desired. However, NP LC is poorly compatible with the standard MS ionization source, electrospray ionization (ESI), which relies on the presence of high concentrations of protic solvents and other ionizable mobile phase reagents to facilitate charge transfer to analytes, while RP and HILIC LC are better suited for MS pairing. Though HILIC solvents are much better suited for ESI than NP, the comparatively low concentrations of water used for HILIC (vs. RP) suggest that ESI ionization efficiency could still be enhanced through post-column reagent infusion to achieve ionization performance similar to that of RP conditions, and therefore improving sensitivity and achieving adequate limits of detection and quantification [13,14]. Recently, the use of post-column ionization reagents has been proposed for improved ESI performance of flavanols [12].

To continue advancing our understanding of the role of procyanidins in human health, the quantification of these large procyanidins must be addressed. Long analysis times require extended instrument use and large quantities of solvents that could otherwise be used for other analyses. Additionally, long analysis times grouped with lengthy sample sets could lead to sample degradation. The objective of this study was therefore to develop an optimized methodology that rapidly and sensitively quantifies individual procyanidins based upon their DP to reduce instrument time, lower laboratory costs, and increase sample throughput. We sought to achieve this by pairing recent improvements in HILIC-UPLC with use of post-column ESI adjuvant infusion.

3.2 MATERIALS AND METHODS

3.2.1. Reagents, standards, and samples. LC-MS grade acetonitrile (ACN), methanol (MeOH), and water were obtained from Thermo Fisher Scientific (Waltham, MA). Glacial acetic acid, methanol, and acetone were obtained from VWR (Radnor, PA). Ammonium formate and (–)-epigallocatechin gallate (EGCG) were obtained from Sigma-Aldrich (St. Louis, MO). Standards of (±)-catechin (C), (–)-epicatechin (EC), and procyanidin B2 (PCB2) were obtained from ChromaDex (Irvine, CA). Standards of procyanidin C1 (PCC1, DP3), cinnamtannin A2 (CinA2, DP4), and DP5 – 9 purified from cocoa (purity: DP 3-5: 93-99%, DP6-9: 80-92%) were obtained from Planta Analytica (New Milford, CT). Raw unfermented cocoa beans were commercially available, sourced from Ecuador, and received from Natural Zing LLC (Mount Airy, MD).

3.2.2. Sample preparation. Flavanol-rich cocoa extract (CE) was obtained using the method developed by Dorenkott et al [5], with minor modifications. Cocoa beans were frozen using liquid nitrogen and then ground in a laboratory blender (Waring Products, Stamford, CT) for 2 min to obtain a powder. To de-fat the cocoa powder, ground powder (40 g) was extracted with 150 mL of hexane and sonicated for 10 min. The mixture was centrifuged at $5000 \times g$ for 5 min and the supernatant was discarded. After repeating the de-fatting step, the residual hexane was evaporated. Extraction solution (150 mL) consisting of 70:28:2 (v/v/v) acetone, water, and acetic acid, and dried defatted cocoa powder were mixed and sonicated (10 min). Supernatant was collected after centrifuging the mixture at $5000 \times g$ for 5 min. This procedure was repeated until colorless supernatant was obtained. Supernatants from each extraction were pooled, and acetone was evaporated by using rotary vacuum evaporator RV 10 basic (IKA®, Wilmington, NC) at 45°C. The remaining extract was frozen at –80 °C and freeze dried. Freeze dried CE was then crushed into powder and stored at –80 °C until further analysis. For analysis, CE was dissolved in extraction solution [70:28:2 (v/v/v) acetone, water, acetic acid] to specified concentrations.

3.2.3. UPLC-MS/MS analysis. Cocoa monomeric flavanols and procyanidins were analyzed by UPLC-MS/MS. A Waters Acquity H-class separation module (Milford, MA) equipped with an Acquity Torus DIOL Column (2.1 mm \times 100 mm, 1.7 μ m particle size, 45 °C) and Torus DIOL VanGuard Pre-column (2.1 mm \times 5 mm, 1.7 μ L particle size) was used to perform the analysis.

Binary gradient elution was performed with 2% acetic acid in acetonitrile (phase A) and 3% water and 2% acetic acid in methanol (phase B). Solvent flow rate was 0.8 mL/min and the linear gradient elution was carried out as follows: 100% A (0 min), 55% A (5.7 min), 5% A (6.0 min), 100% A (6.7-9.0 min). (-)-mode ESI coupled to tandem mass spectrometry (MS/MS) on a Waters Acquity triple quadrupole (TQD) MS was used to analyze the UPLC eluent. Ammonium formate (0.04M in water, 5 μ L/min) was added to the eluent flow stream post-column to enhance ionization of the high molecular weight compounds. Ionization settings were as follows: (-) mode, capillary voltage: -4.5 kV, cone voltage: 60.0 V, extractor voltage: 1.0 V, source temperature: 150 °C and desolvation temperature: 500 °C. N₂ was used for cone and desolvation gasses with flow rates of 50 and 1000 L/h respectively. For MS/MS, Ar was used as a collision gas with 0.1 mL/min flow rate. Parent ions and signature daughter ions followed by collision-induced dissociation (CID) were subjected to multi-reaction monitoring (MRM) with a mass span of 0.2 Da and 1.0 sec of inter-channel delays and inter-scan times. MRM settings for each compound are listed in **Table 3.1**. MassLynx software (version 4.1, Waters) was used to acquire data.

Table 3.1. MS/MS settings for MRM detection of monomer-decamer.

Compound	t_R^a (min)	MW (g mol ⁻¹)	[M - H] ^{-b} (m/z)	Daughter Ion (m/z)
Monomer	0.61	290.27	289.03	245.06
Epigallocatechin	0.74	458.37	305.04	124.98
Dimer	2.03	578.52	577.14	425.10
Trimer	3.05	866.77	865.22	287.07
Tetramer	3.73	1155.02	576.40	125.02
Pentamer	4.26	1443.28	720.41	125.02
Hexamer	4.66	1731.53	864.52	125.02
Heptamer	5.00	2017.81	1008.40	125.17
Octamer	5.28	2308.03	1152.58	125.17
Nonamer	5.53	2596.54	864.12	125.17
Decamer	5.75	2884.54	960.18	125.17

^aretention time

^bAll MRMs used singly-charged parents ions except for pentamer, hexamer, heptamer, and octamer, which are double-charged ([M - 2H]²⁻), and nonamer and decamer, which are triple-charged ([M - 3H]³⁻)

3.2.4. UPLC-MS/MS optimization. Various ionization enhancers were evaluated for their ability to increase analyte peak areas by post-column infusion. 1.0 M solutions of ammonium formate,

sodium carbonate, sodium acetate, sodium citrate, ammonium bicarbonate, as well as water, and control (no infusion) were infused into the flow at 10 $\mu\text{L}/\text{min}$, tested on ionization following injection of a highly concentrated CE (40 mg/mL) with an injection volume of 1 μL . See section 2.3 for conditions.

Various post-column infusion rates of 0.5 M ammonium formate were then evaluated for their ability to increase analyte peak areas (whereas 1 M ammonium formate was used initially, preliminary experiments suggested lower concentrations would be optimal and therefore this experiment was performed with 0.5 M). Using injection of the 40 mg/mL CE under identical conditions, infusion was introduced at 0-30 $\mu\text{L}/\text{min}$ (the maximum flow rate of the built-in Acquity TQD syringe pump). Various concentrations of the infusion enhancer were also evaluated for their ability to increase analyte peak areas. Concentrations of ammonium formate ranging from 0-2.0 M were infused at 5 $\mu\text{L}/\text{min}$ into the flow using during injection of the 40 mg/mL CE. Because of the highly concentrated CE, a wash step (50 μL , 5 min) of phase C [70:28:2 (v/v/v) acetone, water, acetic acid] was injected after every 2 sample injections, followed by a 4 min pre-run to revert to initial starting conditions. Pre-run conditions were as followed: a linear gradient of 100% C, 0.6 mL/min (0 min), 100% A, 0.6 mL/min (.10 min), 100% A, 0.8 mL/min (3-4 min). This wash step was not employed for CE injection concentrations lower than 40 mg/ml (representing typical use).

Due to the use of an ESI enhancer, following infusion selection and optimization, the tune (i.e. ESI source) settings were optimized by infusing .04 M ammonium formate with dissolved CE (1.5 mg/mL) at 5 $\mu\text{L}/\text{min}$ (the final optimized infusion settings) and adjusting the cone and capillary voltages, source and capillary temperatures, and gas flow rates to select conditions maximizing the enhancements due to the enhancer (data not shown, as these data were collected using direct CE infusion). To evaluate the combined effects of the ESI enhancer and modified tune settings, samples were run in triplicate according to the following: no infusion/original tune, no infusion/optimized tune, infusion/original tune, infusion/optimized tune.

In order to assess the impact of injection volume on peak shape, a 5 mg/mL CE was prepared and tested at the following volumes: 0.5, 1, 2, 5, 10, 20, 30, 40, and 50 μL . Because of the fact that increasing the injection volume also increases the total mass injected, a second experiment was performed in which the concentration was varied so that the total mass injected was the same across various injection volumes: 40 mg/mL (1 μL), 20 mg/mL (2 μL), 10 mg/mL (4 μL), 5 mg/mL (8 μL), 2.5 mg/mL (16 μL), 1 mg/mL (40 μL).

3.2.5. Measurement of variability and calibration curve. Intraday variability was assessed by performing HILIC UPLC-MS/MS analysis using the final optimized method on a freshly made aliquot of 5 mg/mL CE nine times in the same day. An internal standard of epigallocatechin gallate (EGCG) was utilized at 0.01 mg/mL. Interday variability was assessed by performing HILIC UPLC-MS/MS analysis on freshly thawed aliquots of CE with 0.01 mg/mL EGCG nine times for three consecutive days.

Calibration curves for standards DP 1-9 were prepared and analyzed in triplicate. 18 dilutions, ranging from 6.93×10^{-7} - 0.091 mg/mL were prepared with 0.01 mg/mL EGCG in all samples. In order to calculate lower limit of detection (LLOD) and lower limit of quantification (LLOQ), analysis was performed on incrementally diluted concentrations of each standard until the signal (peak height):noise ratio was reduced to 3:1 or 10:1, respectively. LLOD or LLOQ for each standard was then defined as the lowest amount (pmol-on-column) that resulted in a signal:noise ratio of >3:1 or >10:1, respectively. LLOD and LLOQ were determined in triplicate and the mean LLOD and LLOQ are reported.

3.2.6. Data analysis. Statistical analyses were performed on XLSTAT-Base (2018.5, New York, NY) and GraphPad Prism 7.03 (GraphPad, La Jolla, CA). Data were analyzed by one-way ANOVA to determine the overall significance and if detected, Tukey's HSD post-hoc test was used to compare all means. Significance was defined *a priori* as $P < 0.05$.

3.3 RESULTS AND DISCUSSION

In the present study, we developed a comparatively rapid HILIC-UPLC-MS/MS method to more efficiently and effectively quantify cocoa flavanols by their DP. We achieved this by employing a UPLC HILIC column to optimize peak resolution and then utilizing post-column ionization of ammonium formate to improve ESI-MS ionization. Although our method meets the definition of traditional NP through the utilization of mobile phases less polar than the stationary phase, it is in fact aqueous NP (HILIC) due to the solvents used. By optimizing the optimal infusion compound, rate, and concentration, as well as modifying the source parameters, we were able to significantly reduce the elution time while enhancing the MS signal of each procyanidin analyzed.

3.3.1 Infusion identification and optimization. In order to identify potential post-column reagents enhancing procyanidin ionization, 1.0 M solutions of various compound were infused post-column at 10 $\mu\text{L}/\text{min}$ as potential ESI enhancers on the basis of their compatibility with mobile phase and ability to improve ionization in HILIC LC-MS (**Figure 3.2**). These were employed during analysis of an injected CE solution. Small organic acids and bases, such as ammonium formate, are especially volatile and can have positive implications on the ionization of higher molecular-weight compounds. The peak areas of each compound (DP 1- 10) obtained with each of the tested ionization enhancers are shown in **Figure 3.2**. The infusion compound was then selected on the basis of generally enhanced maximal peak area across all compounds analyzed. Ionization efficiency was generally good for monomers and other small flavanols regardless of the nature of the infused compound, as expected. Some tested compounds (sodium carbonate and sodium acetate) actually suppressed ionization almost completely for most flavanols. Although water had optimal ionization for smaller flavanols (EGC, monomer, dimer, and trimer), ammonium formate was the best of the tested compounds at enhancing flavanol ionization for the larger flavanols, DP 4 - 10. Therefore, ammonium formate was selected for further optimization.

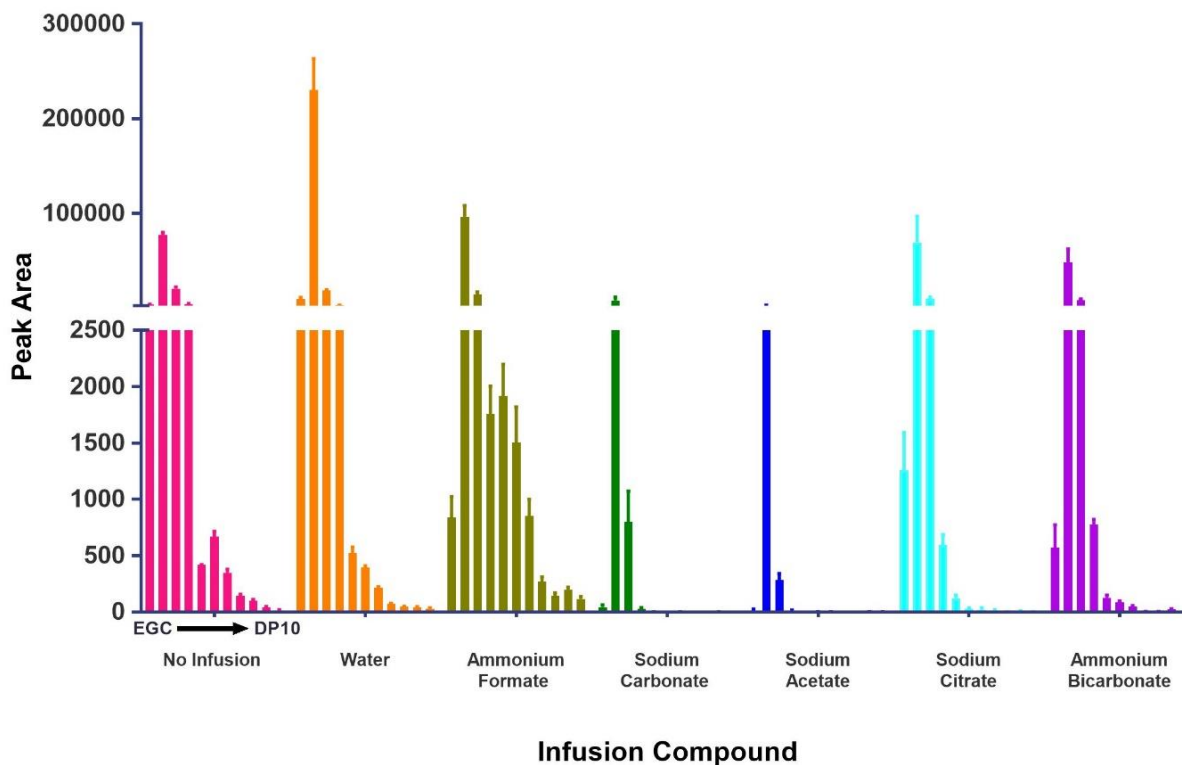


Figure 3.2. Peak areas of cocoa flavanols resulting from post-column infusion of potential ESI enhancer compounds. ESI enhancers (1 M) were infused at 10 $\mu\text{L}/\text{min}$ into the flow path after column elution but before ionization, through the built-in syringe pump of the LC-MS/MS instrument: no infusion, water (LC-MS grade), ammonium formate (1M), sodium carbonate (1M), sodium acetate (1M), sodium citrate (1M), ammonium bicarbonate (1M). A 40 mg/mL cocoa extract was injected into the column at a volume of 1 μL . Each bar represents the peak areas of a different analyte, progressing from EGC, DP1 – DP10. Samples were analyzed in triplicate and values are presented as the mean \pm SEM.

Next, we optimized the rate and concentration of ammonium formate to achieve optimal ionization enhancement. Infusion rate and concentration were the primary factors surrounding ionization optimization. **Figure 3.3** demonstrates various ammonium formate (1.0 M) infusion rates from 0-30 $\mu\text{L}/\text{min}$. Overall, the 5 $\mu\text{L}/\text{min}$ infusion rate resulted in optimal peak areas for all identified procyanidins. With regards to EGC, which was somewhat suppressed by 5 $\mu\text{L}/\text{min}$ infusion, this method is designed to optimize ionization of larger compounds, and we were thus willing to sacrifice the ionization of lower molecular weight compounds (monomers, for which there are numerous existing RP methods with excellent compatibility with ionization) in order to enhance ionization of larger molecular weight compounds. With regards to all other compounds, there are statistically significant differences in peak areas across infusion rates for trimers,

tetramers, and hexamers, as denoted by the superscripts. The lack of statistical difference differences in peak areas across infusion rates for many of the compounds (DP 5, 7-10) is due to the extremely high variability in peak areas that was observed for some of the higher infusion rates. Despite the greater mean peak areas at these higher rates, extreme variability is not optimal for method performance. Because of this, we chose to move forward with 5 $\mu\text{L}/\text{min}$, which was selected as the best combination of enhanced peak areas for larger compounds. Higher infusion rates generally resulted in large variability. Next, we optimized the concentration of ammonium formate from 0-2 M at 5 $\mu\text{L}/\text{min}$ (**Figure 3.4**). 0.04 M ammonium formate consistently resulted in the highest sensitivity among all compounds. Through these steps it was determined that an infusion of 0.04 M ammonium formate at 5 $\mu\text{L}/\text{min}$ produced optimal sensitivity and ionization of the higher molecular weight flavanols.

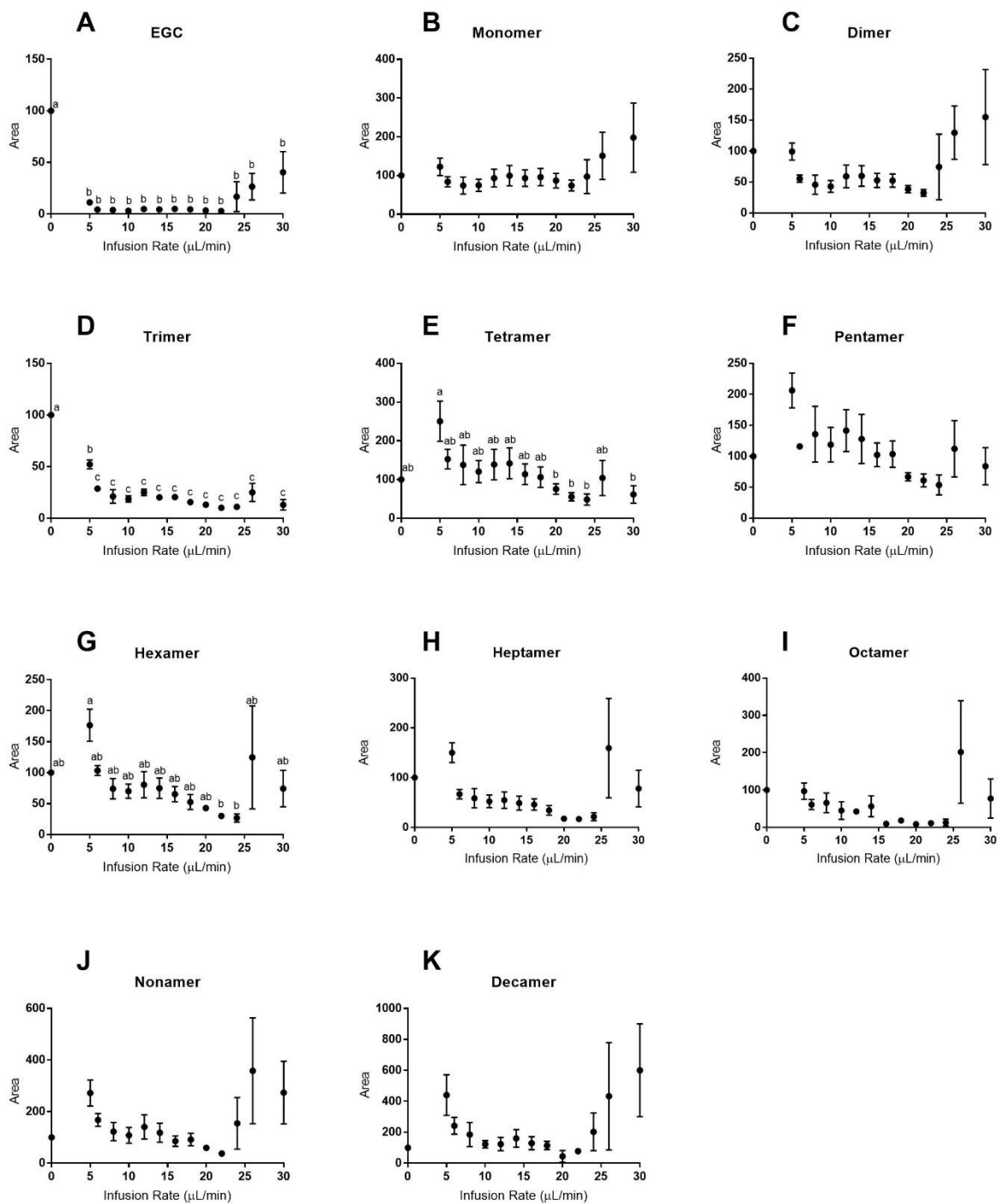


Figure 3.3. Optimization of ammonium formate infusion rate. 1.0 M ammonium formate was infused at various rates from 0-30 $\mu\text{L}/\text{min}$. Injections were performed using a highly concentrated 40 mg/mL CE at an injection volume of 1 $\mu\text{L}/\text{min}$. All values have been normalized to 100% using a no infusion baseline (0 μL). Samples were analyzed in triplicate and values are presented as the mean \pm SEM. Significance between time points within each compound was determined by one-way ANOVA and Tukey's HSD post-hoc test ($P < 0.05$) Time points with superscripts are significantly different and those with no superscripts indicate no significant difference between treatments.

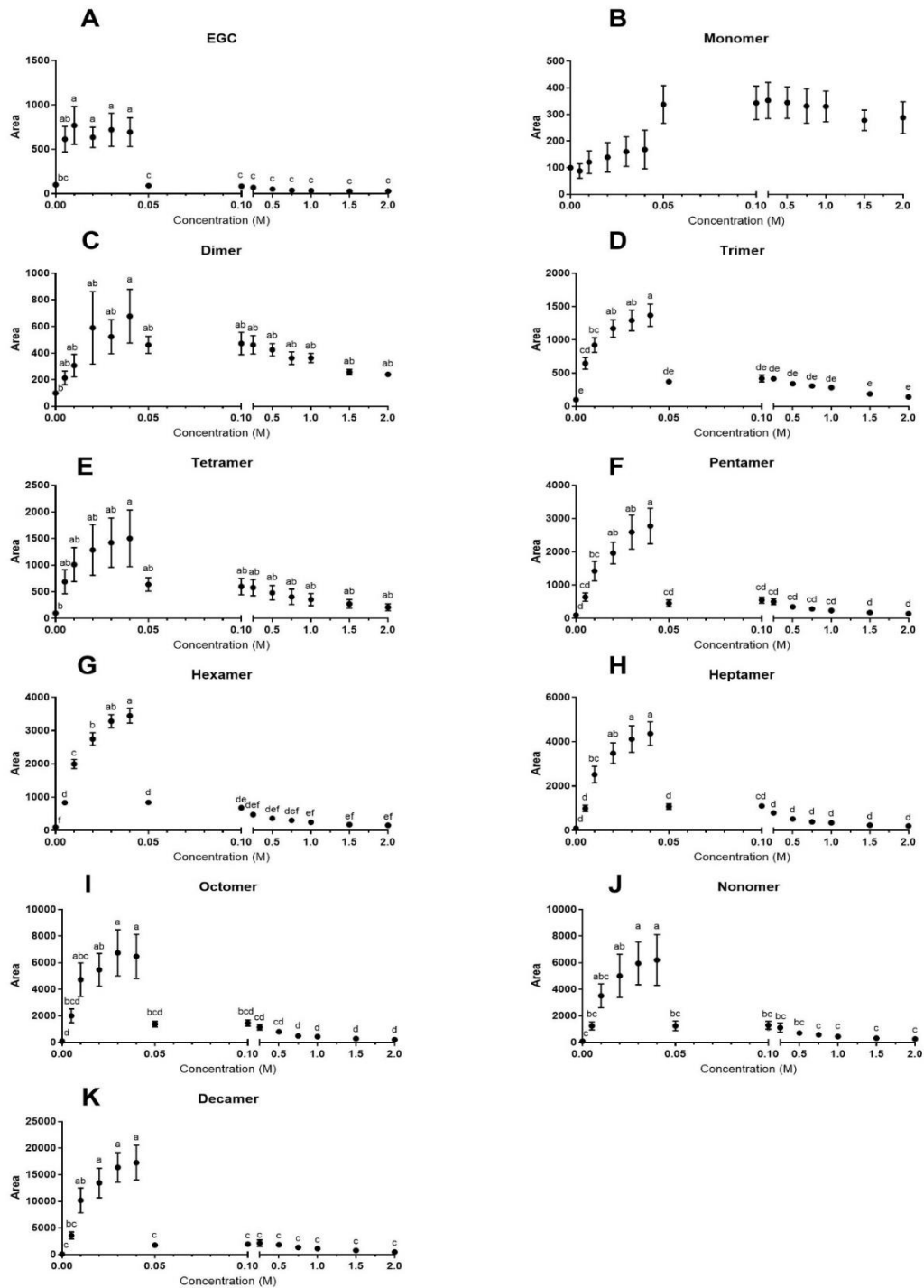


Figure 3.4. Optimization of ammonium formate infusion concentrations. Ammonium formate was infused at various concentrations from 0-2.0 M at 5 μ L/min. Injections were performed during analysis of a highly concentrated 40 mg/mL CE at an injection volume of 1 μ L. All values have been normalized to 100% using a no infusion baseline (0 μ L). Note broken x-axis for ease of interpretation. Samples were analyzed in triplicate and values are presented as the mean \pm SEM. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($P < 0.05$) Time points with superscripts are significantly different and those with no superscripts indicate no significant difference between treatments

Due to the modifications in the ionization, we next manually optimized the tune (i.e. source) settings, in the context of infusing 0.04 M ammonium formate at 5 $\mu\text{L}/\text{min}$, in order to account for the presence of the ammonium formate (data not shown). The original source settings were 60 V (cone), -4.5 kV (capillary), 1 V (extractor), 0 V (RF lens), 150°C (source temp), 1000 L/hr (desolvation gas flow), 50 L/hr (cone gas flow), and after optimization the modified source settings were 45 V (cone), -4.25 kV (capillary), 1 V (extractor), 0 V (RF lens), 150°C (source temp), 1000 L/hr (desolvation gas flow), and 50 L/hr (cone gas flow). Therefore, these modified source settings were employed moving forward. In order to assess the combined impacts of the ammonium formate infusion (0.04 M at 5 $\mu\text{L}/\text{min}$) and the modified tune settings on ionization efficiency, we analyzed CE with and without the infusion and the modified source settings in combination (**Figure 3.5**). Without infusion, there was minimal change to the majority of the procyanidins ionized using the modified tune settings. Once infusion was introduced, we were able to further improve ionization efficiency for the better part of the analyzed procyanidins. It is very clear that the ammonium formate infusion significantly contributes to enhanced ionization of procyanidins beyond trimer. Although the benefit of these conditions is lower in monomers (EGC, C, and EC) and modest for dimers and trimers, larger analytes are increasingly more difficult to individually ionize and the infusion/optimized tune produced signal as much as 100X more amplified than without (**Figure 3.5 E-K**). Although many of the procyanidins did not show a statistically significant difference between the original and optimized tune settings, EGC, monomer, and dimer did significantly improve from original to optimized tune settings, thus using this rationale to move forward with optimized tune settings. Furthermore, it is unknown why some compounds exhibited greater variability in this experiment. This demonstrates the significant improvement in ionization, and by extension the utility of this method.

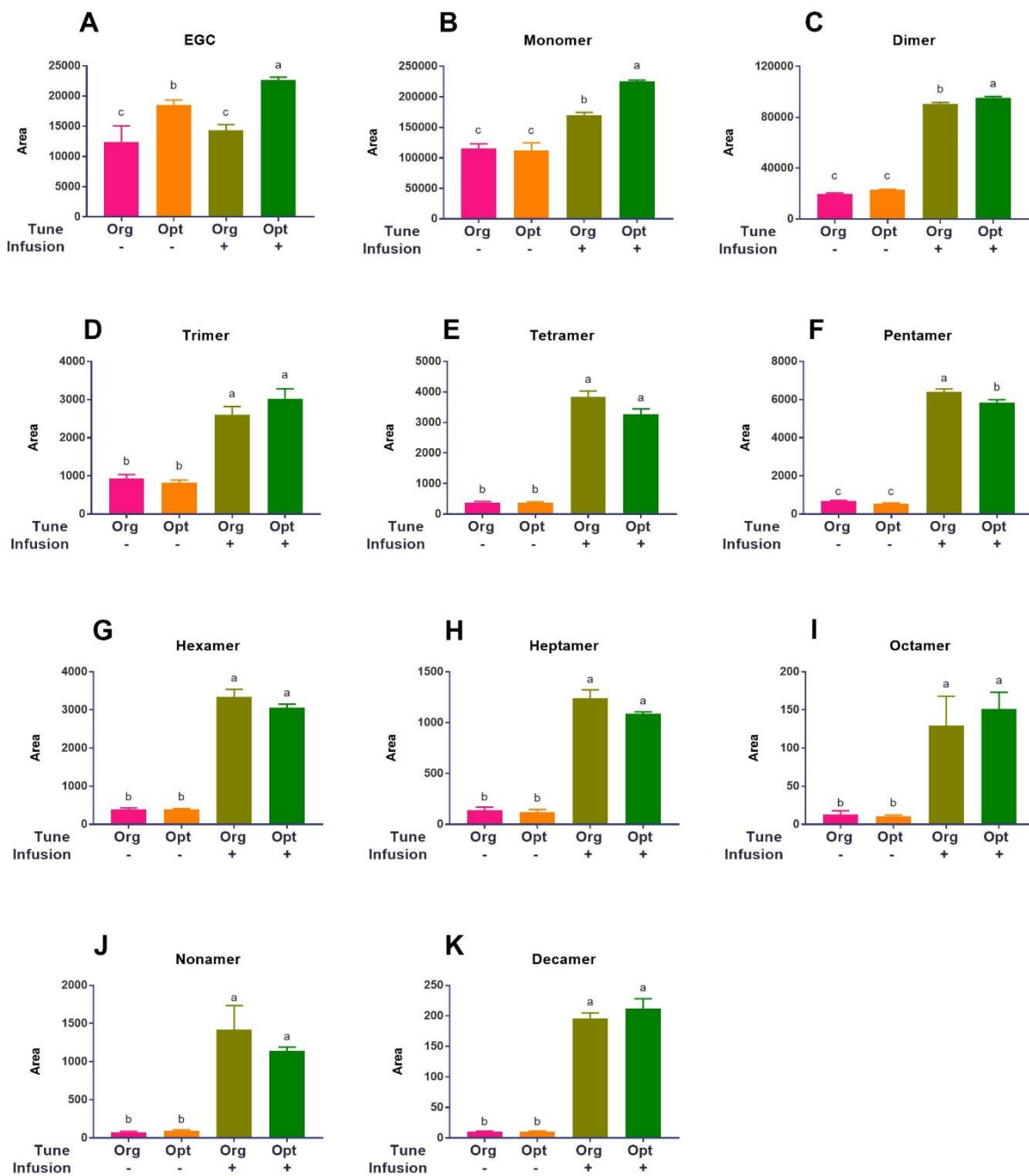


Figure 3.5. Net effect of optimized infusion and MS tune (i.e. source) settings. Samples were run with and without the infusion solution (.04 M ammonium formate infused at 5 $\mu\text{L}/\text{min}$) at original (org) and optimized (opt) tune settings. Injections were performed using a 5 mg/mL CE at an injection volume of 2 μL . Samples were analyzed in triplicate and values are presented as the mean \pm SEM.

3.3.2. Impact of injection volume. Injection volume of the CE can have an impact on the peak intensity. This is due to the fact that the optimal solvent for extraction and dissolution of CE is acetone/water/acetic acid, which is somewhat incompatible with the starting conditions for the LC method and results in poor peak shape [5] if the injection volume is too large. To demonstrate this, a two-factor approach of various injection volumes and concentrations of CE were tested (**Figures 3.6A and 3.6B**). Progressing from 0.5-50 μL injection volume, **Figure 3.6A (A-I) and Figure 3.6B (A-I)**, it is visually apparent how the peak shape deteriorates. When injection mass is held constant across various injection volumes, the same peak deterioration is seen, **Figure 3.6A (J-O) and Figure 3.6B (J-O)**. However, at 50 μL injection volume (**Figure 3.6A (I) and Figure 3.6B (I)**) there is a positive influence in the peak separation. It is possible that for this specific injection, the peak height is higher and thus suppressing the noise relative to the signal. Generally, lower injection volumes are desired as higher injection volumes, independent of analyte mass, hinder effective resolution due to the solvent itself. This confirms the poor compatibility of the extraction solvent (acetone/water/acetic acid) with the starting conditions, and the need to minimize the injection volume. Through this approach we were able to define the limits of this particular solvent and concluded $\leq 5 \mu\text{L}$ as the optimal injection volume.

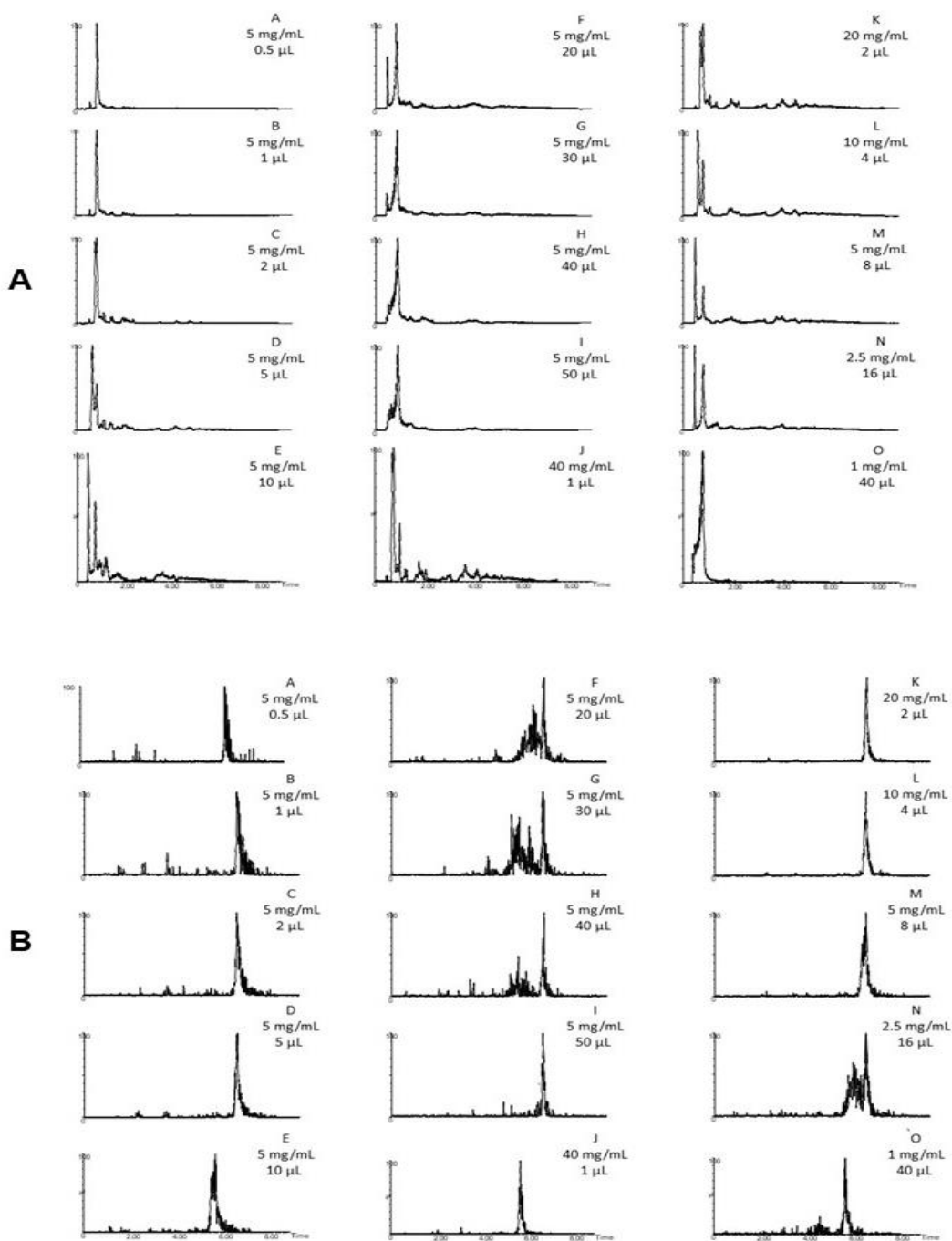


Figure 3.6. (A) MRM chromatograms of flavanol monomers, representing the impact of injection volume on peak intensity. A 5 mg/mL CE was injected at (A) 0.5 μ L, (B) 1 μ L, (C) 2 μ L, (D) 5 μ L, (E) 10 μ L, (F) 20 μ L, (G) 30 μ L, (H) 40 μ L, and (I) 50 μ L. A 40 mg/mL CE was injected at 1 μ L (J), 20 mg/mL CE at 2 μ L (K), 10 mg/mL CE at 4 μ L (L), 5 mg/mL at 8 μ L (M), 2.5 mg/mL CE at 16 μ L (N), and 1 mg/mL CE at 40 μ L (O). (B) Decamer MRM chromatograms representing the impact of injection volume on peak intensity. A 5 mg/mL CE was injected at (A) 0.5 μ L, (B) 1 μ L, (C) 2 μ L, (D) 5 μ L, (E) 10 μ L, (F) 20 μ L, (G) 30 μ L, (H) 40 μ L, and (I) 50 μ L. A 40 mg/mL CE was injected at 1 μ L (J), 20 mg/mL CE at 2 μ L (K), 10 mg/mL CE at 4 μ L (L), 5 mg/mL at 8 μ L (M), 2.5 mg/mL CE at 16 μ L (N), and 1 mg/mL CE at 40 μ L (O).

3.3.3. Standard curve, lower limit of detection, lower limit of quantification. Standards for all analytes except DP10 were available and used for calibration and assessment of performance of the method. Each standard was analyzed in triplicate and the mean of those peak areas were used in the calculation of the calibration curves (**Table 3.2**). For calibration curve calculation, analyte concentration was expressed as mg/mL. For LLOD/LLOQ calculations, analyte levels were expressed as total pmol-on-column, calculated by multiplying the solution concentration by the injection volume (5 μ L). We used pmol-on-column, as opposed to concentration, as performance expressed as pmol-on-column is independent of injection volume and thus is a better reflection of true performance.

Table 3.2 Calibration curve slope and intercept, coefficient of determination (R^2), lower limit of detection (LLOD), and lower limit of quantification (LLOQ). Standards were run in triplicate and values were determined from the mean of those triplicates.

Compound	Equation ^a	R^2	LLOD		LLOQ	
			pmol ^b	\pm SEM	pmol ^b	\pm SEM
Monomer	$y = 60.334x + 0.0692$	0.9995	1.19×10^{-2}	0	2.79×10^{-2}	4.62×10^{-7}
Epigallocatechin	$y = 0.3489x + 0.0009$	0.9959	2.59	2.36×10^{-4}	2.32×10^1	7.10×10^{-4}
Dimer	$y = 21.968x + 0.0057$	0.9999	3.19×10^{-2}	9.25×10^{-7}	6.39×10^{-2}	1.85×10^{-6}
Trimer	$y = 0.9027x - 0.0004$	0.9999	1.28×10^{-1}	0	1.19	7.83×10^{-5}
Tetramer	$y = 0.8035x - 0.0017$	0.999	1.28×10^{-1}	7.40×10^{-6}	8.97×10^{-1}	7.83×10^{-5}
Pentamer	$y = 0.5283x + 0.0003$	0.9992	5.53×10^{-2}	1.42×10^{-5}	8.20×10^{-1}	5.92×10^{-5}
Hexamer	$y = 0.1699x + 0.0004$	0.9936	1.45	4.59×10^{-4}	3.08	3.55×10^{-4}
Heptamer	$y = 0.0649x + 1.21 \times 10^{-5}$	0.9966	8.79×10^{-1}	0	6.45	1.55×10^{-3}
Octamer	$y = 0.0225x + 2.01 \times 10^{-6}$	0.9974	1.79	3.13×10^{-4}	9.23	1.42×10^{-3}
Nonamer	$y = 0.0601x - 0.0002$	0.9692	4.56	1.66×10^{-3}	1.17×10^2	1.52×10^{-2}

^aFor calibration curve calculations, analyte concentration is expressed as mg/mL.

^bLLOD and LLOQ values expressed as pmol-on-column, calculated by multiplying solution concentration by injection volume (5 μ L). Pmol-on-column is independent of injection volume and is a better reflection of true performance.

LLOD/Q values are measured for method performance assessment, and comparison with previously reported values from well-established methods emphasize the advantage of pairing MS with post-column ionization in the present method. NP HPLC with fluorescence detection is generally regarded as the gold standard in cocoa procyanidin quantification and thus provides us

with LLOD/Q values to better understand the difference in detectors. Generally, the values reported in our method for LLOD/Q (**Table 3.2**), are up to 100,000 fold lower for small compounds (DP 1-3) and between 30-8,000 fold lower for larger compounds (DP 4-9) compared to those reported in NP HPLC-FLD methods [9,11]. In comparison to HILIC-HPLC quantification of similar procyanidins, our method brought about LOQ values between 30-7,000 fold lower for smaller compounds (DP 1-5) and 4-141 fold lower for larger compounds (DP6-9) [8]. Without post-column ionization, previously reported LLOD/Q values from UPLC-MS/MS are more comparable than those of HPLC-FLD [15]. Yet, the use of post-column ionization with UPLC-MS/MS in the current method brings a 10 fold decrease in LLOD/Q values, though higher DP procyanidins were not assessed [15]. It is important to note that these previously reported methods utilize different detectors and additionally do not utilize post-column ionization as we do in the current method. Advancements have allowed for the integration of HILIC-LC-MS/MS, and thus cutting down retention time, increased specificity through MS, and increased separation through HILIC. Although FLD methods are useful for samples with high concentrations of analytes (i.e. food), more dilute samples (i.e. biological tissues, fluid, etc.) would be better run on our proposed method. This is confirmed through the increasing values in LLOD/Q as the DP of compounds increase (**Table 3.2**), and mirrored by values seen in the literature [9,11,15].

3.3.4. Repeatability and reproducibility. Intraday variation of retention time and response was quantified by analyzing an aliquot of 5 mg/mL CE, injected at 5 μ L, nine times in one day. Peak area and retention time from each injection were used to calculate the coefficient of variation (CV) for each compound. Interday variation of response was quantified by analyzing a fresh aliquot of 5 mg/mL CE, injected at 5 μ L, nine times each day over the span of three consecutive days. Intraday and interday CV remained <2% for retention time across all compounds (DP 1-10), while intraday retention time CV remained <10% for peak area among DP 1-9, with the exception of DP 10 at 10.13% (**Table 3.3**). Interday CV was much more variable for peak area than intraday. CVs increase with increasing DP, specifically in DP 7-10. Stanley et al [16] utilized a RP HPLC-ECD method to quantify cocoa procyanidins at DP 2-7. Not only is our method more efficient than this method but has similar peak area intraday variation and comparable interday variation. The authors present intraday CVs <10% with the exception of one compound at an average of 11.4% variation over the three-day period, a trend that is also seen in our data. The interday CVs for our method

are higher than those presented in Stanley et al [16], but we believe the increased efficiency and sensitivity of the analysis compensates for this deviation. Additionally, Robbins et al [1] analyzed chocolate samples and cocoa procyanidins by DP (DP 1-10), utilizing a NP HPLC-FLD method. Though values are reported as the summation of the monomeric and oligomeric fractions (DP 1-10), it is stated that intraday variation was kept <10% and interday ranged from 5% – 17.86%. These are consistent with the values reported in Stanley et al [16] and continue to fall within the range of the data presented in the current study, with the exception of interday CVs for monomer and octamer (>20%). Finally, Hollands et al [8] reports the analysis of apple procyanidins through a HILIC-HPLC method. Although intraday CVs correspond with our reported values, interday CVs for our method have a higher variability than those reported in apples. Again, we believe the increased efficiency and sensitivity of our proposed analysis compensates for this deviation in method precision. Overall, we believe that the repeatability and reproducibility of cocoa procyanidins utilizing our method is consistent with the methods currently available and brings about additional advantages to sample analysis, such as reduction in overall retention time and higher sample throughput.

Table 3.3 Coefficient of variation (CV) of retention time (RT) and peak areas for intraday and interday replication of compounds. Nine injections of a 5 mg/mL CE at 5 μ L were run each day for three consecutive days. A fresh aliquot of CE was used each day.

Compound	Intraday %CV (n=9)		Interday %CV (n=27)	
	RT	Area	RT	Area
Monomer	1.44	5.20	1.77	21.68
Epigallocatechin	1.50	6.34	1.79	7.55
Dimer	1.66	3.70	1.84	8.17
Trimer	0.87	6.04	1.88	12.76
Tetramer	0.87	4.26	0.95	9.24
Pentamer	1.03	3.59	1.11	5.86
Hexamer	1.01	3.54	1.08	8.99
Heptamer	1.03	7.29	1.09	14.42
Octamer	1.03	4.87	1.1	33.47
Nonamer	0.99	7.70	1.08	15.79
Decamer	0.74	10.13	1.15	16.13

3.3.5. MRM chromatogram. MRM chromatograms representing the final method are shown in **Figure 3.7**. The total run time of 9 min is significantly reduced from previously established methods, typically ranging from 70-90 min in total, or 16-20 samples per day [1,8,9,12]. Machonis et al [10] initially reduced total run time from a 76 min NP HPLC-FLD method to a 15 min method, but the quantification capability of the method remained the same. On a per day sample throughput basis, our 9 min method can process up to 160 runs per day, a 40% improvement from 15 min and approximately 800% improvement from the original HPLC-FLD method. At 9 min, the total run time is no longer a limiting factor and sample throughput significantly increases. The significant reduction in run time compared to previous published HILIC and NP procyanidin methods was achieved by taking advantage of UPLC columns and instrumentation, whereas previous methods employed HPLC.

It is important to note the peak intensities of **Figure 3.7**, specifically those of DP 6 and DP 9. Due to very minor differences in their MRM transition parent and daughter masses (**Table 3.1**), these compounds provide signal on both MRM channels compounds overlap with one another when analyzed together (such as in CE or mixed standards). By analyzing isolated authentic standards, it is apparent that the nonamer is the second peak, corresponding to overall elution by increasing DP as expected. The multiple peaks could be eliminated by further specifying the retention time window for each compound, but for our purposes, displaying the entire chromatogram was critical for demonstrating the method's ability to both resolve and selectively identify high molecular weight compounds. Furthermore, more distinct daughter ions could be employed for DP 6 and DP 9 MRMs, but the selected MRMs gave the best fragmentation intensities for each authentic standard and were selected in order to maximize LLOD/LLOQ for each compound.

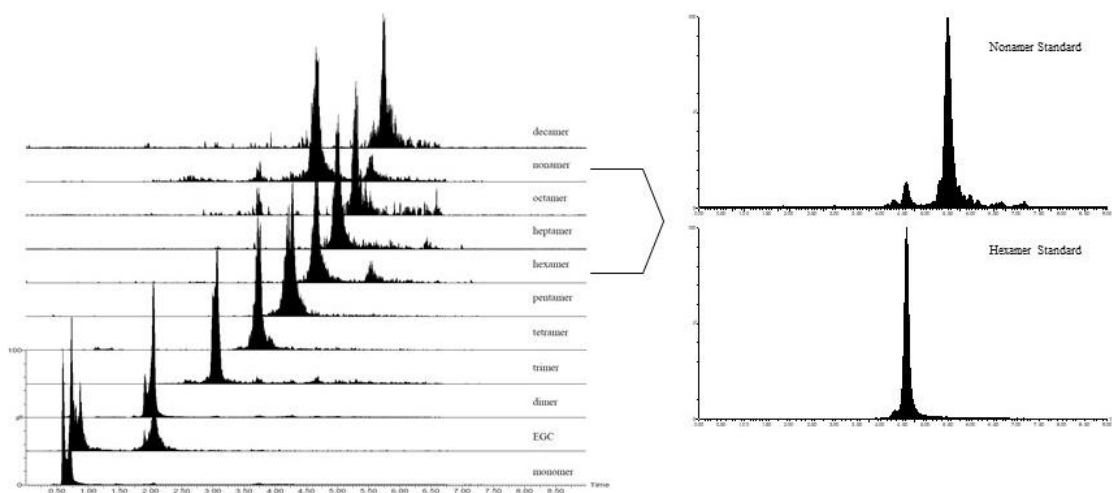


Figure 3.7. LC-MS/MS overlay chromatogram of non-smoothed peaks of each compound analyzed from cocoa extract (left), as well as hexamer and nonamer chromatograms, obtained from analysis of the respective authentic standards separately.

3.4 CONCLUSIONS

Growing interest in cocoa and the relationship between cocoa polyphenols and health has created a gap in the quantification of larger cocoa analytes. These large molecular weight compounds with varying DP are difficult to measure and thus, until recently, have been largely unexplored. Currently the only available methods to quantify these large DP procyanidins require large time commitments, large volumes of solvents, or are not compatible with MS, therefore being unable to identify any unknowns that may present themselves during analysis. Through the use of a UPLC DIOL (HILIC) column we significantly reduced analysis time, improved the compatibility with MS and integrated a post-column ESI adjuvant infusion that enhances ionization along with MS compatibility. To our knowledge, HILIC-UPLC has not been reported with these compounds and this method will be the first of its kind. The method described in this study offers a more sensitive, specific and rapid alternative to current methods for cocoa procyanidin analysis. Utilization of this method has the potential to enable advancements in the field of cocoa polyphenols and health that were not possible due to previous analytical limitations.

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CHAPTER 4. Development and Characterization of a Pilot-Scale Model Cocoa Fermentation System Suitable for Studying the Impact of Fermentation on Putative Bioactive Compounds and Bioactivity of Cocoa

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ABSTRACT

Cocoa is a concentrated source of dietary flavanols—putative bioactive compounds associated with health benefits. It is known that fermentation and roasting reduce levels of native flavonoids in cocoa, and it is generally thought that this loss translates to reduced bioactivity. However, the mechanisms of these losses are poorly understood, and little data exist to support this paradigm that flavonoid loss results in reduced health benefits. To further facilitate large-scale studies of the impact of fermentation on cocoa flavanols, a controlled laboratory fermentation model system was increased in scale to a large (pilot) scale system. Raw cocoa beans (15 kg) were fermented in 16 L of a simulated pulp media in duplicate for 168 h. The temperature of the fermentation was increased from 25–55 °C at a rate of 5 °C/24 h. As expected, total polyphenols and flavanol levels decreased as fermentation progressed (a loss of 18.3% total polyphenols and 14.4% loss of total flavanols during fermentation) but some increases were observed in the final timepoints (120–168 h). Fermentation substrates, metabolites and putative cocoa bioactive compounds were monitored and found to follow typical trends for on-farm cocoa heap fermentations. For example, sucrose levels in pulp declined from >40 mg/mL to undetectable at 96 h. This model system provides a controlled environment for further investigation into the potential for optimizing fermentation parameters to enhance the flavanol composition and the potential health benefits of the resultant cocoa beans.

4.1 INTRODUCTION

Recently, cocoa (*Theobroma cacao*) and its putative bioactive compounds (particularly flavonoids) have been associated with various health benefits, including positive effects on cardiovascular, metabolic and endocrine diseases [1]. There is interest among health researchers, scientists, cocoa suppliers and manufacturers alike in tailoring the processing of cocoa to produce products with maximum health benefits. Three main groups of flavonoids exist within cocoa beans: proanthocyanidins (oligomeric and polymeric flavanols) constitute approximately 58% of the total phenolic content, followed by catechins (monomeric flavanols, ~37%) and anthocyanins (~4%) [2]. It is known that oxidation, condensation and other reactions that take place during cocoa fermentation and roasting reduce levels of native flavonoids, warranting investigation into how these reactions ultimately impact cocoa's health benefits [3–8]. The widely-accepted assumption is that preservation of native flavonoids is critical for retaining bioactivity [9]. However, reactions (oxidation, epimerization, condensation, etc.) during processing may generate compounds with novel activities, potentially preserving or even enhancing health benefits [2,10–13] despite flavonoid loss. Recent findings by Ryan et al. [11] contradict the widely-accepted assumption that loss of native cocoa flavonoids corresponds with reduced activity in some cases. In their study, lower concentrations of flavonoids and total polyphenols in fermented cocoa products were not found to be associated with reduced bioactivity in *in vitro* digestive enzyme inhibition assays. These findings indicate the potential for optimization of processing factors such as fermentation and roasting to maximize the health benefits of cocoa.

Commercial cocoa fermentation is conducted on or in close proximity to the farm of origin in large heaps on the ground or in wooden boxes covered with banana leaves. Tremendous variability exists among on-farm heap fermentations, as differences in environmental microbiota, climate, substrate and fermentation methods all play key roles in microbial ecology and activity. These conditions are poorly documented and beans with differing fermentation histories are commingled into large batches, making post hoc evaluation of the impact of fermentation on bioactivity essentially impossible [8,12,14]. Furthermore, sourcing fermented beans for scientific research is difficult, and complex supply chains have left researchers with uncertainty on cultivar, processing parameters and heap consistency. Sourcing intact cocoa pods is also logistically challenging. With growing interest in the potential for optimization of processing to influence composition and

subsequent bioactivity of cocoa, a controlled model pilot-scale fermentation system is needed. Employing dried, unfermented beans and simulated pulp media eliminates the needs for fresh unopened pods, a major limitation for cocoa fermentation research in regions distant from cultivation. Such a system would provide the ability to control all aspects of fermentation using the exact same starting beans, eliminating confounding variables when sourcing is not under full control of the investigators.

Some preliminary work has been done to explore controlling cocoa fermentation for research purposes (both for characterizing fermentation processes as well as modifying outcomes). Several laboratory bench-scale model fermentations have been conducted in a variety of vessels, including plastic [4,15] and stainless-steel [16], to examine the microbial influence and overall impact of starter cultures on cocoa fermentation. These model fermentations generally use pulp and beans from freshly harvested pods—which is not practical for frequent large-scale use in cocoa fermentation research conducted in non-tropical regions—and use inoculated and ambient pulp mediums [6,17–21]. Our group recently developed a large laboratory bench-scale fermentation using simulated pulp media and dried unfermented cocoa beans as starting material [22]. To our knowledge, ours was the first model of this scale. Along with other laboratory bench-scale model fermentation systems, this model can be used to evaluate the impact of controlled fermentation on putative bioactive compounds in cocoa. Fermentation can cause anywhere from 0–70% loss of total polyphenols, and following fermentation the beans are dried and roasted, causing an additional 15–40% loss [2,3,23–31]. Nonetheless, recent findings have indicated that lower concentrations of specific cocoa flavonoids and total polyphenols in a given product are not always associated with decreased bioactivity [11].

Additional studies employing a combination of analytical, *in vitro* and *in vivo* approaches are needed to advance the understanding of how specific cocoa flavonoid losses during cocoa processing affect the bioactivities of cocoa. Studies are then needed to optimize processing, including fermentation, to maximize the desirable health benefits of cocoa. However, to employ techniques that go beyond analytical characterization of the fermented product, such as *in vivo* bioactivity studies, larger amounts of experimentally fermented cocoa would be required than can be reasonably produced using existing laboratory bench-scale model systems (pilot scale: tens of kgs of fermented beans or more, instead of bench scale: hundreds of grams). Hence, our objective was to develop and characterize a pilot-scale model cocoa fermentation system suitable for

studying the impact of fermentation on putative bioactive compounds. Dried, unfermented beans and a simulated pulp media and ambient microorganisms were used due to the limitations associated with sourcing and transporting fresh whole cocoa pods. Specifically, our hypothesis was that broad microbial and chemical changes similar to those generally observed in heap fermentations could be replicated in non-tropical regions by using a pilot-scale model system designed to simulate the conditions occurring in the middle of a well-turned cocoa heap, and that this system could be used to generate sufficient amounts of fermented cocoa beans for further research on the effect processing has on the potential health benefits of cocoa.

4.2 MATERIALS AND METHODS

4.2.1. Chemicals and standards. Citric acid, yeast extract, malt extract, calcium lactate pentahydrate, tween 80, sodium hydroxide, magnesium sulfate heptahydrate, manganese sulfate monohydrate, sucrose, glucose, fructose, peptone, calcium carbonate and agar were obtained from Thermo Fisher Scientific (Waltham, MA, USA). Cycloheximide was obtained from MP Biomedicals, LLC (Solon, OH, USA) and oxytetracycline dihydrate was obtained from Acros Organics (Springfield Township, NJ, USA). Lactic acid, Folin–Ciocalteu reagent, 4-dimethylaminocinnamaldehyde (DMAC), (\pm)-catechin, (–)-epicatechin and procyanidin B2 (PCB2) were obtained from Sigma-Aldrich (St. Louis, MO, USA). Procyanidin C1 (PCC1) and cinnamtannin A2 (CinA2) were obtained from Planta Analytica (New Milford, CT, USA). Solvents were ACS grade or higher.

4.2.2. Pilot-scale fermentation model. Raw unfermented Criollo cocoa beans (18 kg) (Natural Zing LLC, Mount Airy, MD, USA), sourced from Ecuador, were rehydrated in $66.4 \times 44.3 \times 34.3$ cm plastic fermentation boxes (Polypropylene, Sterilite, Townsend, MA, USA) by submersion in approximately 20 L of distilled, deionized (DI) water for 24 h. The final moisture content of the beans after rehydration was 39.7% (IR-120 Moisture Analyzer, Denver Instrument, Bohemia, NY, USA), close to the lower end of the typical moisture range (40–60%) for fresh beans [32,33]. Rehydrated beans were then drained and 15 kg were mixed with 16 L of simulated pulp media, prepared as described by Lee et al. [22] with minor modifications. Simulated pulp media were obtained by mixing 3 separate solutions (solutions A, B and C). Solution A consisted of citric acid

(10 g/L), yeast extract (5 g/L), peptone (5 g/L), calcium lactate pentahydrate (1 g/L) and tween 80 (1 mL/L); the pH was adjusted to 3.6 using 1 N NaOH and then volume corrected to a total of 9.6 L before autoclaving (121 °C, 15 min) to ensure sterility of the medium. Solution B was a 4.8-L sugar solution, with 1.6 L each of sucrose (83.3 g/L), glucose (133.3 g/L) and fructose (150 g/L). Each sugar solution was autoclaved and cooled prior to fermentation. Solution C was prepared the day of fermentation and consisted of magnesium sulfate heptahydrate (1 g/L) and manganese sulfate monohydrate (0.4 g/L) for a total of 1.6 L. Boxes were loosely covered with their plastic lids and placed inside a pre-heated (25 °C) incubator (Forma 29 cu ft Reach-In Incubator, Model No. 3950, Thermo Fisher Scientific, Waltham, MA, USA). Scale-up from the bench scale was required to produce sufficient material for experiments evaluating the impact of fermentation on cocoa bioactivity using in vivo models. Two factors determined the scale of the pilot system: (1) the amount of fermented product required for animal studies using the fermented material as substrate, and (2) the size of the largest incubator available in our pilot plant. Taking these two factors into account, the batch size was increased by over 10-fold from a 1.2-kg batch of rehydrated beans at the bench scale to a 15-kg batch at the pilot scale. The bench-scale system was under constant agitation in a shaker/incubator, which was not feasible in this pilot system. To maintain maximum dissolved oxygen (DO) possible in a static system, fermentation vessel size and shape were selected to maximize the surface area to volume ratio, and a stirring regime was implemented wherein the contents of the vessel were well-mixed twice daily. Through preliminary work, this mixing regime, in combination with mixing due to gas evolution during fermentation, proved sufficient to maintain a well-mixed condition in the fermentation vessel and to support the microbial succession required for fermentation.

The fermentation was performed in duplicate, simultaneously under identical conditions (2 replicate boxes each employing the conditions described above: 15 kg rehydrated beans and 16 L simulated pulp per box) using ambient microorganisms (i.e., no inoculation) and took place over a period of 168 h (representing the upper end of the spectrum of reported heap fermentation times that occur on-farm). In the future, fermentation time can be varied to obtain different extents of fermentation. The incubator set point was raised 5 °C per 24 h to a final temperature of 55 °C in order to mimic temperature progressions seen in heap fermentation [3,8,34,35]. Beans were manually agitated for 3 min every 12 h to ensure that the simulated pulp media were aerated [14,34–36]. The agitation step was critical to ensure the expected succession of the

microbial communities due to our model's inability to introduce oxygen by draining pulp away, as typically happens during heap fermentations when the pulp is liquefied and the heap is manually turned. Pulp and bean samples were collected every 24 h throughout the fermentation. Pulp dissolved oxygen (DO) and pH values were monitored using benchtop meters (Orion DO Probe 083005MD; Orion Versa Star Pro pH meter; Thermo). After 168 h of fermentation, the beans were drained to remove the remaining pulp media, rinsed with water and spread evenly onto baking sheets. Beans were oven dried (Rational, Landsberg am Lech, Germany; Blodgett, Burlington, VT, USA) at 45–65 °C until the moisture content fell below 8%. These conditions mimicked typical commercial drying protocols [3,34,36,37]. After drying, beans were thoroughly mixed together and stored at 4 °C.

4.2.3. Microbial enumeration. Enumeration methods and selective media were based on the protocols of Nielsen et al. [34] and Ho et al. [38] with minor modifications. Collected pulp media (5 mL) from each time point was diluted with 45 mL sterile 0.1% peptone water, and 1 mL of the resulting mixture was then diluted 10-fold. Aliquots (0.1 mL) were spread inoculated to nutrient agar appropriate for the growth of yeast, lactic acid bacteria (LAB) and acetic acid bacteria (AAB). Yeast cultures were spread on YM media (3 g/L yeast extract, 3 g/L malt extract, 3 g/L peptone, 10 g/L glucose, 20 g/L agar) with 100 mg/L oxytetracycline and incubated at 37 °C. LAB were cultured anaerobically by a BD GasPAK EZ gas generating system (Franklin Lakes, NJ, USA) on de Man–Rogosa–Sharpe (MRS) agar (Sigma) with 400 mg/L cycloheximide at 37 °C, and AAB were cultured on GYC media (50 g/L glucose, 10 g/L yeast extract, 30 g/L calcium carbonate, 20 g/L agar, pH = 5.6) with 400 mg/L cycloheximide by incubating at 25 °C. Bacterial enumeration was performed in duplicate on analytical replicates for each fermentation box and time-point. Colonies were counted and presented as log colony-forming units (CFU)/mL.

4.2.4. Cut test. The cut test is the standard assessment of post-fermentation bean quality and suitability to move forward in processing [3,39]. A reduced sample-size version of the cut test was performed as follows: 6 beans from each 24-h sampling were cut through lengthwise and each half examined for color and quality defects. Although this test is not very applicable to low-anthocyanin beans like Criollo, a purple interior is indicative that the fermentation ended prematurely, while a brown interior is indicative of a successful fermentation [3,40].

4.2.5. Fermentation index. Fermentation index (FI) monitors the color change within the bean cotyledon during fermentation. This color change is due to the decreasing anthocyanin content as beans progress through fermentation. FI was measured based on the method of Romero-Cortes et al. [41] with minor modifications. Five to seven randomly selected cocoa beans from each time point were frozen with liquid nitrogen and ground to a fine powder. A 50-mg sample of the resulting powder was weighed and mixed with 5 mL MeOH:HCl (97:3 v/v). Samples were extracted at 4 °C for 16–18 h on a rotating shaker, centrifuged for 5 min at 3500× g, and the supernatant was collected. Absorbance was measured using a BioTek Synergy 2 plate reader (BioTek, Winooski, VT, USA) on a 96-well plate (Corning Inc., Corning, NY, USA) at 460 and 530 nm. These wavelengths were chosen to express structural properties and distributions through fermentation, as 530 nm is a general λ_{\max} for anthocyanin spectra and 460 nm reflects the glycoside distribution [42]. FI was determined based on the ratio of the absorbance at 460 nm compared to that of 520 nm.

4.2.6. Bean pH. Approximately 5–7 cocoa beans collected at each time point were frozen with liquid nitrogen, the shells were removed and the nibs were ground. Ground nibs (5 g) were collected and mixed with 100 mL hot water (90 °C) and stirred for 30 s. The cocoa water solution (25 mL) was then filtered through Whatman #4 filter paper and collected for pH analysis. It is important to note that this procedure was not for quantifying the actual pH of the cocoa bean itself, but rather to measure the acidity derived when bean acids are diluted into water; it is useful for comparison between the pH of solutions produced by beans at different time points.

4.2.7. High-performance liquid chromatography (HPLC) analysis of fermentation metabolites

4.2.7.1 Pulp media sample preparation. Pulp media samples were diluted 10-fold with distilled water, vortexed and centrifuged for 5 min at 5000× g. Next, 1 mL of supernatant was removed and filtered through a 0.45- μ M polyvinylidene difluoride (PVDF) membrane filter (Thermo Fisher Scientific, Waltham, MA, USA) into vials.

4.2.7.2. Bean sample preparation. Approximately 5–7 cocoa beans were peeled so that the nibs were exposed. Next, 5 g of nib were weighed and added to distilled water at a 10× dilution. The bean water solution was homogenized at high speed for 2 min in a blender (Waring Products,

Calhoun, GA, USA). The blended mixture was then centrifuged for 5 min at 5000× g and 1 mL supernatant was removed and filtered into vials.

4.2.7.3. Analysis. Bean and pulp samples were analyzed by HPLC on an Agilent HPLC 1260 Infinity Series (Agilent Technologies, Santa Clara, CA, USA) using an Aminex HPX-87H column (300 × 7.8 mm, 50 °C) (Bio-Rad Laboratories, Hercules, CA, USA) and a refractive index (RI) detector (35 °C). A 0.005 M H₂SO₄ isocratic mobile phase at a flow rate of 0.6 mL/min was used for analyte separation. The sample injection volume was 5 µL. Triplicate analytical replicates were prepared and analyzed from each fermentation time point. A standard curve was prepared with a range from 0.5 to 5.0 g/L. Sugars (sucrose, glucose, fructose), ethanol, glycerol and organic acids (acetic acid, lactic acid, succinic acid, citric acid) were quantified.

4.2.8. Polyphenol extraction and quantification. Whole cocoa beans (40 g) were frozen with liquid nitrogen and ground into a fine powder. To defat, the powder was mixed with 150 mL hexane and sonicated for 10 min at 22 °C. The mixture was then centrifuged for 5 min at 5000× g, the supernatant was discarded and then the process was repeated. Once defatted, the powder was allowed to dry at room temperature. Once dry, the powder was mixed with 150 mL extraction solution (70:28:2 acetone, water, acetic acid v/v/v), sonicated for 10 min at 22 °C and centrifuged for 5 min at 5000× g. The supernatant was collected, and this procedure was repeated three times for a total volume of 450 mL. All collected supernatant was pooled and placed under vacuum on a rotary evaporator at 40 °C until all acetone had evaporated. The resulting extract was freeze dried for 72 h and the yield was calculated. Total phenolic content (all polyphenols, including flavanols as well as other flavonoids and non-flavonoid phenolics) of both the nib and shell was determined by the Folin–Ciocalteu colorimetric assay and total flavanols (only catechins and proanthocyanidins) measured by the 4-dimethylaminocinnamaldehyde (DMAC) colorimetric assay, as previously described by Dorenkott et al. [10]. These values were expressed in mg gallic-acid equivalents (mg GAE)/g bean and mg PCB₂/g bean, respectively.

4.2.9. Individual polyphenol analysis and reversed phase UPLC-MS. Monomeric catechins and low molecular weight procyanidins were measured by UPLC-MS on an Acquity H-Class UPLC-QDa Mass Detector (Waters Corporation, Milford, MA, USA). Cocoa extract (CE) was diluted with 0.1% formic acid (v/v) in water and 0.1% formic acid in acetonitrile (95:5 v/v), to a

final concentration of 0.1 mg/mL, filtered (13 mm diameter syringe filters, 0.22 μm nylon membrane with propylene housing, Microsolv, Leland, NC, USA) into vials, and held at 10 $^{\circ}\text{C}$. Samples were analyzed on an Acquity HSS T3 column (2.1 \times 100 mm, 1.8 μm particle size) in combination with an Acquity HSS T3 VanGuard pre-column (2.1 \times 5 mm column, 1.7 μm particle size) at 43 $^{\circ}\text{C}$. Binary gradient elution was performed using 0.1% formic acid (v/v) in water (Phase A) and 0.1% formic acid (v/v) in acetonitrile (Phase B). The solvent flow rate was 0.6 mL/min and the linear gradient elution was as follows: 95% A (0–0.5 min), 65% A (6.5 min), 20% A (7.5–8.6 min) and 95% A (8.7–10.5 min). Samples were held at 4 $^{\circ}\text{C}$ and the injection volume was 10 μL . (–)-electrospray ionization (ESI) together with mass spectrometry (MS) was used to analyze the UPLC eluent. The ionization settings were as follows: (–) mode, 0.8 kV capillary voltage, 15 V cone voltage and 600 $^{\circ}\text{C}$ probe temperature. Triplicate analytical replicates were prepared and analyzed from each fermentation time point. Authentic standards of (\pm)-catechin, (–)-epicatechin, PCB2, PCC1 and CinA2 were utilized, and settings for selected ion response (SIR) monitoring of each compound are listed in **Table 4.1**. Data were collected using Empower 3 software (Milford, MA, USA).

Table 4.1. MS settings for individual polyphenol analysis by reverse-phase (RP)-UPLC-MS.

Compound	t_{R}^{a} (min)	$[\text{M} - \text{H}]^{-\text{b}}$ (m/z)
(\pm)-catechin	2.946	288.95
(–)-epicatechin	3.625	289.01
PCB2	3.366	576.84
PCC1	3.904	864.85
CinA2	4.063	1153.19

^aRetention time

^bQDA detector uses singly charged parent ions for selected ion response (SIR) monitoring

4.2.10. HILIC UPLC-MS/MS. Monomeric flavanols and procyanidins were analyzed by hydrophilic interaction liquid chromatography (HILIC) UPLC-MS/MS as previously described [43]. A Waters Acquity H-class UPLC equipped with an Acquity Torus DIOL column (2.1 \times 100 mm, 1.7 μL , 45 $^{\circ}\text{C}$) and Torus DIOL VanGuard Pre-column (2.1 \times 5 mm, 1.7 μL) were used for analysis. Gradient elution was performed with 2% acetic acid in acetonitrile (phase A) and 3%

water and 2% acetic acid in methanol (phase B). Solvent flow rate was 0.8 mL/min and elution was carried out as followed: 100% A (0 min), 55% A (5.7 min), 5% A (6.0 min) and 100% A (6.7–9.0 min). The UPLC eluent was analyzed by (–)- mode ESI coupled to tandem mass spectrometry (MS/MS) on a Waters Acquity triple quadrupole (TQD). Aqueous ammonium formate (0.04 M, 5 μ L/min) was added to the eluent flow stream post-column to enhance ionization. Ionization settings were as follows: (–) mode, capillary and cone voltages: –4.5 kV and 60.0 V, extractor voltage: 1.0 V, source and desolvation temperatures: 150 °C and 500 °C. N₂ was used for the cone and desolvation gas at 50 and 1000 L/h, respectively. For MS/MS, Ar was the collision gas at 0.1 mL/min. Parent and signature daughter ions were subjected to multi-reaction monitoring (MRM) with a mass span of 0.2 Da and 1.0 sec of inter-channel delays and inter-scan times. Calibration curves for standards DP 1-9 (Planta Analytica, New Milford, CT, USA) were prepared and analyzed with dilutions ranging from 6.93×10^{-7} – 0.091 mg/mL. MRM settings for each compound are listed in **Table 4.2**. MassLynx software (version 4.1, Waters) was used to acquire data.

Table 4.2. Tandem MS/MS settings for multi-reaction monitoring (MRM) detection of monomeric-decameric flavanols.

Compound	t_R^a (min)	MW (g mol ⁻¹)	[M–H] ^{-b} (m/z)	Daughter Ion (m/z)
Monomer	0.61	290.27	289.03	245.06
Epigallocatechin	0.74	458.37	305.04	124.98
Dimer	2.03	578.52	577.14	425.10
Trimer	3.05	866.77	865.22	287.07
Tetramer	3.73	1155.02	576.40	125.02
Pentamer	4.26	1443.28	720.41	125.02
Hexamer	4.66	1731.53	864.52	125.02
Heptamer	5.00	2017.81	1008.40	125.17
Octamer	5.28	2308.03	1152.58	125.17
Nonamer	5.53	2596.54	864.12	125.17
Decamer	5.75	2884.54	960.18	125.17

^a Retention time. ^b All MRMs used singly charged parent ions except for pentamer, hexamer, heptamer and octamer, which are double-charged ([M–2H]²⁻), and nonamer and decamer, which are triple-charged ([M–3H]³⁻).

4.2.11. Data analysis and statistics. The fermentation was performed in duplicate, simultaneously under identical conditions. Analyses were performed on samples from each replicate; analytical replicates were averaged together to create a composite value for each fermentation replicate. Data from distinct time points were analyzed by one-way ANOVA to determine overall significance. If significant differences were detected, Tukey's HSD post-hoc test was then used to compare all time point means. Significance was defined as $p < 0.05$. Analyses were performed using GraphPad Prism 7.03 (GraphPad, La Jolla, CA, USA).

4.3 RESULTS

4.3.1. pH, DO, FI, cut test. As shown in **Figure 4.1A**, the mean pH of the simulated pulp media started at approximately 3.6, increased to a maximum value at 72 h and slightly declined to a final mean of 4.6. The solution made from the nib had a mean pH of 5.4, and the pH declined throughout fermentation to a final mean of 4.6. Initial DO levels were high due to the fresh mixing of simulated pulp and beans but decreased rapidly over the first 24 h followed by consistent levels for the remainder of the fermentation. It has been determined that cocoa mass is adequately fermented when FI measurements are ≥ 1 [41] and, as shown in **Figure 4.1B**, FI values began at 0.872 ± 0.065 and values ≥ 1 were initially achieved between 48–72 h. **Figure 4.1C** shows the cut test of beans selected at each time point. There were a variety of colors over the span of the fermentation, from light/dark brown to purple.

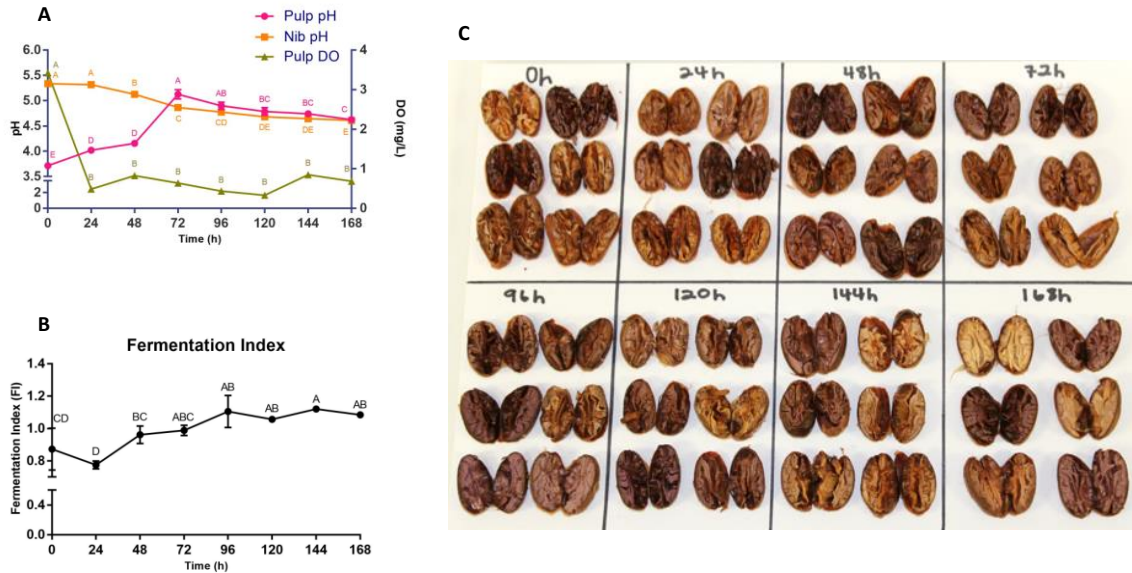


Figure 4.1. (A) pH measurements for both simulated pulp media and bean nib. It is important to note that, for bean nib measurements, these values do not quantify the pH of the cocoa bean itself, but rather of the acidity derived when bean acids are diluted in water. These nib values are useful for comparison between the pH of the solution produced by beans at different time points. Dissolved oxygen (DO) measurements within the simulated pulp media are expressed in mg/L. (B) Fermentation index (FI) expressed as a ratio of absorbance at 460 and 530 nm. (C) Cut test of six randomly selected beans per each timepoint. Beans were selected from both fermentation treatments to form one composite representation. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points for each value was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values.

4.3.2. Microbial enumeration and fermentation products. Microbial population changes are shown in **Figure 4.2**. Yeasts proliferated early (**Figure 4.2A**) with a 6-log increase over the first 48 h followed by a decline over the remainder of fermentation, ending with no measurable colonies. LAB (**Figure 4.2B**) presented a similar but less dramatic trend with approximately a 7-log increase over the first 72 h, followed by a moderate decline. AAB (**Figure 4.2C**) levels fluctuated before peaking at 72–96 h and then exhibiting a similar decline as LAB.

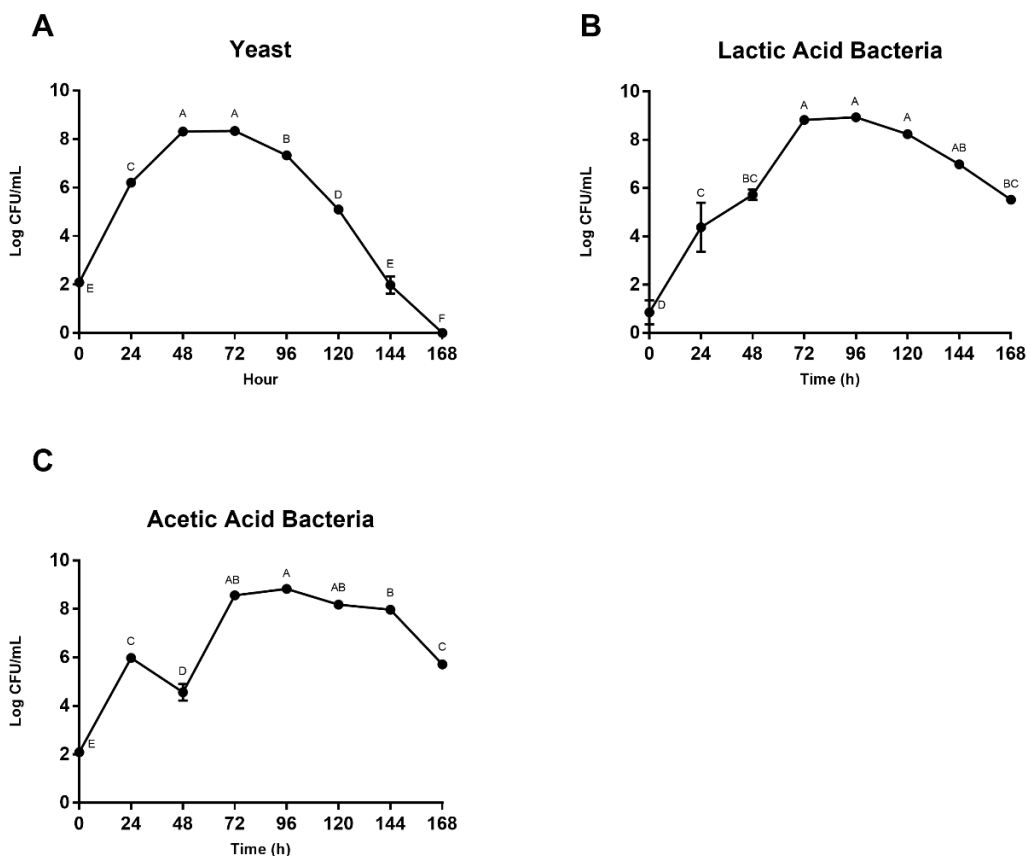


Figure 4.2. Enumeration of (A) yeast, (B) lactic acid bacteria (LAB) and (C) acetic acid bacteria (AAB) in simulated pulp media, expressed in log colony-forming units (CFU)/mL. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values.

Concentration of fermentation substrates and metabolites in simulated pulp media are shown in **Figure 4.3**. During the first 48–72 h of fermentation, sugar and citric acid concentrations dropped significantly and remained close to zero for the remainder of the fermentation. Contrarily, ethanol, glycerol and acetic acid remained relatively constant for the first 24–48 h of fermentation before demonstrating a dramatic increase in simulated pulp media concentrations. Succinic acid concentrations remained constant for the first 48 h followed by a 3-fold increase in simulated pulp media. Lastly, lactic acid was the only metabolite that showed a consistent increase throughout the entire fermentation, increasing almost 6-fold by the end of the 168 h.

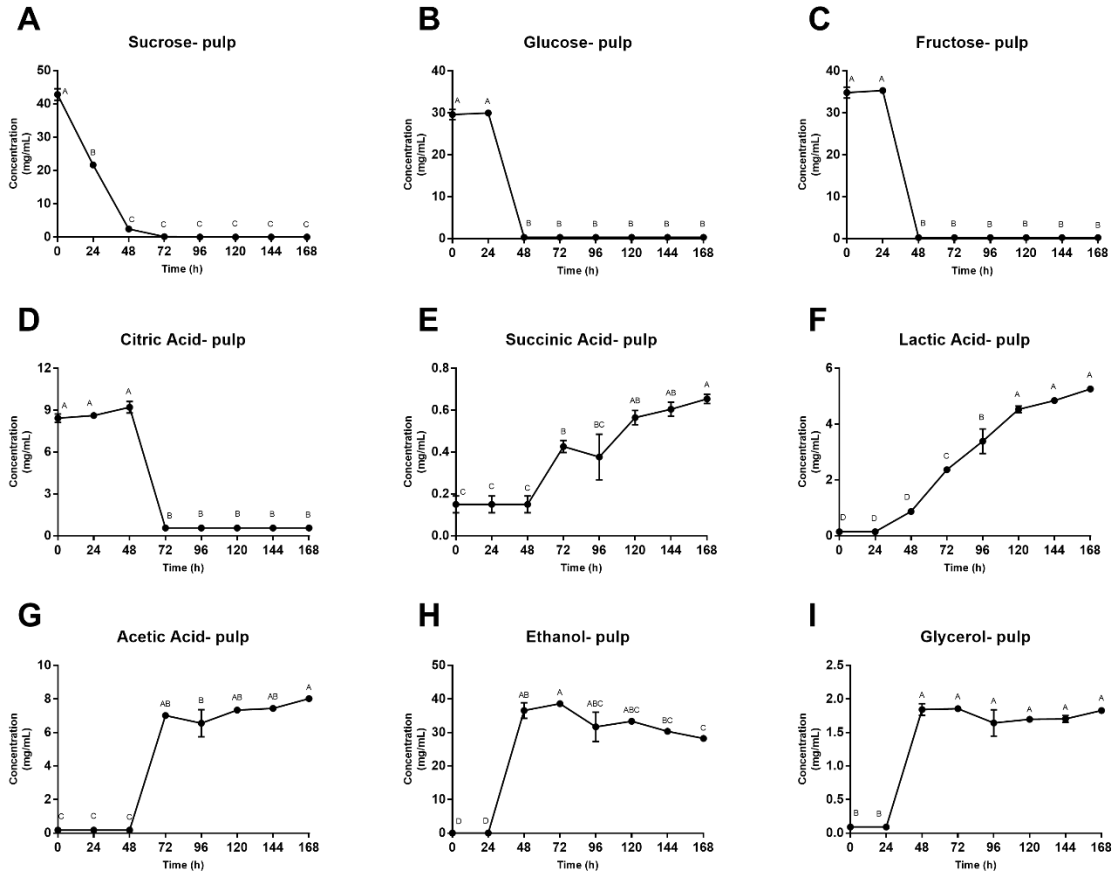


Figure 4.3. Concentration of fermentation substrates and metabolites in simulated pulp media across 168 h. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values.

Concentrations of fermentation substrates and metabolites from the beans are shown in **Figure 4.4**. Fructose, glucose and citric acid concentrations rose significantly over the first 48 h before peaking and then quickly decreasing. Succinic, lactic and acetic acid fluctuated before reaching maximum concentrations at 120 h, followed by decreasing levels for the final 48 h of fermentation. Sucrose is the only compound that showed a quick and sharp decrease in concentration. After a 96-h decline, sucrose concentrations ended at undetectable levels. Bean alcohol trends were like those of the simulated pulp media, with ethanol and glycerol remaining constant for 24 h before demonstrating a sharp increase. Glycerol concentrations fluctuated more than those of ethanol, peaking at 96 h compared to ethanol's 48 h maximum concentration.

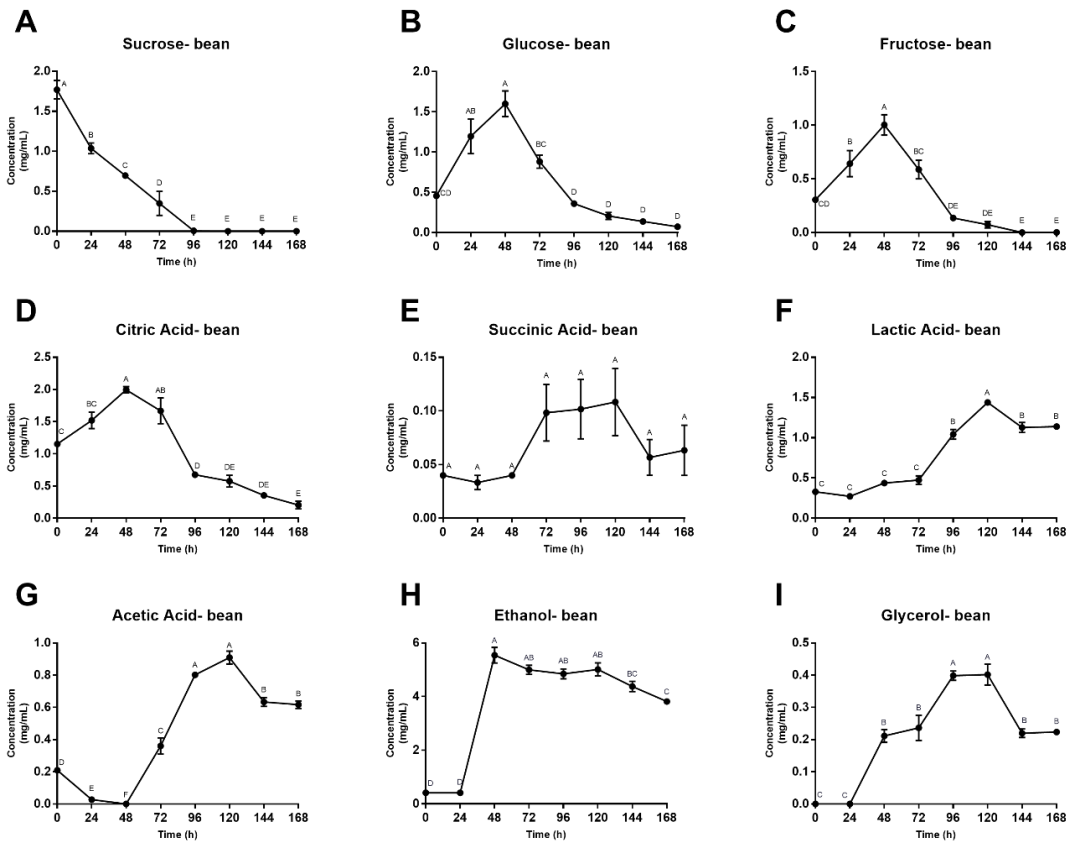


Figure 4.4. Concentration of fermentation substrates and metabolites in cocoa beans across 168 h. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different values.

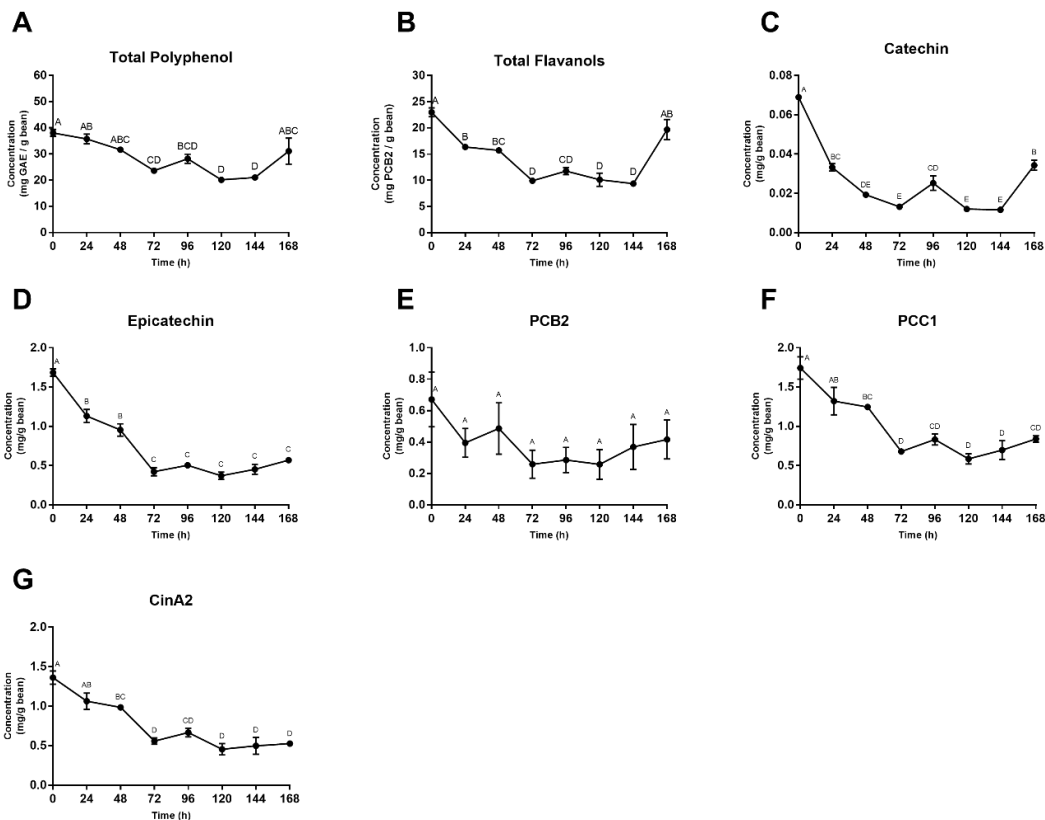


Figure 4.5. (A) Concentration of total polyphenols over the 168-h fermentation, as quantified by the Folin–Ciocalteu colorimetric assay, expressed in mg GAE/g cocoa bean. (B) Concentration of total flavanols over the 168-h fermentation, as quantified by the 4-dimethylaminocinnamaldehyde (DMAC) colorimetric assay, expressed in mg PCB2/g bean. (C–G) Individual polyphenol concentrations (C, EC, PCB2, PCC1, CinA2) over the 168-h fermentation, as quantified by reversed phase UPLC-MS, and expressed as mg/g cocoa bean. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey’s HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values.

4.3.3. Total polyphenol and flavanol content. Mean total polyphenol levels were initially 38.0 mg gallic acid equivalents (GAE)/g bean and after 168 h finalized at 31.1 mg GAE/g bean, for a total loss of 18.3%. Yet after 120 h, there was a more significant net polyphenol loss, quantified at 47.1% loss from initial levels. This difference can be attributed to the 35.3% apparent polyphenol gain in the final 48 h, 120–168 h (Figure 4.5A). When looking at total flavanol concentrations in Figure 4.5B, a similar trend can be seen in the last day of fermentation. A 14.4% loss in flavanol concentration is accounted for when looking at initial and final hours (0 and 168 h), whereas a 59.3% loss is seen between 0 and 144 h, with this difference being attributed to the apparent 52.5% gain in total flavanol concentration between the final 24 h (Figure 4.5B).

4.3.4. Individual polyphenol analysis. Concentrations of (\pm)-catechin, (-)-epicatechin, PCB2, PCC1 and CinA2 are shown in **Figure 4.5C–G**. (-)-Epicatechin levels decreased the most, with 66.2% of initial concentrations lost between 0 h and 168 h. CinA2 concentrations fell by 61.3%, followed by PCC1 at 51.8%, catechin at 51.3% and PCB2 at 38.0%. Each individual compound mirrored the trend seen in total polyphenol concentrations in the final 48 h (120–168 h). The most significant loss in all compounds was within the first 48–72 h, followed by fluctuating values until the final 48 h (120–168 h), where all compounds then increased.

Concentrations of individual procyanidins analyzed by degree of polymerization (DP) from monomer through decamer mirrored trends seen previously in that significant losses occurred in the first 72 h, followed by an increase in concentrations of all compounds from 120–168 h. Dimer concentration (**Figure 4.6B**) increased over 2-fold from 120–168 h, returning to initial (0 h) concentration levels by the end of fermentation. As expected, monomers (**Figure 4.6A**) had the greatest loss with an 80% decline in native compounds from 0–120 h. All other compounds had losses between 42–63% in the first 120 h of fermentation, followed by increases in the final 48 h (120–168 h).

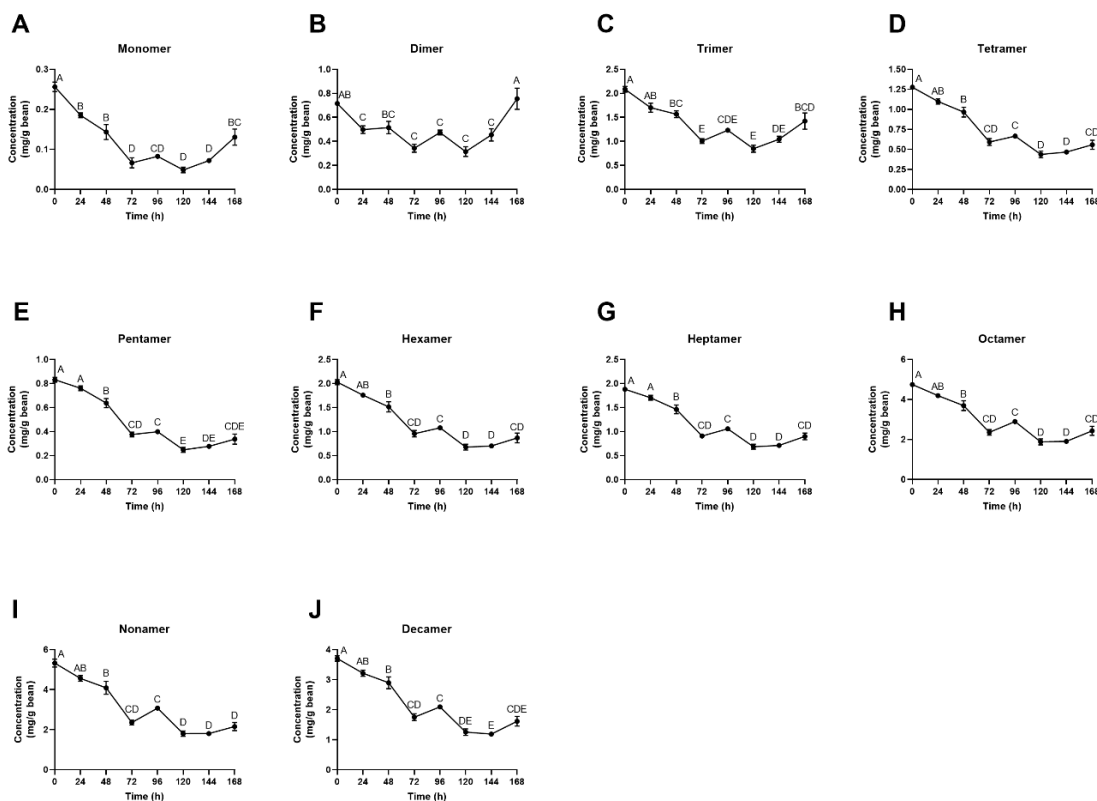


Figure 4.6. Individual polyphenol concentrations by mean degree of polymerization (mDP) over the 168-h fermentation as quantified by HILIC UPLC-MS/MS and expressed as mg/g cocoa bean. Values are presented as the mean \pm SEM of fermentation replicates. Significance between time points was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values.

4.4 DISCUSSION

The primary goal of this work was to develop and characterize a pilot-scale model cocoa fermentation system suitable for conducting cocoa fermentation research in the absence of fresh cocoa pods, and capable of producing sufficient quantities (tens of kg) of material for further evaluating the impact of cocoa fermentation on putative bioactive compounds and cocoa bioactivity in *in vitro* and *in vivo* experiments. Our model was not designed to physically mimic a scaled-down heap fermentation, but rather to serve as a model system suitable for the study of heap fermentation using (1) dried, unfermented beans and a simulated liquid pulp media as the starting material, (2) ambient microbiota and (3) regular stirring. The goal was to achieve similar chemical changes as observed in on-farm heap fermentations by putting beans in similar conditions to those found at the center of a well-turned heap. In cocoa fermentations conducted on farms, highly variable conditions exist between regions, countries, farms and even between specific heaps, as

temperature and environment play important roles in fermentation [44]. Using separate boxes under identical conditions provided some insight into the amount of variability to expect in this controlled model. Variability within our model was generally very minor and the metabolic profiles were similar to those seen in heap fermentations. Although our model was consistent, the replicate fermentations were conducted simultaneously in the same incubator. Further work is needed to determine the consistency between batches conducted at different times and in different incubators.

At an initial pH of 3.6, the pulp media created a favorable environment for yeasts to proliferate within the first 48 h [12]. Citric acid was then metabolized by LAB and ethanol production continued, increasing the pH and encouraging the growth of LAB. As lactic and acetic acids dominated the system, pH declined (72–168 h) and bean cotyledon was penetrated to initiate bean death, where endogenous biochemical reactions began the formation of the characteristic chocolate flavor, and pH concluded at approximately 4.6 [45]. In heap fermentations, turning patterns are a primary factor in pH variability. On average, heaps that are turned at least twice progress from pH 3.9–4.6 [8,12,14,34]. Our system was stirred every 12 h to mimic conditions in the center of a well-mixed heap, and our observed pH values align with previously reported values. DO values stabilized after 24 h as the lag phase of yeast metabolism ended. Likely due to a lack of monitoring equipment, there are no published data regarding DO progression in heap fermentations. Moving forward, aeration in the model could be increased to elevate DO. It would be worthwhile to monitor DO in various on-farm fermentation systems to determine accurate values for modeling a given system. Additionally, comparison of our measured FI values with reported values provide evidence that sufficient fermentation can be achieved under these pilot-scale conditions. Anthocyanins and catechin monomers polymerize during fermentation, rapidly disappearing from the bean cotyledon [2,24]. This can also be observed in the cut test. In traditional cut tests of ≥ 300 beans, bean color should uniformly progress from purple to brown throughout the fermentation, showing the effect of polyphenol oxidase and other reactions that reduce the appearance of color within the bean. Criollo beans have low anthocyanin levels and as such the cut test and FI for these beans does not follow the pattern typically seen with other cultivars such as Trinitario and Forastero [46–50]. However, it is important to include these tests in reference to typical cocoa fermentation quality checks, and future work is needed using this model with other cocoa cultivars.

Yeasts proliferate during the early stages of fermentation, consuming available sugars and converting them to ethanol and carbon dioxide. Sucrose concentrations exhibited a decline in both pulp media and bean, while pulp glucose and fructose concentrations had a 24-h lag period, and bean concentrations of these sugars increased in the beginning hours, likely due to diffusion from the pulp media into the bean. The early decrease in sucrose is likely due to yeast-derived invertase that hydrolyze sucrose into glucose and fructose during the lag period, before the yeasts begin to consume these sugars. Although sugar concentrations vary between replicates, these trends are similar to those seen in traditional heaps [8,16,51]. Ultimately, yeasts consumed all available substrates for growth, inducing inhibition of their own activity, and LAB began to dominate the system with citric acid degradation, subsequently increasing pH and creating an optimal environment for bacterial growth [52]. AAB then thrived in this newly aerobic, less-acidic environment (48–72 h), facilitating the oxidation of ethanol to acetic acid and, further, to carbon dioxide and water, ultimately resulting in bean death. Although the reactions that occur within the bean itself are not well understood, reported consumption and production of metabolites during industrial cocoa fermentation follow a similar pattern to that of the simulated pulp media in the model system described in this study.

During the first days of fermentation, polyphenols are oxidized via polyphenol oxidase and condense into high molecular weight tannins and other complex compounds. These reactions occur as polyphenols, such as (–)-epicatechin, diffuse out of the bean cotyledon and into the media, subsequently aligning with bean death [9,24]. Criollo beans have been reported to have approximately two-thirds of the total polyphenol content of Forastero and Trinitario varieties, yet other studies have indicated that Criollo beans have high levels of procyanidins with no significant difference in total polyphenol content between the three main cultivars [40,53,54]. Total phenolic content of Criollo beans is often not thoroughly analyzed, but values of 40–50 mg GAE/g have been reported, aligning with the data presented in this study (**Figure 4.5A**) [53]. The most dramatic decrease in phenolic concentrations took place in the first 72 h (**Figures 4.5 and 4.6**), confirming this model system's activity and succession of bean death, as well as representing the quick decline of polyphenol compounds seen in Criollo bean fermentation [40]. Additionally, the observed loss of polyphenols from raw to fermented is comparable to that of heap fermentations. The average loss of total polyphenol content previously reported is 40–60%, which is within the range of loss for this study [3,9,17,23,46,55,56]. Payne et al. [55] found that heap fermentation resulted in an

86–94% decrease in (–)-epicatechin and an 83–89% decrease in (±)-catechin levels. Similarly, Kim and Keeney [23] demonstrated that (–)-epicatechin levels declined 77–91% during fermentation, with bean origin and variety playing a key role in rate and total decline. Furthermore, when examining polyphenols based on degree of polymerization, Kealey et al. [30] reported losses of 61% (monomer), 54% (dimer), 60% (trimer) and 68% (tetramer). Although these values align with our data, that fermentation concluded at 120 h, and it cannot be determined if the trend seen in the final 48 h of our model system would correspond with observations from that study. The quantification of high molecular weight procyanidins (trimer-decamer) over the course of fermentation (**Figure 4.6**) is the first of these values to be reported in the literature, as standards are often not commercially available. This data shows the elevated presence of very large molecular weight compounds (**Figure 4.6 I–K**) throughout fermentation and highlights the research gap on these compounds in cocoa, with most of the literature focusing on monomeric compound quantification, specifically (–)-epicatechin and (±)-catechin.

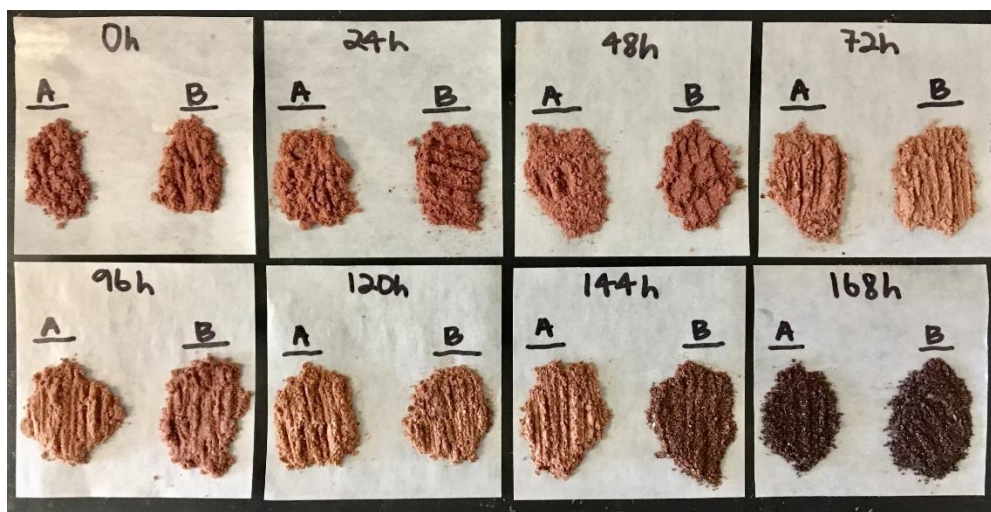


Figure 4.7. Polyphenol-rich cocoa extracts (CE) prepared at each point throughout the 168-h fermentation. See Section 2.8 for methodology. It is important to note the change in color and texture towards the final hours of fermentation.

Elevated temperatures of the fermentation system may also be responsible for phenolic degradation, with further polymerization of these smaller monomers and procyanidins into larger more complex compounds [55]. These could form complex compounds with higher responses in our assays, but further investigation into the relationship between fermentation temperature and polyphenol loss is warranted as this theory has not been adequately investigated. **Figure 4.7** shows the visual appearance of the polyphenol-rich cocoa extract used for the quantification of

total/individual polyphenols and total flavanols. At 144 h, a change in the extract can be noted in the color and texture. Because the four different analyses (Folin-Ciocalteu, DMAC, UPLC-MS, UPLC-MS/MS) were performed at different times and produced similar results in terms of time-course trends, it is unlikely that the phenolic increase in the final hours is due to human error during analysis. An error in extract preparation is possible but also unlikely, as the appearance of the cocoa extracts change in multiple instances. Further investigation into a wider range of compounds is warranted to determine the cause of this phenolic increase, as it is inconsistent with any previously reported data and there is a lack of thorough data quantifying these individual compounds across varying degrees of fermentation. The mechanism by which these late-stage changes occurred warrants further study. It is important to note that the specific beans used for the curt test (**Figure 4.1C**) were not the same actual beans used for extraction and other assays, and furthermore that extraction isolates and concentrates components that cannot always be visibly observed in beans.

Although polyphenol loss may have negative implications on the overall health benefits of cocoa, this relationship is still poorly understood. It is important to understand that these losses correspond with the development of positive flavor profiles, and a balance must be found between optimization of polyphenol content for health outcomes and for acceptable flavor [3]. Furthermore, the chemistry of these losses, and the structures and bioactivity of the subsequent products, remain to be elucidated.

Interest in controlled fermentation systems has emerged as a strategy to experimentally manipulate cocoa fermentation on various scales in regions where cocoa does not grow. Controlled fermentations using a model system offer reliable, reproducible methods to understand the microbial and biochemical reactions that occur. In heap fermentations, beans and pulp are removed directly from the pod, heaped on the ground or in wooden boxes and covered with banana leaves. Traditional systems, while effective for cocoa production, offer little ability to implement experimental conditions or controls to enable research on the impact of environment, materials and fermentation management practices on outcomes of fermentation. In a controlled setting, factors such as temperature, bulk density, relative humidity, oxygenation, microbial inoculation and other influences can be regulated and manipulated, furthering scientific understanding of the complex interactions occurring during cocoa fermentation. Additionally, previously published fermentation-like model systems range in capacity from 25 beans to 1.2 kg rehydrated bean weight

[19,22,57]. With the capacity of our model to ferment approximately 30 kg of rehydrated cocoa beans simultaneously, this novel pilot-scale model can produce relatively large quantities of fermented beans in a controlled setting. Production of a larger quantity of material under controlled experimental fermentation conditions will enable further study of the bioactivity of the resulting cocoa, using animal feeding experiments, for example. Furthermore, this pilot-scale model fermentation can be conducted using food-grade inputs, making it applicable to the production of substrates for human clinical trials as well, where large amounts of material are required.

It is critical to note that the system developed in this study is intended to serve as a model designed to replicate the chemical outcomes of cocoa fermentation, but not to physically duplicate the heap fermentation process on a smaller scale. As such, our model aims to produce conditions mimicking the center of a well-turned heap in simulated pulp media. Our data indicate that this system is a reliable and controlled pilot-scale fermentation model, which replicates the outcomes of heap fermentation with acceptable fidelity. It is important to note that cocoa fermentation varies significantly. Our model system was not tested in the present study to mimic all possible combinations of turning, aeration, temperature gradients or lengths of fermentation. However, the model we describe here can be used to study such variations in a controlled environment. We are currently expanding upon this study by introducing variables such as cool vs. hot fermentations to generate cocoas with distinct chemical profiles for evaluating the impact of composition on health benefits. Although our results show promise moving forward, this model is not without limitations. The beans used were commercially available and of largely unknown origin. Although the beans were food-grade and declared to be dried and unfermented, drying temperature and duration, as well as the conditions between harvest and drying, are unknown. Moving forward, we will address this limitation by obtaining dried unfermented beans from suppliers with more knowledge of the supply chain. The impact of using dried, unfermented beans on the fidelity of our model, compared with fermentation using fresh beans, will need to be evaluated by using a single batch of beans and conducting fermentations using fresh beans, as well as by drying and then employing our model. For example, early flavanol degradation by endogenous polyphenol oxidase may be impacted. Also, aeration could be further optimized to mimic conditions at the center of a well-mixed heap or box fermentation, or at least to gain an understanding of the effects of aeration on the chemical changes observed. Acquiring fresh cocoa pods for use in laboratories distant from production regions without spoilage has proven to be expensive and ineffective.

To summarize the novelty of the present work, several key advances have been made. First, by using dried, unfermented beans and a simulated pulp medium instead of relying on fresh cocoa pods, this model system will allow cocoa fermentation research to progress anywhere in the world regardless of location, climate or season. This greatly expands the ability of researchers distant from cocoa cultivation to control and manipulate cocoa fermentation for research purposes. Second, the increased scale of this model system (from previous controlled lab fermentations using tens or hundreds of grams of beans to the present model employing 2×15 kg beans) will facilitate production of large amounts of custom cocoas designed specifically for animal or human clinical studies. Both of these advances will result in expanded scope of cocoa fermentation research. Thus, the development and characterization of this pilot-scale model system represents a promising new and controlled method for expanding upon cocoa fermentation research.

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CHAPTER 5. Modulation of α -glucosidase activity results from changes in flavanol mean degree of polymerization imparted through controlled fermentation and roasting

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ABSTRACT

Scope

We investigated whether cocoa processing parameters (fermentation and roasting time/temperature) influenced the α -glucosidase inhibitory activity of cocoa powders.

Methods and results

Raw unfermented cocoa beans were fermented using a pilot scale fermentation system, roasted, and then winnowed, ground, and pressed to produce cocoa powders with different combinations of fermentation [unfermented, cool (max 46°C) or hot fermentation (max 60°C)] and roasting [not roasted, cool (120°C) or hot roasted (170°C)]. Powders were chemically characterized and assessed for α -glucosidase inhibitory activity. Low and high molecular weight fractions (8-10 kDa cutoff) were produced from cocoa powder extracts of each treatment. Cocoa processing (fermentation/roasting) contributed to significant ($p < 0.05$) losses of native flavanols. Hot roasting had the greatest impact on flavanol degradation, yet resulted in flavanols with the highest mean degree of polymerization (mDP). All powder treatments dose-dependently inhibited α -glucosidase enzyme activity, with cool fermented/cool roasted powder exhibiting the best inhibition of α -glucosidase at the lowest IC_{50} of 62.2 $\mu\text{g/mL}$. A strong correlation ($R = -0.882$) was observed between increasing flavanol mDP and decreasing IC_{50} values, indicating that flavanol polymerization is a marker of enhanced α -glucosidase inhibition.

Conclusions

Our data demonstrate that cocoa powders are potent inhibitors of α -glucosidase activity. Significant reduction in total polyphenol and flavanol concentrations induced by processing does not necessarily dictate reduced enzyme activity, but rather these steps can actually enhance cocoa bioactivity.

5.1 INTRODUCTION

Cocoa beans (*Theobroma cacao*) are highly concentrated dietary sources of flavanol-compounds thought to be responsible for many bioactive properties of cocoa, such as antitumorigenic, antimutagenic, anti-inflammatory, and antioxidant capacity [1–5]. Native flavanols in cocoa beans are approximately 58% procyanidins, or flavanol oligomers and polymers (monomeric residues linked via 4→β6 or 4→β8 bonds [6]. The major monomeric flavanols in cocoa are (–)-epicatechin and (+)-catechin [roasting epimerizes (+)-catechin to (–)-catechin]. Additionally, cocoa beans contain other bioactives such as lipids, fiber, lignins, melanoidins (after roasting), methylxanthines, and other complex compounds that have not been extensively characterized in cocoa. Depending on variety, beans contain approximately 55% fat, 16% fiber, 10% protein, and 3% ash [7]. Because of the complex reactions that occur during cocoa processing, the health benefits associated with dietary cocoa are likely due to multiple bioactives and their interactions, not one compound or class of compounds [8].

After harvesting, cocoa beans undergo a series of processing steps (fermentation, drying, roasting, winnowing and various other process that may include pressing or alkalization) to produce a final product such as cocoa powder or chocolate, and these processing steps will largely determine chemical composition of the product. Fermentation is the first step in cocoa processing and traditionally occurs in wooden boxes or heaps on the ground, covered with banana leaves. Ambient microorganisms initiate a series of biochemical transformations, developing important flavor, aroma, and color precursors within the beans. Fermentation results in 0-70% loss of total polyphenols (similar losses for the flavanol subclass), followed by an additional 15-40% loss during drying and roasting [9–11]. Roasting is dependent upon time and temperature, with times varying from 5-120 min at 120-150°C, and is responsible for the development of characteristic aroma, color, and texture of cocoa [12]. During this heat treatment, non-enzymatic browning reactions can occur between native cocoa polyphenols and mono- or polysaccharides, proteins and amino acids to produce Maillard reaction products (melanoidins) [6]. Beans can be roasted whole or as nibs, and winnowing, or separating the husks from the nib, can be done prior to or following roasting. The roasted nibs are then ground at elevated temperatures to produce a cocoa liquor and then pressed to separate fat (cocoa butter) from cake, approximately 58% of the total liquor [12]. The cocoa cake is then ground into a homogenous

powder to be used in a variety of finished products. Chemical reactions during cocoa processing alter the structure and reduce measured levels of flavanols, and the accepted paradigm is that preservation of the native flavanols is critical for retaining bioactivity [9, 11, 13]. It is possible, however, that reactions occurring throughout processing may generate compounds with novel activities such as lignin-like complexes and melanoidins, potentially preserving or even enhancing bioactivity compared to the raw cocoa bean [9, 14–22]. Due to analytical challenges such as lack of authentic standards, complexity and size of potential products, low bioavailability of large complex compounds, and the continued focus of researchers on small monomeric flavanols, the levels and activities of these large, complex and diverse compounds are largely unknown.

In the human body, flavanols have highly variable systemic bioavailability, with absorption being inversely proportional to molecular weight and ~0% absorption for compounds \geq tetramer [23–27]. Due to this poor absorption, cocoa is an ideal food for the delivery of these bioactive compounds to the GI tract. Although this limits the activity of native flavanols in the peripheral tissues, delivery to the gut lumen and epithelial surface is high and not subject to various barriers and processes that reduce flavanol activity, ultimately exposing the gut to elevated levels of native unmetabolized flavanols and flavanol processing products. Bioactivity exerted within the lumen of the gut plays a potential role in mitigation and prevention of obesity and related chronic conditions, such as type 2 diabetes mellitus, dyslipidemia, and cardiovascular disease. Specifically, inhibition of gut digestive enzymes to limit macronutrient digestion is a promising mode of bioactivity that does not require systemic bioavailability. Cocoa and cocoa flavanols inhibit lipases, α -amylase and α -glucosidase; with α -glucosidase appearing to be the most affected enzyme based on reported IC_{50} values [15, 28]. α -glucosidase is a brush border enzyme that hydrolyzes starch and maltose into absorbable glucose [29]. Inhibition of α -glucosidase is a potential strategy to inhibit or slow blood glucose absorption in the context of glucose intolerance/hyperglycemia. Commercially available α -glucosidase inhibitors, such as acarbose, miglitol, and voglibose, come with high prices and various side effects (such as GI discomfort), therefore warranting the investigation of dietary flavonoids (from berries, red wine, green tea, cocoa, etc.) as potential inhibitors [19]. While procyanidins are effective α -glucosidase inhibitors, recently we found that various cocoas were effective inhibitors of α -glucosidase despite large reductions in flavanols as a result of fermentation and roasting [15].

These results challenge the existing idea that the presence of native flavonoids is responsible for all bioactivity and therefore warrant further investigation into the factors that determine α -glucosidase inhibition. Specifically, the impact of cocoa processing on subsequent bioactivity, and the identification of non-flavanol cocoa components with bioactivity are of interest.

Fermentation and roasting are the most universally applicable steps in cocoa processing that can be manipulated in order to produce a final product with variable flavanol compositions. Due to the poor documentation and varying practices of fermentation, a controlled model pilot-scale fermentation is necessary in order to conduct research regarding the impact of fermentation and further processing on bean composition and subsequently bioactivity [12, 30, 31]. Furthermore, cocoa powder is a widely consumed commodity worldwide and the harvesting of beans is essential to the economic prosperity of many developing countries. The main objectives of this work were to 1) evaluate the effect of extremes in fermentation temperature and roasting temperature on the chemical composition of cocoa beans and cocoa powder, 2) determine how fermentation and roasting affect α -glucosidase inhibitory activity of cocoa powder, and 3) identify compositional factors and processing conditions that optimize α -glucosidase inhibitory activity of cocoa. The end goal of this research is to develop processing approaches to maximize the health protective activities of dietary cocoa powder.

5.2 MATERIALS AND METHODS

5.2.1 Chemicals and standards. Raw unfermented cocoa beans, sourced from Hispaniola, were provided by Cargill, Inc. (Wayzata, MN). Although not confirmed, the researchers believe the beans to be of the Criollo variety. Beans were stored in burlap sacks at 3.5°C prior to use. LC-MS grade acetonitrile (ACN), methanol (MeOH), citric acid, yeast extract, malt extract, calcium-lactate pentahydrate, tween 80, sodium hydroxide, magnesium sulfate heptahydrate, manganese sulfate monohydrate, sucrose, glucose, fructose, calcium carbonate, agar and water were obtained from Thermo-Fisher Scientific (Waltham, MA). Glacial acetic acid, methanol, and acetone were obtained from VWR (Radnor, PA). Standards of (–)-epicatechin (EC), (±)-catechin (C), and procyanidin B2 (PCB2) were obtained from ChromaDex (Irving, CA). Standards of procyanidin C1 (PCC1), cinnamtannin A2 (CinA2), and DP 5-9 purified from cocoa (purity: DP 3-5: 93-99%, DP6-9: 80-92%) were obtained from Planta Analytica (New Milford, CT).

Ammonium formate, Folin-Ciocalteu reagent, 4-dimethylaminocinnamaldehyde (DMAC), and alpha-glucosidase enzyme were obtained from Sigma-Aldrich (St. Louis, MO). Solvents were ACS grade or higher.

5.2.2 Fermentation model system and processing. As illustrated in **Figure 5.1**, a partial multifactorial approach to cocoa processing was employed to generate cocoas produced from the same batch of raw beans using different combinations of two treatments at three levels each: fermentation (unfermented, cool fermented, and hot fermented) and roasting (unroasted, low temperature roasted and high temperature roasted). The high and low levels of each factor and combinations thereof were evaluated. Due to cost constraints, the high roasting temperature/cool fermentation temperature and the cool roasting temperature/high fermentation temperature conditions were not evaluated. This approach allowed assessment of the effects of two cocoa processing steps, fermentation and roasting, on cocoa composition and activity.

		Fermentation Temperature		
		-	Cool (+3.5°C/24h)	Hot (+6°C/24h)
Roasting Temperature	-	Unfermented Unroasted	Cool Fermentation Unroasted	Hot Fermentation Unroasted
	Cool (120°C)	Unfermented Cool Roast	Cool Fermentation Cool Roast	
	Hot (170°C)	Unfermented Hot Roast		Hot Fermentation Hot Roast

Figure 5.1. Multivariate approach to evaluating the impact of combined fermentation and roasting parameters, producing 7 total cocoa powders: unfermented/unroasted (UF/UR), unfermented/cool roast (UF/CR), unfermented/hot roast (UF/HR), cool fermentation/unroasted (CF/UR), cool fermentation/cool roast (CF/CR), hot fermentation/unroasted (HF/UR), hot fermentation/hot roast (HF/HR).

5.2.2.1 Fermentation. Raw unfermented cocoa beans were rehydrated, fermented and dried based on the previously established pilot-scale cocoa fermentation protocols of Racine et al [32] and Lee et al [33] with minor modifications. Unfermented cocoa beans (32 kg) were rehydrated in 66.4 cm × 44.3 cm × 34.3 cm plastic fermentation boxes (polypropylene, Sterilite, Townsend, MA) by submersion in approximately 45 L of distilled, deionized (DI) water for 24 h at room

temperature. The final moisture content of the beans after rehydration was between 35-50% (IR-120 Moisture Analyzer, Denver Instrument, Bohemia, NY). Rehydrated beans were then drained and 60 kg were mixed with 60 L of simulated pulp media (3 replicate fermentation boxes per fermentation batch; approximately 20 kg rehydrated beans and 20 L simulated pulp media per box). For preparation of simulated pulp medium, three solutions were prepared separately and combined with the rehydrated beans to begin fermentation. Solution A consisted of citric acid (10 g/L), yeast extract (5 g/L), peptone (5 g/L), calcium lactate-pentahydrate (1 g/L), and tween 80 (1 mL/L). pH was adjusted to 3.6 using 1 N NaOH and then autoclaved (121°C, 15 min) for a total of 36 L. Solution B was an 18 L sugar solution of sucrose (83.3 g/L), glucose (133.3 g/L), and fructose (150 g/L), autoclaved and cooled prior to fermentation. Solution C was prepared the day of fermentation and consisted of magnesium sulfate heptahydrate (1 g/L) and manganese sulfate monohydrate (0.4 g/L) for a total of 6 L. Boxes were loosely covered with their plastic lids and placed inside a pre-heated (25°C) incubator (Forma 29 cu ft Reach-In-Incubator, Model No. 3950, Thermo Fisher Scientific, Waltham, MA).

In total, four fermentation runs were conducted, two cool fermentation runs and two hot fermentation runs. Each fermentation run continued for a total duration of 168 h. For each run, the material was fermented in three separate boxes within this same incubator, with 20 kg rehydrated beans and 20 L simulated pulp in each box. The incubator set point was raised 3.5 °C/24 h for the cool fermentation runs and 6°C/24 h for the hot fermentation runs, to final temperatures of 46°C (cool) and 60°C (hot) (**Figure 5.1**). For all boxes in all fermentation runs, beans were manually agitated for 5 min every 8 h to ensure that the simulated pulp media was well-mixed and properly aerated. Pulp dissolved oxygen (DO) and pH values were monitored using benchtop meters (Orion DO Probe 083005MD; Orion Versa Star Pro pH meter; Thermo Fisher Scientific). After 168 h of fermentation, the beans were drained to remove the remaining simulated pulp media, spread evenly onto baking sheets and oven dried (Rational, Germany; Blodgett, Burlington, VT) at 65.5°C until the moisture content fell below 8%. After drying, all beans from both cool fermentation runs were thoroughly commingled to mix all batches/boxes and stored at 3.5°C until roasting, and the same was done for all beans from both hot fermentation runs. The beans subjected to the unfermented treatment were rehydrated, drained, and immediately oven dried according to the procedures above.

5.2.2.2 *Roasting and further processing.* Roasting was performed in a gas-fired drum roaster (180 kg capacity, Probat, Inc., Vernon Hills, IL) at a drum speed of 15 Hz in collaboration with Epiphany Craft Malt (Durham, NC). Each unique fermentation/roasting treatment was roasted separately in batches of approximately 30 kg. The cool roasted treatment temperature was 120°C and the hot roasted treatment temperature was 170°C (**Figure 5.1**). Roasting treatments were conducted for 20 min each. After roasting, beans were placed on a rotating cooling table and then stored at 3.5°C until further processing.

The beans were further processed into cocoa powder in collaboration with Blommer Chocolate Company (East Greenville, PA). The beans were first winnowed to remove shells and ground into a liquor. The liquor was then heated to approximately 200°C and pressed (Cacao Cucino, Model No. 306487, Clearwater, FL) for 133 min to produce a solid cake that was then ground into a homogenous cocoa powder. All 7 treatments were uniformly processed into 7 different cocoa powders. Powders were stored at -20°C until further analysis. Moisture and fat content for liquors and cake (ORACLE Rapid Fat Analyzer, CEM, Matthews, NC) and particle size of liquors (Microtrac S3500, Microtrac, Montgomeryville, PA) was measured for each treatment per Blommer SOPs. Standard product specifications for resulting cocoa liquors and cakes are listed in **Table 5.1**.

Table 5.1. Specifications for cocoa liquors and cakes of each treatment

Treatment	Liquor		Cake		Liquor Particle Size (µm)			
	Fat	Moisture	Fat	Moisture	99% through	95% through	75% through	50% through
UF/UR	55.96%	1.43%	9.15%	5.23%	88.00	52.00	18.50	11.00
UF/CR	58.10%	1.36%	8.70%	3.43%	124.50	74.00	18.50	11.00
UF/HR	56.78%	0.73%	15.36%	2.01%	209.30	114.10	20.17	10.09
CF/UR	58.20%	2.37%	10.97%	4.38%	191.90	104.60	23.99	12.00
CF/CR	58.04%	1.37%	9.32%	2.82%	191.90	104.60	22.00	11.00
HF/UR	56.03%	1.98%	9.17%	4.80%	67.86	47.98	20.17	11.00
HF/HR	58.06%	1.09%	7.50%	3.00%	148.00	74.00	16.96	10.09

5.2.3 Bean pH. Cocoa bean pH was determined every 24 h during fermentation as previously reported based on the method described by Racine et al [32].

5.2.4 Cut test. A representative cut test was performed on a sample of whole beans from each of the four fermentation runs (2 cool batches, 2 hot batches). Beans (6) from each 24 h sampling period (0-168 h) were cut through the middle lengthwise so that color and quality could be assessed. This test is a standard assessment of post-fermentation bean quality and suitability to move forward in processing [34, 35].

5.2.5 Fermentation index. Cocoa bean fermentation index (FI) was measured every 24 h during fermentation based on the method of Romero-Cortes et al [36] with minor modifications. Randomly selected whole cocoa beans (3-5 beans) were frozen with liquid nitrogen and ground into a powder in an electric spice grinder. The powder (50 mg) was mixed with 5 mL MeOH HCl (97:3 v/v) and extracted at 4°C for 16-18 h on a rotating platform. Samples were then centrifuged (5 min, 3500 × g), supernatant collected (300 µL), and absorbance measured at 460 nm and 530 nm using a 96-well microplate. The FI was calculated using the equation below and all analyses were performed in analytical triplicate.

$$FI = \frac{A_{460}}{A_{530}}$$

5.2.6 Polyphenol extraction and characterization. Polyphenol rich extracts were made from raw beans, the fermented cocoa beans (cocoa bean extract, CBE) and powders (cocoa powder extract, CPE) for all seven treatments as described previously [15, 32, 37]. Total phenolic content of the freeze dried cocoa extracts was approximated by the Folin-Ciocalteu colorimetric assay and total flavanols measured by the 4-dimethylaminocinnamaldehyde (DMAC) colorimetric assay, as previously described in Dorenkott et al [14]. These values were expressed in mg Gallic Acid Equivalents (mg GAE)/g bean and mg PCB2/g bean, respectively. The mean degree of polymerization (mDP) of the flavanols was determined using a thiolysis method based on the protocol of Dorenkott et al [14] with minor modifications. Cocoa monomeric flavanols and procyanidins (DP 1-10) were quantified by HILIC UPLC-MS/MS as previously described based on the method of Racine *et al*[38] . Refer to *Appendix A* for full methodological details.

5.2.7 Melanoidin dialysis. The dialysis method proposed by Sacchetti et al [39] was followed with modifications to fraction high and low molecular weight (HMW, LMW) CPE fractions.

CPE was re-dissolved in extraction solution (70:28:2 acetone, water, acetic acid) at a concentration of 40 mg/mL. Dialysis was performed in triplicate using acidified methanol: water (60:40, 0.1% formic acid) as the dialysis solvent. For each replicate, 2.5 mL of dissolved CPE was placed inside presoaked dialysis tubing (8-10 kDa MW cutoff, Spectrum Spectra/Por Biotech-Grade RC Dialysis, Fisher) and clipped closed. This MW cutoff was chosen based on preliminary data showing that the majority of early, intermediate, and final Maillard reaction products (MRP) are eluted from the 3.5-5 kDa and 8-10 kDa tubing, with very little in 20 kDa, followed by a significant increase in 50 kDa (see *Appendix A*). The tubing was then submerged in 250 mL of dialysis solvent and the beaker was stirred at 4°C for 24 h. Dialysis beakers were continually sparged with nitrogen throughout the process. Following the 24 h dialysis period, the 250 mL dialysis solvent outside the tubing and the CPE components remaining within the tubing were separately rotary evaporated at 55°C, frozen at -80°C, and then freeze dried. Following freeze drying, solids were weighed, and yield was calculated.

To selectively quantify melanoidins, each dialysate (<8-10 kDa) was resolubilized in 0.05 M H₂SO₄ to a concentration of 0.15625 (early MRP), 2.5 mg/mL (intermediate MRP), and 5 mg/mL (late MRP). The non-dialyzable CPE (>8-10 kDa) were resolubilized in 0.05 M H₂SO₄ to a concentration of 0.15625 mg/mL (early MRP), 2.5-1.25 mg/mL (intermediate MRP), and 2.5 mg/mL (late MRP). Starting CPE at 40 mg/mL was freshly made with extraction solution and diluted with 0.05 M H₂SO₄ 0.15626 mg/mL (early MRP), 2.5-1.25 mg/mL (intermediate MRP), and 10 mg/mL (late MRP). A standard curve was prepared with quinine sulfate dissolved in 0.05 M H₂SO₄ (1-1000 ppm). Each diluted dialysate, non-dialyzable CPE, starting CPE, and standard was transferred (300 µL) into a UV-Star 96-well plate. The absorbance was read at 280 nm, 360 nm, and 420 nm, and early (280 nm), intermediate (360 nm) and late (420 nm) MR products (MRP) quantified based on the standard curve. Due to the lack of standard response at 420 nm, late MRP are reported as absolute absorbance values (single dilution used for each fraction to facilitate direct comparisons of absorbances: 5 mg/mL (<8-10 kDa), 2.5 mg/mL (>8-10 kDa), and 10 mg/mL (unfractionated CPE).

5.2.8 Three stage *in vitro* digestion. In order to determine digestively stable and soluble compounds (i.e. diffusible across the unstirred water layer), cocoa powders from all treatments were digested *in vitro* in three phases (oral, gastric, and intestinal) protocol as described by Li *et*

al [40] with modifications. Each cocoa powder (10 g) was diluted to a final volume of 500 mL. After the intestinal phase, the final digesta was divided into 2-250 mL aliquots. One aliquot was immediately frozen at -80°C (total digesta), and the second solution was centrifuged for 10 min ($5000 \times g$, 37°C), the supernatant was collected, and then frozen at -80°C (solution digesta). Both fractions were freeze dried and yields were calculated. A blank digestion (using 10 mL saline instead of 10 g cocoa) was performed to account for the digestion reagents. Refer to *Appendix A* for full methodological details.

5.2.9 In vitro α -glucosidase inhibition. CPE and soluble digesta fractions were screened for α -glucosidase inhibitory activity *in vitro* as described previously [15]. A 0.1 M phosphate buffer (pH 6.9) was prepared in water with sodium phosphate monobasic anhydrous (8.05 g/L), and sodium phosphate dibasic anhydrous (4.67 g/L). pH was adjusted to 6.9 with 1 N NaOH. CPE was diluted to obtain concentrations of 0.3125-8,000 $\mu\text{g/mL}$ (all in 10% DMSO). Using calculated extraction and digesta yields, soluble digesta fractions for each corresponding cocoa powder were weighed according to an equivalent of 20 mg CPE (i.e. in the amount of digesta resulting from digestion of the amount of cocoa powder that yielded 20 mg CPE). Soluble digesta fractions were diluted to obtain concentrations equivalent to 0.3125-8,000 $\mu\text{g/mL}$ CPE in the starting cocoa (all in 10% DMSO). A negative control (no inhibitor, i.e. 0 $\mu\text{g/mL}$ CPE) was prepared with only 10% DMSO. The α -glucosidase solution was prepared in 0.1 M phosphate buffer to a final concentration of 1 U/mL. The *p*-nitrophenyl α -D-glucopyranoside (*p*NPG) substrate solution was prepared at a final concentration of 1 mM in 0.1 M phosphate buffer. In 96-well plates ($n=6$ wells/treatment), 50 μL of each working sample solution or negative control was mixed with 100 μL of α -glucosidase solution. The plate was then incubated at room temperature for 10 min followed by the addition of 50 μL of *p*NPG solution to each well. The final concentrations of each inhibitor solution was thus 0-2,000 $\mu\text{g/mL}$ (CPE) or 0-2,000 μg CPE starting material/mL (digesta). The plate was then read at 405 nm. The positive control was acarbose in 10% DMSO matched to CPE concentrations (0-2,000 $\mu\text{g/mL}$ final concentration in the assay). The cocoa extracts were compared to the controls at each concentration and the values expressed as % α -glucosidase activity via the following equation:

$$\% \alpha - \text{Glucosidase Activity} = \left(\frac{\Delta A_{\text{sample}}}{\Delta \bar{A}_{\text{negative control}}} \right) \times 100$$

where:

ΔA_{sample} = the change in the individual absorbance value of the product of the inhibitor, substrate, and enzyme at each inhibitor dose before and after incubation

$\Delta A_{\text{negative control}}$ = the average change in absorbance of the negative control (0 $\mu\text{g/mL}$) before and after incubation

5.2.10 Data analysis and statistics. All fermentation data (pH, FI, DO), compositional data (Folin-Ciocalteu, DMAC, thiolysis, melanoidins, individual flavanols/procyanidins), and enzyme activity (% activity) at individual concentrations near IC_{50} values were analyzed by one-way ANOVA. If a significant overall treatment effect was detected, Tukey's HSD post hoc test was performed to determine differences between all treatment means. Median inhibitory concentration (IC_{50}) values for α -glucosidase were calculated for each CPE treatment using a four-parameters sigmodal analysis. Simple linear regression analysis was performed to correlate individual compositional factors (predictors: X) to α -glucosidase activity (IC_{50} , outcomes: Y). The mean compositional values and IC_{50} for each CPE treatment were plotted (7 points per analysis), and R and R^2 were calculated. Statistical significance was defined *a priori* as $p < 0.05$. Analyses were performed on XLSTAT-Base (2018.5, New York, NY) and GraphPad Prism v7.03 (GraphPad, La Jolla, CA).

5.3 RESULTS

5.3.1 Fermentation model system and cocoa processing. Monitored fermentation parameters (pH, DO) progressed similarly across the 168 h for CF and HF, with initial (0 h) pulp pH values at 3.99 ± 0.05 and 3.84 ± 0.01 , respectively, and ending (168 h) values at 3.51 ± 0.02 and 3.36 ± 0.07 , respectively (**Figure 5.2**). At the end of fermentation, pulp of both CF and HF concluded with more acidic internal environments. Furthermore, initial bean pH values ranged from 5.61 ± 0.01 (CF) to 5.75 ± 0.16 (HF) and concluded at 3.89 ± 0.04 (CF) and 3.95 ± 0.01 (HF) after 168 h. Dissolved oxygen remained ≤ 1 mg/L after the first 24 h of fermentation. Initial FI values (**Figure 5.2**) for both CF and HF were above 1.0 and remained within ± 0.01 throughout the entire 168 h fermentation. Cut test results, although performed at a much lower sample size than the

traditional 300+ cut beans, showed similar results as there was no true progression of color from purple to brown beans.

The fat and moisture content of liquors and cake, as well as the particle size of liquors, are reported in Table 1. While liquor fat content was generally similar across all treatments (~56-58%), UF/HR had much higher cake fat content (15.4%) and lower cake moisture (2.0%) than the other treatments. HF/HR had the lowest cake fat content at 7.50%.

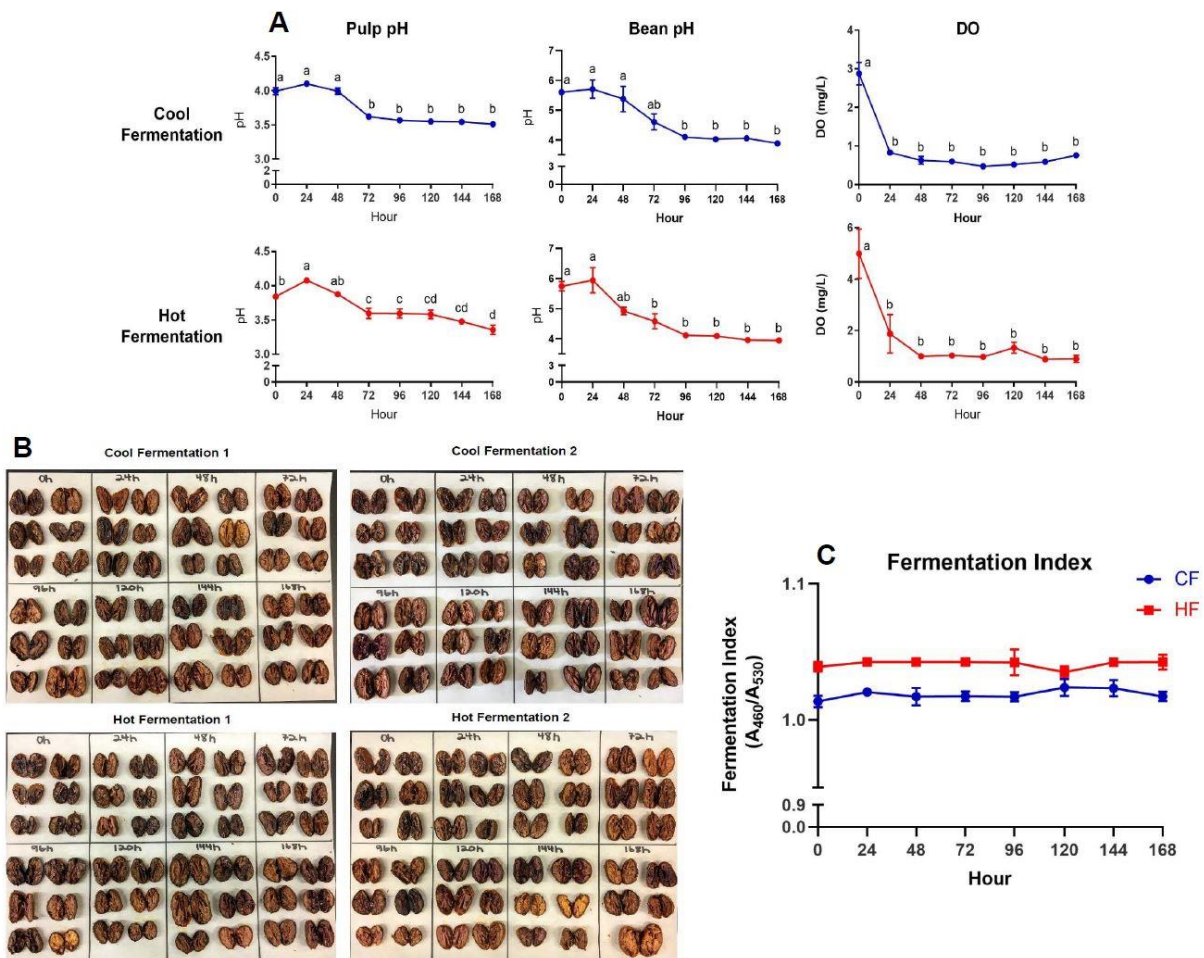


Figure 5.2. **A.** pH of simulated pulp media/bean nib and dissolved oxygen (DO). It is important to note that for bean nib measurements, these values do not quantify the pH of the cocoa bean itself, but rather the acidity derived from bean acids diluted in water. These nib values are useful for comparison between the pH of the solution produced by beans at different time points. **B.** Cut test for all fermentations performed. **C.** Fermentation index as a ratio of 460 nm:530 nm, with values ≥ 1 indicating a complete fermentation. Note broken axes for ease of interpretation on select graphs. Values are presented as the mean \pm SEM of fermentation replicates within treatments. Significant between time points for each value was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Time points with different letters are significantly different within values. No letters indicate no statistical difference within values.

5.3.2 Characterization and quantification of polyphenols. Total polyphenols and total flavanols were measured by the Folin-Ciocalteu and DMAC assays, respectively (**Figure 5.3**), in beans and powders resulting from each treatment. Powders had a 2-3-fold higher total polyphenol and total flavanol concentrations compared to the corresponding beans due to differences in fat content. Treatments with less harsh processing conditions (UF/UR, UF/CR, CF/CR) generally had higher levels of total compounds than those that endured a more heat intensive processing (HF/UR, HF/HR, UF/HR), as expected. Interestingly, CF/UR powder had significantly lower levels compared to CF/CR and UF/CR when assessing total polyphenols and total flavanols (**Figure 5.3 A, C**), whereas across measured individual procyanidins (**Figure 5.4**) there are no significant differences between CF/UR and CF/CR.

Concentrations of compounds DP 1-10 were quantified from CPE and CBE from each of the 7 treatments via HILIC UPLC-MS/MS. For HILIC data, concentrations in powders were normalized to the percentage of fat-free mass in each respective treatment to account for the effect of pressing (i.e. fat content) and to present values influenced only by fermentation and roasting (**Figure 5.4**). Unnormalized values for CPE and CBE are shown in **Figure A2** and **Figure A3**. **Figure 5.5** illustrates total procyanidins, organized by DP, per treatment. As expected based on Folin and DMAC results discussed above, UF/UR and UF/CR powders had the highest concentrations of individually quantified procyanidins in CPE ranging from 0.174 ± 0.002 - 3.30 ± 0.16 mg/g and 0.175 ± 0.001 - 3.77 ± 0.11 mg/g respectively. Alternatively, HF/HR powder had significantly lower levels of total compounds (polyphenols, flavanols, DP 1-10) across all treatments. Yet, HF/HR had the highest mDP of all treatments, at approximately 10, when calculated factoring in only oligomeric and polymeric procyanidins (**Figure 5.3 F**). UF/HR had a lower mDP than both HF/UR and HF/HR when calculated factoring in monomers originally present in the sample. (**Figure 5.3 E**).

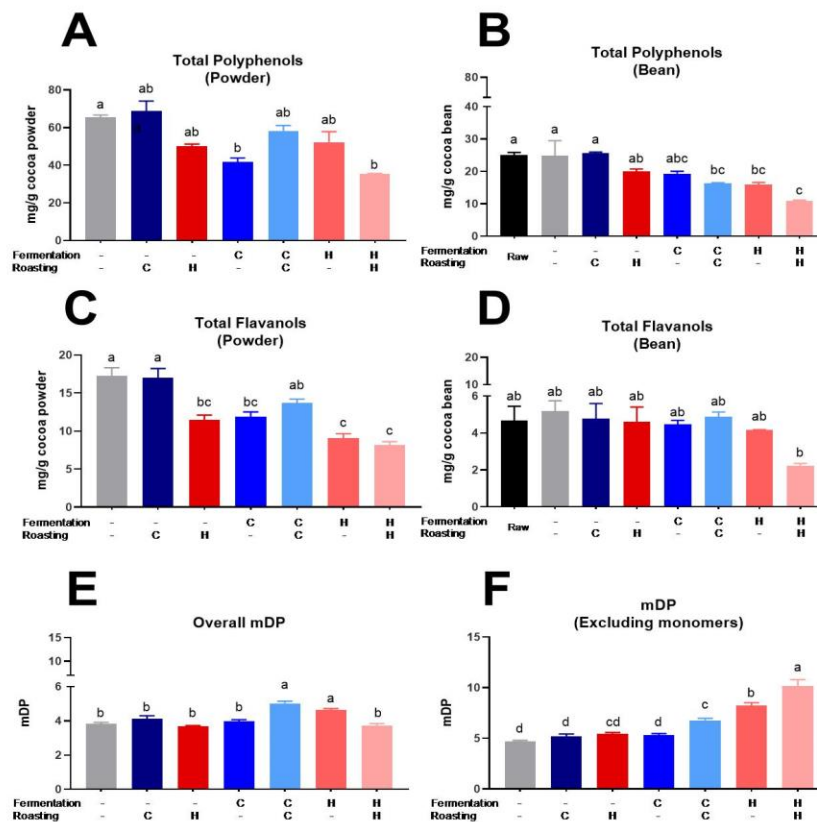


Figure 5.3. Total polyphenols in each cocoa powder (A) and cocoa bean (B) expressed in gallic acid equivalents. Total flavanols from cocoa powder (C) and cocoa bean (D) expressed in procyanidin B2 equivalents. (E) Overall mean flavanol degree of polymerization for the total flavanols in cocoa powder- native monomers were accounted for in calculation. (F) Mean flavanol degree of polymerization for oligomers and polymers in cocoa powder (not including native monomers); Note broken axes (B,D,E) for ease of interpretation. Raw bean (B,D) indicates the extract prepared from the cocoa beans as received from the supplier and is different from UF/UR (-/-) as these beans were rehydrated and dried. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

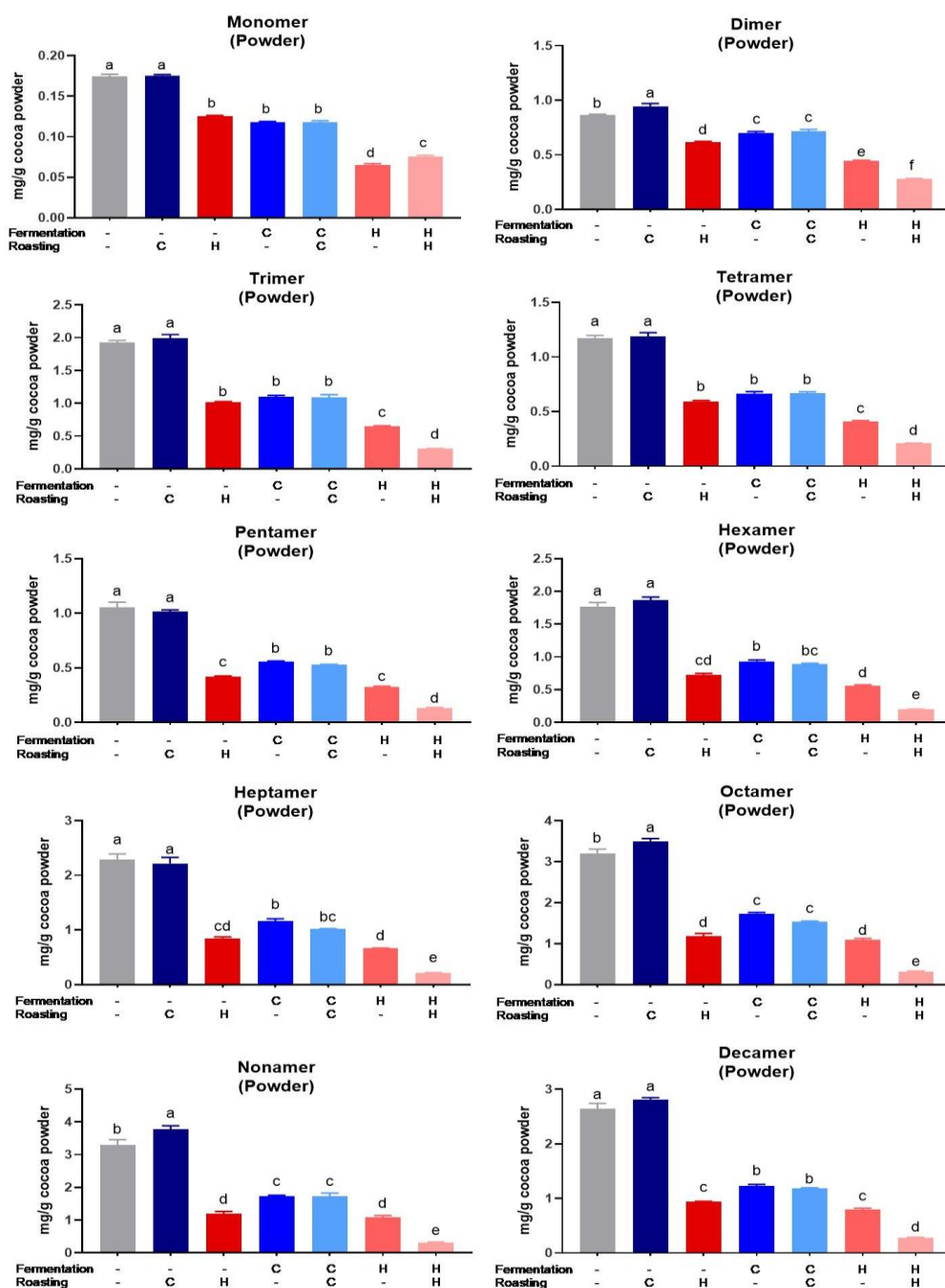


Figure 5.4. Levels of individual procyanidin compounds in cocoa powders. Values are normalized to the fat-free mass of each treatment to account to varying fat content. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

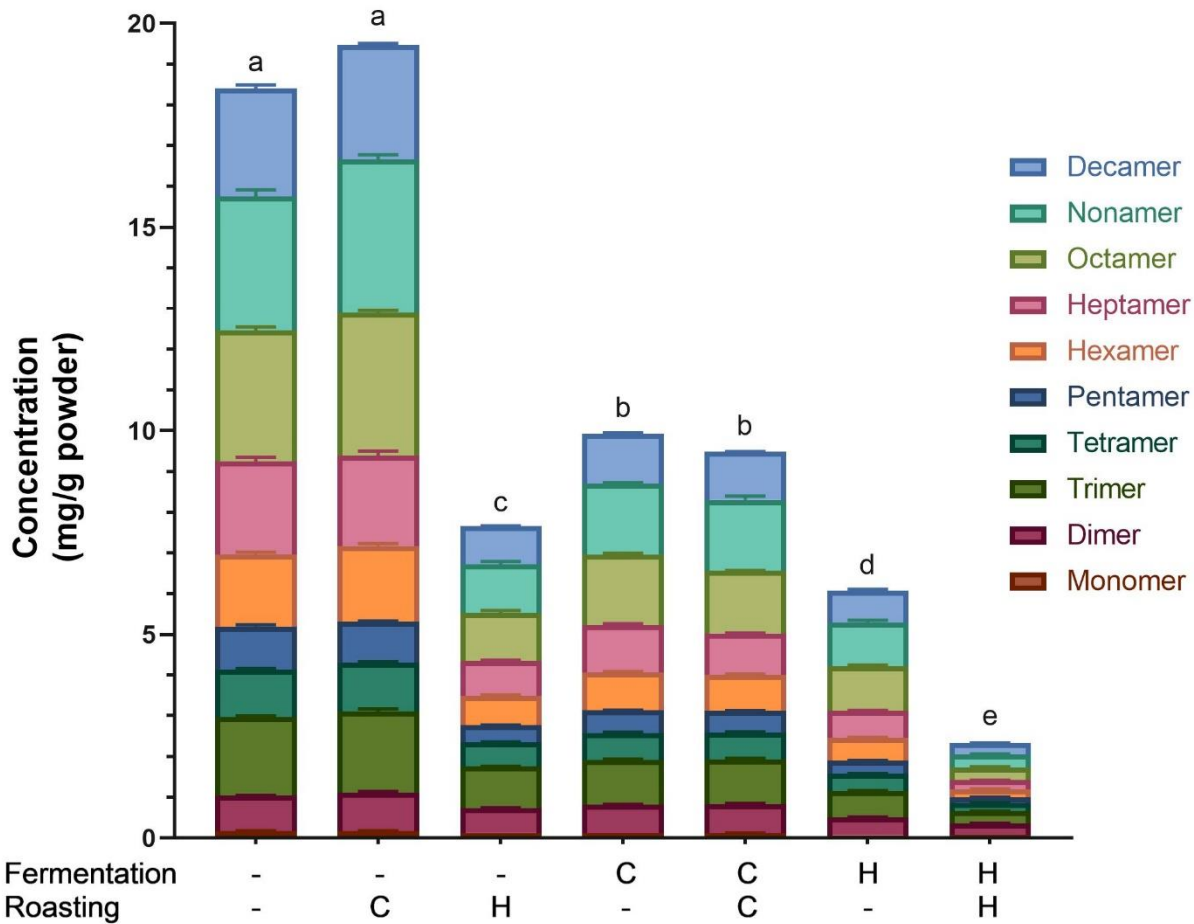


Figure 5.5. Total procyanidins (DP 1-10) per cocoa powder treatment as measured by HILIC UPLC-MS/MS. Each segment represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

5.3.3 Quantification of Maillard reaction products. Early, intermediate, and late MRP were quantified at 280, 360, and 420 nm, respectively, and illustrated in **Figure 5.6**. Due to lack of standard response at 420 nm, late MRP is presented as absolute absorbance, which is proportional to concentration. Hot roasted treatments (UF/HR and HF/HR) had the highest levels of LMW compounds (<8-10 kDa) across intermediate and late MRP, while HF/UR had significantly higher values of HMW compounds (>8-10 kDa) in the late stages of the MR. UF/UR and CF/UR had the lowest concentrations of early, intermediate, and late MRP in the LMW fraction. The original unfractionated CPE (40 mg/mL CPE) was quantified in order to demonstrate the MRPs in the total extract.

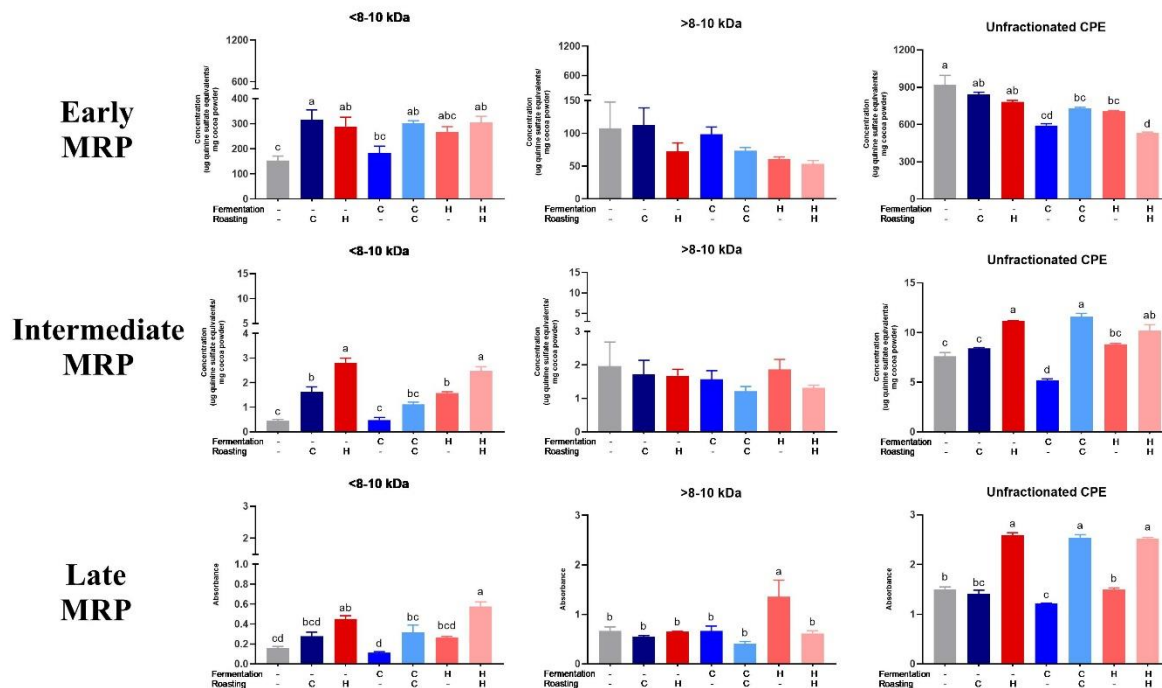


Figure 5.6. Analysis of LMW and HMW CPE fractions and the starting 40 mg/mL CPE for early, intermediate, and late MRP. Early MRP were quantified at 0.15625 mg/mL at 280 nm, intermediate MRP were quantified at 2.5-1.25 mg/mL at 360 nm, and late MRP were quantified at 5 mg/mL (<8-10 kDa), 2.5 mg/mL (>8-10 kDa), and 10 mg/mL (unfractionated CPE) at 420. Due to the lack of standard response at 420 nm, absolute absorbance of these compounds is reported, but this absorbance is relative to concentration. Each bar represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. No letters indicate no statistical difference within values.

5.3.4 Three stage in vitro digestion. The yields for each digestion are shown in **Table 5.2**. Soluble digesta fractions were 33-80% of the total digesta mass. A control digestion was performed with an equivalent amount of saline solution (10.03 g) and the mass yields therefore quantify the material added during the digestion other than cocoa powder. Soluble digesta fractions were used in the assessment of α -glucosidase inhibition and calculated to determine the amount of digesta yielded from digesting the amount of powder equivalent to the corresponding concentrations of extract used to evaluate the inhibitory activity of extracts. An average CPE yield of 15.38% was used to calculate the equivalent cocoa powder mass in 20 mg CPE. That mass, along with digesta yields for each treatment, was then used to calculate the amount of soluble digesta resulting from the digestion of cocoa powder that yielded 20 mg CPE.

Table 5.2. Total and soluble digesta yields from three-stage in vitro digestion

Treatment	Digested Cocoa Powder (g)	Total Digesta ^b (g)	Soluble Digesta ^b (g)
UF/UR	10.00	10.25	6.17
UF/CR	10.03	12.58	5.58
UF/HR	10.01	12.47	5.78
CF/UR	10.00	12.13	5.06
CF/CR	10.02	12.17	5.80
HF/UR	10.00	12.49	4.75
HF/HR	10.01	12.37	6.01
Control	10.03 ^a	5.20	4.13

^aControl digestion was performed with 10.03 g of saline solution instead of cocoa powder

^bmasses represent 1/2 each of the original digestion of 10 g cocoa powder

5.3.5 α -glucosidase enzyme inhibition. All CPEs, soluble digesta fractions, and the positive control were assessed at physiologically relevant doses. The highest concentration, 2,000 $\mu\text{g/mL}$ CPE (or corresponding powder extract equivalents for digesta) is equivalent to approximately 13,333 μg powder/mL in the intestinal lumen (i.e. 13,333 ppm), when accounting for a 15% yield from extraction of powders. At an estimated 2 L upper digestive volume, this would equal approximately 26.67 g of cocoa product, or just under 1 square of baker's chocolate (1 square \approx 28 g). At a lower concentration such as 100 $\mu\text{g/mL}$ (666.67 μg original product/mL in the intestinal lumen), this would be equivalent to 1.33 g of original cocoa product or approximately 0.0475 squares of baker's chocolate, a very achievable and physiologically relevant amount. Alternatively, acarbose is typically administered at 50-200 mg per dose [41]. At a 2 L upper digestive volume these would translate to 25-100 $\mu\text{g/mL}$, a range assessed in this assay and further confirming the physiological relevance of our concentrations.

CPEs dose-dependently inhibited α -glucosidase activity (**Figure 5.7 A**). CF/CR was the most inhibitory of all treatments, having significantly better inhibition than acarbose (+ control) at equivalent doses from 62.5 $\mu\text{g/mL}$ -2000 $\mu\text{g/mL}$. At 250 $\mu\text{g/mL}$, all treatments but UF/HR and HF/HR significantly inhibited enzyme activity when compared to acarbose, and at concentrations \geq 500 $\mu\text{g/mL}$, all treatments were significantly better inhibitors than acarbose (**Figure 5.7 D-G**). CPEs had the following IC_{50} values from most inhibitory to least inhibitory: 62.2 (CF/CR) $>$ 112 (Acarbose) $>$ 116 (UF/CR) $>$ 129 (HF/UR) $>$ 144 (UF/UR) $>$ 149 (HF/HR) $>$ 153 (CF/UR) $>$ 160

(UF/HR). Alternatively, soluble digesta fractions did not have better inhibitory activities compared to CPE (**Figure 5.7 B**). Yet, when compared to the control digesta (no cocoa powder), all treatments had lower levels of enzyme activity, indicating that the soluble components do inhibit α -glucosidase (all digesta containing cocoa reached 50% inhibition at the highest dose).

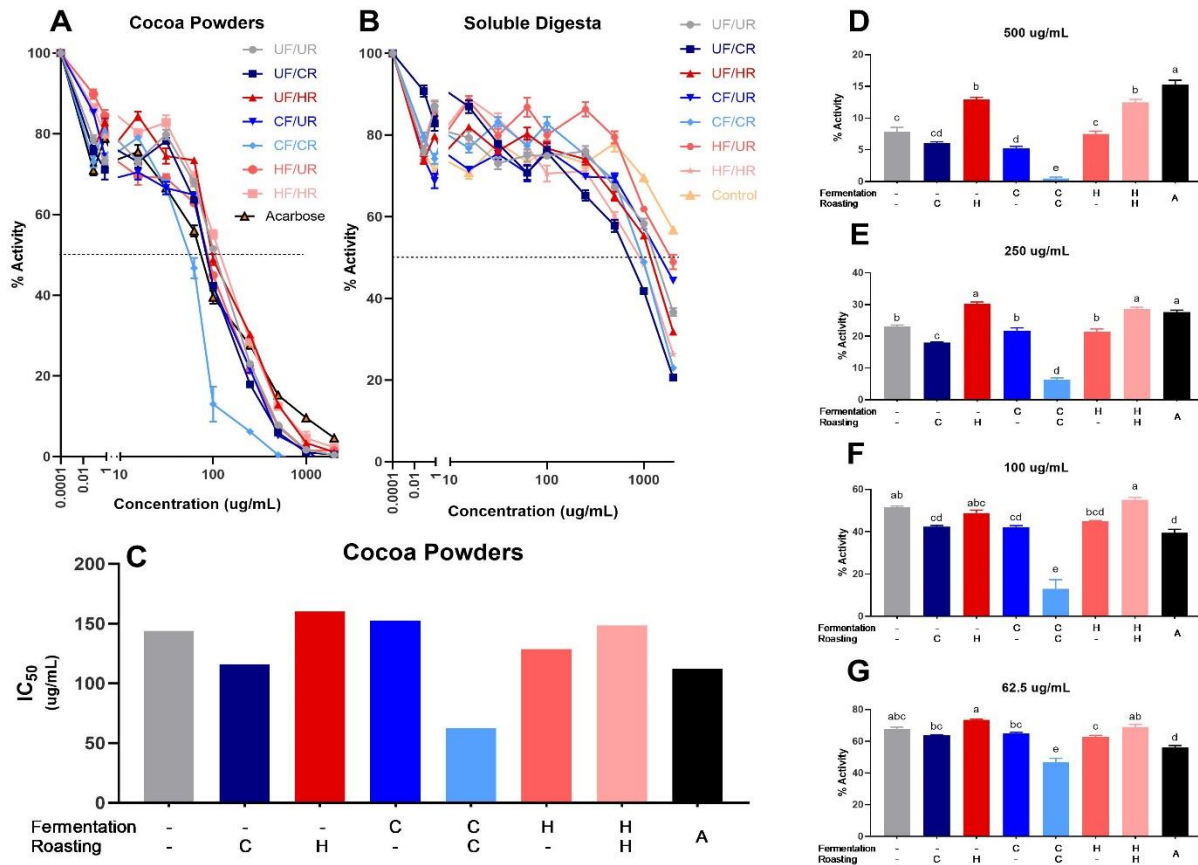


Figure 5.7. α -glucosidase activity (%A compared to no inhibitor) for cocoa powder extracts (A) and soluble digesta fractions (B) with Acarbose positive control (extracts only). IC_{50} values are representative of cocoa powder extract inhibitory activity (C) with R^2 values for each treatment as follows: 0.9625 (UF/UR), 0.9539 (UF/CR), 0.9593 (UF/HR), 0.9511 (CF/UR), 0.9543 (CF/CR), 0.9702 (HF/UR), 0.9777 (HF/HR), 0.9476 (Acarbose (A)). Specific cocoa powder extract concentrations (62.5-500 μ g/mL) at %A above and below IC_{50} value (D-G). Note that IC_{50} values do not have error bars, as values were interpolated from inhibition curves. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

5.3.6 Identifying predictors of α -glucosidase enzyme inhibitory activity. Simple linear regression was employed to determine whether a linear relationship existed between inhibitory activity (IC_{50}) and any of the chemical composition parameters of CPE (**Figure 5.8**). A strong

negative correlation would indicate that IC_{50} decreases as mDP or compound concentration increases, and a strong positive correlation would indicate the exact opposite- that IC_{50} increases as mDP or compound concentration increases. The majority of results showed minimal or no correlations except for mDP (All)- the overall mDP calculated when factoring in monomers originally present in the sample. This strong negative correlation ($R = -0.882$) demonstrates that as overall mDP increases, the enzyme activity decreases, (i.e. inhibition increases). On the other hand, a strong positive correlation was observed between IC_{50} and intermediate MRP from HMW CPE fractions, demonstrating that as the concentration of these very large and complex compounds increase, the enzyme activity also increases (i.e. inhibition decreases), suggesting that these MRPs either interfere with enzyme inhibition, or are markers of the loss of compounds that inhibit enzyme activity.

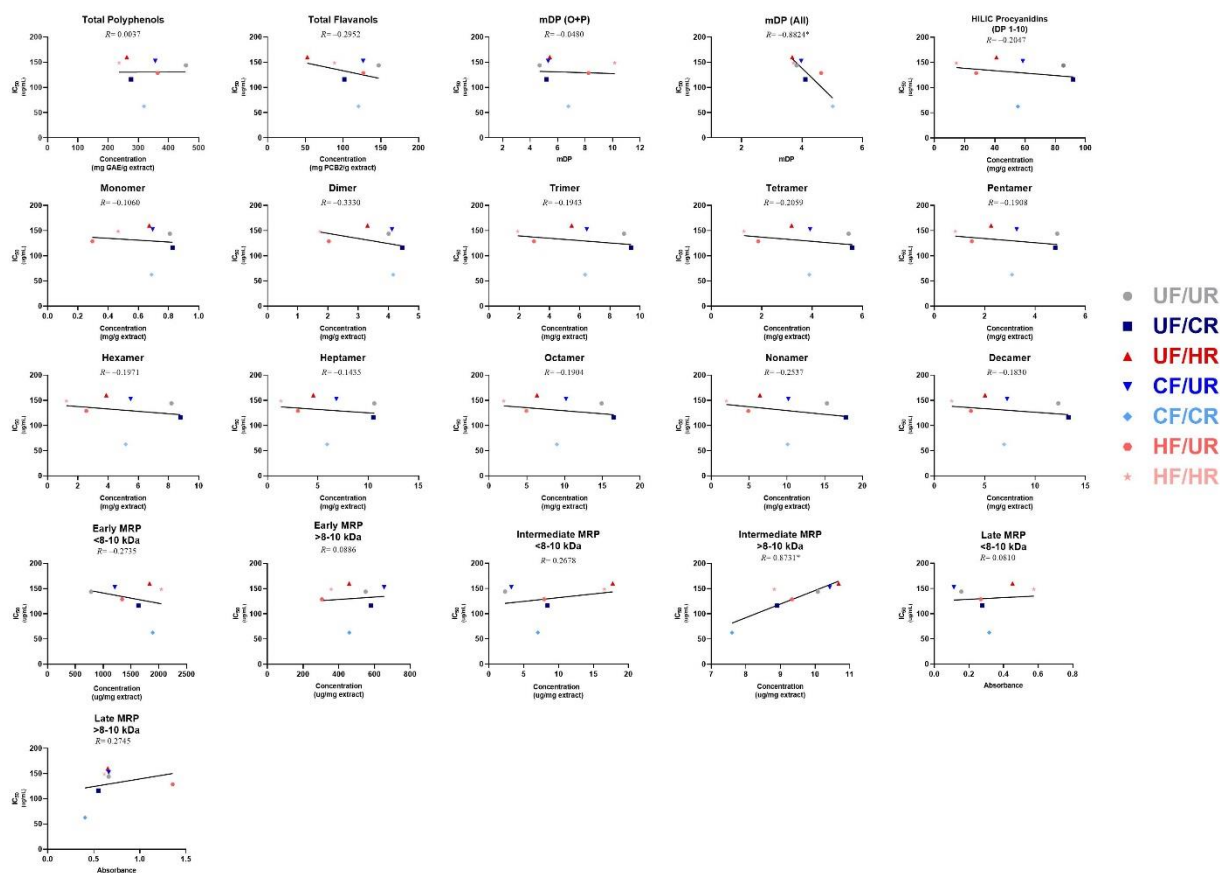


Figure 5.8. Correlations between cocoa powder extract composition and enzyme IC_{50} values. Note the x-axis for mDP (All) and mDP (O+P) has a minimum value of 1 mDP because there cannot be a mDP value of zero. Note that late MRP are presented as absolute absorbance. Individual points represent mean composition values and calculated IC_{50} values for each treatment. Lines represent the least-squares regression line for each plot. Note that composition values are for the cocoa extract, not powders, since the extract was evaluated for enzyme activity.

5.4 DISCUSSION

Through the utilization of a controlled fermentation model system and further processing steps, we generated and then assessed compositional and bioactivity differences of seven different cocoa powders representing a range of possible processing conditions. This approach allowed us to attribute differences solely to processing since all products were produced from the same starting beans. Cocoa fermentation, as mentioned previously, is reliant upon multiple and highly variable physical and environmental factors, and thus fermentation conditions employed in cocoa production around the world vary tremendously.

Reported heap fermentations appear to start uniformly around pH 3.6 but our model system started slightly out of these ranges [12, 30, 31, 42–44]. Both our cool and hot fermentations concluded under more acidic conditions as well. Beans of Trinitario and Forastero varieties typically range in initial pH from 6.3-6.8, decreasing to approximately 5.0-6.0 by the end of fermentation, whereas Criollo beans, while not as widely produced or studied as the Trinitario and Forastero varieties, have been noted for their characteristically low pH [43–45]. The high initial DO values can be attributed to the fresh mixing of bean and simulated pulp media, dropping significantly after 24 h and remaining ≤ 1 mg/L for the remainder of the fermentation. This model system fermentation is liquid based, and therefore designed to mimic the conditions in the center of a well-mixed cocoa heap. FI and cut test are traditional quality controls conducted on farm to assess post-fermentation bean quality. Both are based upon anthocyanin degradation and aglycone release throughout fermentation. The FI of raw unfermented beans range from 0.3-0.6 and increase to 1.3-1.4 during fermentation, with a value of ≥ 1 indicating adequate and complete fermentation [2, 46, 47]. However, our FI values started at >1 (**Figure 5.2C**). These data, along with the acidic values for both pulp and bean in CF and HF systems, lead us to believe that these beans are of Criollo or Nacional variety. Criollo beans have low levels of anthocyanins compared to other varieties like Trinitario and Forastero, and have a naturally low pH, possibly explaining the high acidity in our fermentation systems and inconclusive FI and cut test results [45]. Nacional beans grow in Ecuador and have a very similar genetic composition with Criollo beans [45]. Traceability is often not possible in global commodity supply chains, such as that of cocoa beans. Although the exact variety of these beans is unknown, reported data from heap fermentations allowed us to make a suggested conclusion into the cultivar variation of these beans and its impact on fermentation and quality controls. Overall, these two fermentation models were generally similar in pH, DO and FI with each other, and produced results that are in agreement with the ranges reported for traditional heap fermentations.

Total polyphenol and flavanol content differed between powder and bean products, with powders having higher total concentrations of both polyphenols and flavanols. This is likely due to the removal of flavanol-free cocoa butter during processing as cocoa powder is the ground product of the pressed cake. Overall, our data align with previously published reports that fermentation and roasting significantly reduce native flavanol levels in cocoa beans [5, 13, 17,

20, 34, 48–50]. While most previous studies have investigated the implications of fermentation and roasting independently of each other, our model assess these processing techniques as consecutive steps in varying combinations. Roasting is often considered the key phase in cocoa processing in terms of defining the sensory characteristics of a finished product by producing characteristic aromas, flavors, and texture of beans. Yet, roasting is an extension of the flavanol reduction that begins during fermentation. Epimerization reactions and polymerization of flavanols to one another, as well as reaction of these compounds with larger polymeric structures such as proteins, polysaccharides, and Maillard reaction products can all influence flavonoid levels in processed cocoa [5, 51]. This is demonstrated clearly by our data through the distinction between the broad range of total polyphenol and flavanol quantification (via Folin-Ciocalteu and DMAC assays) and a more specific quantification broken down by DP (via HILIC UPLC-MS/MS). CF/UR powder has significantly lower levels of total polyphenols and flavanols than CF/CR and UF/CR powders, yet there are minimal differences between CF/UR and CF/CR across individually quantified procyanidins (DP 1-10)- likely explained by slight differences in each individual procyanidin making a large difference in total levels. One potential explanation is that roasting induces the production of complex high molecular weight compounds (DP>10) and the release of bound polyphenols, ultimately measured by Folin-Ciocalteu and DMAC assays and thus increasing total polyphenol and flavanol quantities, but not compounds quantified in our targeted analysis of individual compounds (i.e. compounds for which standards were obtained). Additionally, the significantly lower levels of all measured compounds in HF/HR demonstrate that prolonged high temperature exposure via hot fermentation followed by hot roasting suppress polyphenol and flavanol concentrations. However, the high mDP reported for both the HF/UR and HF/HR suggests that fermentation parameters may have a larger influence on polymerization of larger molecular weight compounds than originally thought, or that the synergy between fermentation and roasting at high temperatures is crucial in the development of large procyanidins. This correlates with previous research suggesting that levels of high molecular weight procyanidins increase with prolonged roasting time and high roasting temperatures [6, 20]. Although our roasting treatments were conducted at a uniform time (20 min), increased and prolonged heat exposure was most prominent in the HF/UR and HF/HR treatments and present similar results, as the mDP (excluding monomers) of these treatments

were highest of all at approximately 8 and 10, respectfully (**Figure 5.3 F**). When accounting for monomers, the overall mDP of these treatments were 4.6 and 3.7, respectively (**Figure 5.3 E**).

Large HMW dietary flavanols have poor intestinal absorption, and therefore we chose to examine inhibition of a digestive enzyme present in the lumen of the intestine such as α -glucosidase, in order to examine a mechanism of action where these compounds are likely at their highest physiological concentrations. We chose to examine α -glucosidase based on previous data suggesting that cocoa compounds exerted a greater inhibitory effect on this enzyme than on other digestive enzymes, pancreatic α -amylase and lipase [15]. Through inhibition of α -glucosidase, cocoa compounds have the potential to slow down carbohydrate digestion and subsequently slow post-prandial absorption of glucose into the bloodstream, ultimately blunting glucose spikes and decreasing gastrointestinal transit of carbohydrates. CPEs produced in this study appear to be effective dietary inhibitors of α -glucosidase, especially the CF/CR treatment. The IC_{50} value of this treatment was 62.7, or approximately 50% that of acarbose, a major finding in this study. The level of acarbose typically present in the gut is between 25-100 $\mu\text{g/mL}$ per dose. At an IC_{50} of 62.7 $\mu\text{g/mL}$, CF/CR falls within the typical acarbose range but is 2-fold more effective at inhibiting 50% of enzymatic activity. CF/CR processing parameters applied in this study are within ranges used in industrial cocoa powder production and have promising potential to surpass the activity of acarbose *in vivo*, without the negative gastrointestinal side effects that often limit acarbose usage. CF/CR was the only treatment to have a lower IC_{50} than acarbose, but all treatments have the capacity to be more effective at higher doses as all treatments had lower %A than acarbose at 500 $\mu\text{g/mL}$ (**Figure 5.7 D**). While 500 $\mu\text{g/mL}$ is approximately 5-fold higher than typical acarbose concentrations within the gut, it is still a relevant dietary dose at 6.67 g of original cocoa product or approximately 0.24 squares of baker's chocolate. At 250 $\mu\text{g/mL}$, all treatments but UF/HR and HF/HR had better inhibitory effects than acarbose, yet these treatments were not significantly different than acarbose (**Figure 5.7 E**). Although it is shown that select processing conditions improve IC_{50} values, even the harshest of conditions have approximately the same or similar inhibitory activity compared to UF/UR (raw beans). UF/UR was not the best inhibitor nor was HF/HR far worse than all other treatments, suggesting that, in this particular instance, processing at worst doesn't negatively affect activity and at best can actually greatly enhance inhibitory activity and that the paradigm of less processing equating to better health benefit is not upheld by our data.

Furthermore, it is important to distinguish that these conclusions were made from the assessment of powder extracts. When assessing the soluble digesta from each cocoa powder treatment (more representative of a cocoa food than a cocoa extract supplement), the inhibitory effect of each digesta was much lower than that of the corresponding CPE, yet all still managed to reduce inhibition to 50% (**Figure 5.7 B**). These soluble digesta fractions were used simply to confirm that analyzing the enzyme inhibitory effects of CPE had physiological relevance to cocoa powder consumption. Although IC_{50} values could not be calculated from this data, it is visually apparent that digestive release, stability and solubility can be influential factors on the inhibitory effects of cocoa. Further work is needed to identify the bioactive components of each soluble digesta fraction but it is clear that the process of digestion merits consideration when evaluating how cocoa inhibits α -glucosidase activity.

To determine whether measured concentrations of cocoa compounds were associated with inhibitory activity, we employed a simple linear regression approach, similar to our previous studies [15, 52]. **Figure 5.8** illustrate correlations between enzyme inhibition (IC_{50}) and concentrations of total polyphenols, total flavanols, individual procyanidins, mDP, and the LMW/HMW fractions of early, intermediate, and late MRP. A strong negative correlation would indicate decreasing enzyme activity (increasing inhibition) with increasing compound concentration or increasing mDP and a positive correlation would indicate the exact opposite-increasing enzyme activity (decreasing inhibition) with increasing compound concentration or mDP. Of all compositional measures, the only strong correlation seen was between IC_{50} and the overall flavanol mDP, with decreasing IC_{50} as mDP increased. The lack of correlations for most measures in **Figure 5.8** align with previous work demonstrating that although processing induced significant losses in total polyphenols and total flavanols, these compositional changes did not uniformly influence bioactivity, but rather increasing mDP had a stronger influence on cocoa bioactivity [15, 28, 53, 54]. This finding provides strong evidence suggesting that cocoa processing could be tailored specifically to promote flavanol polymerization as a means to enhance α -glucosidase activity. On the other hand, a slightly strong positive correlation was observed between IC_{50} and intermediate MRP quantified in the HMW fraction, indicating that as concentration of these large complex compounds increase, the ability of CPE to inhibit α -glucosidase declines. The quantification of these compounds is a relatively new area with limited understanding of structure and activity. Through our results we can preliminarily suggest that

longer and higher roasting times/temperatures, often resulting in increased production of these MRP, negatively impact the α -glucosidase inhibitory activity of CPE, but further investigation into these compounds is needed to fully elucidate the impact they have on specific digestive enzymes.

This study is novel in its use of a single uniform batch of raw cocoa beans as the starting material for all processing treatments followed by control and monitoring of fermentation, roasting and all other downstream processing conditions. This approach provided us with direct knowledge of how the cocoa powders we evaluated were produced. Furthermore, we were able to modify the fermentation and roasting conditions to produce seven cocoa powders made from the same starting material, but subject to different processing conditions. Previous studies have often relied on information reported through various levels of the cocoa supply chain, often resulting in unknowns regarding processing conditions, as most cocoa production processes, especially fermentation, lack robust controls or recordkeeping, resulting in considerable variation and poor traceability. Our controlled system eliminates many of these external challenges, providing confidence that differences between the cocoa powders evaluated were due to the fermentation and roasting treatments, rather than unknown factors throughout the supply chain. While the model fermentation system used in our study is not designed to physically mimic conditions found in on-farm cocoa fermentation, fermentation of cocoa beans using this system results in biochemical changes analogous to those reported in on farm fermentation. Conducting the fermentation step in this model system allowed us to produce cocoa powders with acceptable chemical composition, that were subject to known and controlled fermentation conditions. We are currently expanding on this research by investigating each cocoa powder's ability to prevent obesity-induced GI and systemic inflammation and gut barrier dysfunction *in vivo*.

This study is not without limitations. Quantifying individual procyanidins ranging from DP 1-10, although expanding beyond the monomeric flavan-3-ols often focused on in cocoa products, still leaves many large molecular weight compounds yet to be quantified individually. Additionally, α -glucosidase inhibition is just one specific mode of bioactivity that we chose to focus on, based on potential for this inhibition demonstrated in previous reports. Although our results begin to expand on this powerful inhibitory effect, the exact compositional factors involved remain to be elucidated. To address these limitations moving forward, our processing parameters could be expanded to include a wider range of processing conditions, to further

optimize α -glucosidase inhibitory activity. This expansion of treatment conditions tested, as well as further fractionation of powder extracts to identify specific components associated with α -glucosidase inhibitory activity, would allow a more comprehensive understanding of the impact each processing step has on various compositional factors and bioactivity of dietary cocoa. By extending characterization to lignins and speciation of melanoidins, further evidence could be provided to explain this enzymatic activity. The *in vitro* work also needs to be extended *in vivo* to further reinforce and clarify the mechanisms behind cocoa's enzymatic inhibition influence in both animals and humans, including but not limited to maltose versus glucose tolerance tests with cocoa consumption, diet-induced obesity, and glucose intolerance. Furthermore, yeast-derived α -glucosidase is a good, inexpensive starting point to screen for α -glucosidase inhibitory activity *in vitro*. However, moving forward, work to understand specific mechanisms of α -glucosidase inhibition by cocoa will need to move into mammalian systems such as rat intestinal powders and murine and/or human recombinant α -glucosidases [55].

5.5 CONCLUSION

Overall, the present study demonstrates that the components of processed cocoa powders are promising inhibitors of α -glucosidase, despite a significant reduction in native flavanol composition during fermentation and roasting, and that fermentation and roasting conditions influence the inhibitory activity. These observations support our hypothesis that reductions in native polyphenols and flavanols do not necessarily dictate a reduction in activity, and furthermore that products of fermentation and roasting do in fact contribute to cocoa bioactivity. Although many of the compositional factors quantified in this study lack strong correlation with enzyme inhibition (IC_{50}), we report the novel finding that α -glucosidase inhibitory activity increases with increasing mDP. Further investigation is needed to determine the identity of compounds that better correlate with this activity.

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CHAPTER 6. CONCLUSIONS AND FUTURE WORK

The overall goal of the work was to establish a relationship between cocoa processing techniques and health protective activities of dietary cocoa, specifically the α -glucosidase inhibitory activity. In order to achieve this goal, a rapid and sensitive method of detection for cocoa procyanidins was developed (Chapter 3), a fermentation model system was scaled up to produce controlled cocoa beans on a large scale (Chapter 4), and finally, this model system and further processing was utilized to produce various controlled treatments of cocoa powder and determine the bioactive properties of each (Chapter 5). The data presented in this work and previously cited work shows exciting and promising potential for the use of fermented and roasted cocoa as a prevention strategy and/or method to control T2D and obesity-induced chronic conditions. Although our results have promise, there is still a need for continued investigation and development of processing steps that maintain or enhance bioactivity while preserving desirable sensory characteristics, as the concept of processed cocoa enhancing bioactivity is relatively unexplored.

To build upon the results presented in this work, a long-term research goal could be to characterize and understand the structural composition and health protecting activities of melanoidins and high molecular weight compounds, produced through thermal processing, and ultimately optimize cocoa processing conditions to produce cocoa with maximum activity. To achieve this goal, future work will have to overcome many limitations. While we observed powerful inhibitory effects of processed cocoa powders, the specific compounds and mechanisms driving these activities is still largely unknown. Additionally, the variety of beans used to produce cocoa powders of 7 different treatments was unknown. In the future it would be valuable to look at different bean varieties from various growing regions to determine how these factors play into the implications of processing (fermentation and roasting) and bioactivity. Processing conditions can also be expanded upon to include a more focused range of optimal conditions and techniques. Beneficial studies to perform in the future would be to expand this *in vitro* work *in vivo* to begin to elucidate the mechanisms of various cocoa compounds that exhibit health protective activities. Extracts of controlled processed cocoas could be fractionated into low, intermediate, and high molecular weight MR products and melanoidins and used *in vitro* and *in vivo* to determine the enzyme inhibiting potential and ultimately the behavior of these fractions

in the GI track. Utilization of MALDI-TOF and NMR techniques could assist in characterizing these various fractions and determining structural characteristics.

The research conducted for this thesis begins to delve into the relationship between cocoa processing and bioactivity, as well as identifying and developing various strategies to quantify and preliminarily characterize large complex cocoa compounds. This work continues to challenge the widely accepted assumption that degradation of native cocoa polyphenols subsequently results in a decrease in overall bioactivity. The results from these data directly contradict this assumption and begin to focus on the newly discovered concept that cocoa processing may in fact enhance bioactivity.

APPENDIX A: SUPPLEMENTARY INFORMATION FOR CHAPTER 5

A1. SUPPLEMENTARY MATERIALS AND METHODS

Polyphenol extraction and quantification: Randomly selected whole cocoa beans (30 g) were frozen with liquid nitrogen and ground into powder. Cocoa powders (40 g, from pressing or from ground beans) were mixed with 150 mL hexane and sonicated (10 min, 22°C), centrifuged for (5 min, 5000 × g), supernatant discarded, and then repeated. Once defatted, the powder was dried at room temperature. Once dry, defatted powder was mixed with 150 mL of extraction solution (70:28:2 acetone, water, acetic acid v/v/v), sonicated (10 min, 22°C), and centrifuged for (5 min, 5000 × g). The supernatant was collected and this procedure was repeated three more times for a total volume of 600 mL. All collected supernatant was pooled and placed under vacuum on a rotary evaporator at 40°C until all acetone evaporated. The resulting cocoa extract was frozen at –80°C, freeze dried, and the final extract was weighed to calculate extract yield. The freeze dried extract was stored at –80°C until further analysis.

Folin-Ciocalteu colorimetric assay: Cocoa extracts ($n=3$) were diluted with 40% EtOH to a final concentration of 0.2 mg/mL. In a 96-well plate, each solution (5 µL) was mixed with MQ water (45 µL) and 0.2 N Folin-Ciocalteu reagent (125 µL). 100 µL sodium carbonate solution (7.5% v/v) was added to the samples and mixed. The plate was incubated for 2 h at room temperature and the absorbance read at 765 nm. Samples were compared to gallic acid standard curves ($n=2$). Total polyphenol concentrations were expressed as mg Gallic Acid Equivalents (GAE)/g cocoa bean.

4-dimethylaminocinnamaldehyde (DMAC) colorimetric assay: DMAC solution was prepared by combining 3.0 mL stock HCl with 27 mL EtOH and chilling at 4°C for 15 min, 0.03 g DMAC was added to the solution and mixed well. Cocoa extracts were diluted with EtOH to a final concentration of 100 ppm. Standard curve ($n=2$) was prepared by diluting procyanidin B2 with 1:1 EtOH:water to concentrations of 1, 10, 50, and 100 ppm. In a 96-well plate, each diluted cocoa extract, PCB2 standard (1, 10, 50, 100 ppm), and EtOH blank (50 µL) was mixed with 250 µL of DMAC solution. Absorbance was read at 640 nm.

Thiolysis: Cocoa extracts were diluted with MeOH to 0.5 mg/mL and then mixed (50 μ L) with 50 μ L HCl (3.3%, water) and 100 μ L benzyl mercaptan (5%, MeOH). Samples were placed in a 90°C water bath for 5 min and then cooled on ice for 5 min. Unthiolized controls were prepared with cocoa extract and MeOH without heating in the water bath. Each thiolized sample (100 μ L) was combined with 900 μ L of 0.1% formic acid in water and 0.1% formic acid in ACN (95:5 v/v). Samples were analyzed on a Waters Acquity H-Class separations module with an Acquity UPLC HSS T3 column (2.1 mm \times 100 mm, 1.8 μ m) at 40°C. Binary gradient elution was performed using 0.1% formic acid in water (Phase A) and 0.1% formic acid in ACN (Phase B). Solvent flow rate was 0.6 mL/min and the linear gradient elution was as followed: 95% A (0-0.5 min), 65% A (6.5 min), 20% A (7.5-8.6 min), 95% A (8.7-10.5). (–)-electrospray ionization (ESI) together with tandem mass spectrometry (MS/MS) was used to analyze UPLC effluent on a Waters Acquity triple quadrupole (TQD) MS. (–) mode electrospray ionization (ESI) was performed with capillary, cone, and extractor voltages of –4.24 kV, 30.0 V, and 3.0 V respectively. Source temperature was 150°C and desolvation temperature was 400°C/ Cone gas flowed at a rate of 75 L/h and desolvation gas at 900 L/h. Argon (0.25 mL/min) was used as the collision gas in MS/MS. Multi-reaction monitoring (MRM) with a mass span of 0.2 Da was performed on parent ions and collision-induced dissociation (CID) on daughter ions. Inter-channel delays and interscan time was 1.0 s each. Additional calculations were done to account for the native monomers and were reported as DP of total flavanols. mDP oligomers and polymers and mDP of total flavanols were calculated as follows:

$$mDP (O + P) = \frac{\text{net number of monomers} + \text{net number of thiolytic derivatives}}{\text{net number of monomers}}$$

$$mDP (\text{total flavanols}) = \frac{\text{total monomers} + \text{net number of thiolytic derivatives}}{\text{total monomers}}$$

HILIC UPLC-MS/MS: A Waters Acquity H-class separation module equipped with an Acquity Torus DIOL column (2.1 mm \times 100 mm, 1.7 μ L, 45°C) and Torus DIOL VanGuard Pre-column (2.1 mm \times 5 mm, 1.7 μ L) was used to perform the analysis. Binary gradient elution was performed with 2% acetic acid in acetonitrile (phase A) and 3% water and 2% acetic acid in methanol (phase B). Solvent flow rate was 0.8 mL/min and the linear gradient elution was

carried out as followed: 100% A (0 min), 55% A (5.7 min), 5% A (6.0 min), 100% A (6.7-9.0 min). (-) mode ESI coupled to tandem mass spectrometry (MS/MS) on a Waters Acquity triple quadrupole (TQD) MS was used to analyze the UPLC-eluent. Ammonium formate (0.04 M in water, 5 μ L/min) was added to the eluent flow stream post-column to enhance ionization of the high molecular weight compounds. Ionization settings were as follows (-) mode, capillary voltage: -4.5 kV, cone voltage: 60.0 V, extractor voltage: 1.0 V, source temperature: 150°C, and desolvation temperature: 500°C. N₂ was used for cone and desolvation gasses with flow rates of 50 and 1000 L/h respectively. For MS/MS, Ar was used as a collision gas with 0.1 mL/min flow rate. Parent ions and signature daughter ions followed by collision-induced dissociation (CID) were subjected to multi-reaction monitoring (MRM) with a mass span of 0.2 Da and 1.0 sec of inter-channel delays and inter-scan times. A calibration curve for standards DP 1-9 were prepared and analyzed with dilutions ranging from 6.93×10^{-7} – 0.091 mg/mL. MRM settings for each compound are listed in **Table A1**. MassLynx software (version 4.1, Waters) was used to acquire data.

Preliminary melanoidin dialysis: A polyphenol-rich cocoa extract was prepared by our standard method of defatting 2X with hexane and extracting a minimum of 3X (or until the supernatant has no color) using an extraction solvent of acetone, water, and acetic acid (70:28:2 v/v/v). Pooled extracts were dried by rotary evaporation to remove acetone and then freeze dried to remove water. The dialysis method proposed by Sacchetti et al [1] was followed with modifications. Cocoa extract was re-dissolved in extraction solvent to a final concentration of 40 mg/mL. Dialysis was performed in triplicate using acidified MeOH:water (60:40 v/v, 0.1% formic acid). For each replicate, 10 mL of 40 mg/mL cocoa extract was placed inside approximately 30 cm of presoaked dialysis tubing (3.5-5.0 kDa MW cutoff, Spectrum Spectra/Por Biotech-Grade RC Dialysis, Fisher) and clipped closed. The tubing was submerged in 1L of dialysis solvent and stirred at 4°C for 24 h. After 24 h, the remaining cocoa extract constituents within the dialysis tubing was transferred into a new presoaked tube (8.0-10.0 kDa MW cutoff) and clipped closed. This tubing was placed into a new 1 L beaker of fresh dialysis solvent and stirred at 4°C for 24 h. This sequence was repeated with MW cutoff of 20 kDa and 50 kDa. Dialysis beakers were continually sparged with nitrogen throughout the 24 h period. Samples of the acidified MeOH:water were taken after every 24 h period and the cocoa extract

remaining within the dialysis tubing was collected upon completion, and all samples were frozen at -80°C until analysis.

To selectively quantify MRP, each dialysate ($<3.5\text{-}5\text{ kDa}$, $<8\text{-}10\text{ kDa}$, $<20\text{ kDa}$, $<50\text{ kDa}$) was diluted 10-fold with $0.05\text{ H}_2\text{SO}_4$. The non-dialyzable cocoa extract ($>50\text{ kDa}$) was diluted 10-fold with $0.5\text{ M H}_2\text{SO}_4$ and then further diluted with $0.05\text{ M H}_2\text{SO}_4$ until the solution was colorless. The starting cocoa extract (40 mg/mL) was diluted 10-fold with $0.5\text{ M H}_2\text{SO}_4$ and then further diluted with $0.05\text{ M H}_2\text{SO}_4$ until the solution was colorless. A standard curve was prepared with quinine sulfate dissolved in $0.05\text{ M H}_2\text{SO}_4$ ($100\text{-}0.1\text{ ppm}$). Each diluted dialysate, diluted non-dialyzable cocoa extract, diluted starting cocoa extract, and standard was transferred ($300\text{ }\mu\text{L}$) into a UV-Star 96-well plate. The absorbance was read at 280 , 360 , and 420 nm and early, intermediate, and late MRP were reported as absolute absorbance values in **Table A2**.

Three stage in vitro digestion: In order to determine digestively stable and soluble compounds (i.e. diffusible across the unstirred water layer), cocoa powders from all treatments were digested *in vitro* in three phases (oral, gastric, and intestinal) protocol as described by Li *et al* [2] with modifications. Oral phase base solution was prepared the week of analysis by combination of water (1L) with potassium chloride (1.792 g), sodium phosphate (1.776 g), sodium sulfate (1.140 g), sodium chloride (0.596 g), and sodium bicarbonate (3.388 g). Gastric and small intestinal phase solutions were prepared the day of analysis, as follows: pancreatin-lipase solution was prepared by mixing 10 mg/mL pancreatin (100 mM sodium bicarbonate) and 5 mg/mL lipase (100 mM sodium bicarbonate), bile solution was prepared by dissolving bile extract in 100 mM sodium bicarbonate to a final concentration of 40 mg/mL , and pepsin was dissolved in 0.1M HCl to a final concentration of 40 mg/mL .

Each cocoa powder (10.0 g) was digested in a 500 mL reaction bottle. Oral phase began by adding 60 mL of oral phase base solution to a beaker, followed by the addition of urea (0.4 mg/mL base solution), uric acid (0.03 mg/mL base solution), α -amylase (10.6 mg/mL base solution), and mucin (0.05 mg/mL base solution), and mixing for approximately 15 min . This solution (60 mL) was then added to the reaction bottle, blanketed with nitrogen gas, and incubated in a shaking water bath (37°C , 100 rpm) for 10 min . The reaction bottle was removed after the incubation period and placed immediately on ice to begin the gastric phase. The volume was brought to 300 mL with saline solution and the pH adjusted to 2.5 ± 0.1 using 1.0 N HCl .

Pepsin solution (20 mL) was then gently added to the reaction bottle, volume corrected to 400 mL with saline solution, blanketed with nitrogen gas, and incubated in a shaking water bath (37°C, 100 rpm) for 1 h. The reaction bottle was removed after the incubation period and placed again on ice to begin the intestinal phase. pH of the solution was adjusted to 6.0 ± 0.1 with 1 N NaOH. Pancreatin-lipase solution (20 mL) and bile solution (30 mL) was added to the reaction bottle and then pH adjusted again to 6.0 ± 0.1 . The solution was then volume corrected to 500 mL with saline solution, blanketed with nitrogen gas, and incubated in a shaking water bath (37°C, 100 rpm) for 2 h. Following the 2 h incubation period, the solution was divided into 2 250 mL solutions- one was immediately frozen at -80°C (total digesta) and the second solution was centrifuged for 10 min at 37°C , the supernatant was collected, and then frozen at -80°C (solution digesta). Both fractions were freeze dried and yields were calculated.

A2. SUPPLEMENTARY RESULTS

Preliminary melanoidins dialysis: Early, intermediate, and late MRP of cocoa extract were identified from LMW (<3.5-5 kDa, <8-10 kDa, <20 kDa, <50 kDa) and HMW (>50 kDa) fractions. The majority of these MRP were eluted from the 3.5-5 and 8-10 kDa membranes, followed by minimal compounds in 20 kDa, and increasing amounts of early, intermediate and late MRP eluted from the 50 kDa membrane. Additionally, the non-dialyzable HMW cocoa extract (>50 kDa) had significant levels of compounds detected, suggesting that a large quantity of MRP compounds within roasted cocoa are extremely large and warrant further investigation into their identification and quantification.

Table A1. MS/MS settings for MRM detection of monomer-decamer flavanols

Compound	t_R^a (min)	MW (g mol⁻¹)	[M – H]^{-b} (m/z)	Daughter Ion (m/z)
Monomer	0.61	290.27	289.03	245.06
Epigallocatechin	0.74	458.37	305.04	124.98
Dimer	2.03	578.52	577.14	425.10
Trimer	3.05	866.77	865.22	287.07
Tetramer	3.73	1155.02	576.40	125.02
Pentamer	4.26	1443.28	720.41	125.02
Hexamer	4.66	1731.53	864.52	125.02
Heptamer	5.00	2017.81	1008.40	125.17
Octamer	5.28	2308.03	1152.58	125.17
Nonamer	5.53	2596.54	864.12	125.17
Decamer	5.75	2884.54	960.18	125.17

^aretention time

^bAll MRMs used singly-charge parent ions except for pentamer, hexamer, heptamer, and octamer, which are double-charged ([M – 2H]²⁻), and nonmaer and decamer, which are triple-charged ([M – 3H]³⁻)

Table A2. Preliminary melanoidin identification

Fraction	Early MRP^a (280 nm)	Intermediate MRP^a (360 nm)	Late MRP^a (420 nm)
<3.5-5 kDa	2.295	0.11	0.052
<8-10 kDa	0.162	0.046	0.038
<20 kDa	0.106	0.043	0.037
<50 kDa	0.401	0.064	0.05
>50 kDa	2.922	0.455	0.327
Starting extract	3.711	0.287	0.152

^aValues are reported as absolute absorbance



Figure A1. Progression of one cool fermentation batch from 0 h-168 h, followed by bean oven drying. Fermentation started at 25°C and concluded at 46°C, increasing 3.5°C/24 h. Note the large production of CO₂ bubbles at 48-72 h of fermentation.

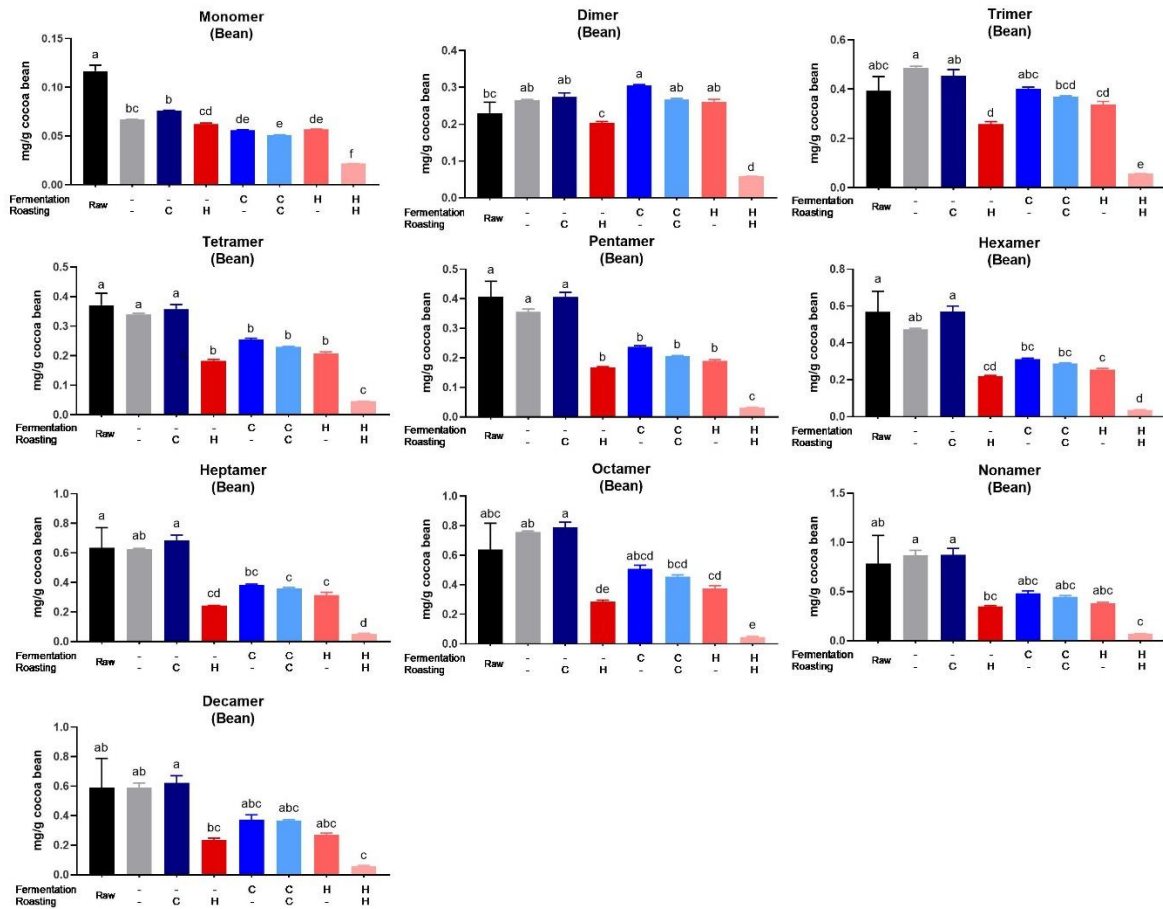


Figure A2. Levels of individual procyanidin compounds in cocoa beans, as quantified by HILIC UPLC-MS/MS. Raw bean indicates the extract prepared from the cocoa beans as received from the supplier and is different from UF/UR (-/-) as these beans were rehydrated and dried. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

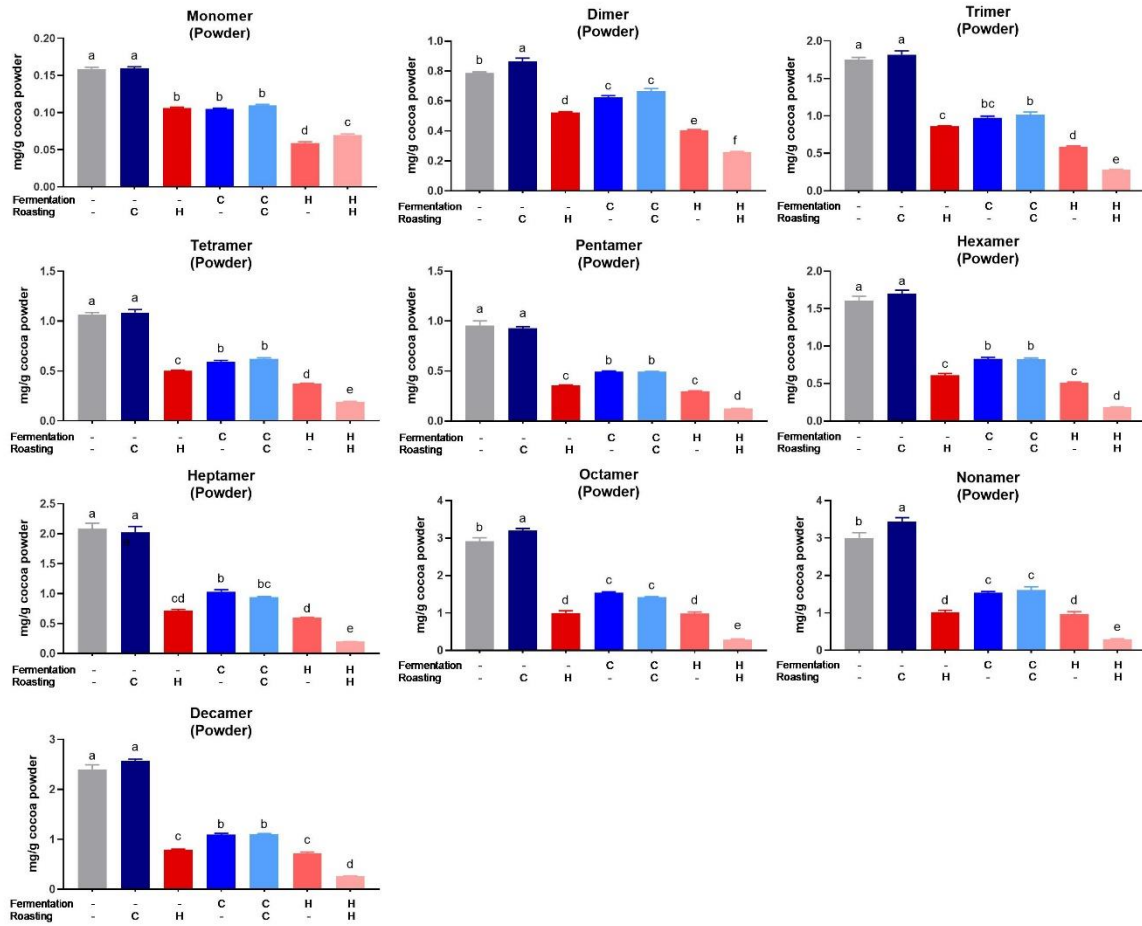


Figure A3. Levels of individual procyanidin compounds in cocoa powders, as quantified by HILIC UPLC-MS/MS. All values are presented as the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values.

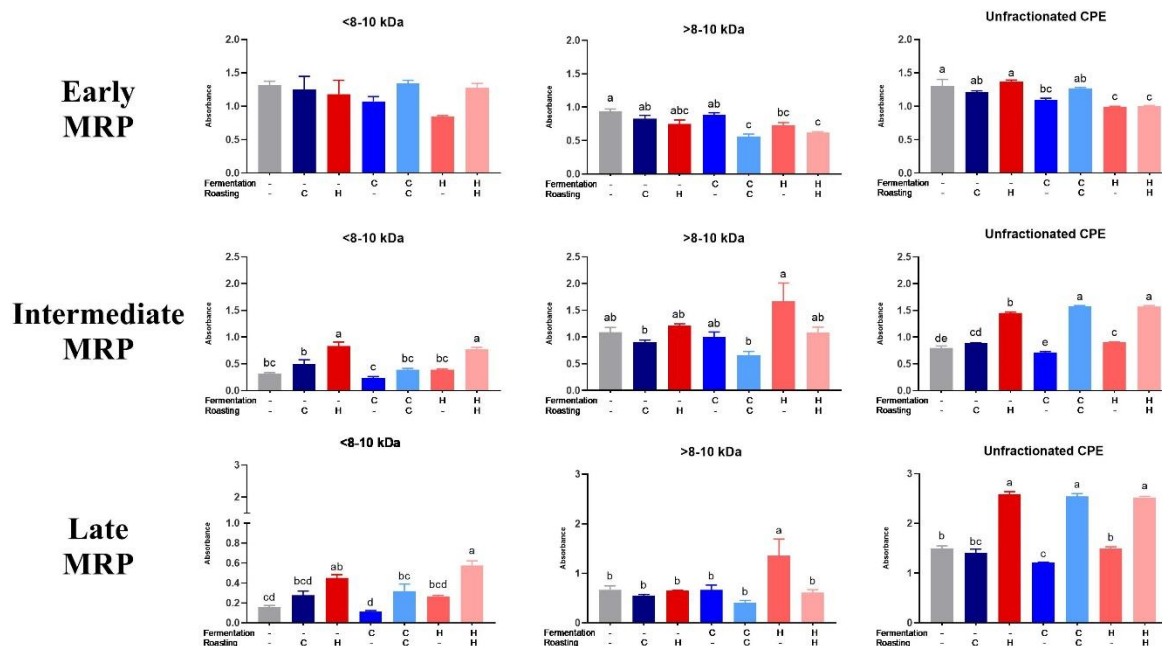


Figure A4. Analysis of LMW and HMW CPE fractions and the starting 40 mg/mL CPE for early, intermediate, and late MRP. Early MRP were quantified at 0.15625 mg/mL at 280 nm, intermediate MRP were quantified at 2.5 mg/mL at 360 nm, and late MRP were quantified at 5 mg/mL (<8-10 kDa), 2.5 mg/mL (>8-10 kDa), and 10 mg/mL (unfractionated CPE) at 420. Note that absolute absorbance of these compounds is reported, but this absorbance is relative to concentration. Each bar represents the mean \pm SEM. Significance between treatments was determined by one-way ANOVA and Tukey's HSD post-hoc test ($p < 0.05$). Treatments with different letters are significantly different within values. No letters indicate no statistical difference within values.

APPENDIX B: COPYRIGHT RELEASE

Chapter 3: Development of a Rapid HILIC UPLC-MS/MS Method for Procyanidins with Enhanced Ionization Efficiency

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Title: Development of a rapid ultra performance hydrophilic interaction liquid chromatography tandem mass spectrometry method for procyanidins with enhanced ionization efficiency

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Chapter 4: Development and Characterization of a Pilot-Scale Model Cocoa Fermentation System Suitable for Studying the Impact of Fermentation on Putative Bioactive Compounds and Bioactivity of Cocoa

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