

**FINE COAL DEWATERING**

by

Gul Bahar Basim

Thesis submitted to the Faculty of the  
Virginia Polytechnic Institute and State University  
in partial fulfillment of the requirements for the degree of

Master of Science

in

Mining and Minerals Engineering

Approved by

Roe-Hoan Yoon, Chair  
Gregory T. Adel  
Gerald H. Lutrell  
Cesar I. Basilio

December 5, 1997  
Blacksburg, Virginia

Keywords: coal, vacuum filtration, centrifugation

Copyright 1997, Gul Bahar Basim

## **FINE COAL DEWATERING**

Gul Bahar Basim

(ABSTRACT)

Fine coal constitutes a relatively small portion of a product stream in a coal cleaning plant. However, its processing cost is approximately three times higher than the cost of processing coarse coal. Therefore, many coal companies chose to discard the fines to refuse ponds, causing a loss of profit and creating environmental concerns. This problem can be solved by developing more efficient fine coal dewatering processes, since bulk of the cost associated with processing fine coal is due to dewatering. For this reason, Virginia Tech has developed new chemicals that can increase the efficiency of mechanically dewatering coal fines.

To determine the performance of the novel reagents on fine coal dewatering, laboratory vacuum filtration and centrifugation tests were conducted. The utilization of the novel dewatering aids in the dewatering systems decreased the final moisture contents of the filter cakes to sufficiently low values. There was approximately 50% reduction in the cake moisture of many coal samples with the usage of the novel dewatering aids. The tests were performed on various coal samples from different coal preparation plants. This gave the advantage of testing the novel dewatering aids at many different conditions since each sample had its own characteristics.

The vacuum filtration tests were extensively used to compare the efficiency of each novel reagent in dewatering. The best performing dewatering aids were determined and they were further utilized to analyze the effects of operational variables, such as; drying cycle time, cake thickness, vacuum pressure level and slurry temperature on dewatering. A statistical analysis was also performed to observe the effect of each factor quantitatively. The analyses were very useful in terms of determining the synergistic effects of these factors in dewatering of fine coal.

The centrifuge tests were conducted to examine the efficiency of the novel reagents in a different dewatering application. The experimental results showed a significant improvement in centrifuge dewatering with the usage of proper coal sample. The moisture contents of fairly thick cakes decreased down to 5-10%. This outcome was very satisfactory since most of the

dewatering aids commonly used in the coal industry were observed to increase the final cake moisture in centrifuge dewatering instead of decreasing it.

Finally, surface chemistry analyses were performed on the coal samples and slurries to analyze the changes in the chemistry of the dewatering system in the presence of the novel dewatering aids. It was observed that there was a favorable improvement in the system chemistry, which was helpful in terms of decreasing the cake moisture content. These observations were also consistent with the results of the dewatering tests. The combined effect of the novel additives in decreasing the surface tension of the slurry and increasing the contact angle of the coal surface at the same time was concluded to be the reason for their significant performance as dewatering aids.

## ACKNOWLEDGMENTS

The author would like to extend her gratitude and appreciation to Dr. Roe-Hoan Yoon for his guidance and support throughout the course of this study. She also would like to thank Dr. Cesar Basilio for teaching her the fundamentals of the dewatering project and sharing his knowledge during her research studies and Dr. Gregory T. Adel and Dr. Gerald H. Luttrell for their advice during the progression of this project.

The author would like to thank to Bird Machine Company for their assistance to perform the centrifuge tests. Special thanks to her colleagues Subramanian Vivek, Neeraj Mendiratta, Rajesh Pazhianur, Zhuo Chen and Eric Yan for their friendship, assistance and valuable discussions.

Finally, the author would like to convey her deepest thanks to her parents and her husband for their invaluable support, patience, encouragement and special love that made this study possible.

## TABLE OF CONTENTS

	Page
TITLE PAGE.....	i
ABSTRACT.....	ii
ACKNOWLEDGMENTS.....	iv
TABLE OF CONTENTS.....	v
LIST OF FIGURES.....	vii
LIST OF TABLES.....	xi
1. INTRODUCTION.....	1
1.1. Background.....	1
1.2. Literature Review.....	2
1.2.1. Dewatering of Coal.....	2
1.2.1.1. Water in Coal and Filter Cake Structure.....	2
Nature of Coal Surfaces.....	2
Water in Coal.....	7
Filter cake Formation and Water in cake Structure.....	8
1.2.1.2. Surface Chemistry of Coal Dewatering.....	16
Adsorption on the Coal Surface.....	16
Capillary Theory of Dewatering.....	20
Surface Tension Lowering.....	22
Change in Hydrophobicity.....	23
Flocculation Effect.....	26
1.2.1.3. Dewatering Kinetics.....	28
1.2.2. Dewatering Techniques.....	34
1.2.2.1. Vacuum Filtration.....	34
1.2.2.2. Centrifugation.....	35
1.3. Objectives.....	37
1.4. Organization.....	38
2. VACUUM FILTRATION ANALYSES.....	39
2.1. Introduction.....	39
2.2. Sample Collection.....	40
2.3. Dewatering Reagents.....	40

2.4. Laboratory Vacuum Filtration Tests.....	40
2.4.1. Experimental Set-up.....	40
Apparatus.....	40
Procedure.....	41
2.4.2. Vacuum Filtration Tests Results and Discussions.....	42
2.4.3. Statistical Analysis.....	60
2.5. Conclusions.....	67
3. CENTRIFUGE TESTS.....	71
3.1. Introduction.....	71
3.2. Experimental Methods and Materials.....	71
3.3. Results and Discussions.....	74
3.4. Conclusions.....	85
4. SURFACE CHEMISTRY ANALYSES.....	87
4.1. Introduction.....	87
4.2. Experimental Methods and Materials.....	87
4.3. Results and Discussion of Surface Analysis.....	90
4.4. Conclusions.....	98
5. CONCLUSIONS.....	99
REFERENCES.....	100
APPENDIX I. STATISTICAL ANALYSES EXPERIMENTAL RESULTS.....	104
VITA.....	105

## LIST OF FIGURES

	Page
Figure 1.1. Estimated coal dewatering costs at different particles sizes (Couch, 1991).....	1
Figure 1.2. The typical pore types found on the surfaces (Porous Materials Inc, 1997).....	4
Figure 1.3. Functional groups in coal (Whitehurst, 1978).....	5
Figure 1.4. Schematic representation of possible portion of coal surface (Oven, 1988).....	5
Figure 1.5. Water associated with coal (Gala, 1989).....	7
Figure 1.6. Operating scheme of a filtration process (Cheremisinoff and Azbel, 1983).....	9
Figure 1.7. Postulated interaction between the cake particulates and the filter media (Willis, 1986).....	9
Figure 1.8. The three possible equilibrium conditions of a fluid in a filter cake (Phillips and Thomas, 1955).....	12
Figure 1.9. Generalized pressure/moisture relationship for cake filtration (Veal at al., 1995).....	13
Figure 1.10. Equilibrium state between pressure gradient and capillary forces for pore moisture in a cake (Cheremisinoff and Azbel, 1983).....	14
Figure 1.11. Distribution of pore-bonded moisture in different zones (Cheremisinoff and Azbel, 1983).....	15
Figure 1.12. Illustration of the electrical double layer (Stelma, 1978).....	17
Figure 1.13. The electrical double layer variation of the potential with distance, showing the inner and outer Helmholtz planes (Stelma, 1978).....	18
Figure 1.14. Adsorbed surfactant orientation as a function of total surface coverage (Myers, 1988).....	19
Figure 1.15. Capillary rise and interfacial tensions at the point of three phase contact in a capillary (Stelma, 1978).....	20
Figure 1.16. Schematic representation of surface charge reversal due to bilayer adsorption of the oppositely charged surfactant molecules (Myers,1988).....	24
Figure 1.17. Moisture retention between non-wetting particles, (a) low contact angle, (b) high contact angle (Veal et al, 1995).....	25
Figure 1.18. Effect of diameter on inhibition and two-phase flow in capillary tubes (Brownell and Katz, 1947).....	31
Figure 1.19. Bird countercurrent flow Solid Bowl Decanter Centrifuge.....	36

Figure 1.20.	Bird Screen Bowl Centrifuge.....	37
Figure 2.1.	Experimental setup for laboratory vacuum filtration tests.....	41
Figure 2.2.	Results of the filtration tests conducted on the floated coal sample slurry (100 x 0) from the Middle Fork coal preparation plant as a function of the reagent dosage (EGMO, PMHS).....	43
Figure 2.3.	Results of the filtration tests conducted on the floatation products (100 mesh x 0) from the Middle Fork coal preparation plant as a function of the slurry pH with and without the dewatering aid (1.25 lbs/ton of EGMO).....	44
Figure 2.4.	Results of the filtration tests conducted on the floatation products (100 mesh x 0) from the Middle Fork coal preparation plant as a function of the applied vacuum with and without the dewatering aid (1.25 lbs/ton of EGMO).....	45
Figure 2.5.	Effects of drying cycle time on the cake moisture. Filtration tests were conducted on a Microcel flotation product from the Middle Fork coal preparation plant with and without dewatering aid (1.25 lbs/ton of EGMO).....	46
Figure 2.6.	Effects of drying cycle time on cake moisture content as a function of the reagent dosage (EGMO). Filtration tests were conducted on Middle Fork coal sample (100 mesh x 0).....	47
Figure 2.7.	Effects of the change in cake thickness on cake moisture content. Filtration tests were conducted on the flotation products (100 mesh x 0) obtained from the Middle Fork preparation plant with and without dewatering aid (1.25 lbs/ton of EGMO).....	48
Figure 2.8.	Results of the filtration tests conducted on the flotation products from the Middle Fork coal preparation plant as a function of reagent dosage (EGMO).....	49
Figure 2.9.	Effect of the conditioning method and time on moisture content at the varying dosages of EGMO.....	51
Figure 2.10.	Results of the filtration tests conducted on the flotation products (28 mesh x 0) from Elkview Mining Company as a function of reagent dosage (EGMO).....	53
Figure 2.11.	Results of filtration tests conducted on the flotation product of BMCH Australian coal sample as a function of reagent dosage (EGMO) at ambient and elevated temperatures and different cake thicknesses.....	55



Figure 2.12.	Effects on flotation on reduction of the moisture content of the filter cake. Filtration tests were conducted on the flotation product of Elkview run of mine coal sample as a function of reagent dosage (EGMO) on floated and non-floated sample slurries.....	56
Figure 2.13.	Effect of particle size distribution on moisture content reduction of the filter cakes. Figure 13-a shows the particle size distribution of the sample after different periods of grinding. Figure 13-b represents the results of the filtration tests on these samples.....	57
Figure 2.14.	Results of filtration experiments conducted on Middle Fork coal sample as a function of EGMO, Magnafloc 1011 & starch dosage.....	59
Figure 2.15.	The outlier values for the linear model.....	61
Figure 2.16.	Change in the moisture content of the BMCH Australian coal sample as a function of the dosage of the dewatering aid (EGMO) and volume of the sample slurry. The plots were taken for 22°C slurry temperature and drying cycle times of 1minute (a) and 5 minutes (b).....	63
Figure 2.17.	Change in the moisture content of the BMCH Australian coal sample as a function of the dosage of the dewatering aid (EGMO) and volume of the sample slurry. The plots were taken for 60°C slurry temperature and drying cycle times of 1minute (a) and 5 minutes (b).....	65
Figure 2.18.	Change in the moisture content of the BMCH Australian coal sample as a function of the dosage of the dewatering aid (EGMO) and drying cycle time. The plots were taken for 100-ml slurry volume and slurry temperatures of 22°C (a) and 60°C (b).....	66
Figure 3.1.	Lab-scale solid bowl centrifuge unit.....	72
Figure 3.2.	Lab-scale screen bowl centrifuge.....	73
Figure 3.3.	Results of the centrifugation tests conducted on Pittsburgh No. 8, (28 mesh x 0) sample slurry.....	75
Figure 3.4.	Resolution of the centrifuge tests results on Pittsburgh coal sample.....	77
Figure 3.5.	Superimposed results of the control tests and the tests conducted in the presence of EGMO (2 Lbs./ton).....	78

Figure 3.6.	Results of the centrifugation tests conducted on Middle Fork (100 mesh x 0) coal sample slurry.....	79
Figure 3.7.	Results of the centrifugation tests conducted on Holston (28 mesh x 0) coal sample slurry.....	81
Figure 3.8.	Results of the filtration tests conducted on Middle Fork sample slurry. The experiments were conducted at three different slurry volumes (cake thicknesses). Reagents A and E were used as the dewatering aids each at a dosage of 2Lbs/ton.....	82
Figure 3.9.	Results of the filtration tests conducted on Holston (28 mesh x 0) sample slurry. The experiments were conducted at three different drying cycle times and at two different cake thicknesses.....	84
Figure 4.1.	Results of the surface tension measurements of the EGMO solutions in water at different concentrations.....	91
Figure 4.2.	Results of the contact angle measurements on polished Elkview coal sample under filtration conditions. The tests were conducted in the presence of Kerosene and EGMO at different dosages.....	92
Figure 4.3.	Results of the contact angle tests conducted on the Elkview coal sample in the presence of EGMO.....	94
Figure 4.4.	Results of the vacuum filtration tests organized on the Elkview coal sample slurry. The tests were conducted in the presence of the novel dewatering aid EGMO at varying concentrations.....	95
Figure 4.5.	Comparison of the surface tension results of the solution prepared with EGMO in the absence of the coal particles and the surface tension of filtrates collected from the vacuum filtration tests.....	96

## LIST OF TABLES

	Page
Table 1.1. Percentage oxygen functionality in coal (Ruberto and Cronauer, 1978).....	6
Table 2.1. Results of the filtration tests conducted on Middle Fork coal sample (100 mesh x 0) using EGMO (2 lbs/ton).....	50
Table 2.2. Results of the filtration experiments conducted on the oxidized Elkview coal sample (28 mesh x 0).....	54
Table 2.3. Results Obtained Using EGMO on the Pittsburgh Coal Sample (28 mesh x 0). The cake thickness was 0.2 inches and the drying cycle time was set to 2 minutes.....	60
Table 2.4. The application ranges of the selected factors for statistical analyses.....	61
Table 4.1. Change in contact angle of the Sunny Side Coal Sample with EGMO and PMHS.....	90